



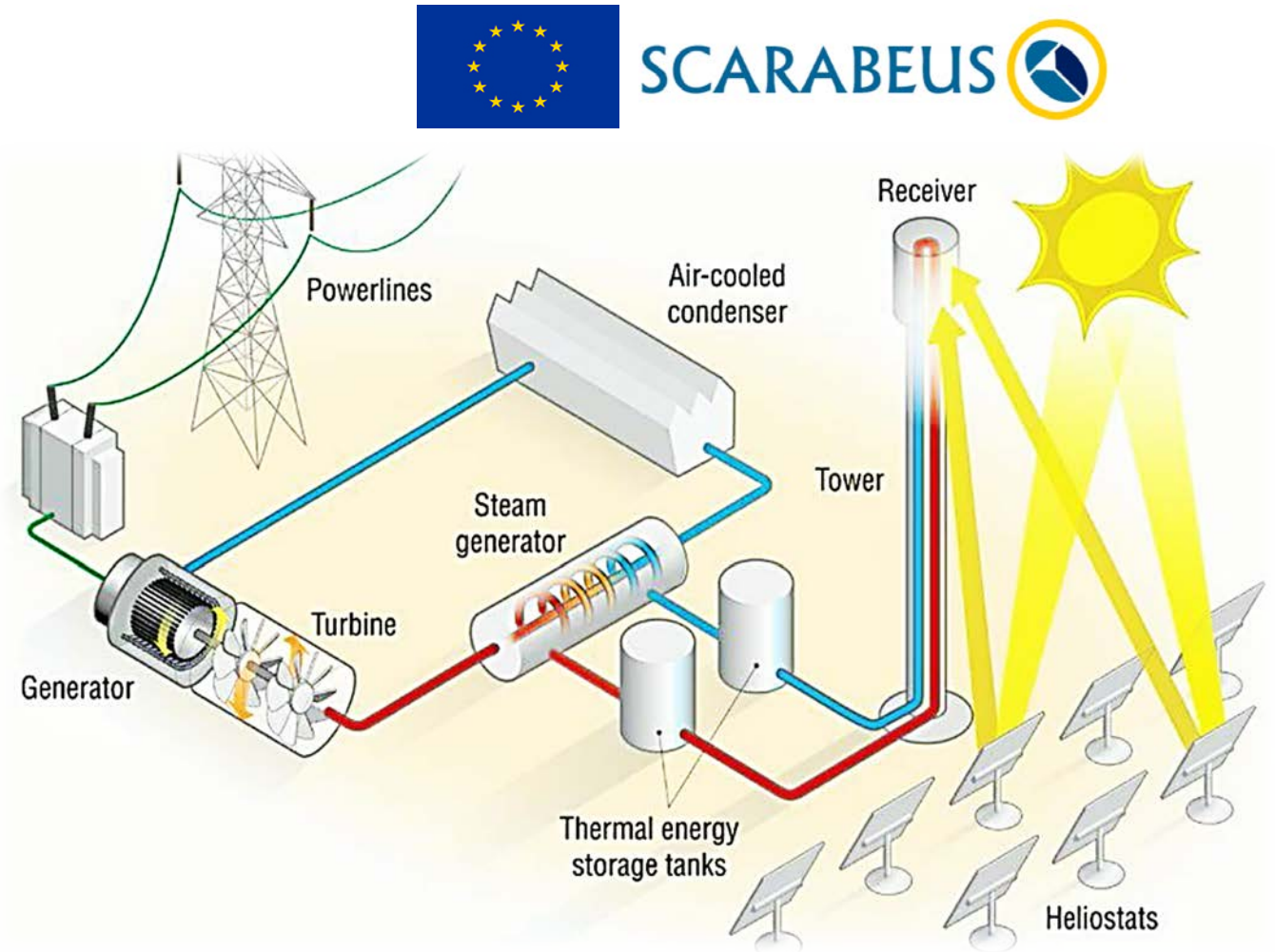
Binary interaction parameter uncertainty in the optimisation of a transcritical cycle: consequences on cycle and turbine design

Omar Aqel, Martin White, Abdulnaser Sayma

The 4th European sCO₂ Conference for Energy Systems, 23-24th March 2021

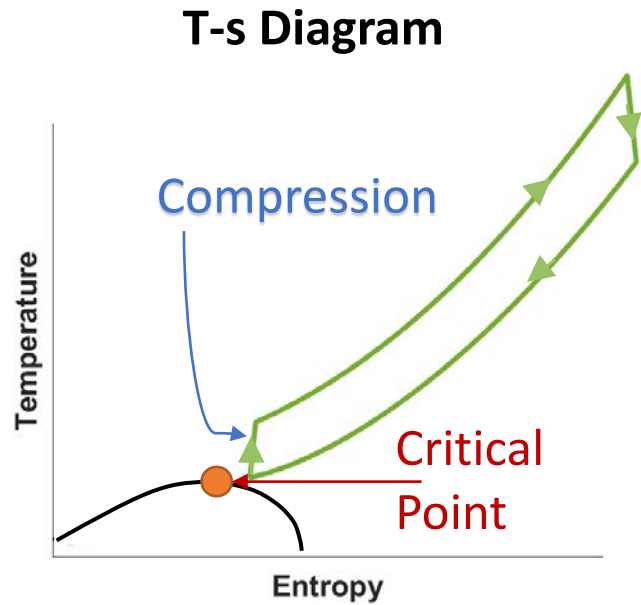
Motivation

- The cost of Concentrated Solar Power (CSP) plants may be lowered by increasing power block efficiency, thus reducing solar field size
- The **SCARABEUS** project (H2020 funded) aims at developing CO₂ blends in CSP plants with maximum temperatures of 700°C, power block efficiency above 50% and cost of electricity below 96 €/MWh [2]
- CO₂ blends may achieve power block efficiencies above 50% by enabling condensation cycles



Typical Heliostat field connected to simple Rankine cycle through thermal energy storage tanks [1].

**Brayton Cycle
(pure CO₂)**



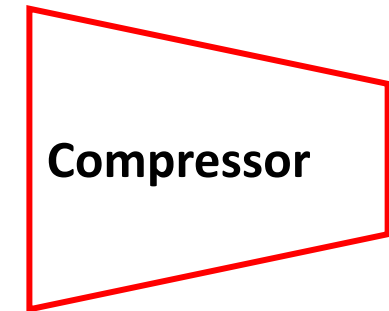
Compression Temp. & Press.

$$T > \textit{Critical Temperature}$$

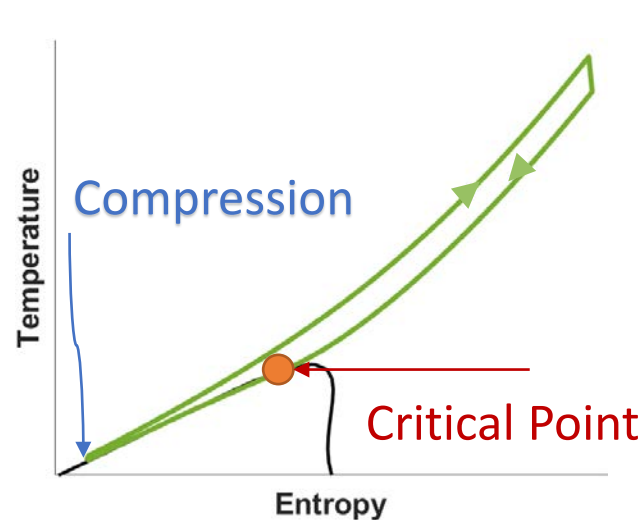
$$P > \textit{Critical Pressure}$$

**Compression phase
and device**

Gas phase



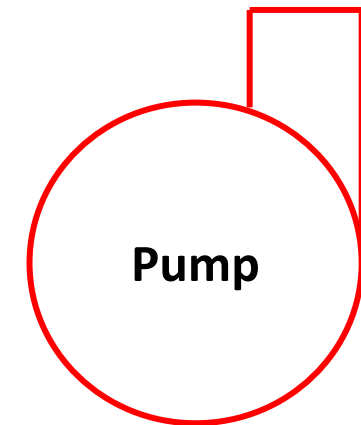
**Rankine Cycle
(CO₂ mixture)**



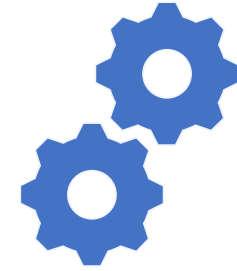
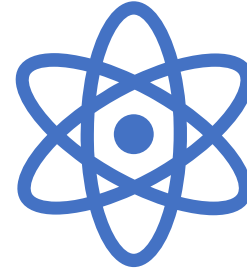
$$T < \textit{Critical Temperature}$$

$$P < \textit{Critical Pressure}$$

Liquid phase



(Lower compression work)



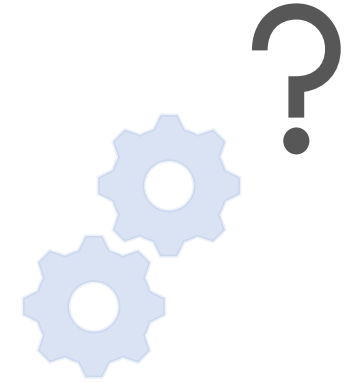
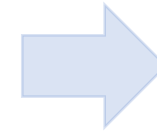
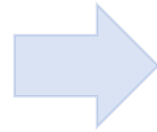
Selection of working fluid
mixture

Setup of thermophysical
property model

Process modelling

*For more details, please see:

G. Di Marcoberardino, C.M. Invernizzi, P. Iora, A. Ayub, D. Di Bona, P. Chiesa, M. Binotti, G. Manzolini,
Experimental and analytical procedure for the characterization of innovative working fluids for power plants applications,
Applied Thermal Engineering,
Volume 178,
2020,



Selection of working fluid mixture

Setup of thermophysical property model

Process modelling

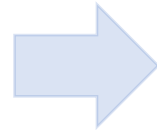
- ✓ Choice of Equation of State (EoS)
- ✓ Value of Binary Interaction Parameters (k_{ij})



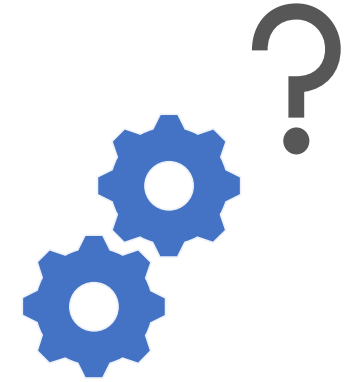
Uncertainty in estimated properties



Selection of working fluid mixture



Setup of thermophysical property model



Process modelling

- ✓ Choice of Equation of State (EoS)
- ✓ Value of Binary Interaction Parameters (k_{ij})



Uncertainty in estimated properties



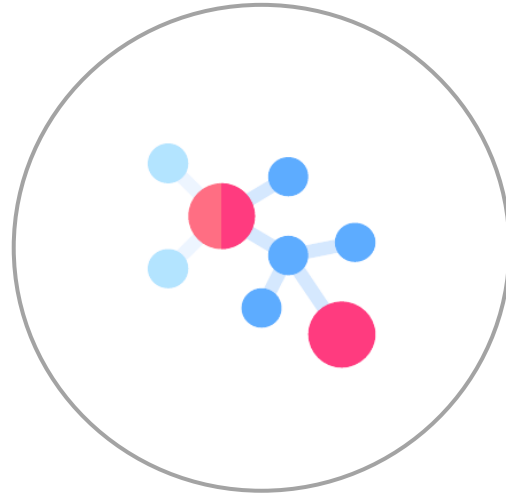
Uncertainty in process modelling

Methodology

Procedure:

(1)

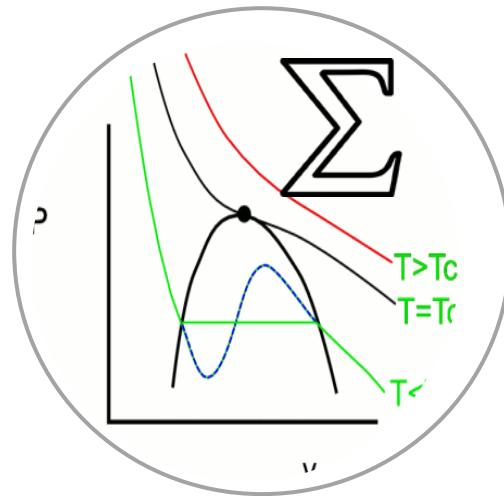
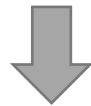
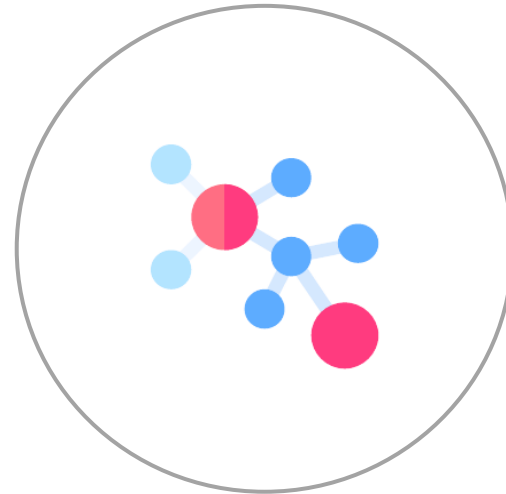
1. Select Dopant (H_2S , NOD, C_6F_6)



Procedure:

1. Select Dopant (H_2S , NOD, C_6F_6)
2. Select EoS (PR, BWRS, SRK, PC-SAFT)

(1)

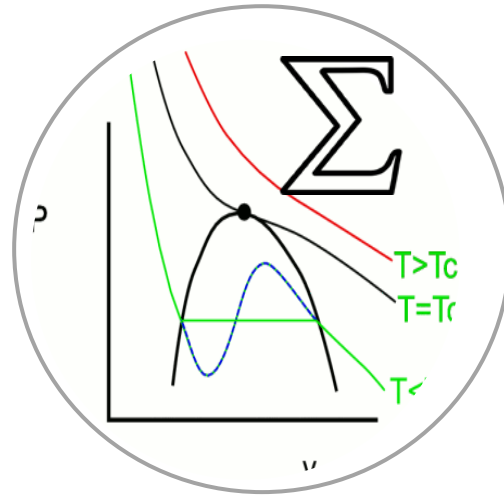
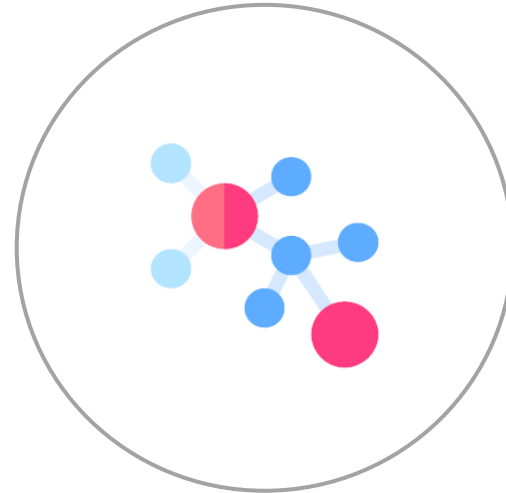


(2)

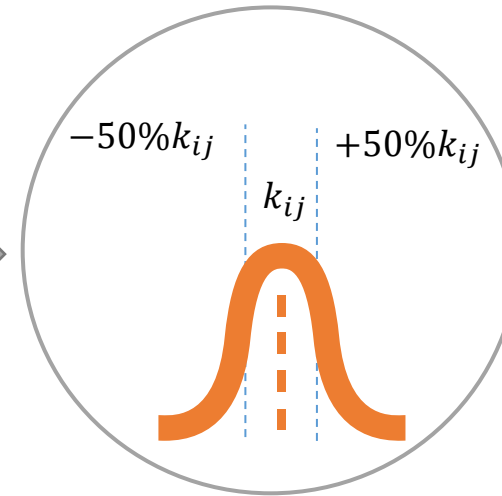
Procedure:

1. Select Dopant (H_2S , NOD, C_6F_6)
2. Select EoS (PR, BWRS, SRK, PC-SAFT)
3. Set binary interaction parameter

(1)



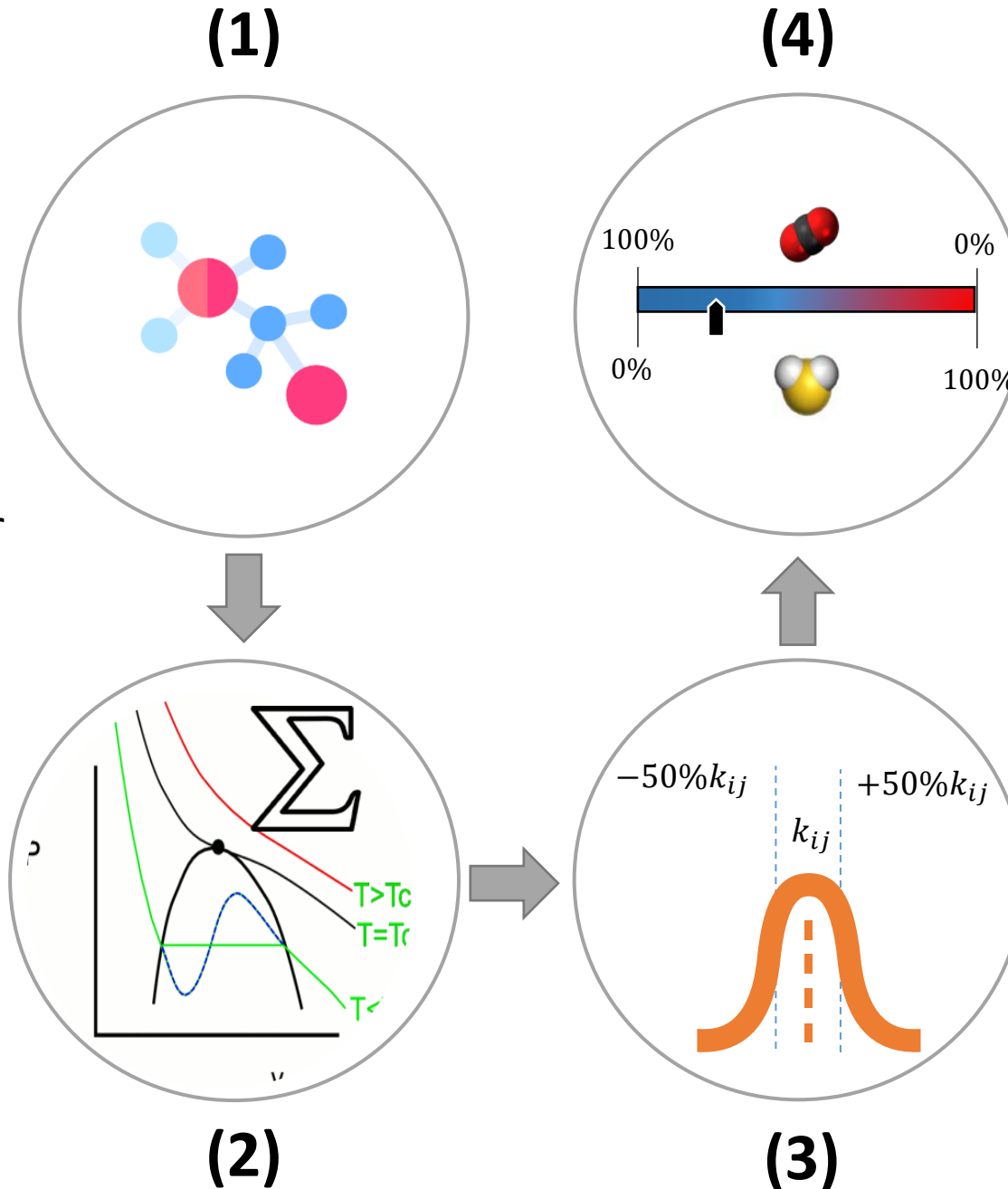
(2)



(3)

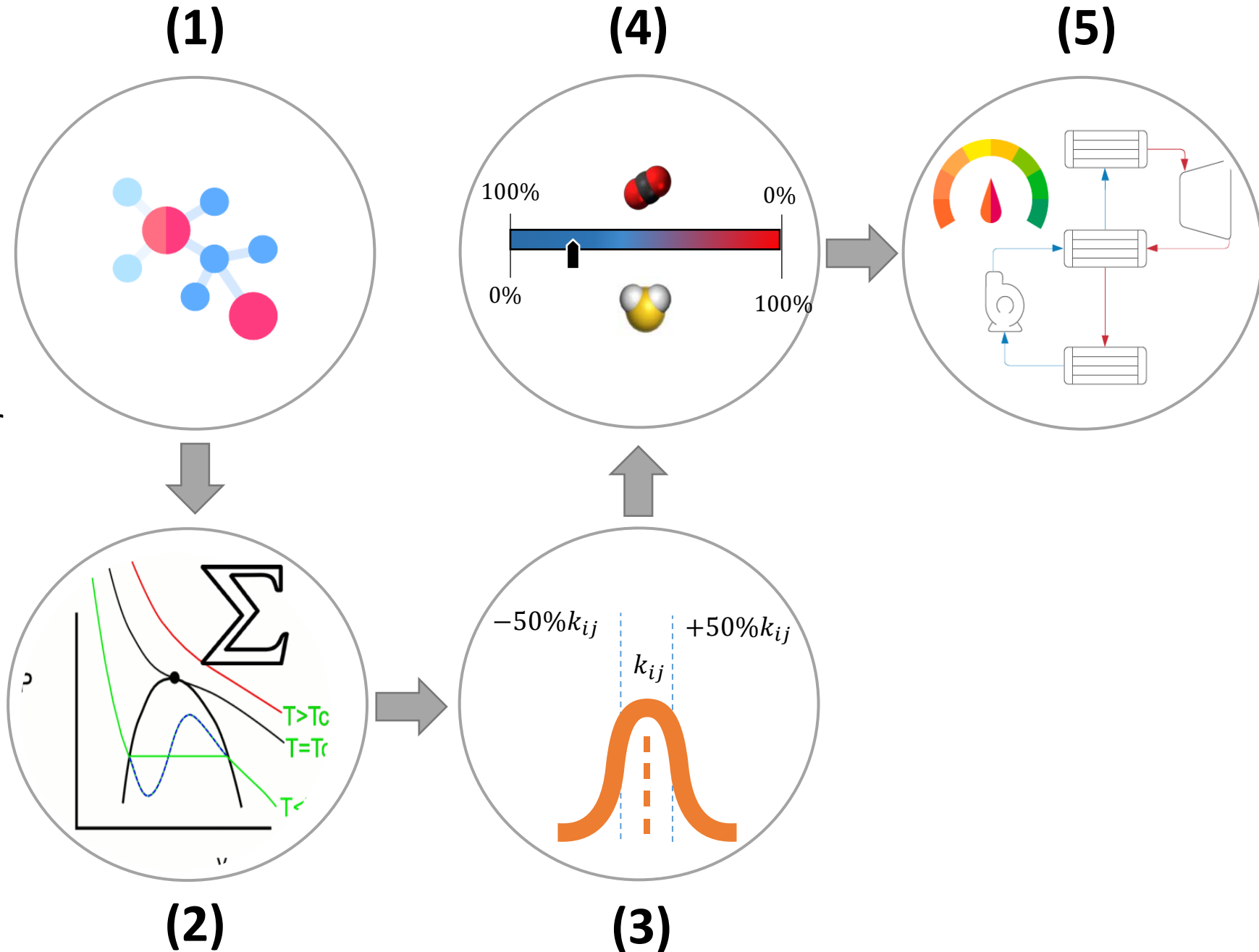
Procedure:

1. Select Dopant (H_2S , NOD, C_6F_6)
2. Select EoS (PR, BWRS, SRK, PC-SAFT)
3. Set binary interaction parameter
4. Set mixture composition



Procedure:

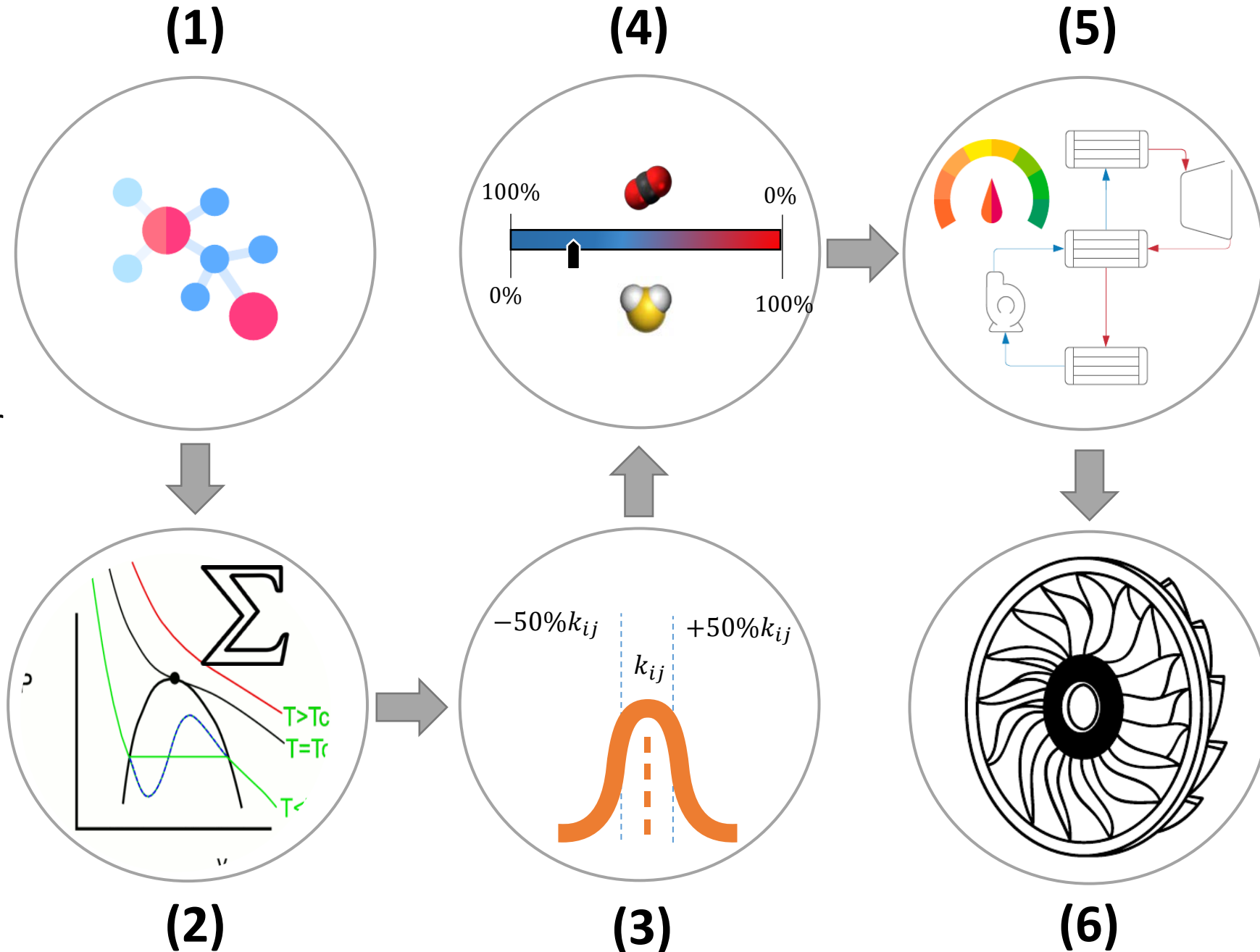
1. Select Dopant (H_2S , NOD, C_6F_6)
2. Select EoS (PR, BWRS, SRK, PC-SAFT)
3. Set binary interaction parameter
4. Set mixture composition
5. Optimise cycle efficiency



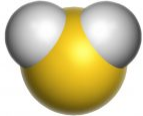
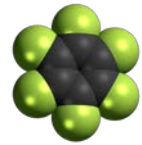





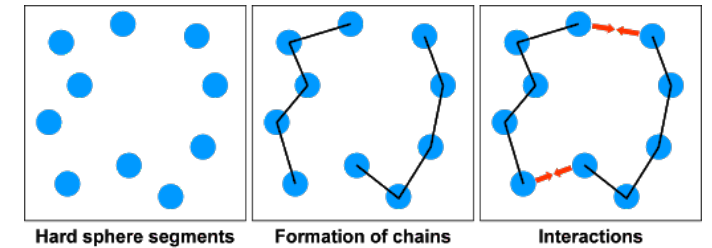
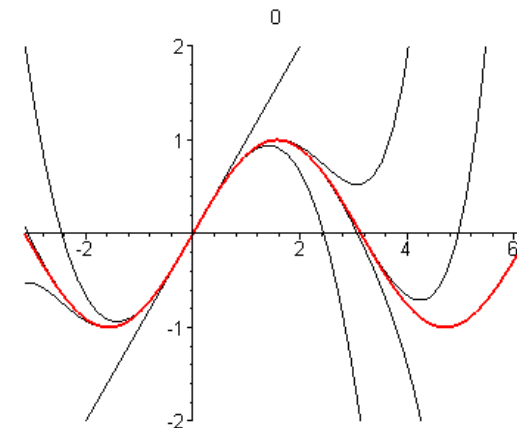
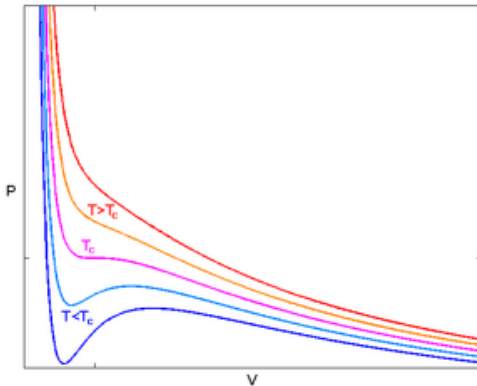
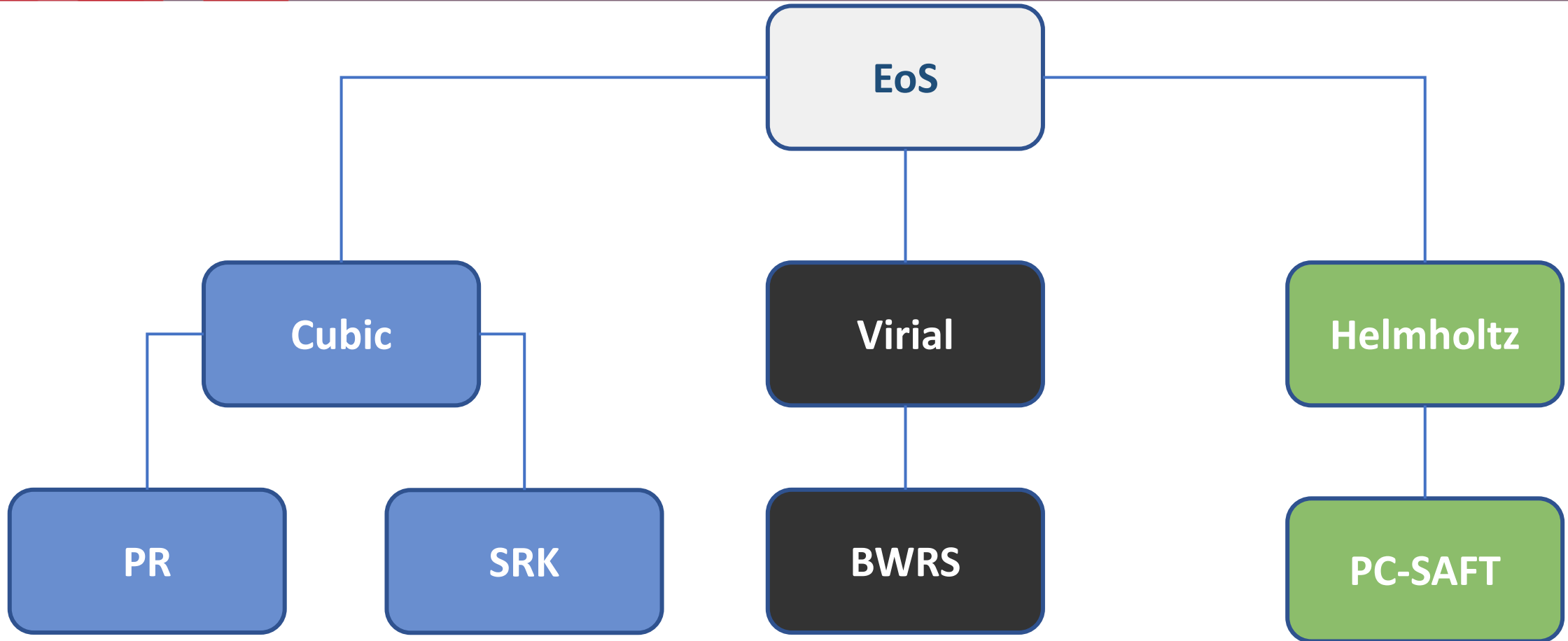
Procedure:

1. Select Dopant (H_2S , NOD, C_6F_6)
2. Select EoS (PR, BWRS, SRK, PC-SAFT)
3. Set binary interaction parameter
4. Set mixture composition
5. Optimise cycle efficiency
6. Generate turbine geometry

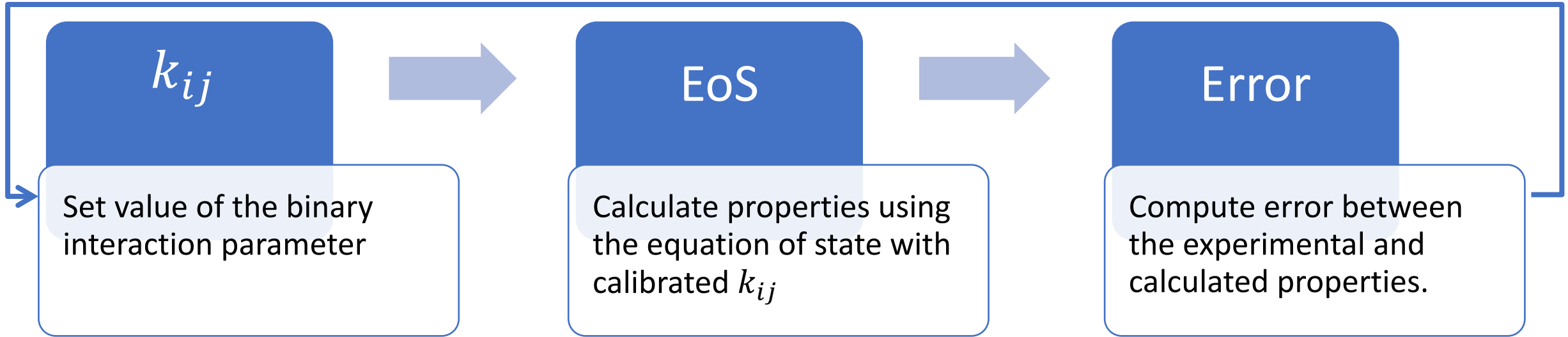
Steps 2 to 6 are repeated for each mixture



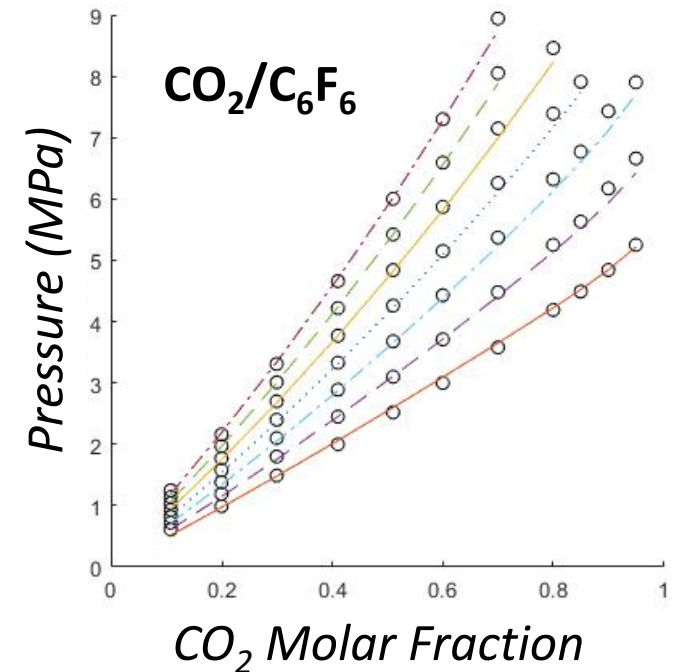
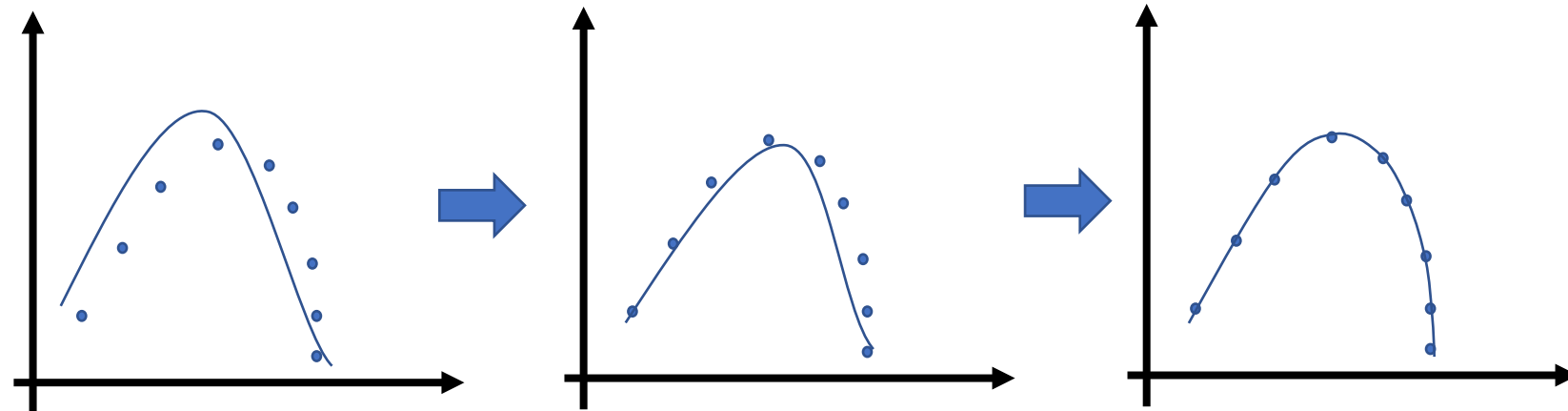
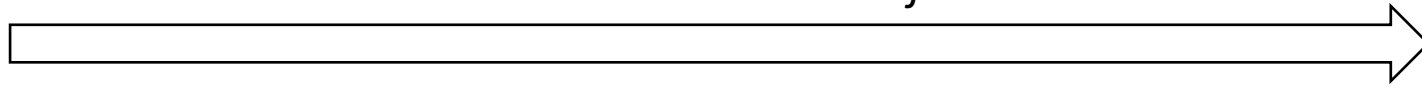
	Base Fluid	Dopants		
	Carbon Dioxide (CO ₂)	Hydrogen Sulphide (H ₂ S)	Non-Organic Dopant (NOD)	Hexafluorobenzene (C ₆ F ₆)
 Molecular Shape				
 Molecular Weight (g/mol)	44.01	34.08	60<	186.1
 Critical Temperature (°C)	31.10	100.4	150<	243.6
 Critical Pressure (bar)	73.82	89.63	70<	32.73

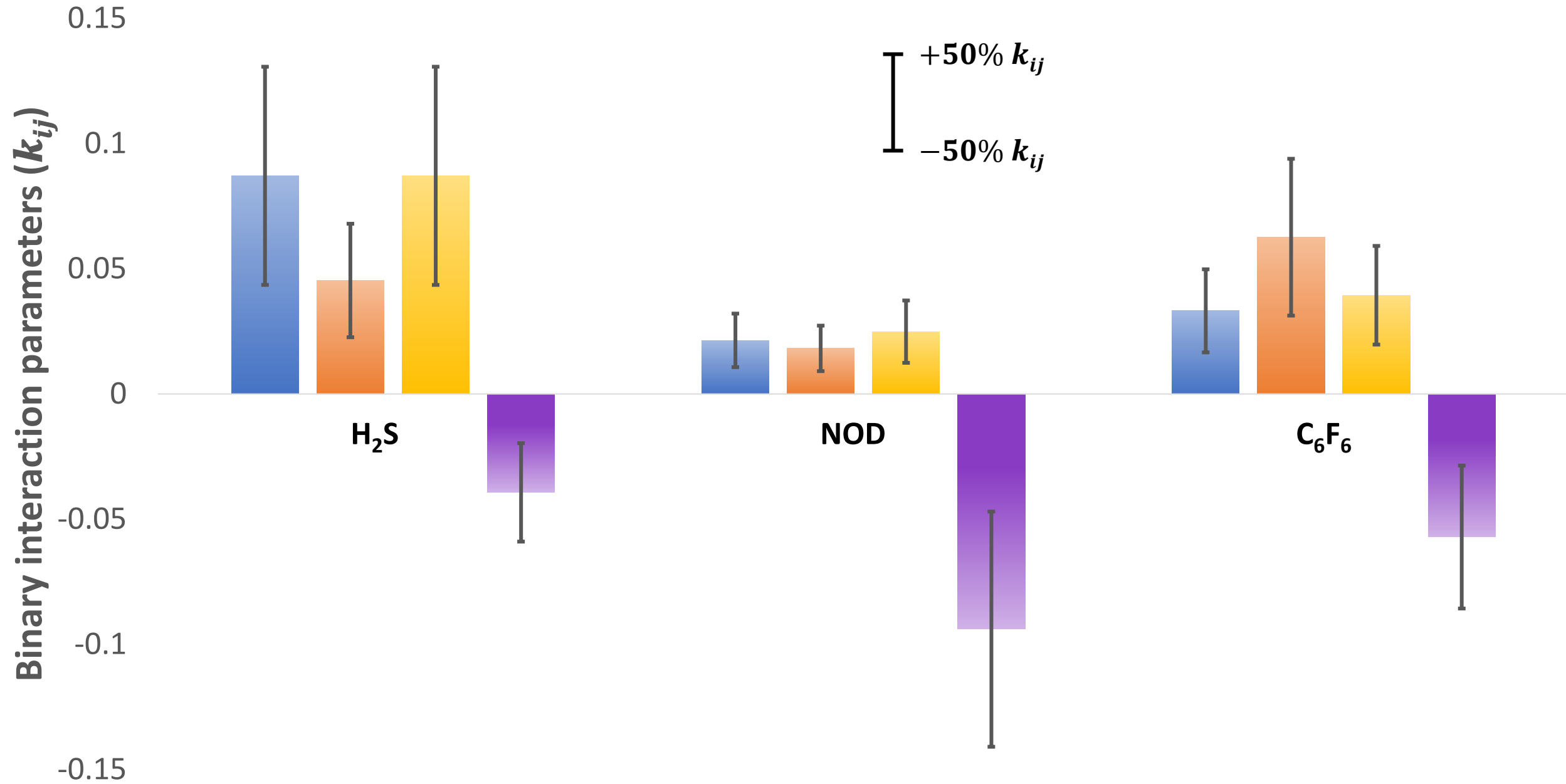


Repeat to minimise error



Calibration of k_{ij}

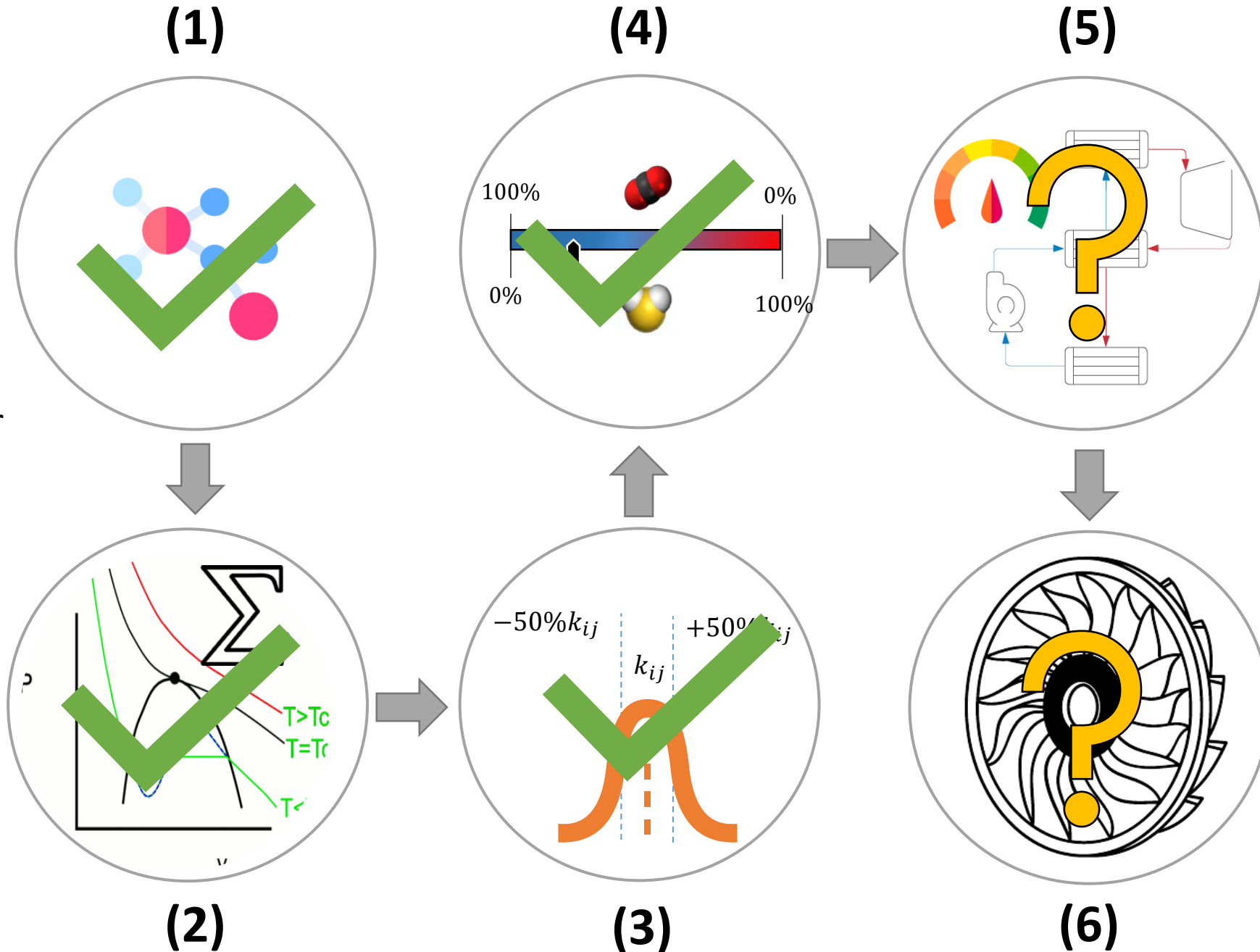




Procedure:

1. Select Dopant (H_2S , NOD, C_6F_6)
2. Select EoS (PR, BWRS, SRK, PC-SAFT)
3. Set binary interaction parameter
4. Set mixture composition
5. Optimise cycle efficiency
6. Generate turbine geometry

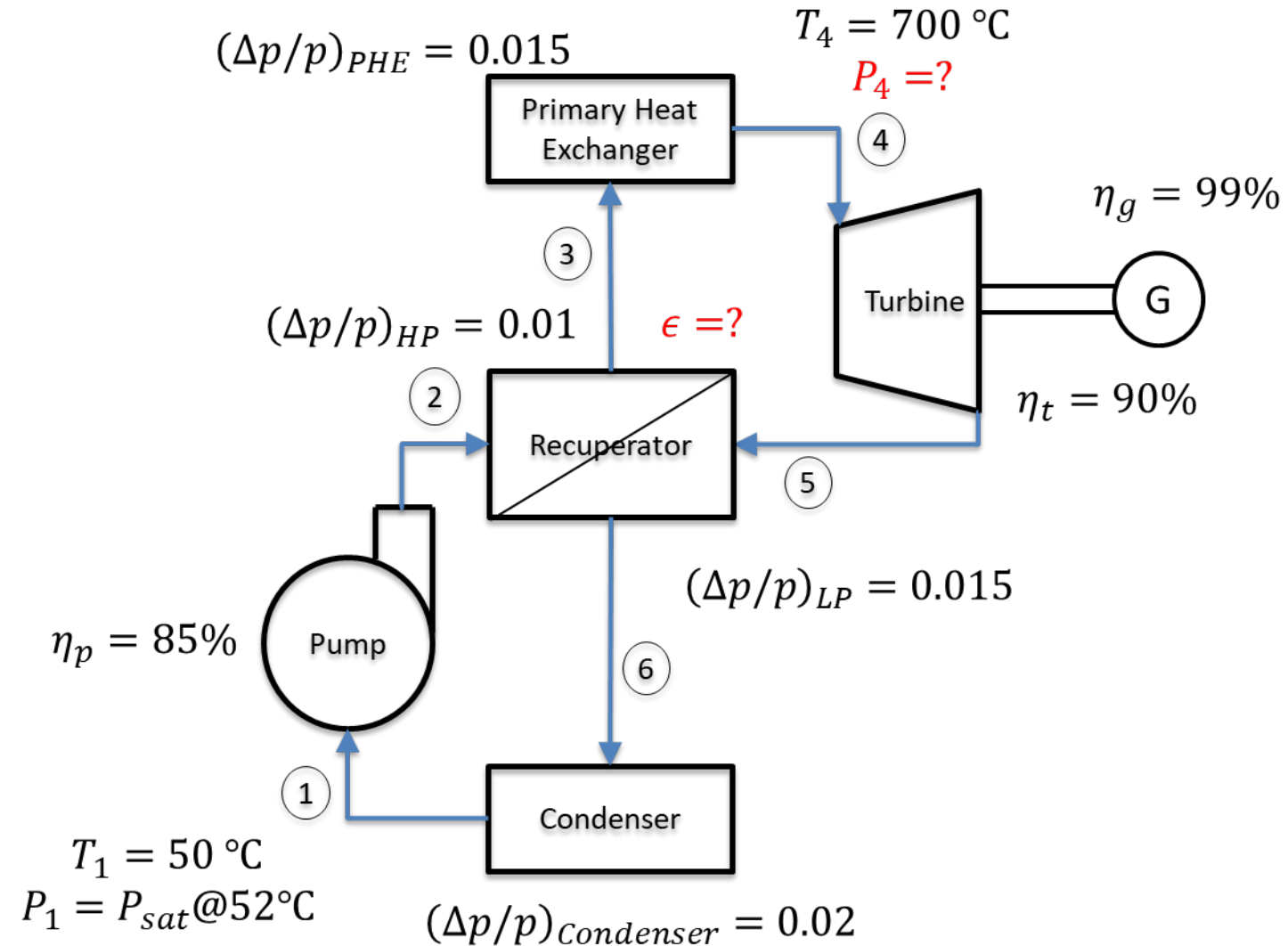
Steps 2 to 6 are repeated for each mixture



Cycle assumptions:

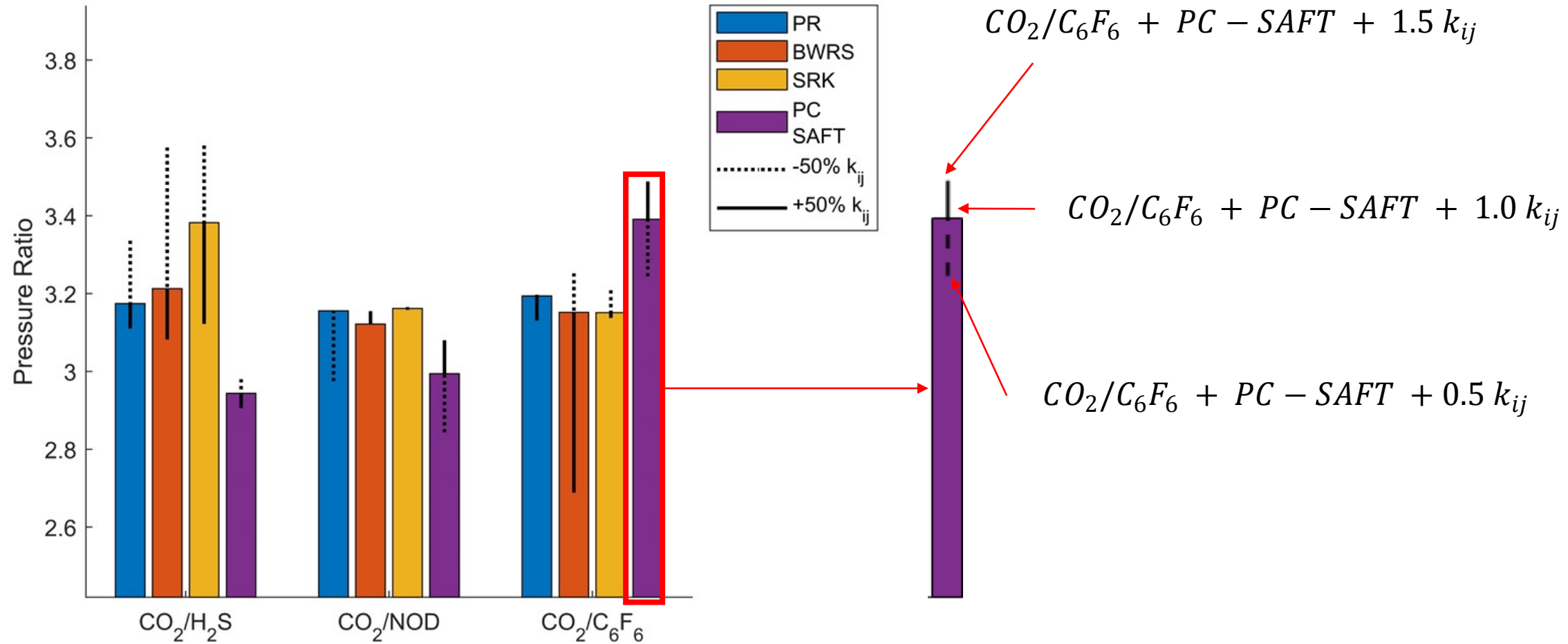
- 100 MW_e plant capacity
- Minimum Internal Temperature Approach (MITA) of 5 °C in recuperator
- Pump inlet pressure is chosen based on 2 °C subcooling in the condenser

Turbine Design Parameter	Value
Rotational speed (RPM)	3000
Number of stages (%)	4
Turbine efficiency (η_t)	90
Loading coefficient (ψ)	1.65
Flow coefficient (ϕ)	0.23
Degree of reaction (Λ)	0.5



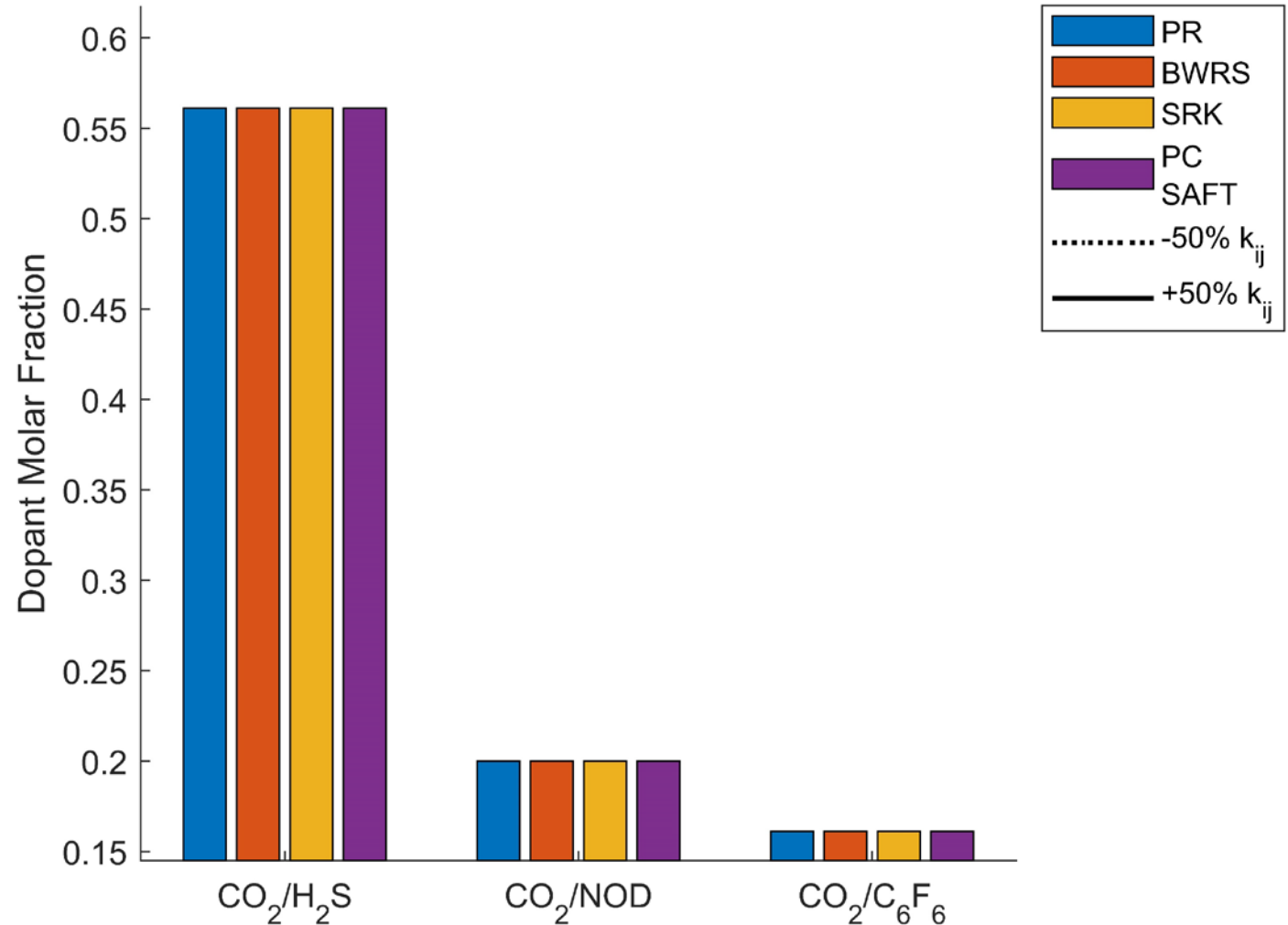
Results

Legend overview



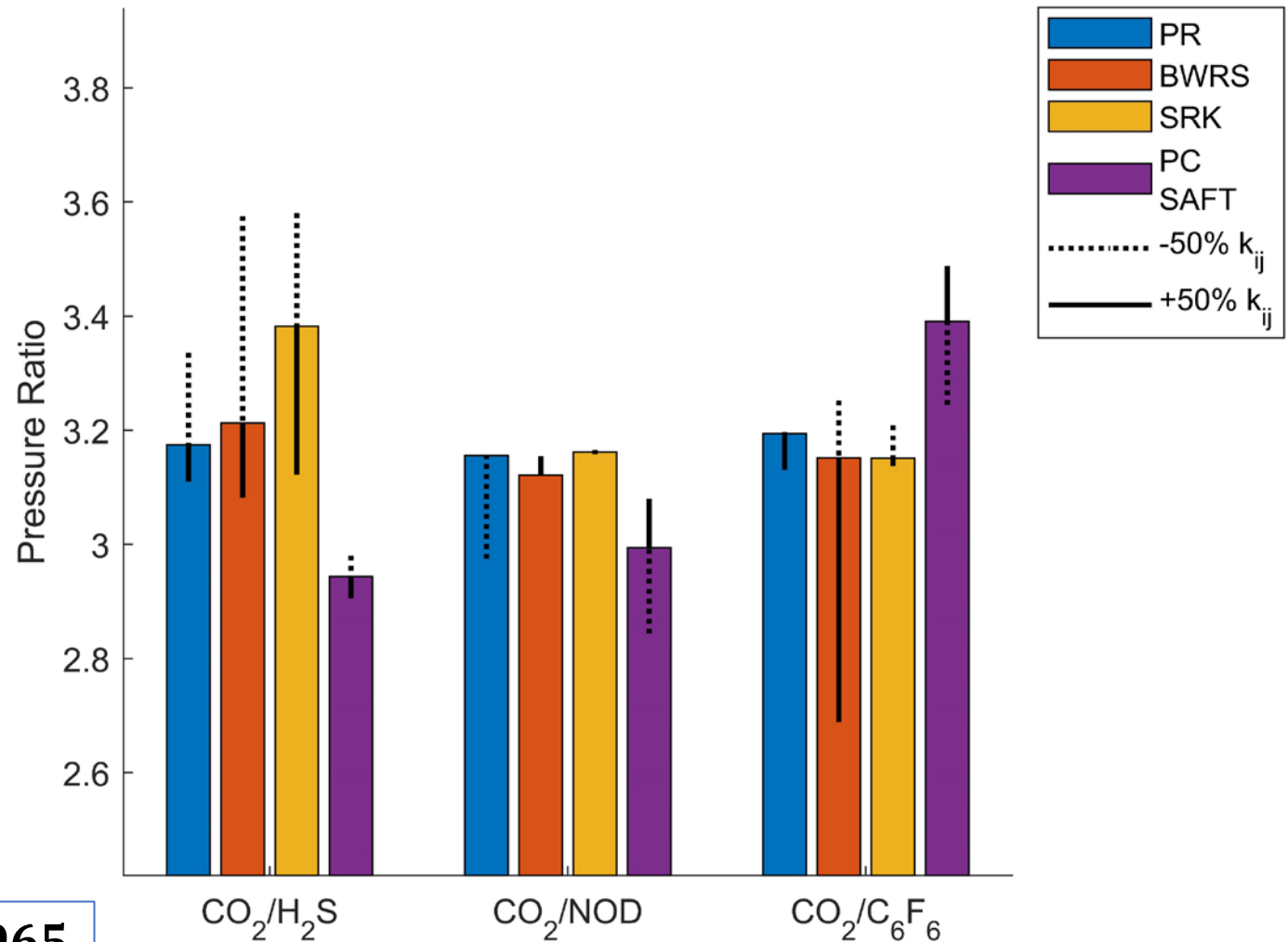
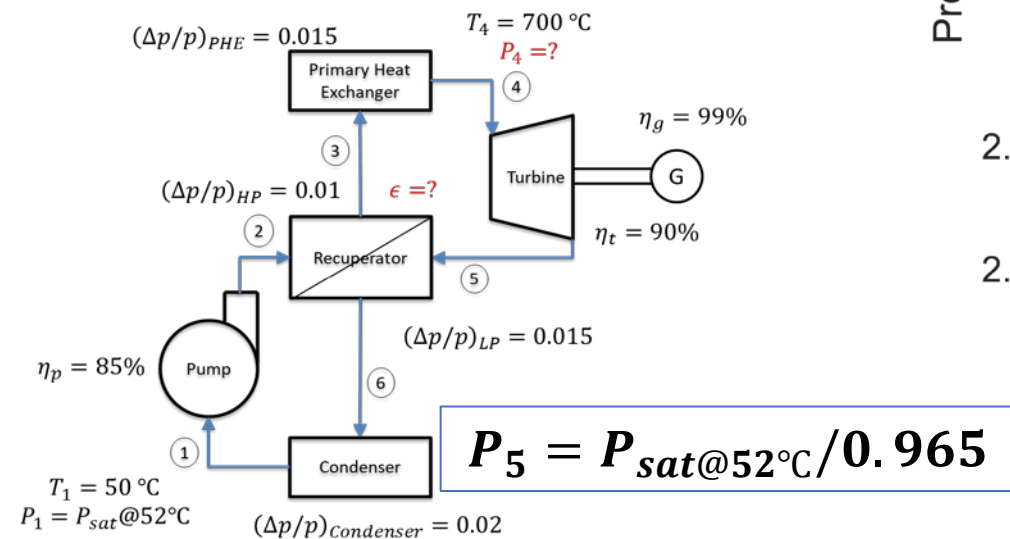
Optimal dopant fraction

- Neither the choice of the EoS nor the variation in k_{ij} effect the choice of the optimal dopant fraction which maximises efficiency.
- In other words, the same mixture composition will be chosen regardless of the thermophysical property model being used.



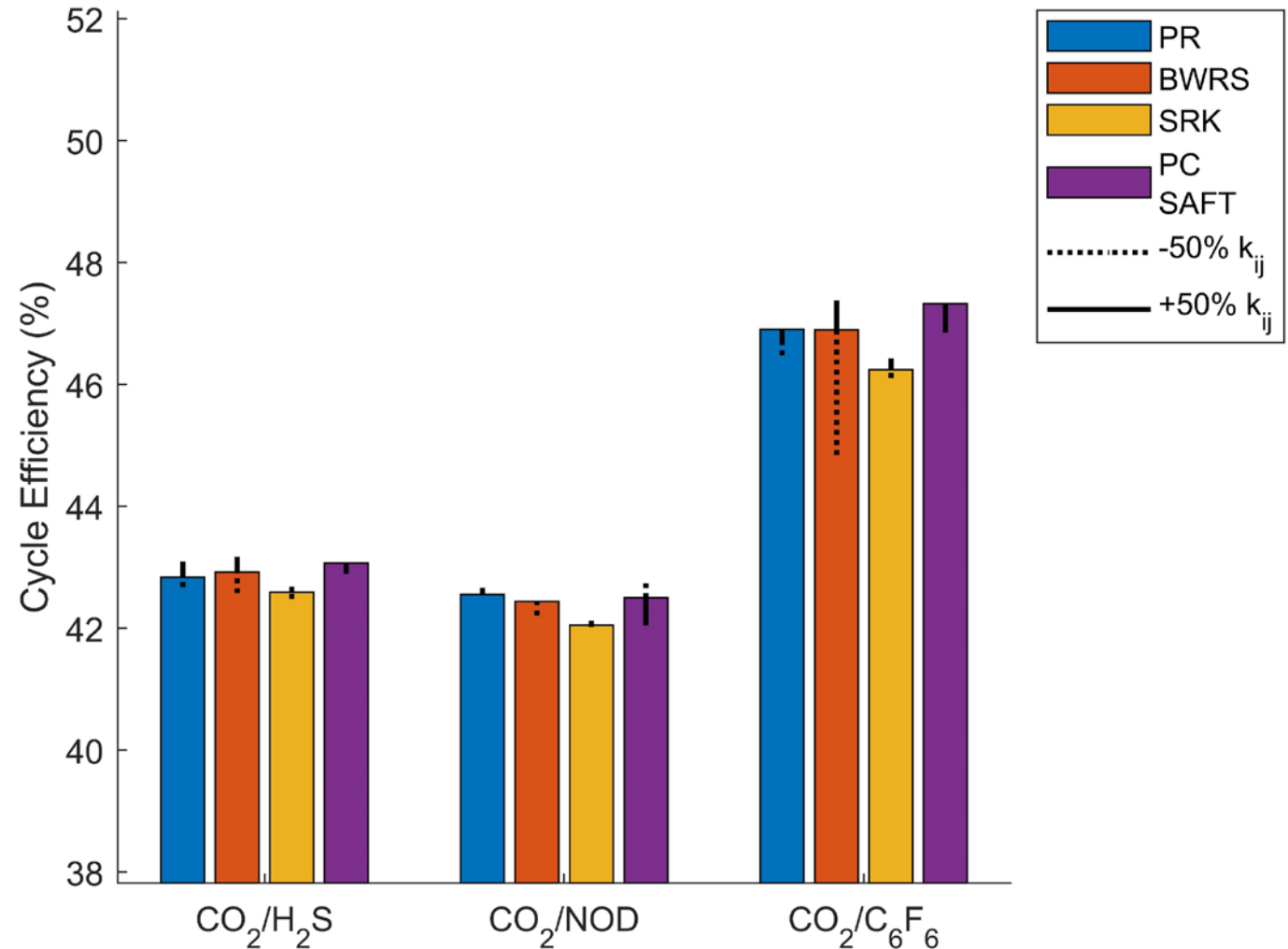
Pressure ratio

- The pressure ratio corresponding to the optimal cycle conditions varies with the fluid model.
- Since the cycle max pressure is uniform for all cycles (250 bar), then the change in pressure ratio is a direct consequence of the calculated pump inlet pressure ($P_1 = P_{sat@52^\circ\text{C}}$).



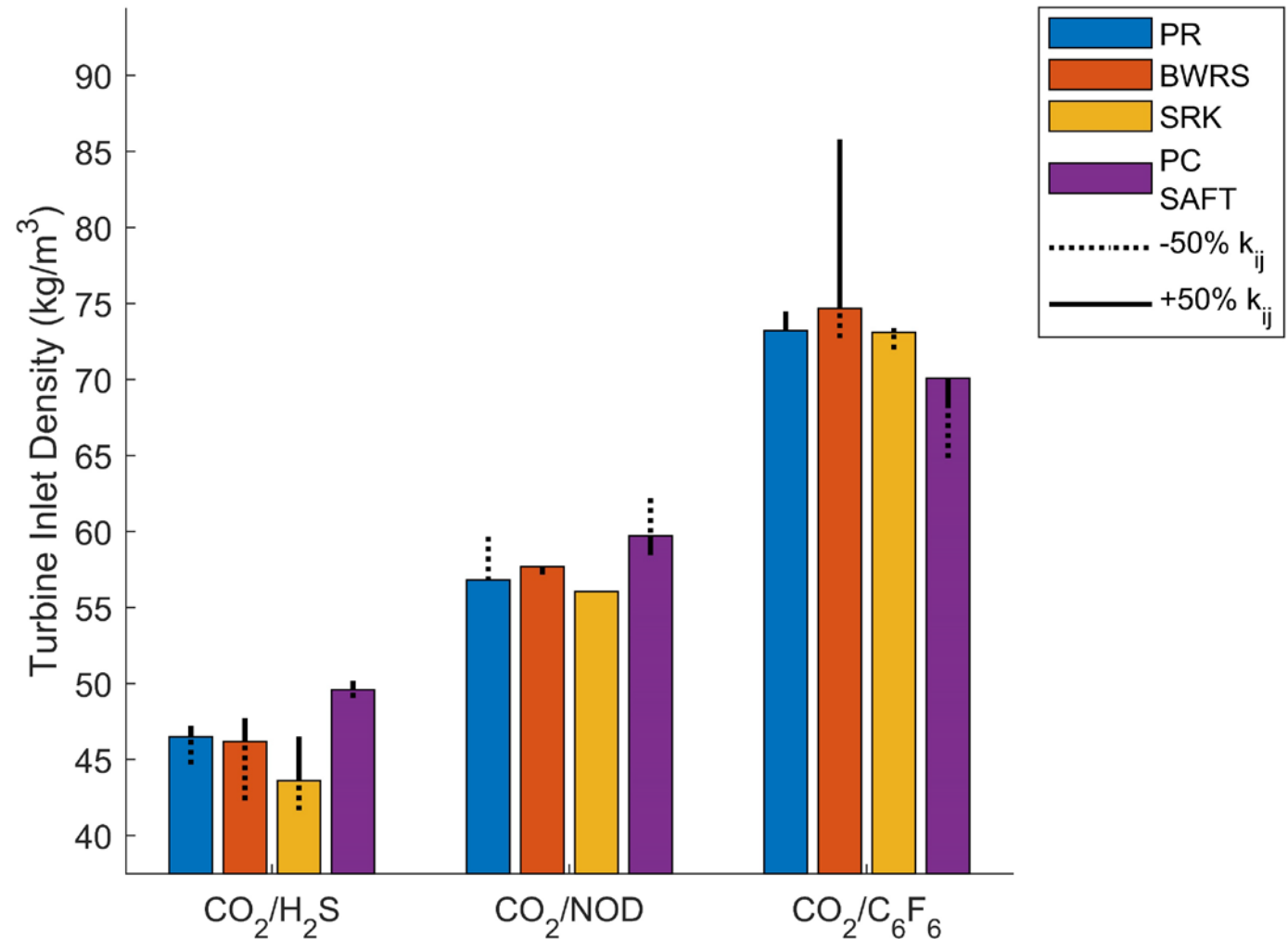
Thermal efficiency

- Thermal efficiency is affected by the EoS and the value of k_{ij} , but this effect differs depending on the mixture.
- 1% difference between SRK and PC-SAFT for $\text{CO}_2/\text{C}_6\text{F}_6$.
- Less than 0.5% difference between the EoS of $\text{CO}_2/\text{H}_2\text{S}$ and CO_2/NOD .
- More than 2% drop in efficiency with -50% variation in k_{ij} when modelling $\text{CO}_2/\text{C}_6\text{F}_6$ using BWRS.



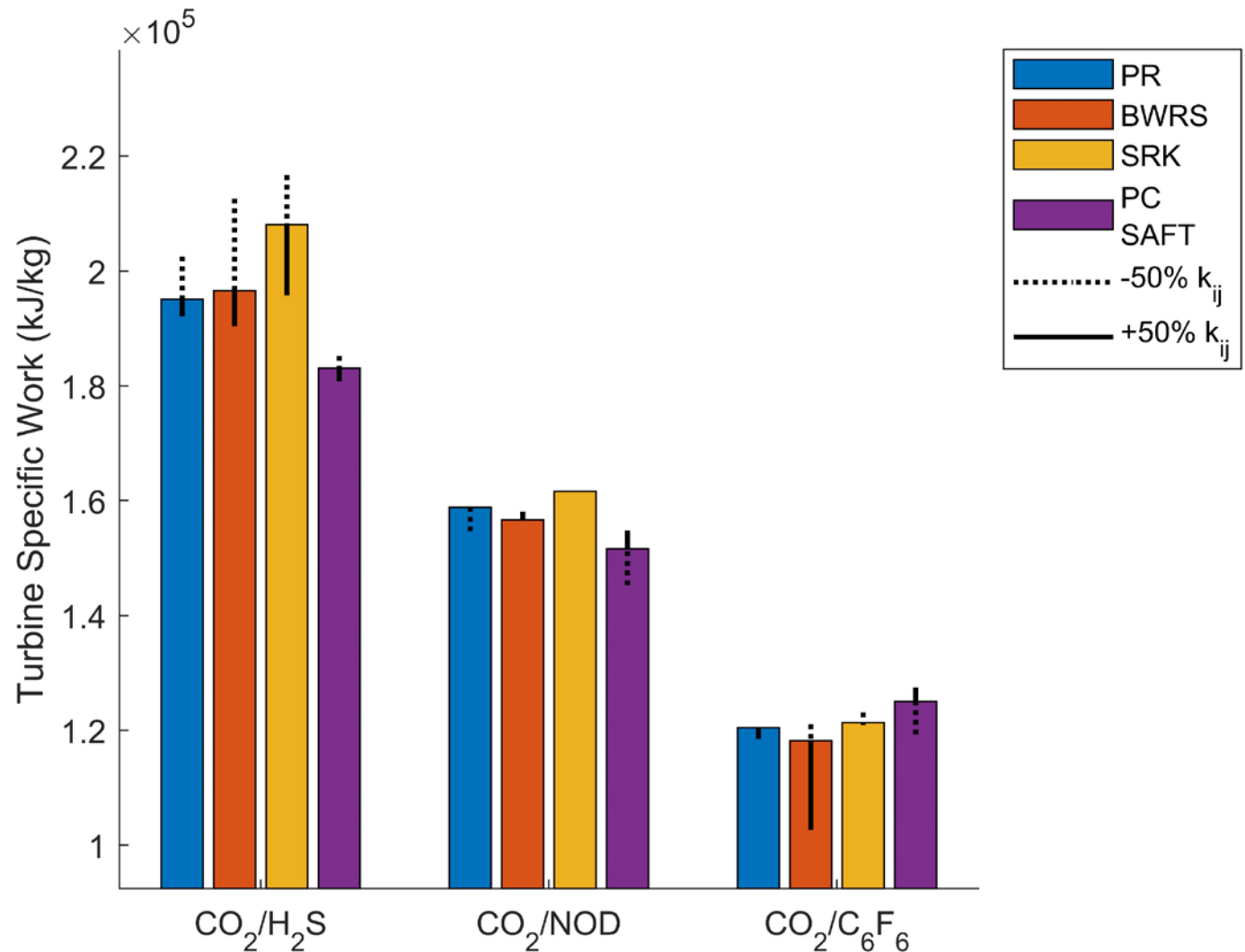
Turbine Inlet Density

- $\text{CO}_2/\text{H}_2\text{S}$ is affected the most by the choice of the EoS (SRK vs PC-SAFT).
- The cubic EoS (PR and SRK) and PC-SAFT are generally less sensitive to k_{ij} than BWRS.
- BWRS is affected the most by k_{ij} variation, especially for $\text{CO}_2/\text{C}_6\text{F}_6$, therefore precise k_{ij} values are recommended when employing the BWRS EoS.



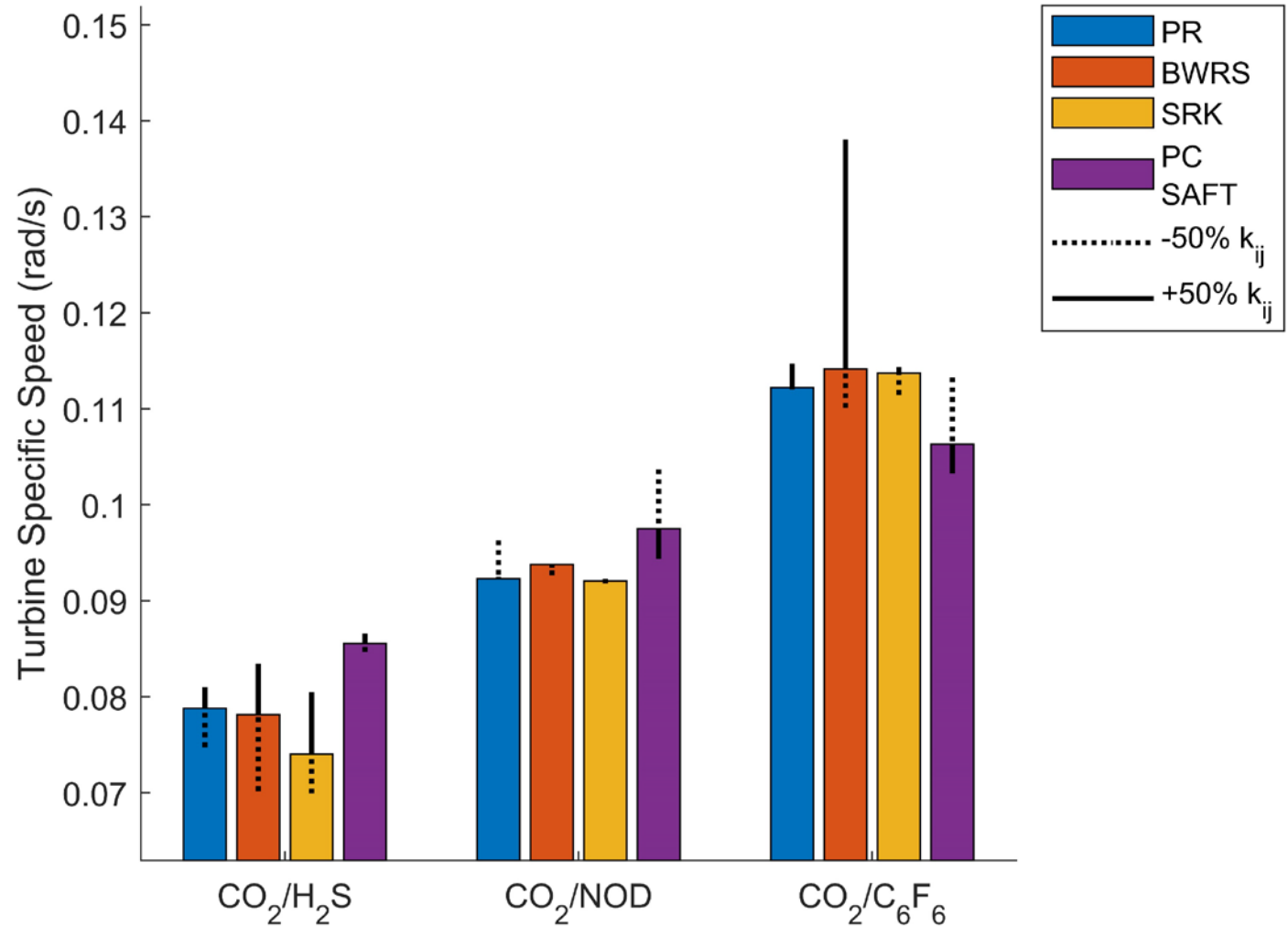
Turbine Specific Work

- Simpler working fluid mixtures have higher specific work.
- Specific work may affect turbine geometry for a set of fixed design parameters.
- 13.7% difference observed between SRK and PC-SAFT for $\text{CO}_2/\text{H}_2\text{S}$ could produce slightly different turbine designs, as seen later.

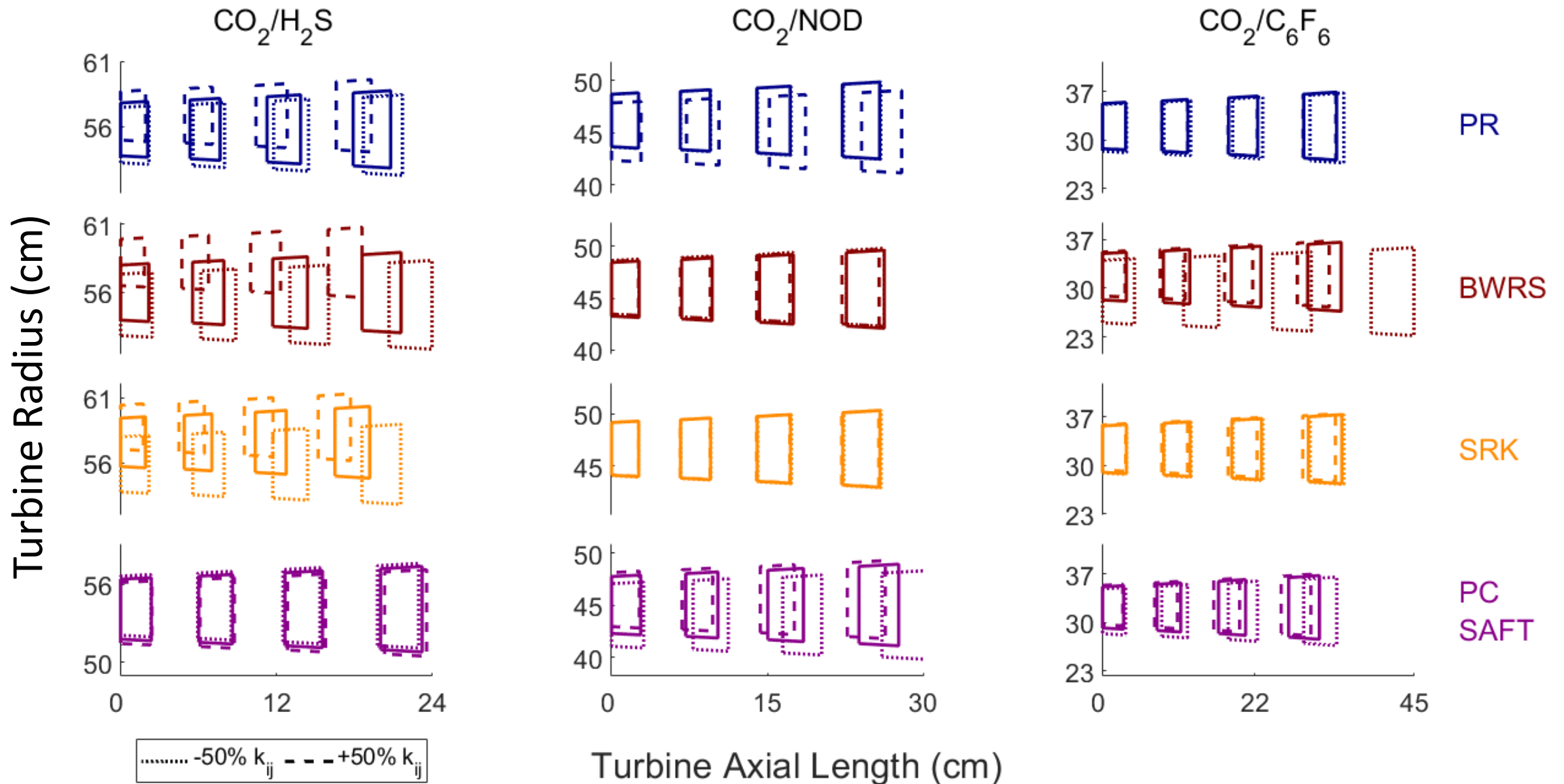


Specific Speed

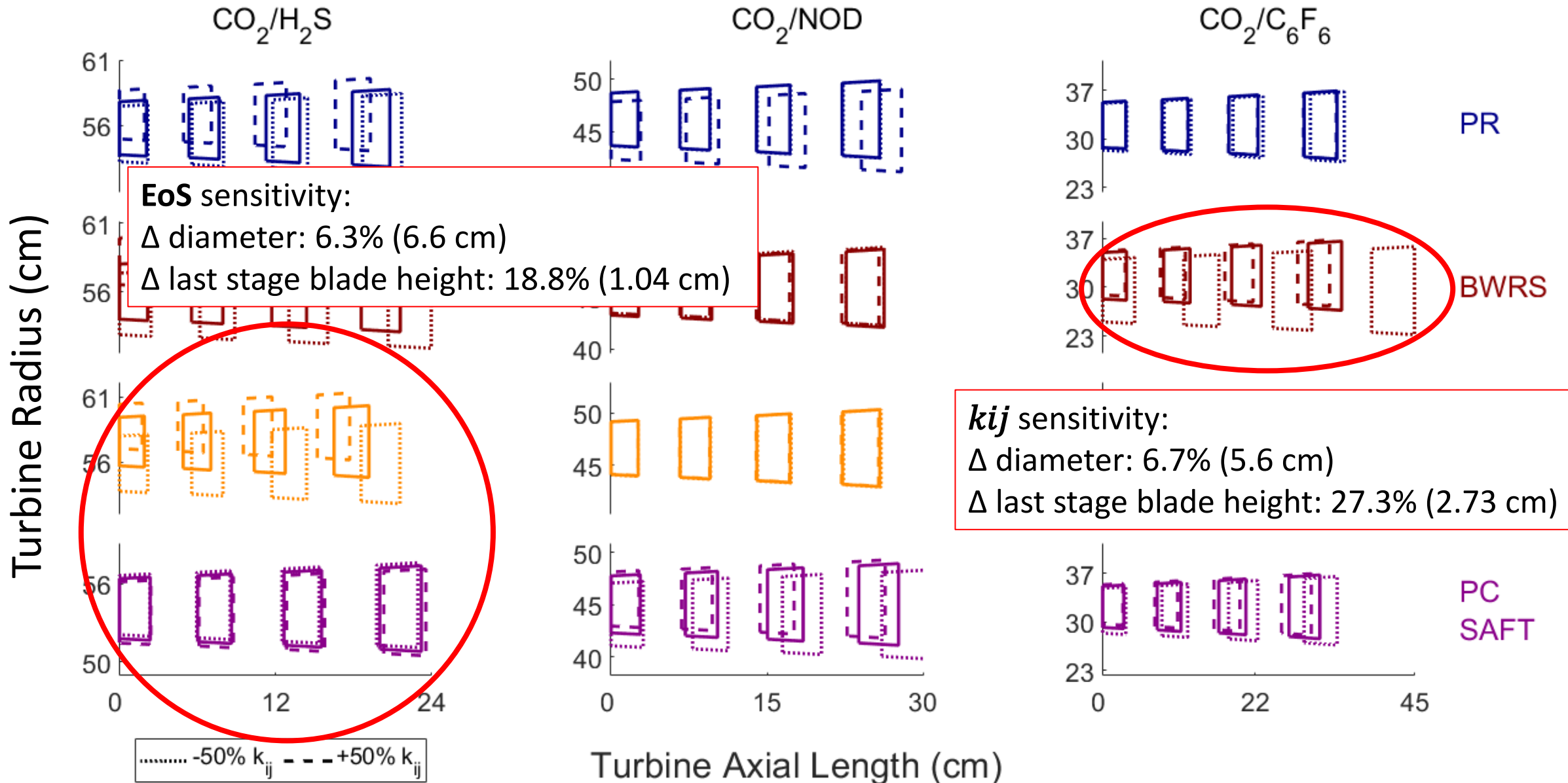
- Calculated at exit conditions.
- Indication of turbine shape and size.
- 21% difference due to +50% increase in k_{ij} for BWRS of $\text{CO}_2/\text{C}_6\text{F}_6$. But only 0.2 rad/s change.



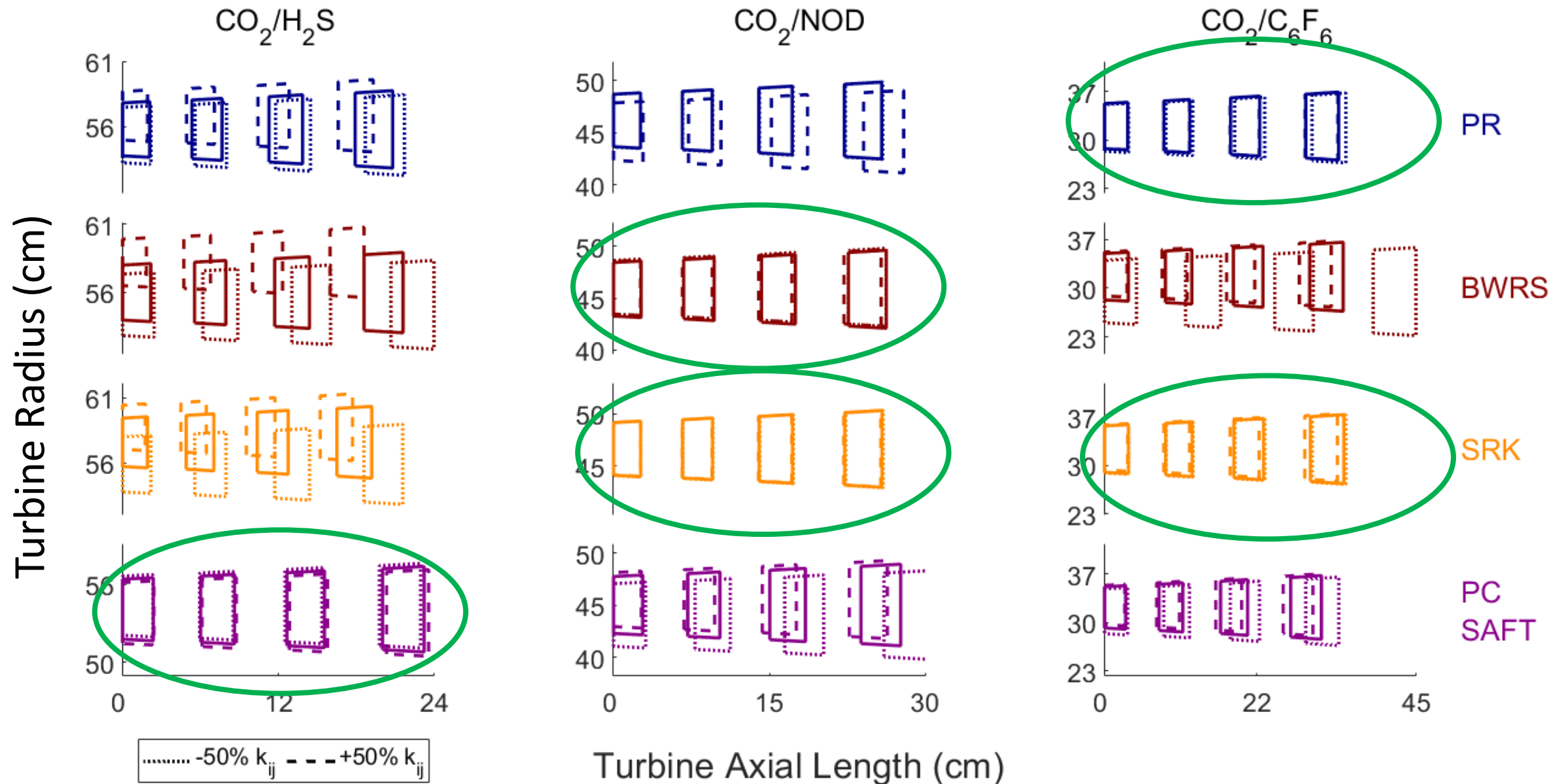
Rotor Blade Geometry



Rotor Blade Geometry

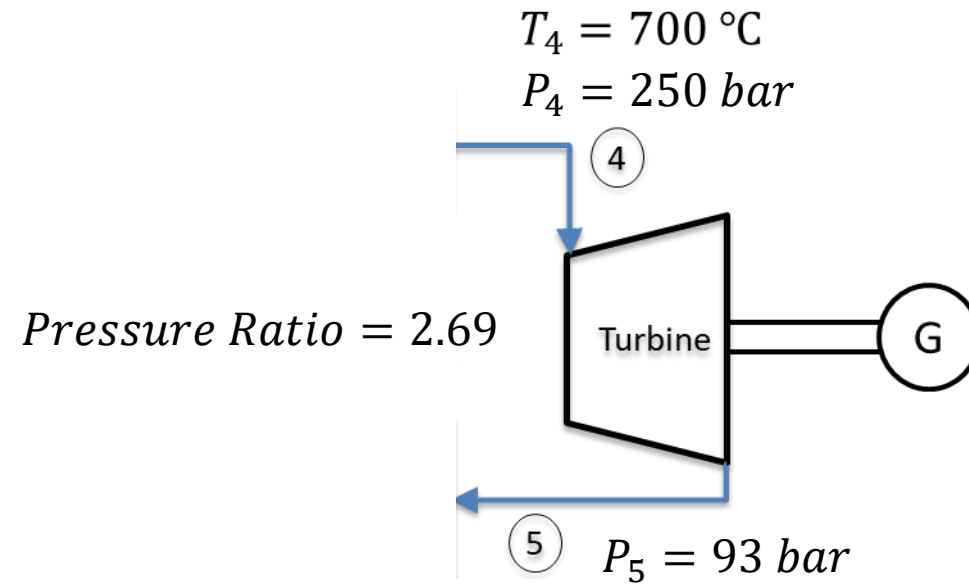


Rotor Blade Geometry

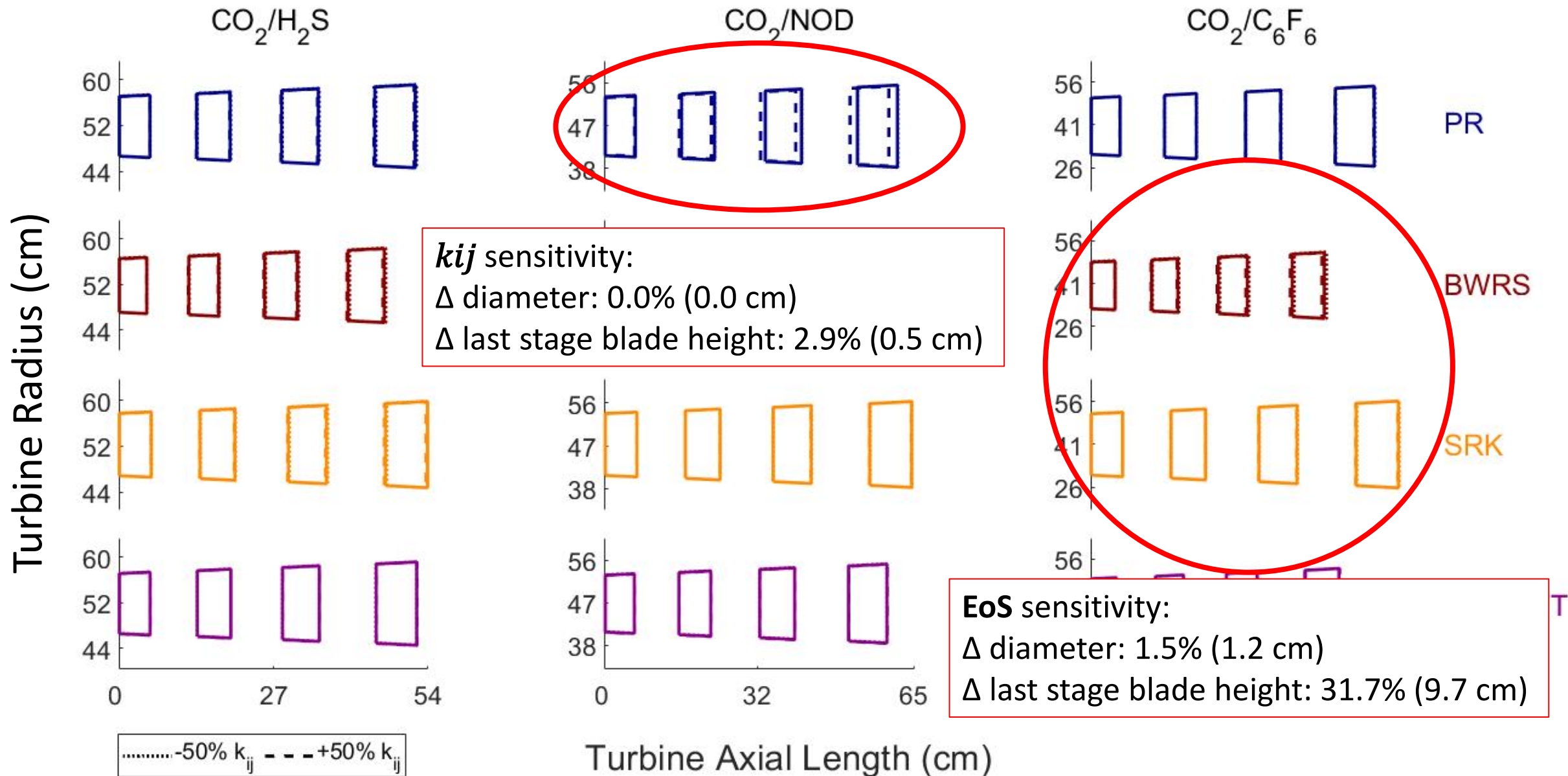


Fixed turbine model assumptions:

- Detachment of turbine from varying cycle conditions.
- Fixed turbine back pressure for all fluid models
- Fixed pressure ratio.



Rotor blade geometry for fixed back pressure



Conclusion and future work

- Sensitivity to the fluid model depends on the mixture being used.
- Avoid BWRS in the absence of experimental data.
- It is recommended to use either the cubic or PC SAFT EoS as they are the least sensitive to the interaction parameter uncertainty
- CO₂/H₂S showed the highest sensitivity to the fluid model.
- Recommended to account for turbine aerodynamic losses.
- Most of the interaction parameter sensitivity stems from the variation in turbine back pressure.



The SCARABEUS project has received funding from the European Union's Horizon 2020 research and innovation programme under grant agreement N° 814985

The image features a dark purple background with a large, stylized 'V' shape formed by two thick red lines. The top-left corner of the 'V' is decorated with a pattern of overlapping red squares. The text 'Thank You!' is centered in the upper right portion of the image.

Thank You!

References

1. Praveen, R., Performance analysis and optimization of central receiver solar thermal power plants for utility scale power generation. *Sustainability*, 2020. 12(1): p. 127.
2. M. Binotti, G. Di Marcoberardino, P. Iora, and C. Invernizzi, “SCARABEUS : Supercritical carbon dioxide / alternative fluid blends for efficiency upgrade of solar power plants SCARABEUS : Supercritical Carbon Dioxide / Alternative Fluid Blends for Efficiency Upgrade of Solar Power Plants,” vol. 130002, no. December, 2020.