



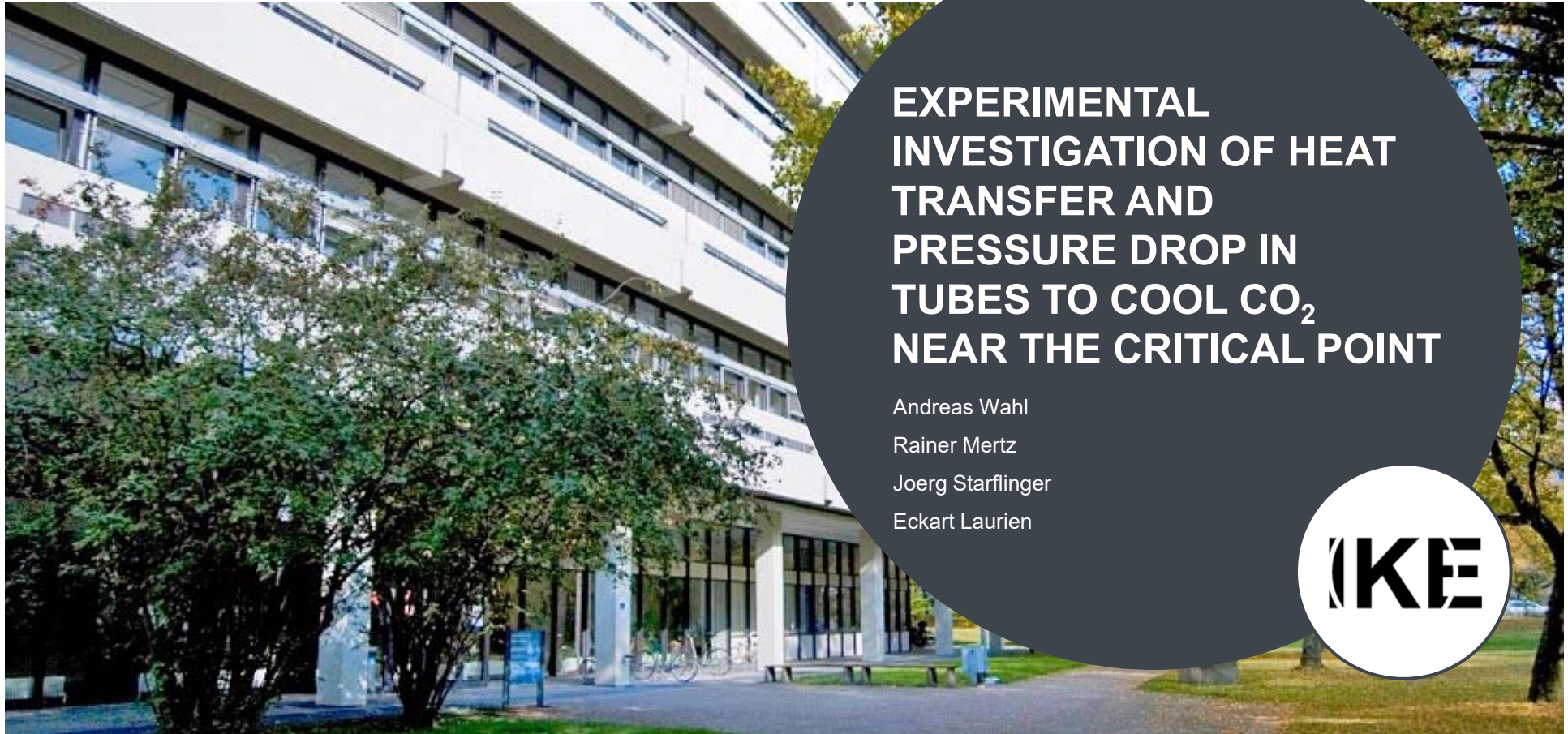
University of Stuttgart
Germany



EXPERIMENTAL INVESTIGATION OF HEAT TRANSFER AND PRESSURE DROP IN TUBES TO COOL CO₂ NEAR THE CRITICAL POINT

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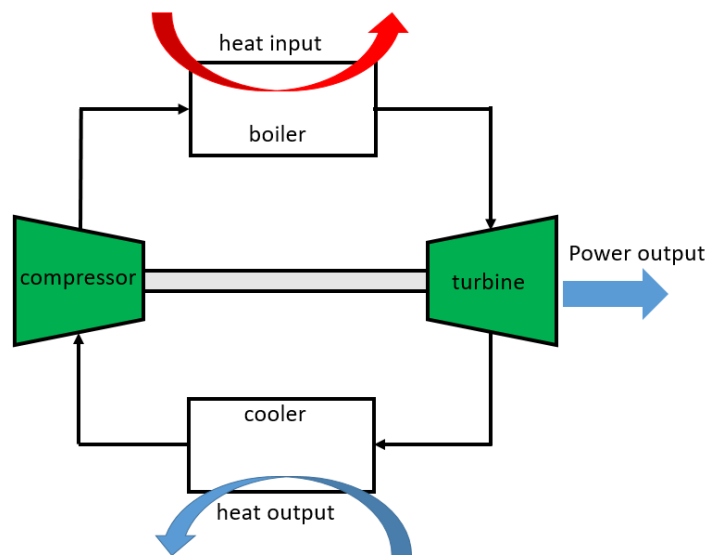


Outline

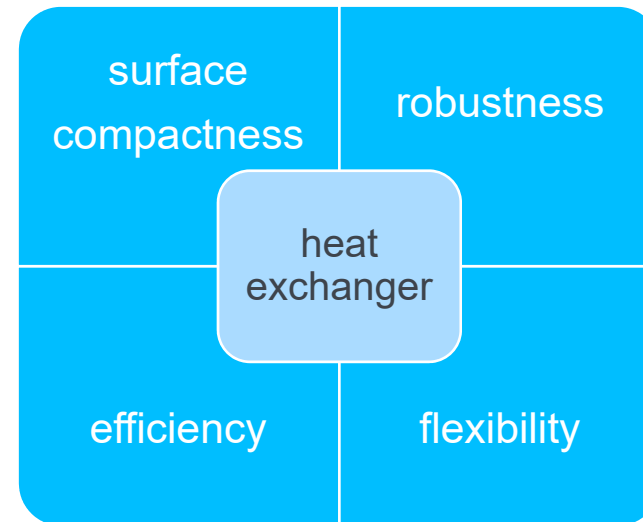
- Motivation and aims
- Experimental setup
- Data reduction
- Results
- Conclusion and next steps

Motivation

- flexible and efficient 25 MWe sCO₂ brayton cycle



sCO₂flex[®]



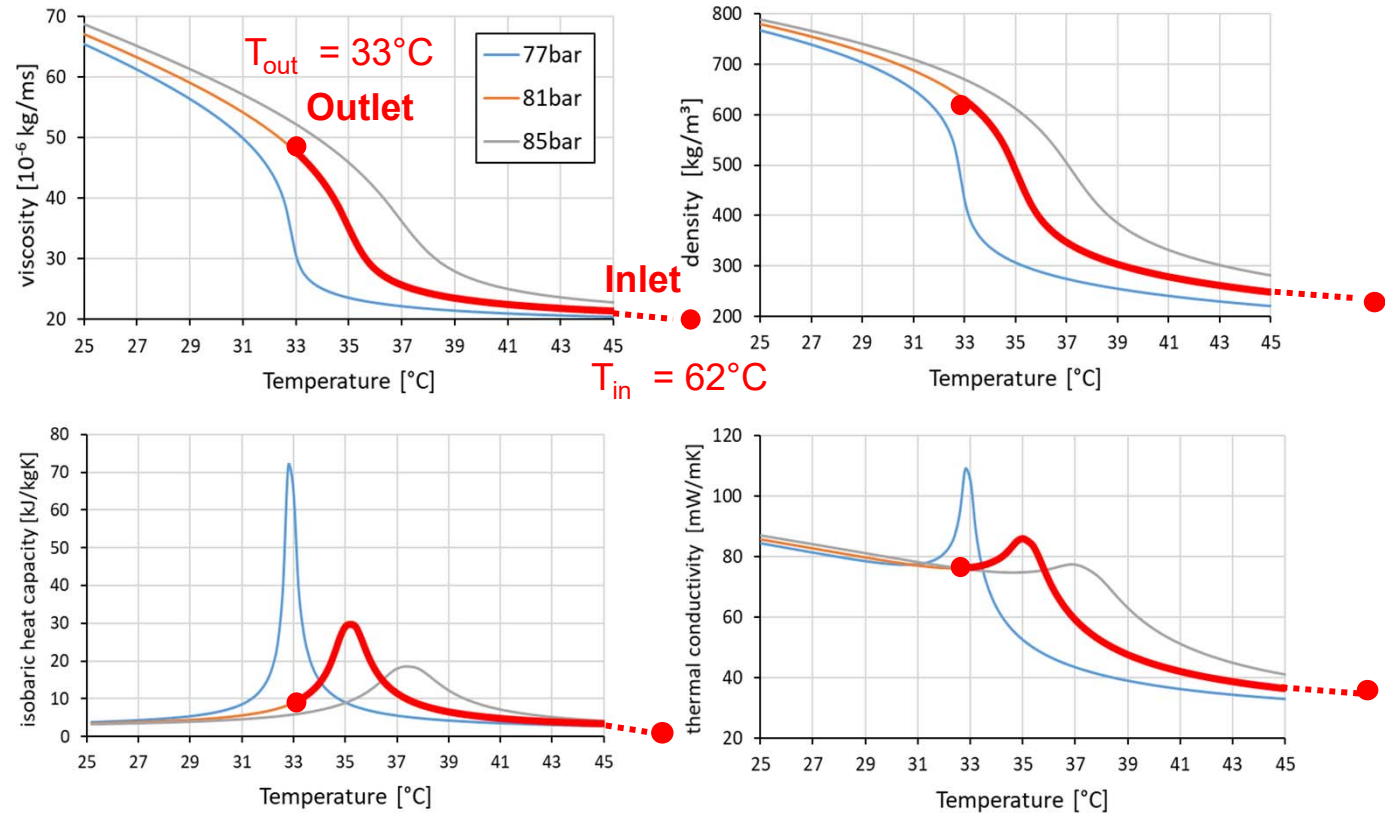
- Support of the development of compact heat exchanger
 - surface compactness
 - robustness

Variabel fluid properties near the critical point of CO₂

- Design point
 - $p_{in} = 81 \text{ bar}$,
 - $T_{in} = 62^\circ\text{C}$,
 - $T_{out} = 33^\circ\text{C}$
- Variable fluid properties influence local heat transfer

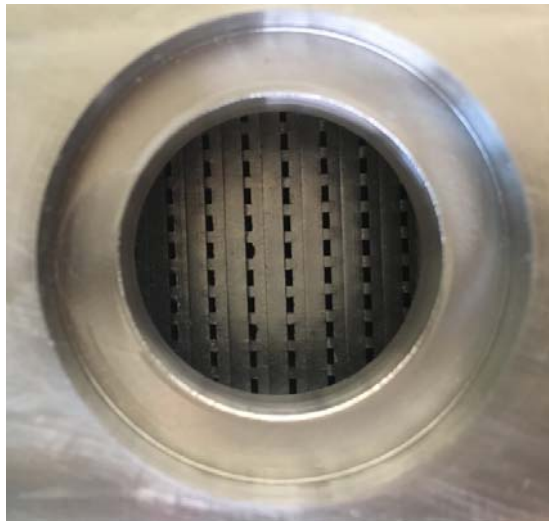
127 — CONFIGURATION OF A FLEXIBLE AND EFFICIENT SCO₂ CYCLE FOR FOSSIL POWER PLANT

156 — PART-LOAD OPERATION OF COAL FIRED SCO₂ POWER PLANTS



Aim of work

- Experimental cooling heat transfer and pressure drop in 2 mm single channel flow
- recommendation of heat transfer correlation to be used for design of compact HX



Compact HX, IKE, Stuttgart

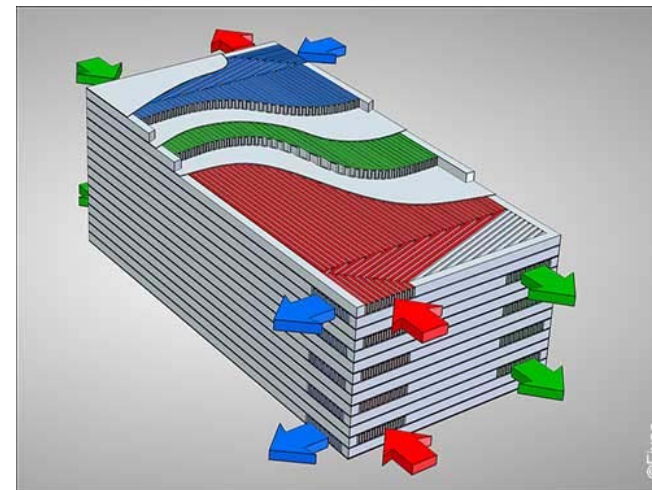
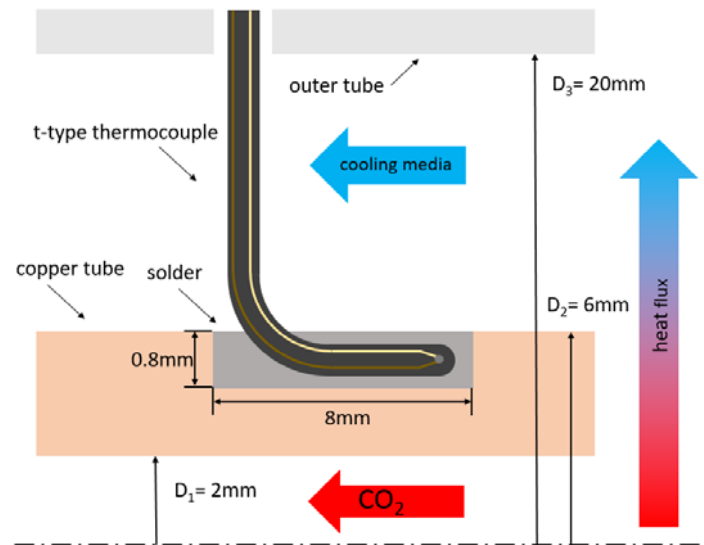
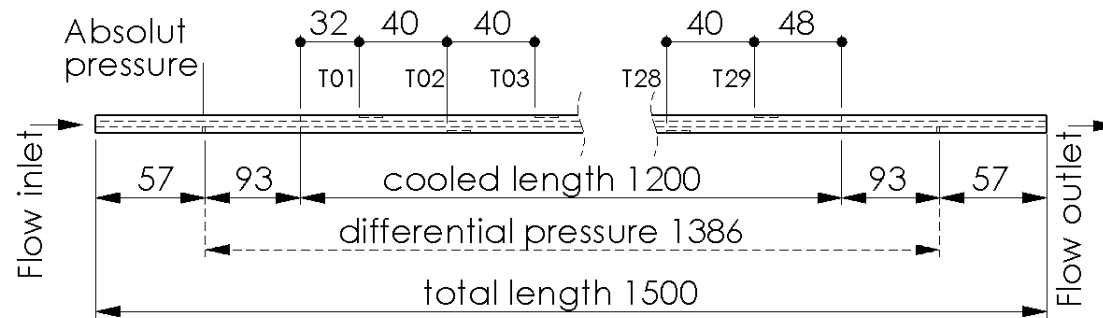


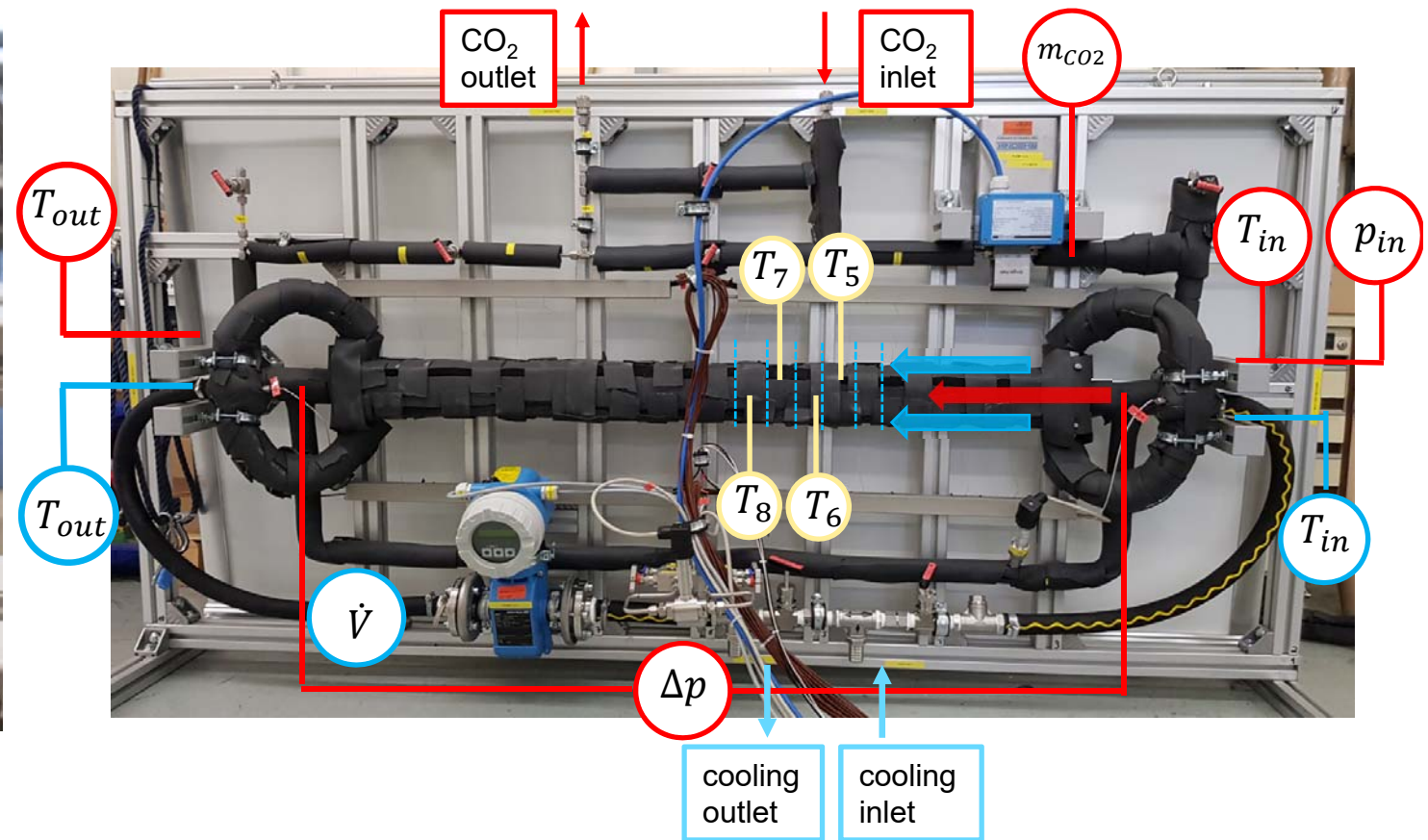
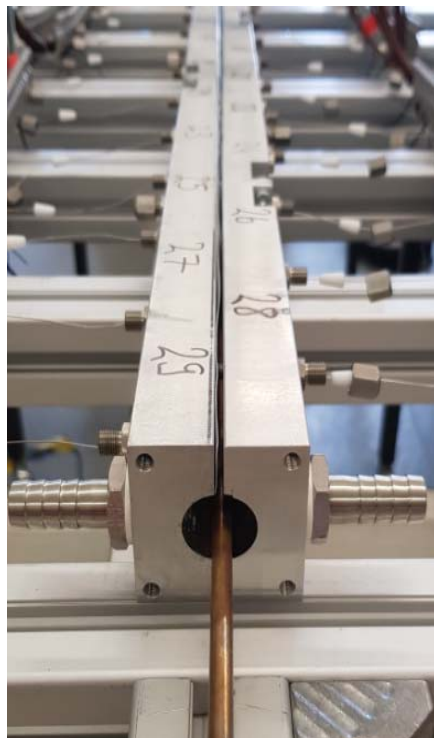
Plate and Fin HX, Fives Cryo, France
150 – HIGHLY EFFICIENT PLATE-FIN HEAT EXCHANGER (PFHE)
TECHNICAL DEVELOPMENT FOR S-CO₂ POWER CYCLES

Experimental setup for cooling heat transfer (I)



Experimental setup for cooling heat transfer (II)

150 — OPERATIONAL EXPERIENCES
AND DESIGN OF THE SCO₂-HERO LOOP



Experimental matrix

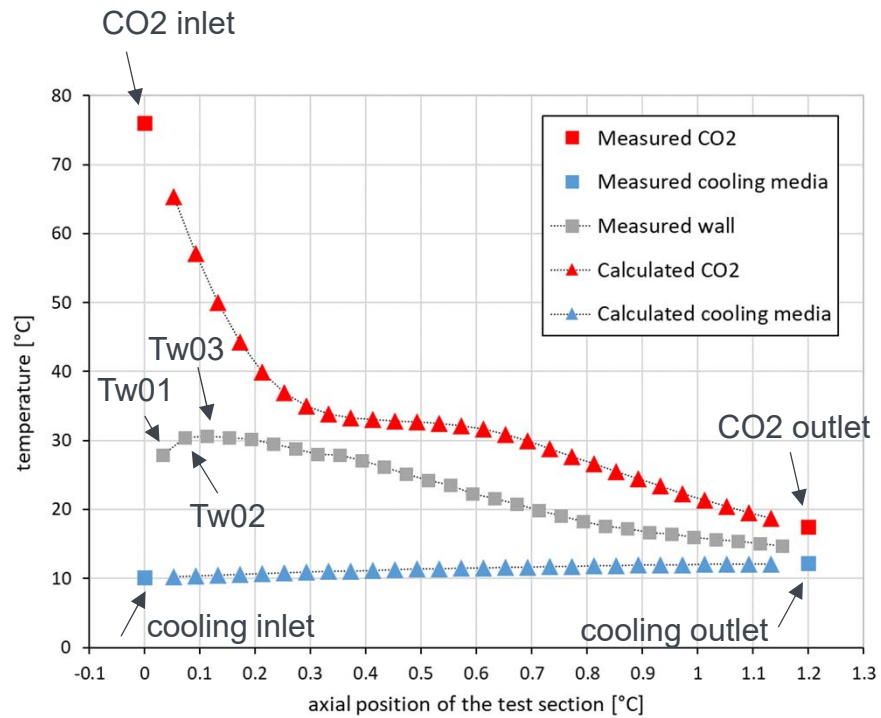
CO ₂		
Temperature [° C]	Pressure [bar]	Mass flux [kg/m ² s]
60	77	400
80	81	850
	85	1400

Cooling media	
Temperature [° C]	Volumetric flow [l/s]
10-25	0.1-0.2

condition	Flow direction	Number of experiments
isothermal	horizontal	91
cooled	horizontal	64
cooled	upwards	25
cooled	downwards	18

} = 198

Data reduction



- Assumption:

1. $h_{tc_{cool}} = \text{constant}$

Calculation:

1. $\dot{Q}_{cool} = h_{tc_{cool}} \cdot A_{out} \cdot (T_{wall} - T_{cool})$

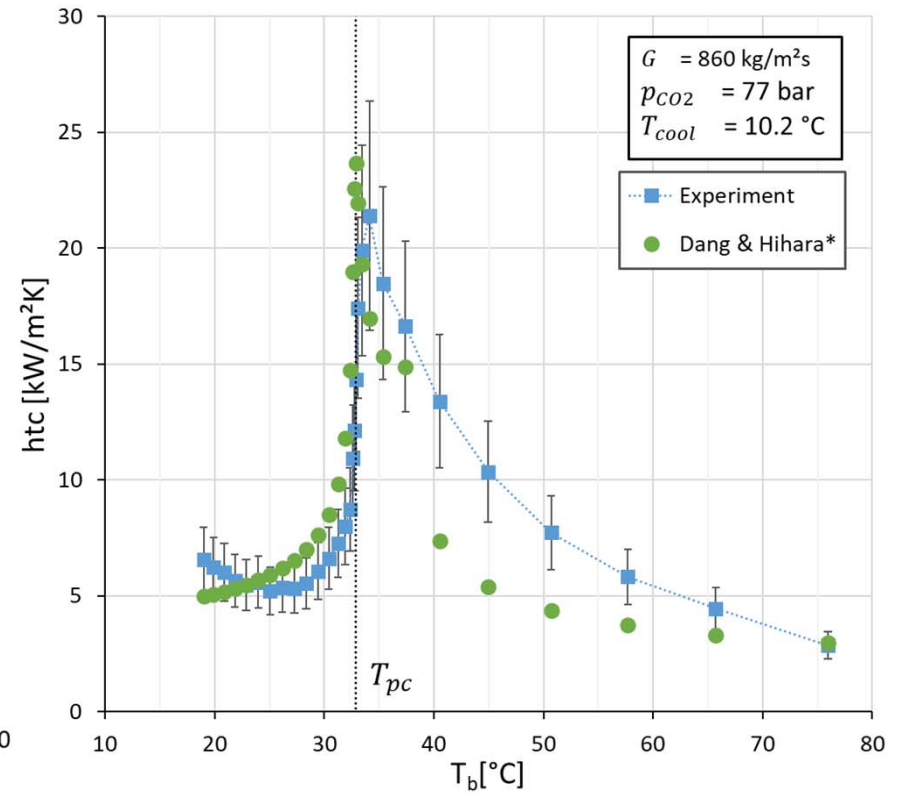
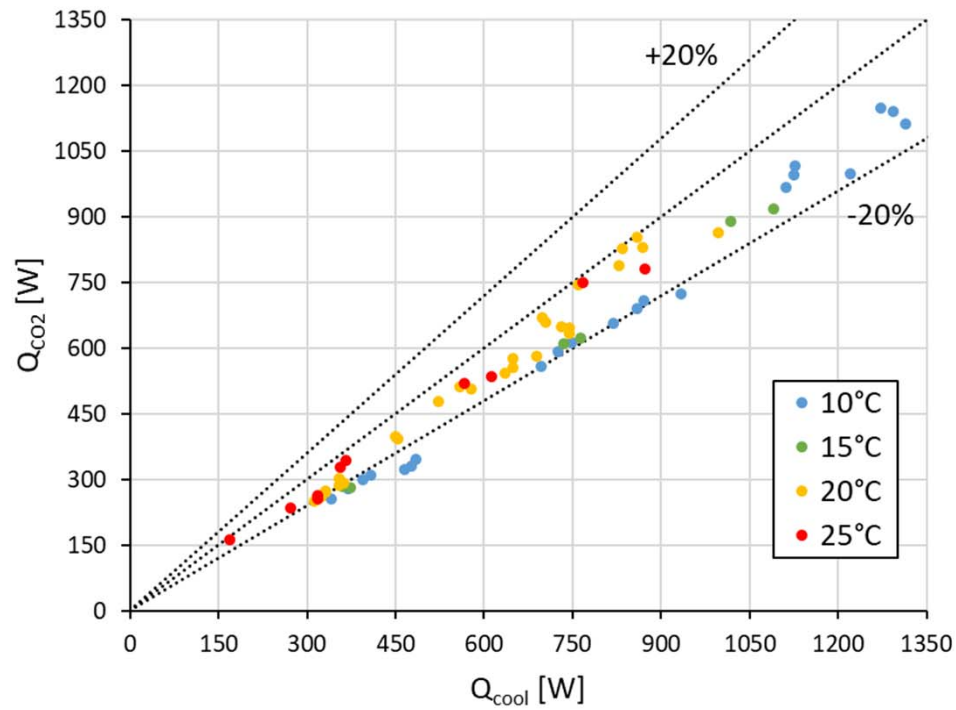
2. $\dot{Q}_{CO2} = \dot{Q}_{cool} = h_{tc_{CO2}} \cdot A_{in} \cdot (T_{CO2} - T_{wall})$

3. $H_{cool}(x) = H_{cool}(0) + \frac{\pi d}{\dot{m}_{cool}} \int_0^x \dot{q}(x) dx$

4. $H_{CO2}(x) = H_{CO2}(0) - \frac{\pi d}{\dot{m}_{CO2}} \int_0^x \dot{q}(x) dx$

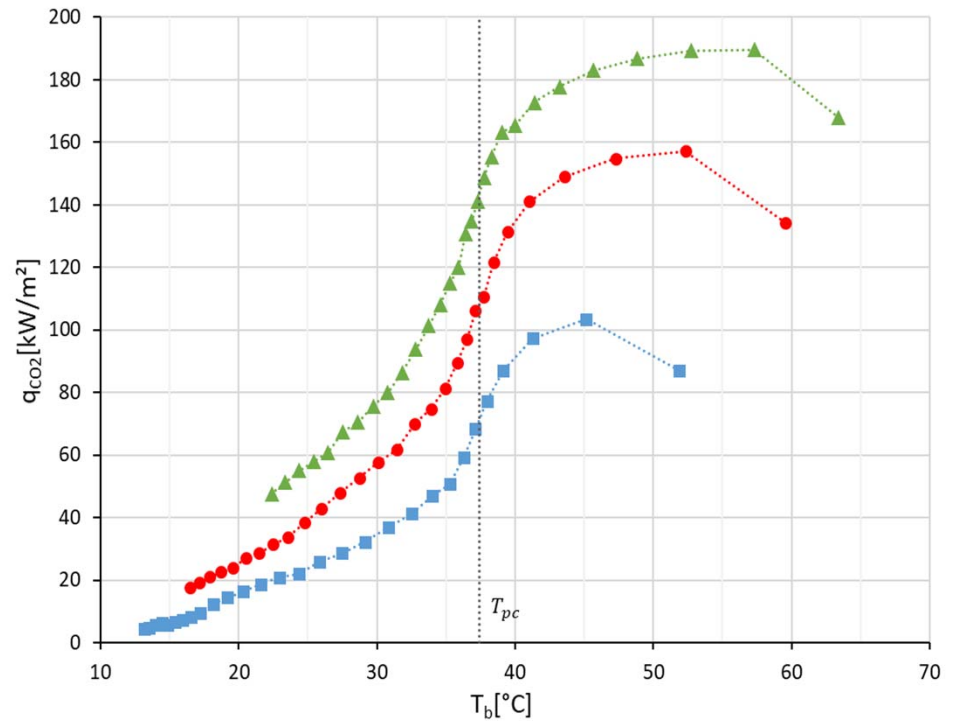
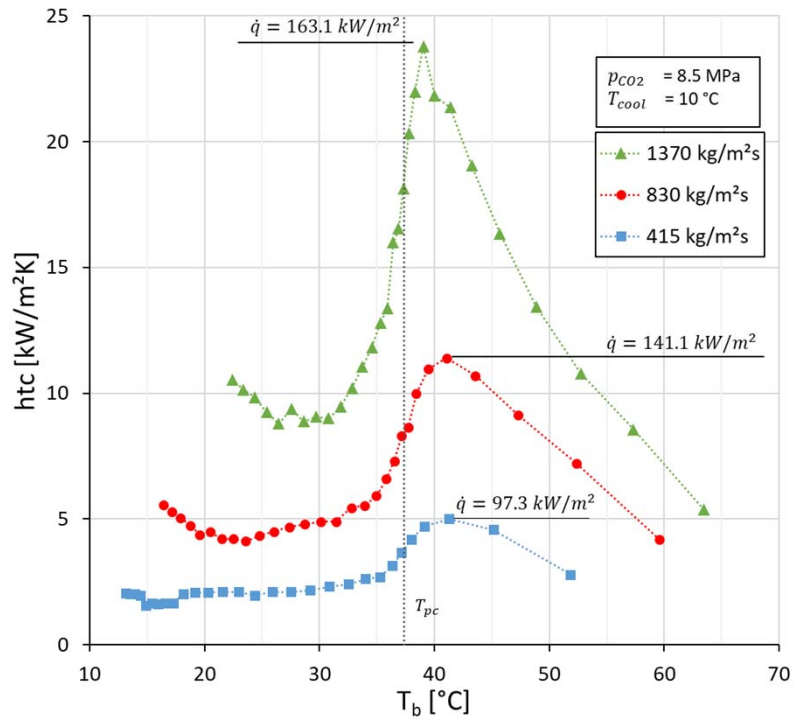
- Fluid properties: NIST-REFPROP

Experimental system validation

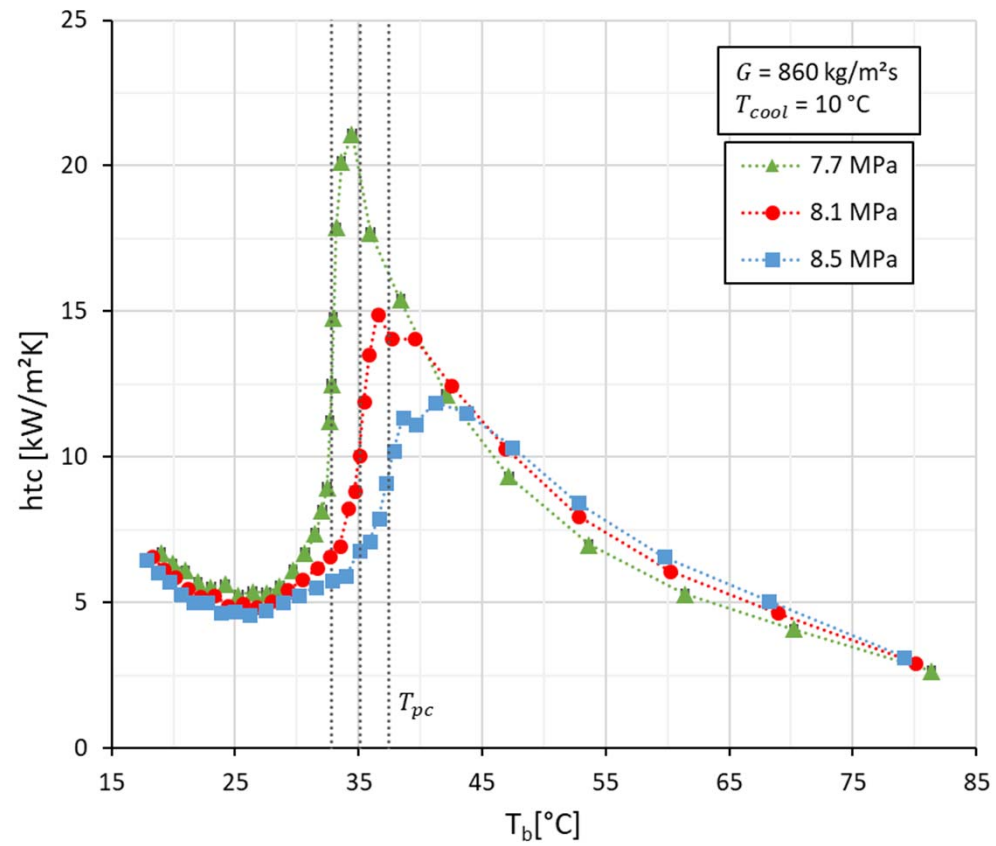


* C. Dang and E. Hihara, "In-tube cooling heat transfer of supercritical carbon dioxide. Part 1. Experimental measurement", *International Journal of Refrigeration* (7), pp. 736–747 (2004).

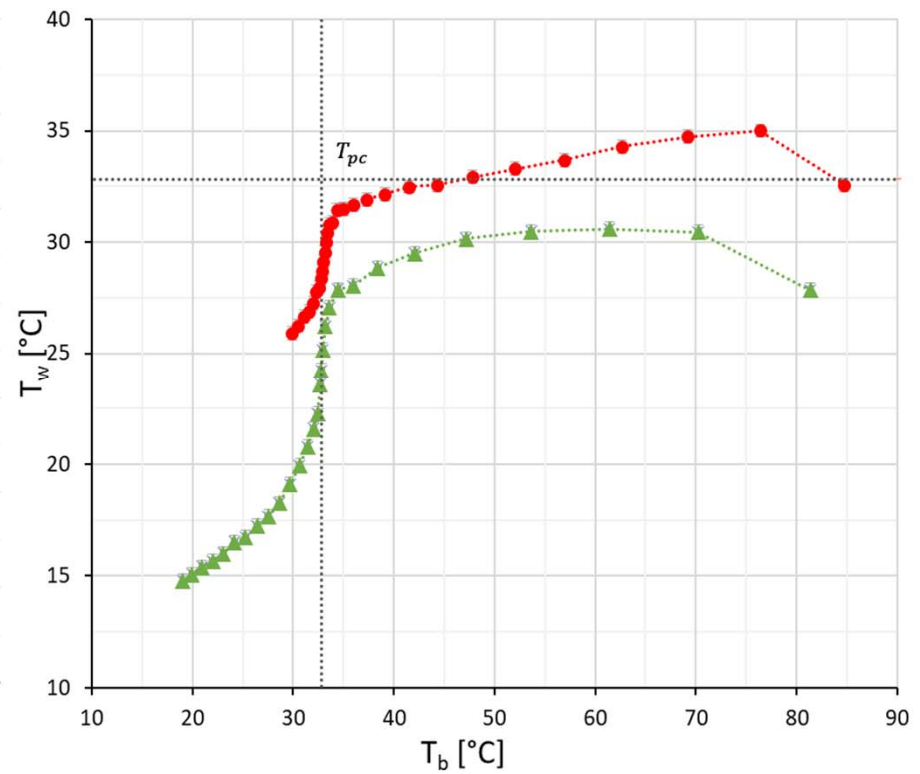
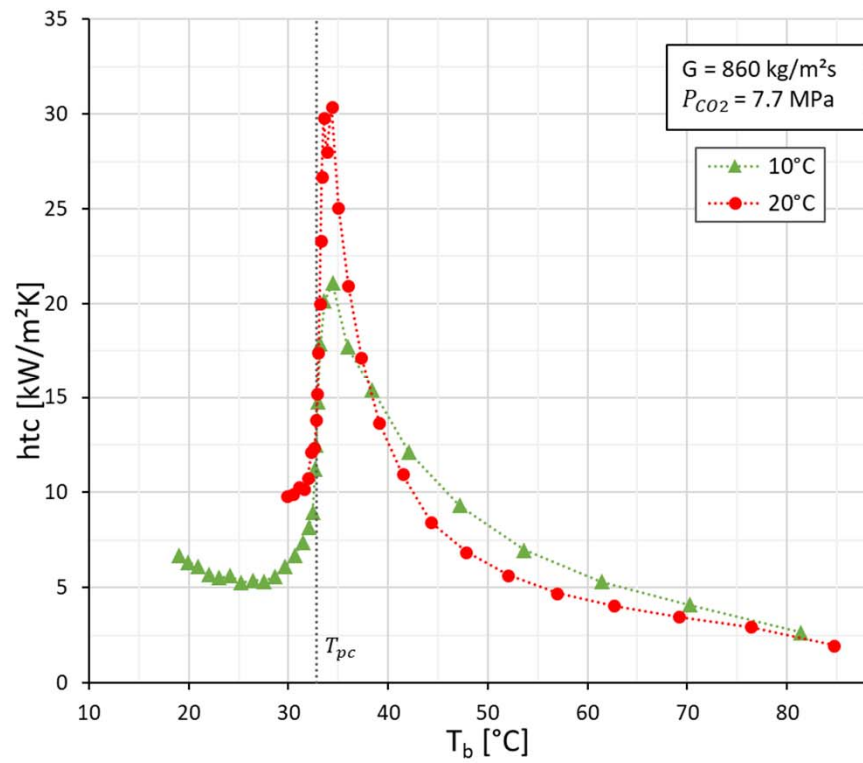
Effect of mass flux variation



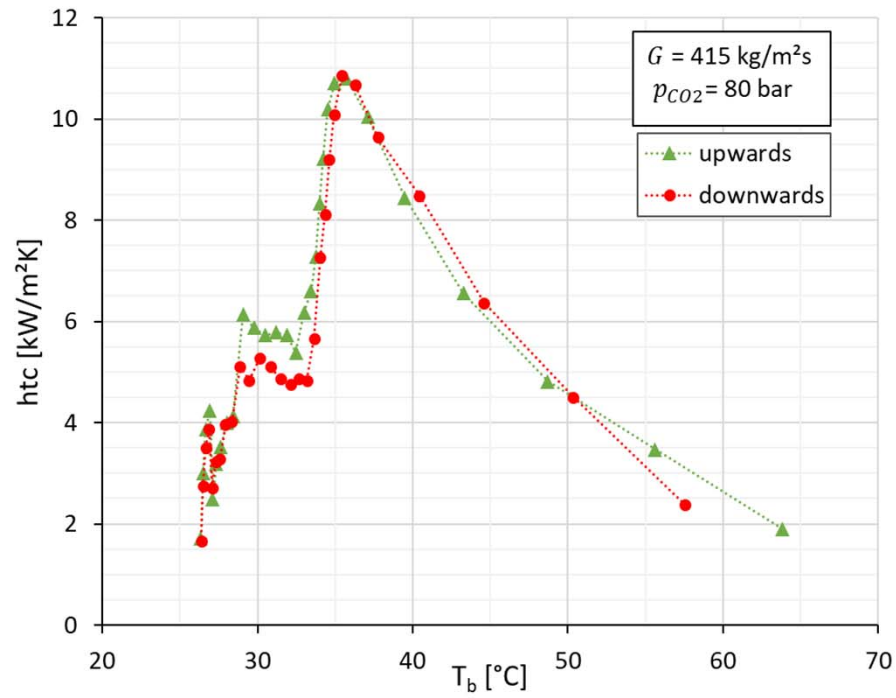
Effect of inlet pressure variation



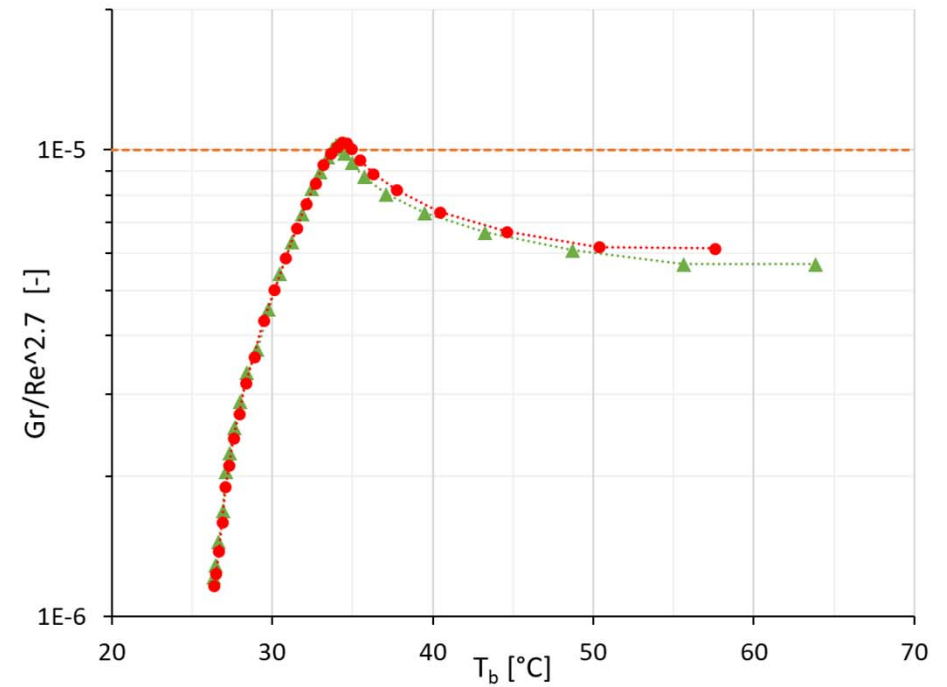
Effect of cooling media temperature variation



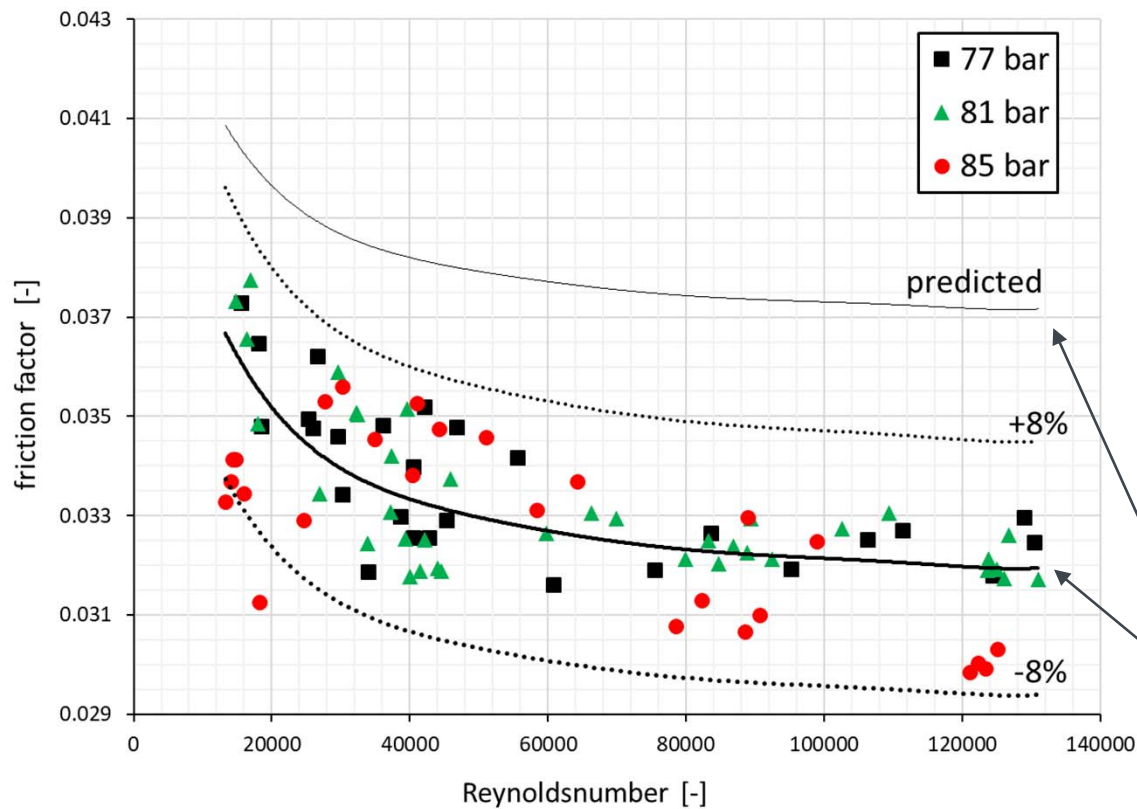
Effect of flow direction variation



$$\frac{Gr}{Re^{2.7}} > 10^{-5} \text{ * Jackson and Hall}$$



Isothermal pressure drop



- pressure drop equation:

$$\Delta p = \zeta \frac{l \rho u^2}{d} = \frac{8}{\pi^2} \zeta \frac{l \cdot \dot{m}^2}{d_i^5 \cdot \rho(T, p)}$$

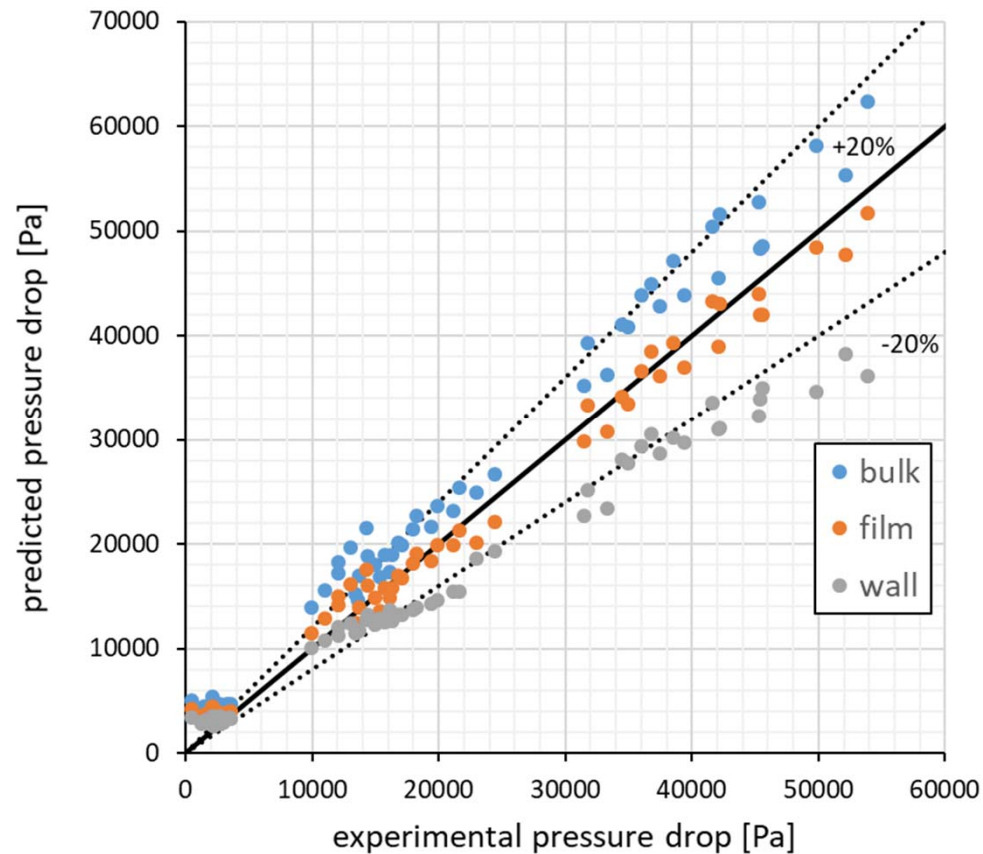
- friction factor for rough tubes:

$$\frac{1}{\sqrt{\zeta}} = -2 \lg \left[\frac{2,51}{Re_i \sqrt{\zeta}} + \frac{K}{3,71} \right]$$

3 measurements $\varnothing K = 18.2 \mu m$

$K = 10.8 \mu m$

Cooled pressure drop



prediction by:

- $\Delta p = \zeta \frac{l}{d} \frac{\rho u^2}{2} = \frac{8}{\pi^2} \zeta(Re_{b,f,w}, K) \frac{l \cdot \dot{m}^2}{d_i^5 \cdot \rho(T_{b,f,w,p})}$
- $K = 10.8 \mu m$
- $T_f = (T_b + T_w)/2$
- ✓ best prediction with film properties

Conclusion and next steps

□ 198 experiments performed at IKE, University of Stuttgart

- Effect of mass flux on htc enhances near the pseudo-critical-point
- Increasing inlet pressure leads to smaller peak
- Heat transfer is enhanced with smaller temperature difference between CO₂ and cooling media
- No difference between up- and downwards flow was found
- Friction factor of isothermal measurements shows trend like expected in rough tubes
- Pressure drop of cooled experiments can be predicted with the properties of the film

□ Next steps:

- 3 mm diameter tube to investigate influence of flow direction
- small-scale heat exchanger plate with multiple channel and comparison with results of single channel heat transfer

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Thank you!



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