

# Large Eddy Simulation of sCO<sub>2</sub> with a Discontinuous Galerkin Method

Aldo Hennink  
a.hennink@tudelft.nl

Delft University of Technology

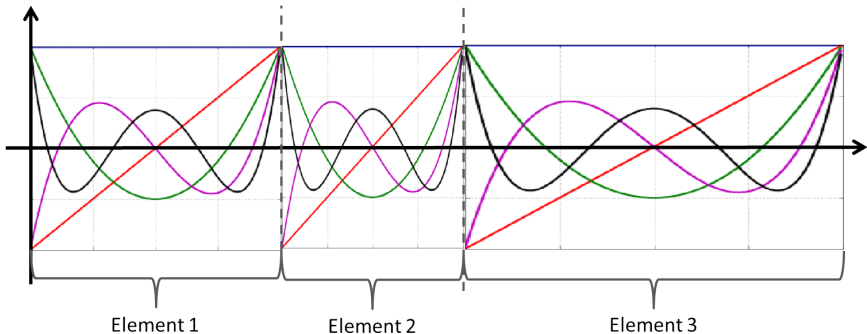
2019-09-20

# Discontinuous Galerkin

## Basis functions

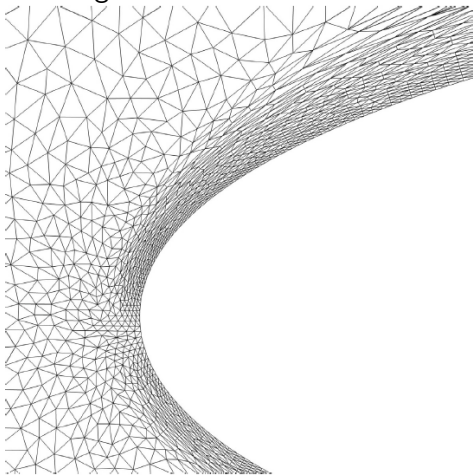
- basis functions in Element  $k$ :  $\{\phi_i^{(k)}\}_i = \{\phi_1^{(k)}, \phi_2^{(k)}, \phi_3^{(k)}, \dots\}$
- approximation in Element  $k$ :  
$$f \approx \sum_i c_i^{(k)} \phi_i^{(k)} = c_1^{(k)} \phi_1^{(k)} + c_2^{(k)} \phi_2^{(k)} + \dots$$

**arbitrarily high polynomial orders** (“high-order finite volume”)



# Discontinuous Galerkin

inhomogeneous and unstructured meshes



(<sup>1</sup>)

---

<sup>1</sup>F. Bassi, L. Botti, A. Colombo, A. Crivellini, C. De Bartolo, N. Franchina, A. Ghidoni, and S. Rebay (2015). "Time Integration in the Discontinuous Galerkin code MIGALE - Steady Problems". In: *Notes on Numerical Fluid Mechanics and Multidisciplinary Design* 128, pp. 179–204

## Compressible vs. Incompressible Solvers

### Incompressible Solvers (pressure-based)

- ✓ Highly mature numerical methods and computer codes.

## Compressible vs. Incompressible Solvers

### Incompressible Solvers (pressure-based)

- ✓ Highly mature numerical methods and computer codes.
- ✗ Assumes  $\nabla \cdot \mathbf{u} = 0$  (often even  $\rho = \text{constant}$ ), which is not a valid assumption for heat transfer in sCO<sub>2</sub> flows.

# Compressible vs. Incompressible Solvers

## Incompressible Solvers (pressure-based)

- ✓ Highly mature numerical methods and computer codes.
- ✗ Assumes  $\nabla \cdot \mathbf{u} = 0$  (often even  $\rho = \text{constant}$ ), which is not a valid assumption for heat transfer in sCO<sub>2</sub> flows.

## Compressible Solvers (density-based)

- ✓ Mature numerical methods, straightforward, and no inaccurate assumptions.

# Compressible vs. Incompressible Solvers

## Incompressible Solvers (pressure-based)

- ✓ Highly mature numerical methods and computer codes.
- ✗ Assumes  $\nabla \cdot \mathbf{u} = 0$  (often even  $\rho = \text{constant}$ ), which is not a valid assumption for heat transfer in sCO<sub>2</sub> flows.

## Compressible Solvers (density-based)

- ✓ Mature numerical methods, straightforward, and no inaccurate assumptions.
- ✗ Very expensive and sensitive to errors, because
  - it accounts for heat generation due to friction and compression;
  - all fluid properties depend on the density  $\rho$  and the enthalpy  $H$ .
  - determining the pressure by  $p = p(\rho, H)$  is very sensitive to errors;
  - the flow compresses the fluid  $\Rightarrow \rho$  increases  $\Rightarrow p$  increases.There is a finite speed of sound.  
*This is not the physics at low Ma;*

# Compressible vs. Incompressible Solvers

## Incompressible Solvers (pressure-based)

- ✓ Highly mature numerical methods and computer codes.
- ✗ Assumes  $\nabla \cdot \mathbf{u} = 0$  (often even  $\rho = \text{constant}$ ), which is not a valid assumption for heat transfer in sCO<sub>2</sub> flows.

## Compressible Solvers (density-based)

- ✓ Mature numerical methods, straightforward, and no inaccurate assumptions.
- ✗ Very expensive and sensitive to errors, because
  - it accounts for heat generation due to friction and compression;
  - all fluid properties depend on the density  $\rho$  and the enthalpy  $H$ .
  - determining the pressure by  $p = p(\rho, H)$  is very sensitive to errors;
  - the flow compresses the fluid  $\Rightarrow \rho$  increases  $\Rightarrow p$  increases.

There is a finite speed of sound.

*This is not the physics at low Ma;*

$\Rightarrow$  **high resolution, and 'stiff' linear systems.**



## Low-Mach Solver

Transport equations in the limit  $Ma \rightarrow 0$

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{u}) = 0 \quad \text{mass}$$

$$\frac{\partial m_i}{\partial t} + \nabla \cdot (\mathbf{u} m_i) = \frac{\partial}{\partial x_j} \tau_{ij} - \frac{\partial p}{\partial x_i} \quad \text{momentum}$$

$$\frac{\partial \rho h}{\partial t} + \nabla \cdot (\mathbf{u} \rho h) = \nabla \cdot ((\lambda/c_p) \nabla h) \quad \text{enthalpy}$$

The fluid properties ( $\rho, \nu, \lambda, \dots$ ) only depend on the enthalpy  $h$ .

## Low-Mach Solver

Transport equations in the limit  $Ma \rightarrow 0$

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{u}) = 0 \quad \text{mass}$$

$$\frac{\partial m_i}{\partial t} + \nabla \cdot (\mathbf{u} m_i) = \frac{\partial}{\partial x_j} \tau_{ij} - \frac{\partial p}{\partial x_i} \quad \text{momentum}$$

$$\frac{\partial \rho h}{\partial t} + \nabla \cdot (\mathbf{u} \rho h) = \nabla \cdot ((\lambda/c_p) \nabla h) \quad \text{enthalpy}$$

The fluid properties ( $\rho, \nu, \lambda, \dots$ ) only depend on the enthalpy  $h$ .

Low-Mach: the principled approach, not as well studied

- ✓ Assumptions are valid for heat transfer in sCO<sub>2</sub> for many flows.
- ✓ Pressure-based  $\Rightarrow$  no speed of sound  $\Rightarrow$  larger time steps.

# Low-Mach Solver

Transport equations in the limit  $Ma \rightarrow 0$

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{u}) = 0 \quad \text{mass}$$

$$\frac{\partial m_i}{\partial t} + \nabla \cdot (\mathbf{u} m_i) = \frac{\partial}{\partial x_j} \tau_{ij} - \frac{\partial p}{\partial x_i} \quad \text{momentum}$$

$$\frac{\partial \rho h}{\partial t} + \nabla \cdot (\mathbf{u} \rho h) = \nabla \cdot ((\lambda/c_p) \nabla h) \quad \text{enthalpy}$$

The fluid properties ( $\rho, \nu, \lambda, \dots$ ) only depend on the enthalpy  $h$ .

Low-Mach: the principled approach, not as well studied

- ✓ Assumptions are valid for heat transfer in sCO<sub>2</sub> for many flows.
- ✓ Pressure-based  $\Rightarrow$  no speed of sound  $\Rightarrow$  larger time steps.
- ✗ Less straightforward than the fully compressible formulation.  
Numerical methods are less mature, especially for finite elements.

# The pressure-correction method

## The Algorithm

- 1 Solve the enthalpy transport equation.
- 2 Solve the momentum transport equation.
- 3 Solve a Poisson equation ( $-\Delta\phi = \dots$ ).
- 4 Correct the pressure and the mass flux (with  $\phi$ ).

This is a time-splitting method: the transport equations are solved one by one in each time step. **This is much cheaper than a compressible solver.**

Our method is stable without iterating within a time step, with **full second-order temporal accuracy.**

## Unresolved issues with Low-Mach Solvers: An Example

### What enthalpy/energy variable to choose?

Solving for the volumetric enthalpy  $H = \rho h$  [J/m<sup>3</sup>]

- ✓ The temporal derivative is easy:

$$\frac{\partial H}{\partial t} \approx \frac{1}{\delta t} (H^{n+1} - H^n) .$$

## Unresolved issues with Low-Mach Solvers: An Example

### What enthalpy/energy variable to choose?

Solving for the volumetric enthalpy  $H = \rho h$  [J/m<sup>3</sup>]

- ✓ The temporal derivative is easy:

$$\frac{\partial H}{\partial t} \approx \frac{1}{\delta t} (H^{n+1} - H^n) .$$

- ✗ There is no one-to-one correspondence between  $H$  and  $\rho$ .

# Unresolved issues with Low-Mach Solvers: An Example

## What enthalpy/energy variable to choose?

Solving for the volumetric enthalpy  $H = \rho h$  [J/m<sup>3</sup>]

- ✓ The temporal derivative is easy:

$$\frac{\partial H}{\partial t} \approx \frac{1}{\delta t} (H^{n+1} - H^n) .$$

- ✗ There is no one-to-one correspondence between  $H$  and  $\rho$ .

Solving for specific enthalpy  $h$  [J/kg]

- ✓ All fluid properties can be calculated from  $h$ .
- ✗ The temporal derivative is hard:

$$\frac{\partial \rho h}{\partial t} \approx \frac{1}{\delta t} ((\rho h)^{n+1} - (\rho h)^n) .$$

# Unresolved issues with Low-Mach Solvers: An Example

## What enthalpy/energy variable to choose?

Solving for the volumetric enthalpy  $H = \rho h$  [J/m<sup>3</sup>]

- ✓ The temporal derivative is easy:

$$\frac{\partial H}{\partial t} \approx \frac{1}{\delta t} (H^{n+1} - H^n) .$$

- ✗ There is no one-to-one correspondence between  $H$  and  $\rho$ .

Solving for specific enthalpy  $h$  [J/kg]

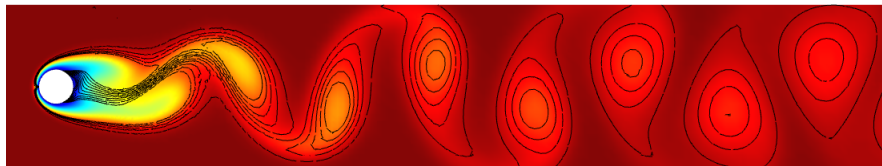
- ✓ All fluid properties can be calculated from  $h$ .
- ✗ The temporal derivative is hard:

$$\frac{\partial \rho h}{\partial t} \approx \frac{1}{\delta t} ((\rho h)^{n+1} - (\rho h)^n) .$$

The term  $(\rho h)^{n+1}$  is nonlinear, because  $\rho^{n+1}$  is a function of  $h^{n+1}$ .



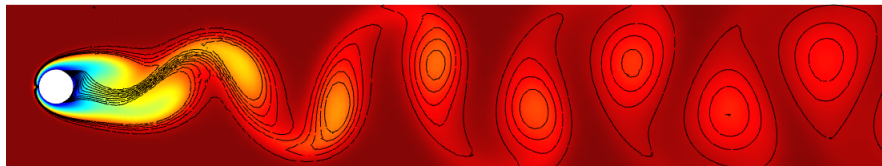
## Heated Vortex Shedding: a DNS Example



$\rho$ , overlaid with isolines of  $\text{curl}(\mathbf{u})$ .

$$\rho_{\max}/\rho_{\min} \approx 1.7$$

## Heated Vortex Shedding: a DNS Example



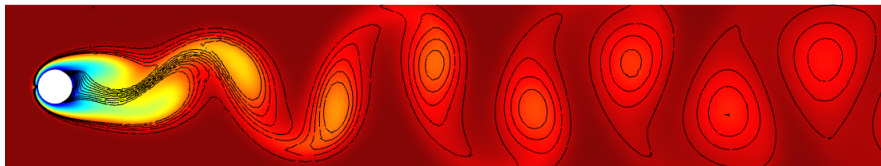
$\rho$ , overlaid with isolines of  $\text{curl}(\mathbf{u})$ .

$$\rho_{\max}/\rho_{\min} \approx 1.7$$

### Flow past a circular wire

- Generates a Kármán vortex street behind the wire.
- Heating the wire alters  $\rho$  and  $\mu$

# Heated Vortex Shedding: a DNS Example



$\rho$ , overlaid with isolines of  $\text{curl}(\mathbf{u})$ .

$$\rho_{\max}/\rho_{\min} \approx 1.7$$

## Flow past a circular wire

- Generates a Kármán vortex street behind the wire.
- Heating the wire alters  $\rho$  and  $\mu$
- The shedding frequencies can be compared to experimental data. Our results agree to within 1%.

# Large Eddy Simulation (LES): the idea

The code is very similar to a DNS solver.

- The same governing equations, but add extra viscosity:

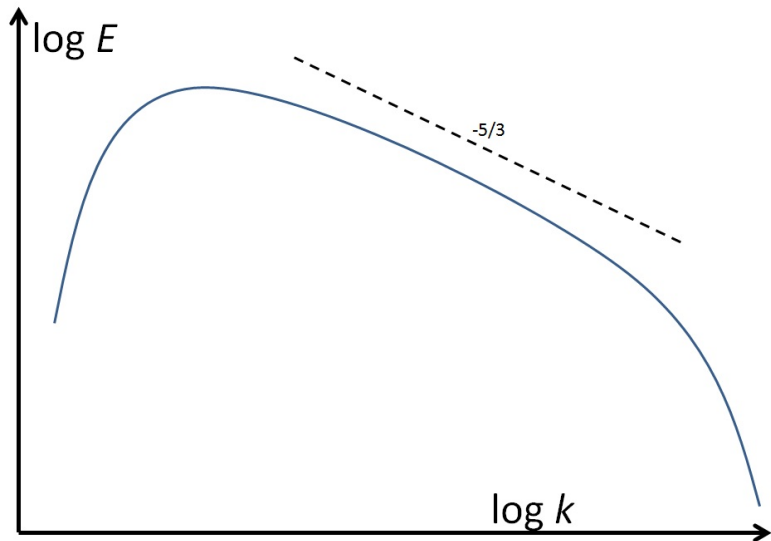
$$\nu \leftarrow \nu + \nu_{\text{SGS}} .$$

$\nu_{\text{SGS}}$  is the sub-grid-scale viscosity.

- This suppresses small-scale vortices that cannot be simulated.
- $\nu_{\text{SGS}}$  is based on the velocity field.

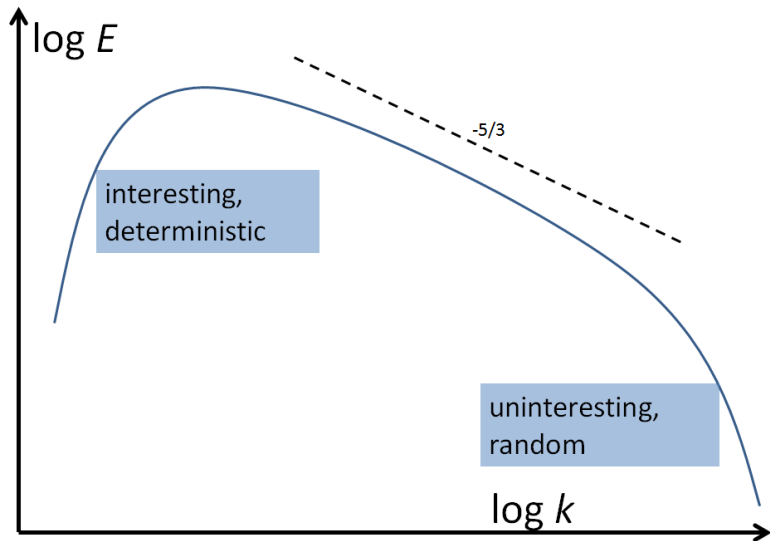
# Large Eddy Simulation (LES): the idea

Large scales vs. small scales: energy spectrum



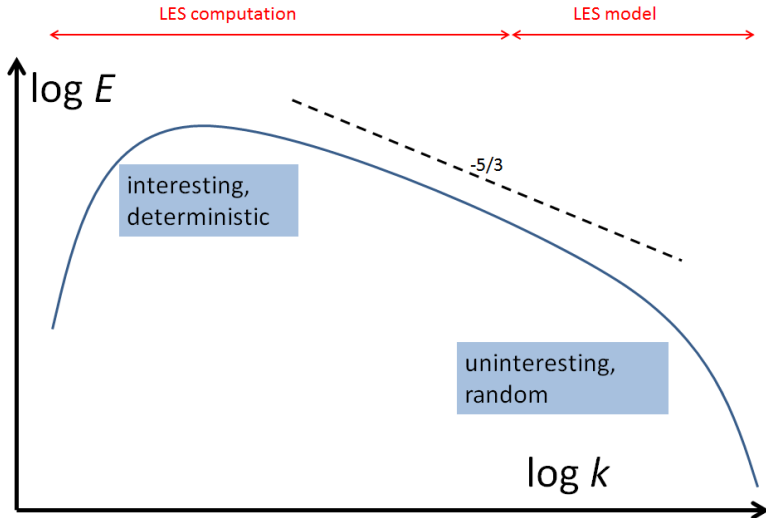
# Large Eddy Simulation (LES): the idea

Large scales vs. small scales: energy spectrum



# Large Eddy Simulation (LES): the idea

- Compute large movements, model small scales.
- **Isolate the deterministic part.**



## Examples of LES models

$$\nu \leftarrow \nu + \nu_{\text{SGS}}$$



## Examples of LES models

$$\nu \leftarrow \nu + \nu_{\text{SGS}}$$

### The Smagorinsky model

- Simple, and traditionally by far the most widely used.
- Linear in the rate of strain:  $\nu_{\text{SGS}} \propto |S|$

$$S = \nabla \mathbf{u} + \nabla \mathbf{u}^T - \frac{2}{3}(\nabla \cdot \mathbf{u})I \quad (1)$$

## Examples of LES models

$$\nu \leftarrow \nu + \nu_{\text{SGS}}$$

### The Smagorinsky model

- Simple, and traditionally by far the most widely used.
- Linear in the rate of strain:  $\nu_{\text{SGS}} \propto |S|$

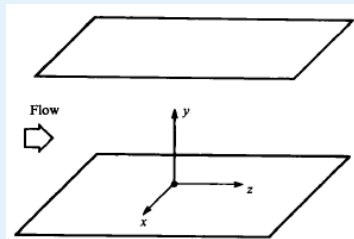
$$S = \nabla \mathbf{u} + \nabla \mathbf{u}^T - \frac{2}{3}(\nabla \cdot \mathbf{u})I \quad (1)$$

### The WALE model

- WALE: Wall-adapted Local Eddy Viscosity.
- Non-linear in the rate of strain.  
 $\nu_{\text{SGS}}$  is a function of both both  $\nabla \mathbf{u}$  and  $\nabla \mathbf{u} \cdot (\nabla \mathbf{u})^T$
- Constructed to get the correct scaling near a wall:  $\nu_{\text{SGS}} \propto (y^+)^3$ .

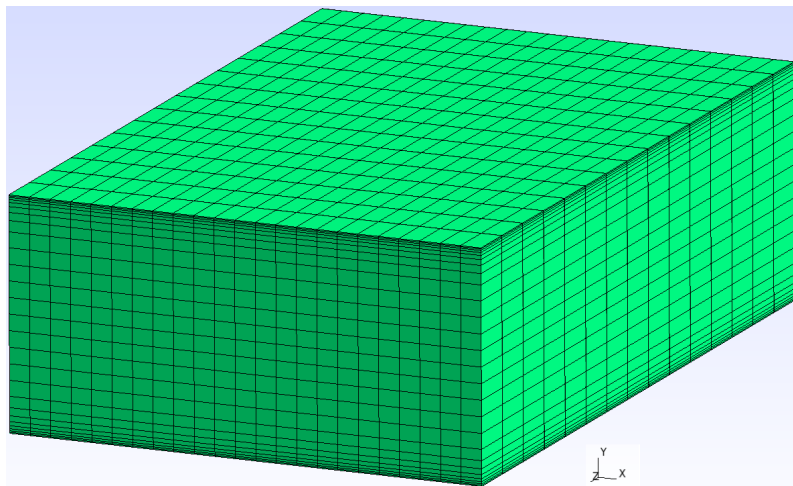
# Start 'Simple': Plane Channel Flow

## The most basic wall-bounded flow



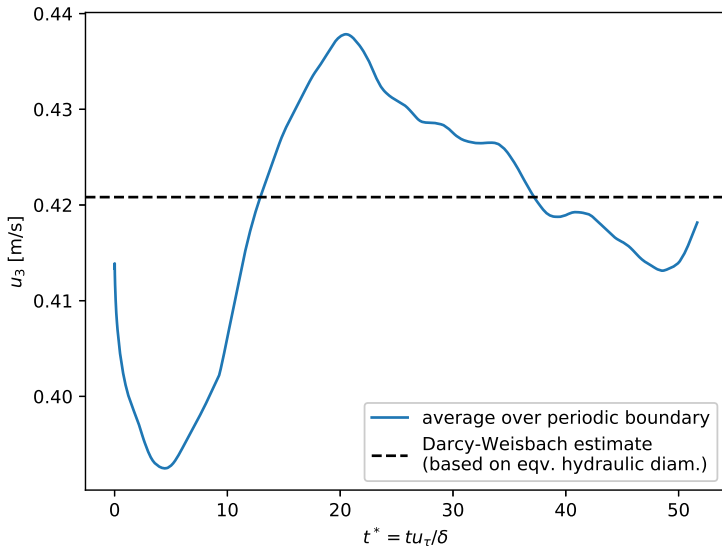
- Still far from trivial.
- Bedrock for first DNS papers, and a large part of LES literature.
- New papers are being published all the time.
- There are experimental results, but DNS is better.

## LES with DG: Isothermal Results



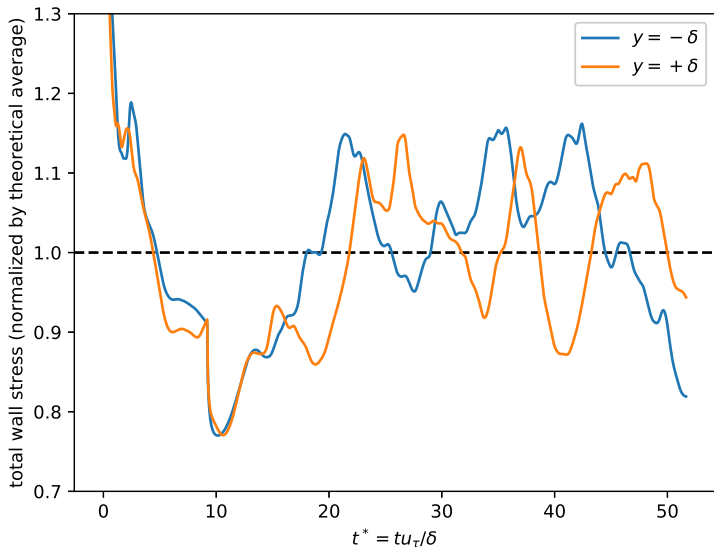
# LES for isothermal Flow: Converge to statistical average

Mass flow:

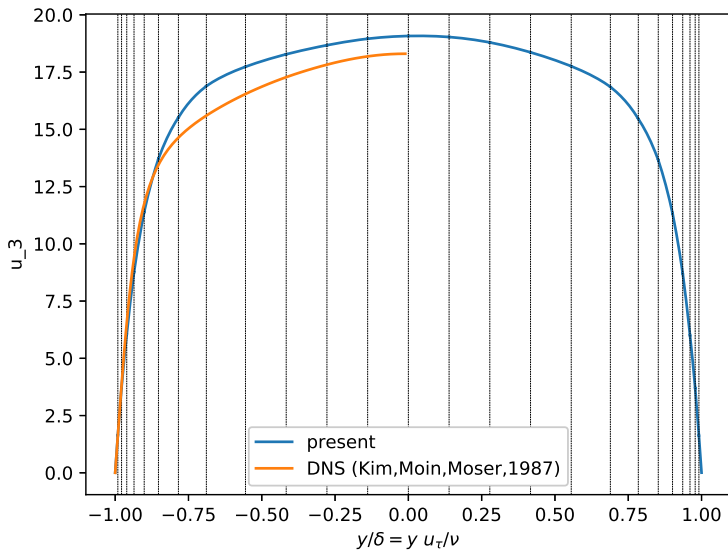


# LES for isothermal Flow: Converge to statistical average

Wall stress:



# LES for isothermal Flow: Average velocity profile



# LES with DG: Isothermal Results

- Friction Reynolds number:  $Re_\tau = 180$
- 1 wall unit =  $\delta/Re_\tau$
- Kolmogorov length  $\approx 2$  wall units
- **LES** (present case):
  - # DOFs: **0.1 M**
  - max. element size:  $\sim 23$  wall units
  - Completely general method, for all geometries.
- **DNS** (Kim, Moin, and Moser, 1987)<sup>2</sup>:
  - # DOFs: **4 M**
  - max. element size: 4.4 wall units
  - Highly specialized code and method for this particular geometry.
- Domain shape and averaging time: same for DNS and LES

---

<sup>2</sup>J. Kim, P. Moin, and R. Moser (1987). "Turbulence statistics in fully developed channel flow at low Reynolds number". In: *Journal of Fluid Mechanics* 177.-1, p. 133. DOI: 10.1017/S0022112087000892

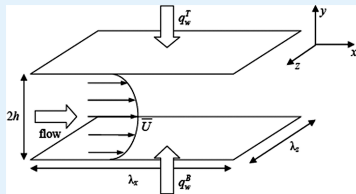


## LES with DG: Isothermal results

- stresses are not great
- velocity is OK ( $\sim 10\%$  off)
- I adjusted the mesh and the LES filter width independently. The error is mainly due to LES model, not the discretization.
- The simulation is very well resolved. . . too well resolved.

# Channel Flow with sCO<sub>2</sub>: Compare LES to DNS

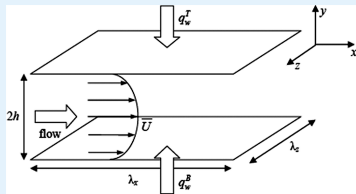
## The most basic wall-bounded flow



- $p = 8.0 \text{ MPa}$
- $T = 335.0 \text{ K}$  at  $y = -\delta$   
 $T = 345.0 \text{ K}$  at  $y = \delta$
- No Buoyancy

# Channel Flow with sCO<sub>2</sub>: Compare LES to DNS

## The most basic wall-bounded flow



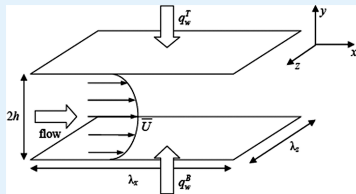
- $p = 8.0$  MPa
- $T = 335.0$  K at  $y = -\delta$   
 $T = 345.0$  K at  $y = \delta$
- No Buoyancy

## DNS with compressible solver

- DG-based code Flexi, developed in Stuttgart.
- $Ma = 0.2$   
The thermodynamic pressure fluctuates about 8.0 MPa.
- **degrees of freedom: 198M**

# Channel Flow with sCO<sub>2</sub>: Compare LES to DNS

## The most basic wall-bounded flow



- $p = 8.0$  MPa
- $T = 335.0$  K at  $y = -\delta$   
 $T = 345.0$  K at  $y = \delta$
- No Buoyancy

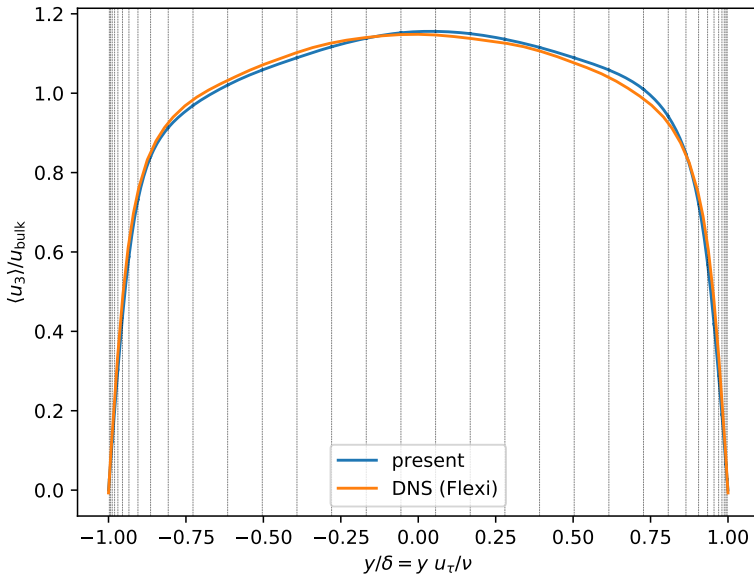
## DNS with compressible solver

- DG-based code Flexi, developed in Stuttgart.
- $Ma = 0.2$   
The thermodynamic pressure fluctuates about 8.0 MPa.
- **degrees of freedom: 198M**

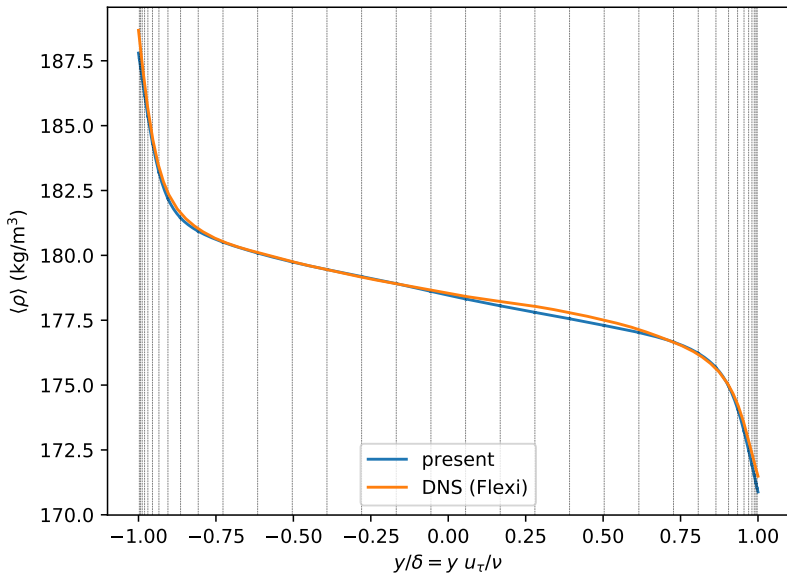
## LES with low-Mach solver

- DG-based code DGFloWS, developed in Delft.
- $Ma \rightarrow 0$   
The thermodynamic pressure is 8.0 MPa.
- **degrees of freedom: 0.46M**

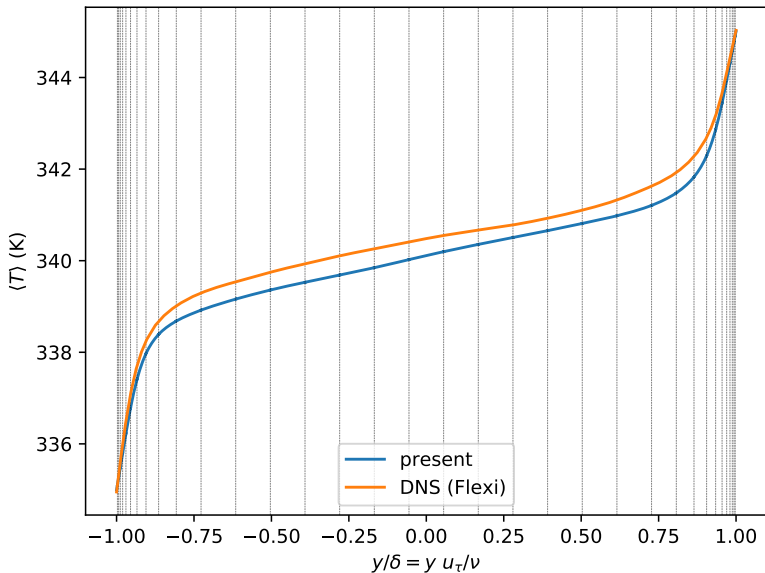
# LES for sCO<sub>2</sub> Channel Flow: Average Velocity



# LES for sCO<sub>2</sub> Channel Flow: Average Temperature



# LES for sCO<sub>2</sub> Channel Flow: Average Density



## LES for sCO<sub>2</sub> Channel Flow: How well do our results compare?

### DNS with compressible solver

- DG-based code Flexi, developed in Stuttgart.
- $Ma = 0.2$   
The thermodynamic pressure fluctuates about 8.0 MPa.
- **degrees of freedom: 198M**

### LES with low-Mach solver

- DG-based code DGFlows, developed in Delft.
- $Ma \rightarrow 0$   
The thermodynamic pressure is 8.0 MPa.
- **degrees of freedom: 0.46M**

### How do they compare?

- Maximum differences are low (3% for the velocity)



# LES for sCO<sub>2</sub> Channel Flow: How well do our results compare?

## DNS with compressible solver

- DG-based code Flexi, developed in Stuttgart.
- $Ma = 0.2$   
The thermodynamic pressure fluctuates about 8.0 MPa.
- **degrees of freedom: 198M**

## LES with low-Mach solver

- DG-based code DGFlows, developed in Delft.
- $Ma \rightarrow 0$   
The thermodynamic pressure is 8.0 MPa.
- **degrees of freedom: 0.46M**

## How do they compare?

- Maximum differences are low (3% for the velocity)
- The difference in Mach number is probably more significant than the modeling errors and the numerical errors.

## Is LES physics or numerics?

LES is a physical model.

- There is a theoretical foundation for the Smagorinsky model in bulk flow.
- LES models are qualitatively correct.

## Is LES physics or numerics?

LES is a physical model.

- There is a theoretical foundation for the Smagorinsky model in bulk flow.
- LES models are qualitatively correct.

LES is a numerical technique.

## Is LES physics or numerics?

LES is a physical model.

- There is a theoretical foundation for the Smagorinsky model in bulk flow.
- LES models are qualitatively correct.

LES is a numerical technique.

- $\nu_{\text{Smag}}$  does not correlate well with actual subgrid tensor from DNS data. (0.3 at best)

## Is LES physics or numerics?

LES is a physical model.

- There is a theoretical foundation for the Smagorinsky model in bulk flow.
- LES models are qualitatively correct.

LES is a numerical technique.

- $\nu_{\text{Smag}}$  does not correlate well with actual subgrid tensor from DNS data. (0.3 at best)
- Some models correlate much better (e.g., the self-similarity model), but often perform worse.

## Is LES physics or numerics?

LES is a physical model.

- There is a theoretical foundation for the Smagorinsky model in bulk flow.
- LES models are qualitatively correct.

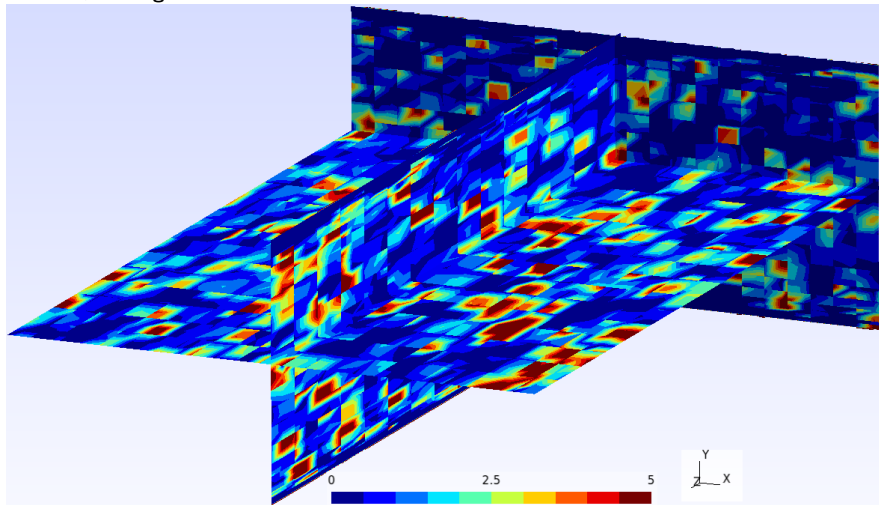
LES is a numerical technique.

- $\nu_{\text{Smag}}$  does not correlate well with actual subgrid tensor from DNS data. (0.3 at best)
- Some models correlate much better (e.g., the self-similarity model), but often perform worse.
- Highly effective models (e.g., WALE) often have artificial motivations.

Another example: The QR model is new, promising, and *purely* designed to stabilize the numerical method.

## Comparing $\nu_{\text{WALE}}$ to $\nu_{\text{Smag}}$

$\nu_{\text{WALE}}/\nu_{\text{Smag}}$  is totally erratic.



## Some Conclusions



## Some Conclusions

- ① Using a pressure-based low-Mach solver is much better than pushing a density-based compressible solver to  $Ma = 0.2$ .

## Some Conclusions

- ① Using a pressure-based low-Mach solver is much better than pushing a density-based compressible solver to  $Ma = 0.2$ .
- ② Large Eddy Simulation can work wonders for the computational cost, even if the underlying model is not accurate.

## Some Conclusions

- ① Using a pressure-based low-Mach solver is much better than pushing a density-based compressible solver to  $Ma = 0.2$ .
- ② Large Eddy Simulation can work wonders for the computational cost, even if the underlying model is not accurate.
- ③ If you want 'just want results' for heat transfer in  $sCO_2$ , then consider implementing a few new LES ideas into an established code.

# Acknowledgements

I am grateful to

the [sCO<sub>2</sub>-HeRo project](#) , European research and training program 2014-2018 (grant agreement ID 662116) for funding my PhD;

the [University of Stuttgart](#) , Institut für Kernenergetik und Energiesysteme (IKE), for hosting me, computational resources, and a very pleasant collaboration;

the [ENEN+ project](#) , that has received funding from the Euratom research and training Work Programme 2016-2017 - 1 #755576, for supporting my work with a travel grant to Stuttgart.

Thank you!

# Large Eddy Simulation of sCO<sub>2</sub> with a Discontinuous Galerkin Method

Aldo Hennink  
a.hennink@tudelft.nl

Delft University of Technology

2019-09-20