

3rd European supercritical CO₂ Conference
September 19-20, 2019, Paris, France

CSP Development in China and sCO₂ Research at Zhejiang University

Gang Xiao¹, Kaixiang Xing¹, Jinyi Zhang², Yann Le Moullec²,
Pan Zhou², Tianfeng Yang¹, Mingjiang Ni¹ and Kefa Cen¹

¹State Key Laboratory of Clean Energy Utilization, Zhejiang University, Hangzhou, China

²EDF R&D China Beijing, China

Emails: xiaogangtianmen@zju.edu.cn

3120102460@zju.edu.cn

Paris, Sep. 20, 2019



Zhejiang University, Hangzhou, China






◆ Capital of Zhejiang Province
◆ 1100km from Beijing
◆ 180 km from Shanghai

Shanghai
上海

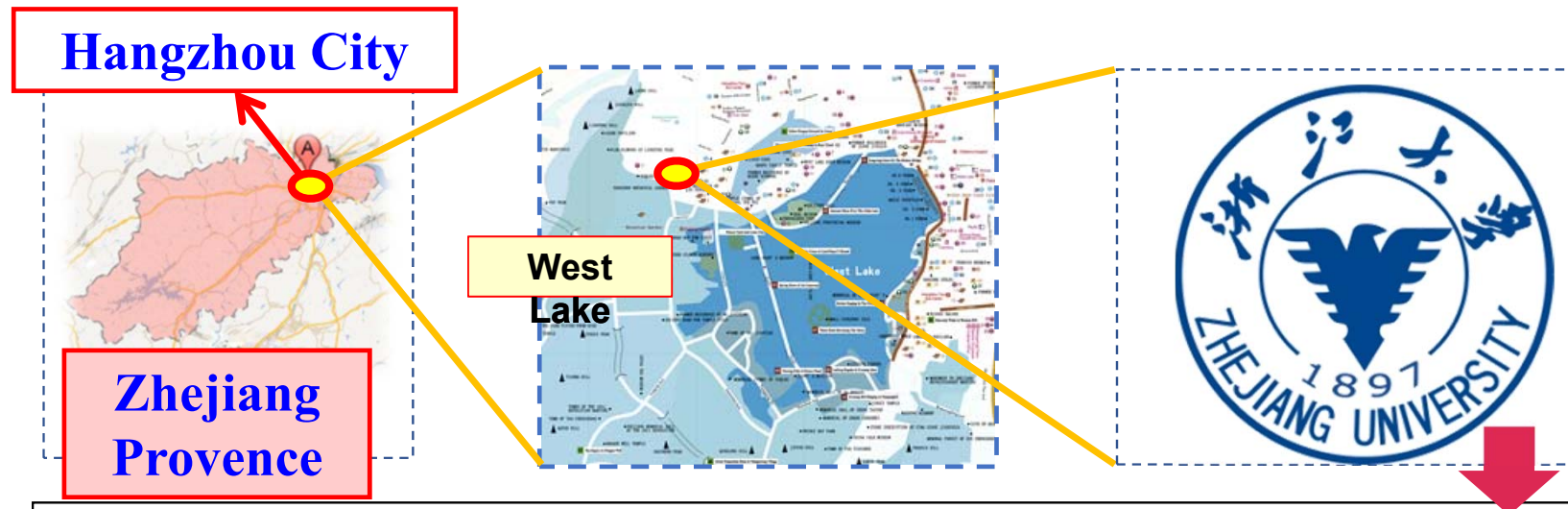
Hangzhou
杭州

Introduction of Hangzhou

- A historical and cultural city
- The most famous national tourist city in China

Spring	
Summer	
Autumn	 <div data-bbox="1039 927 1912 1182"><p>Longest and Earliest man-made canal of world (Grand Canal: Beijing-Hangzhou)</p></div>
Winter	 <div data-bbox="1039 1182 1912 1385"><p>World Cultural Heritage (West Lake, 2011)</p></div>

Zhejiang University, Hangzhou, China



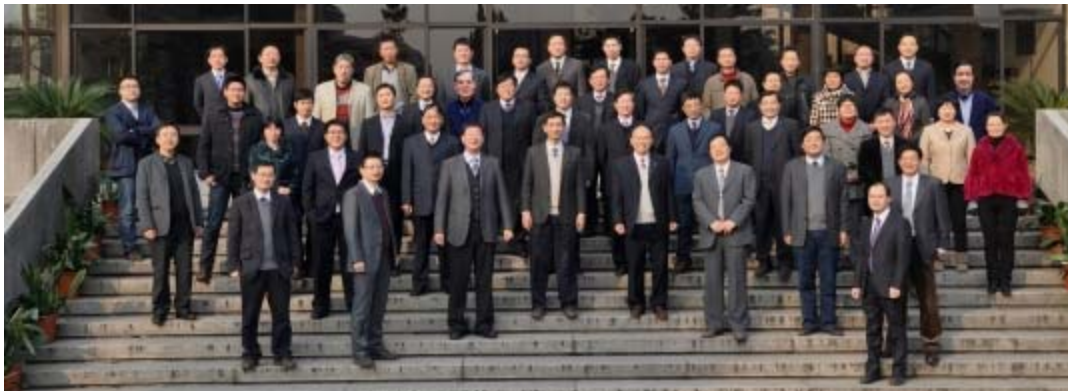
7 campuses: 5 in Hangzhou, 1 in Zhoushan and 1 in Haining; ~50,000 Students

- Top 5 in Engineering of World (US News 2017)
- One of the Best Universities in China (C9 Union)

State Key Lab of Clean Energy Utilization @ Zhejiang University

Faculties and Students

- 50 faculties
- ~50 staffs
- ~500 graduated students



International Cooperation Centers

- **ZJU-Princeton Univ.**
Joint Research Center on Hydrogen Energy
- **ZJU-Stanford Univ.**
Joint Research Center on Combustion Chemistry
- **ZJU-UIUC (University of Illinois at Urbana-Champaign)**
International Center for Bioenergy
- **ZJU-Leeds Univ.**
International Center for Sustainable Energy Science and Tech.
- **ZJU-KTH**
Joint Research Center on Clean Energy Utilization
- **ZJU-Lund Univ.**
International Center for Laser Diagnostics in Energy Science
- **ZJU-Purdue**
International Center for Clean Energy Research Initiative
- **ZJU-Australia**
BHP Billiton Joint lab
-

Research fields

Energy

Research Fields of Our Lab

Renewable Energy and Advanced Energy System

Simulations of Multiphase Reaction System

Clean Utilization of Low Grade Energy

High-efficiency Utilization of Fossil Fuel

Pollution Control

Combustion

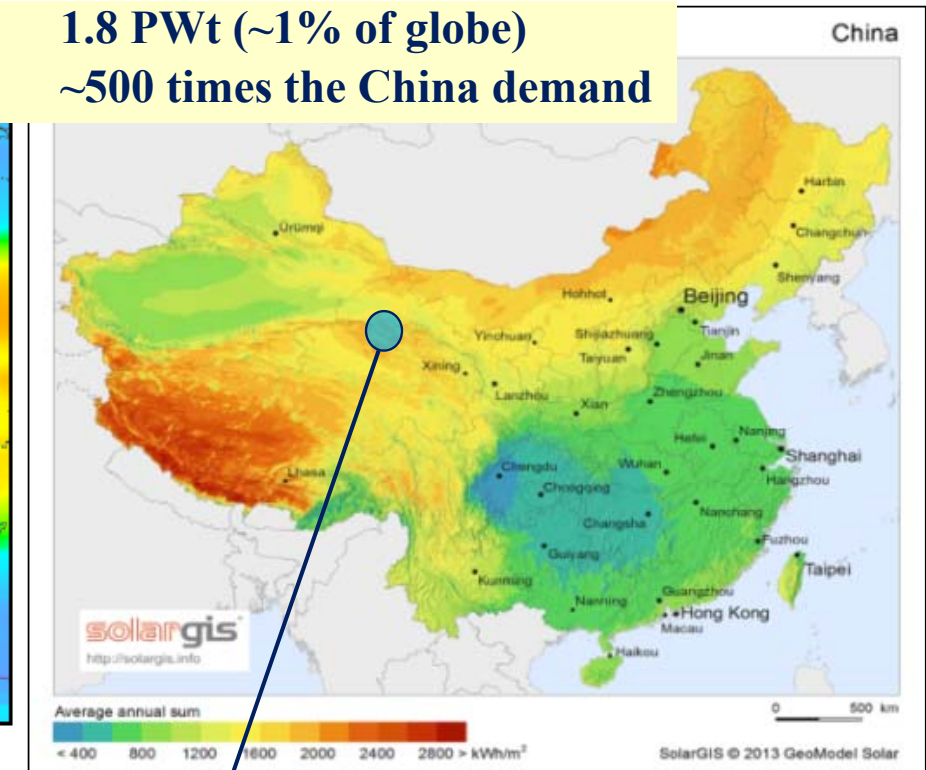
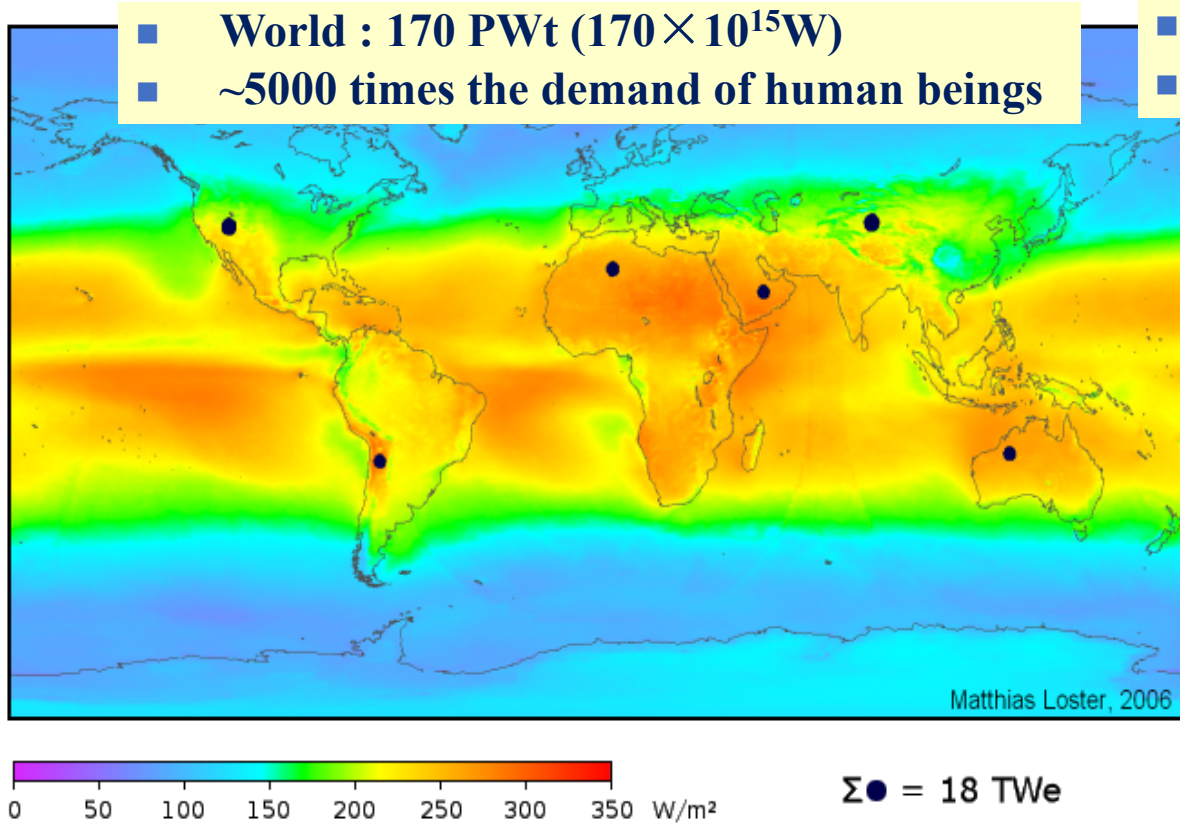
Environment

Our research : CSP

- **High-temperature receiver and storage**
 - ✓ Air/particle receiver
 - ✓ sensible/chemical storage
- **Advanced cycles**
 - ✓ Air Brayton
 - ✓ S-CO₂ Brayton
 - ✓ Stirling cycle
 - ✓ PETE



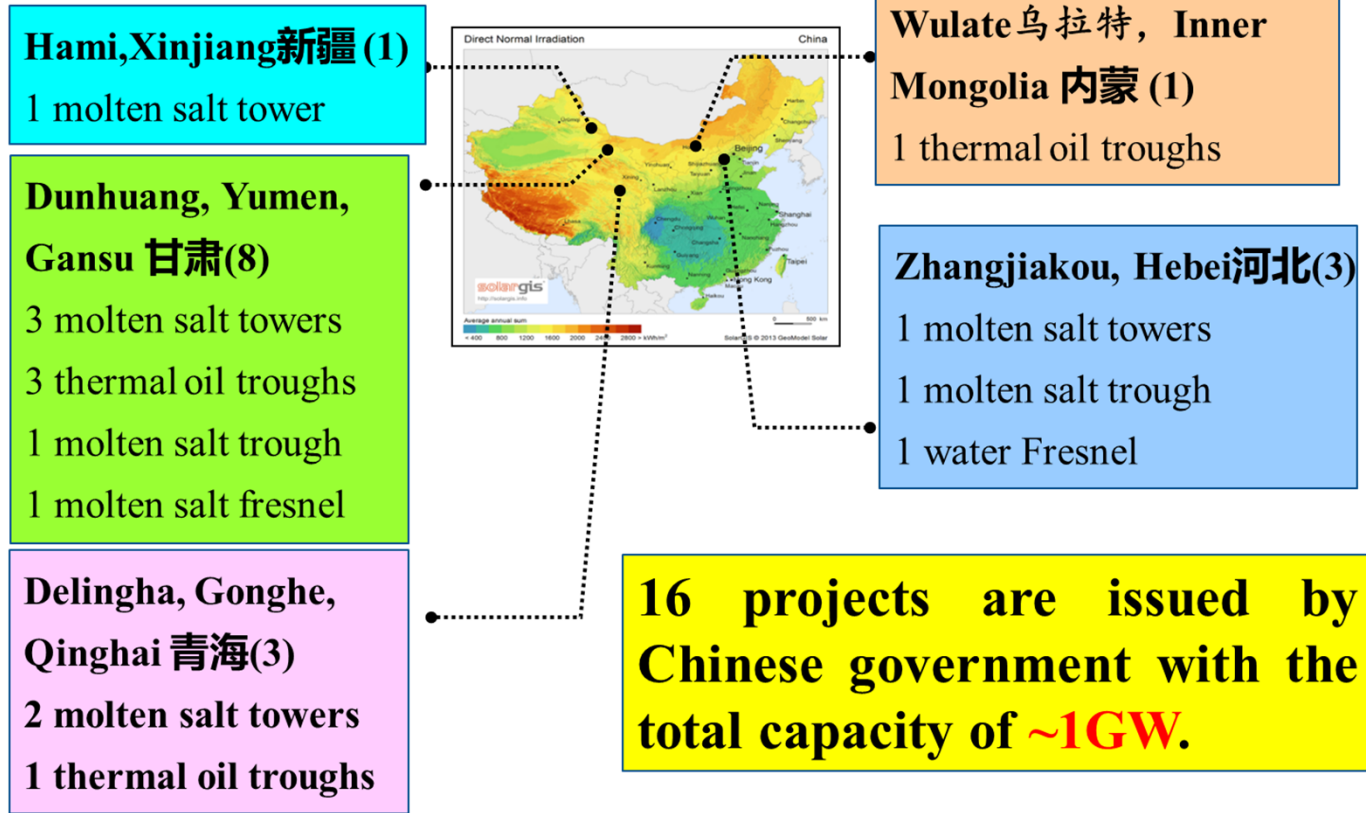
Solar resources: potential renewable energy



○ The six points = the global electricity demand (@ η 8%)

➤ 200,000 km² can afford the electricity demand of China in 2020

CSP Development in China



中广核CGN 50MW Parabolic Trough



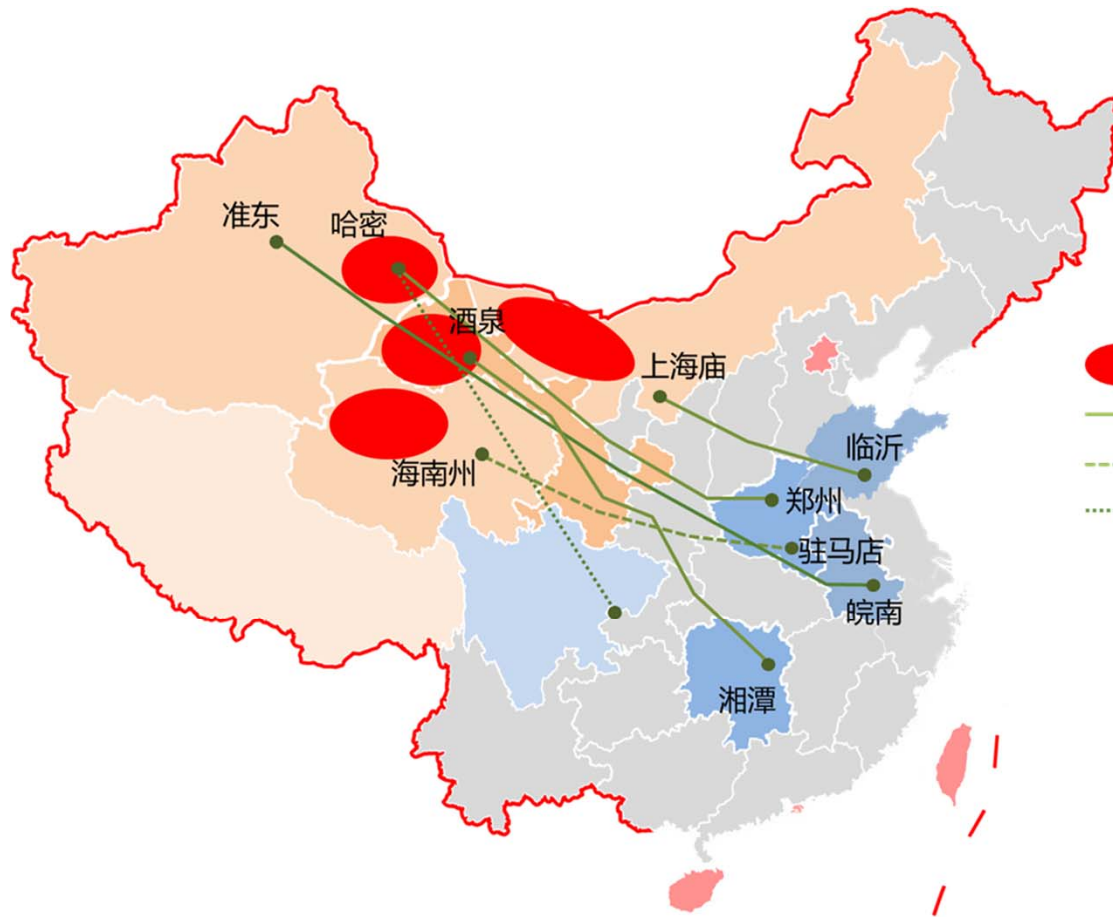
首航Shouhang 100MW tower



中控Supcon 50MW tower

3 has been built, 5 will be completed in 2019, 8 will be finished in 2020

Electricity transmission from West to East of China



**Feasibility reports of
~40GW CSP projects
have been made**

-  Large-scale CSP parks -planning
-  Ultra HVDC Transmission-operating
-  Ultra HVDC Transmission- under construction
-  Ultra HVDC Transmission-planning

UHVDC > 800kV



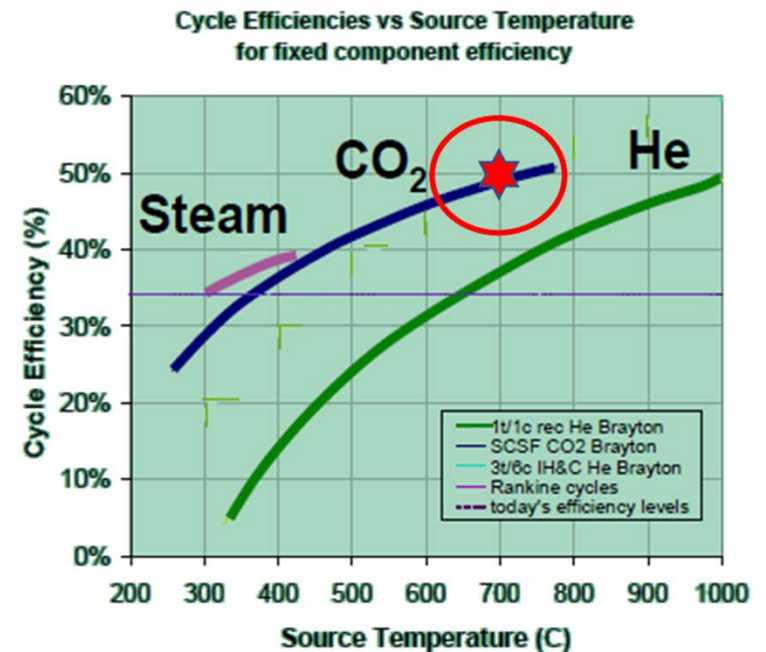
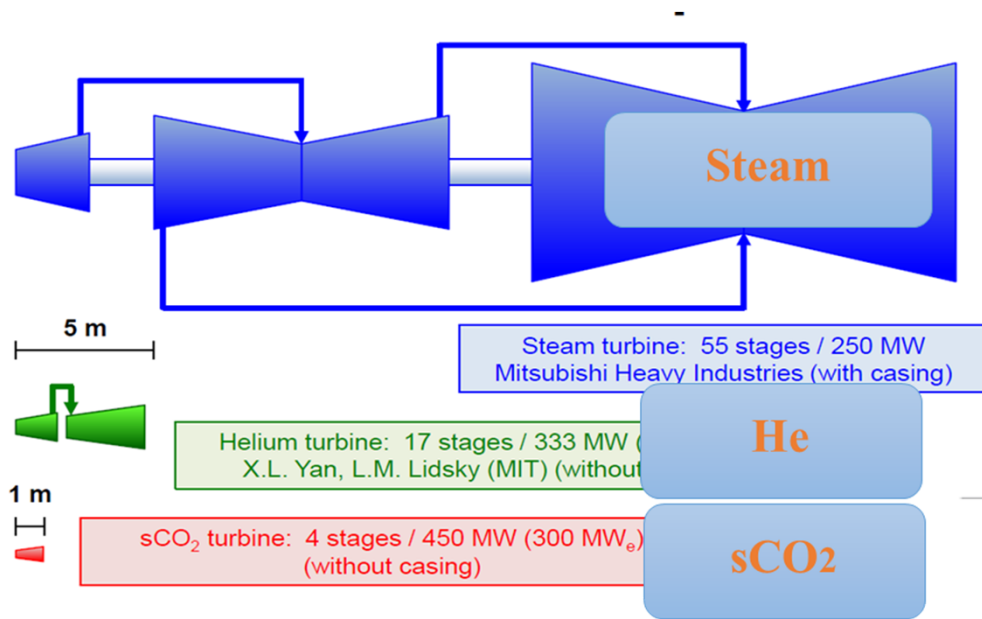
- Water is challenging**
- Advanced technology is expected**

Challenges & next generation technologies

Items	Trough&Fresnel	Tower	Dish
Concentration ratio	60~130	400~600	500-1000	400-2000
Heat transfer	Oil/steam/MS	molten salt/DSG	H2/He	gas/solid
Working medium	water/steam	water/steam	H2/He	gas/solid
Cycle	Rankine	Rankine	Stirling	Brayton/combined
Temperature	<400°C	<580°C	700-800°C	700-1400°C
η_e	<15%	<20%	<32%	25-40%
Water kg/(kWh)	~0.3	~0.2	~0.01	~0.01

High temp. → high eff. & less water (flexible & suitable for adjusting the grid peaks)

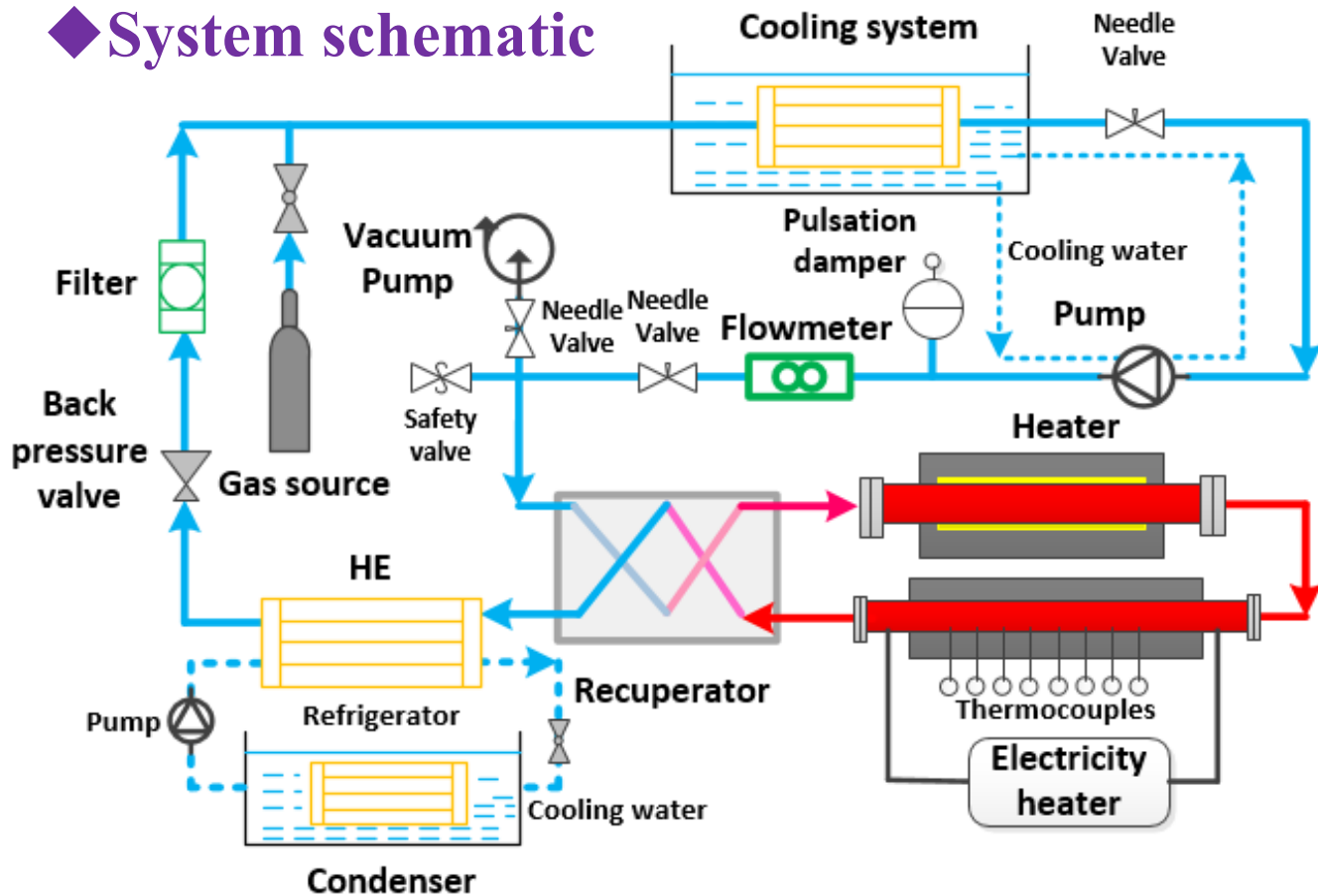
sCO₂ Brayton is potential for next generation of CSP (compact, high efficiency)



- High efficiency (Cycle efficiency >50% when TIT is higher than 700°C).
- Compact (smaller than steam cycle).
- Low water consumption.

sCO₂ test loop at ZJU campus

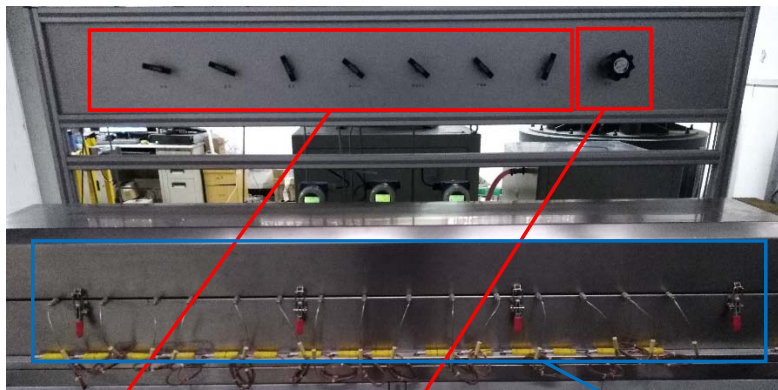
◆ System schematic



Parameter	Value
Mass flow rate	10~60 kg/h
Working temperature	30~500 °C
Working pressure	7~15 MPa

- The purpose of this work: investigate the dynamic performance of sCO₂ test loop.
- Three input variables for the system: the mass flow rate, the working temperature and the working pressure.
- Used the experiment results to develop simulation model.

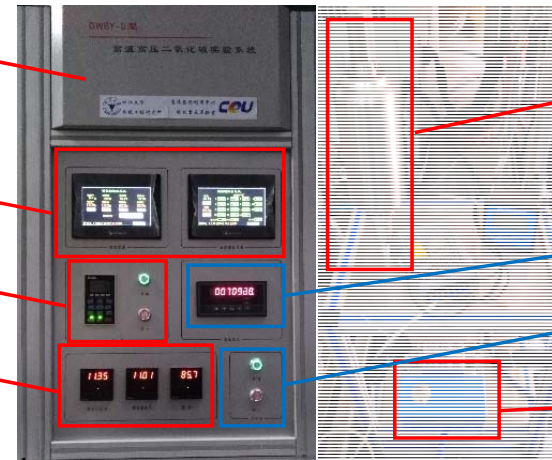
sCO₂ test loop--System pictures



Control Valve Back pressure Valve Test section
Cooler Condenser Pump and Gas bottle

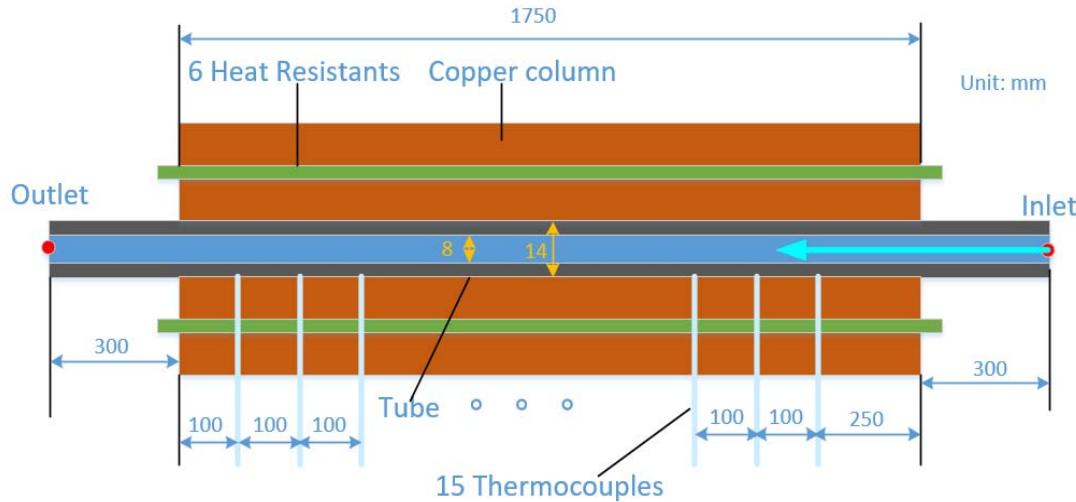


Four-stage heater Pressure transducer Heat exchanger Filter
Recuperator



Control block Temperature control Pump control Pressure Buffer tank Accumulated Q Start/stop button Mass flow meter

Experimental conditions



➤ Calculation method:

$$Nu = \frac{hd_i}{\lambda_{CO_2}}$$

$$h = \frac{q}{LMTD}$$

$$LMTD = \frac{(t_{b,in} - t_{b,out})}{\ln \left(\frac{t_{b,in} - t_{w,i}}{t_{b,out} - t_{w,i}} \right)}$$

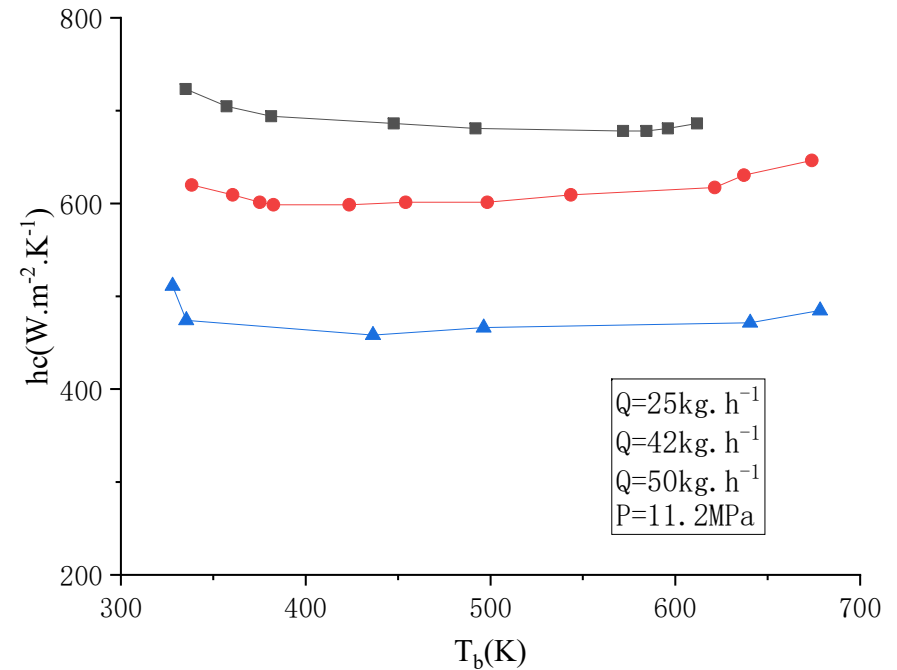
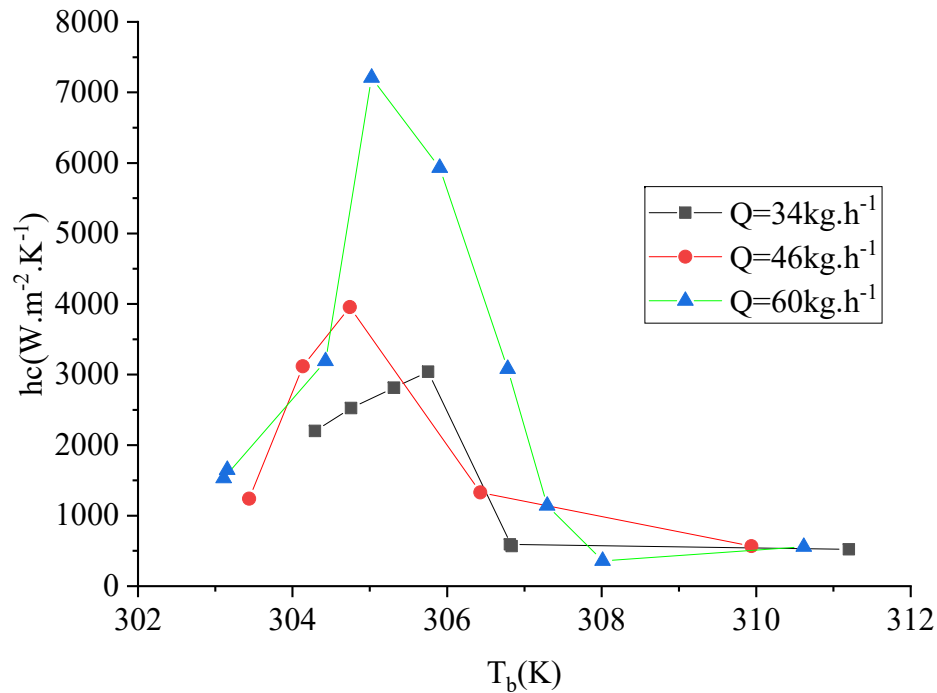
$$t_{w,o} = \frac{\left(\frac{\sum_{j=1}^{10} t_{w,i}}{10} + \frac{\sum_{j=3}^{13} t_{w,i}}{13} \right)}{2}$$

$$t_{w,i} = t_{w,o} + \frac{Q}{2\pi\lambda_c l} \ln \frac{d_o}{d_i}$$

$$t_b = \frac{t_{b,in} + t_{b,out}}{2}$$

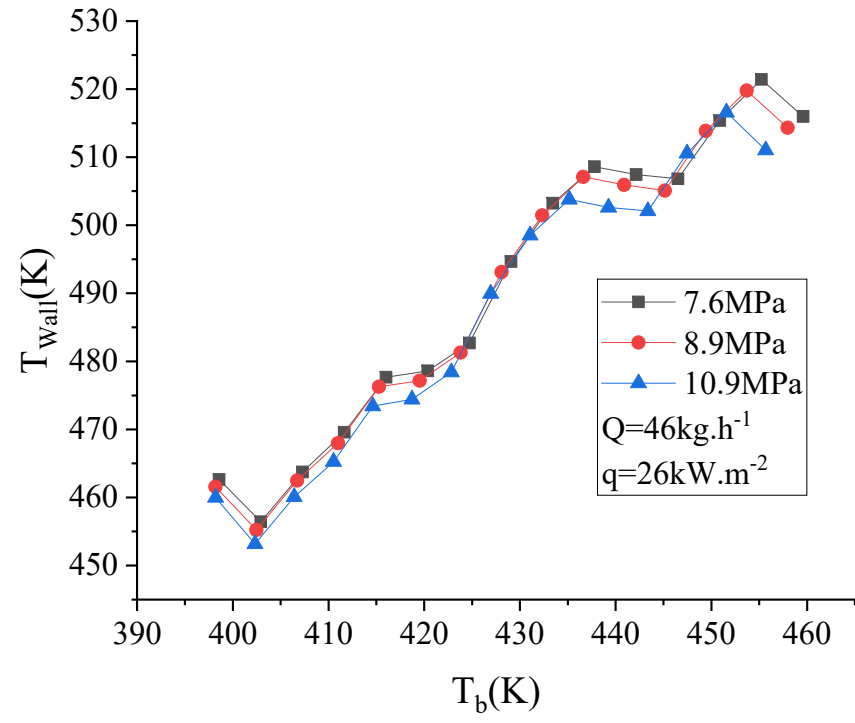
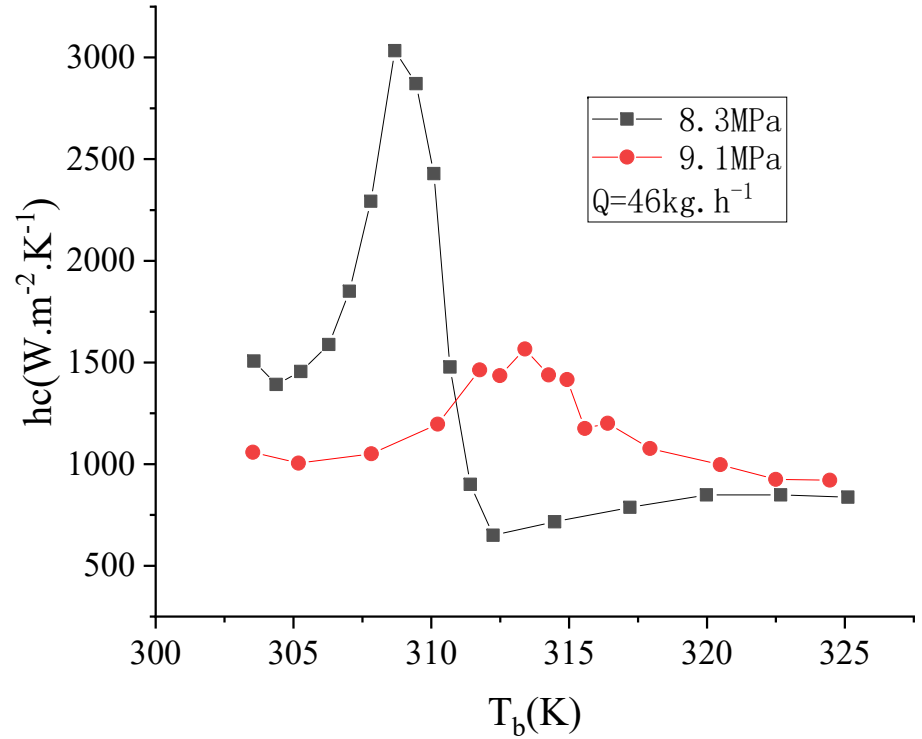
Items	CO ₂
Flow direction	Horizontal
Pressure	15MPa
Mass flow rate	20-60 kg/h
temperature	30~500 °C
Heat flux q	0~60kW/m ²
Reynolds number	2×10 ⁴ ~1.1×10 ⁵

Effect of mass flux



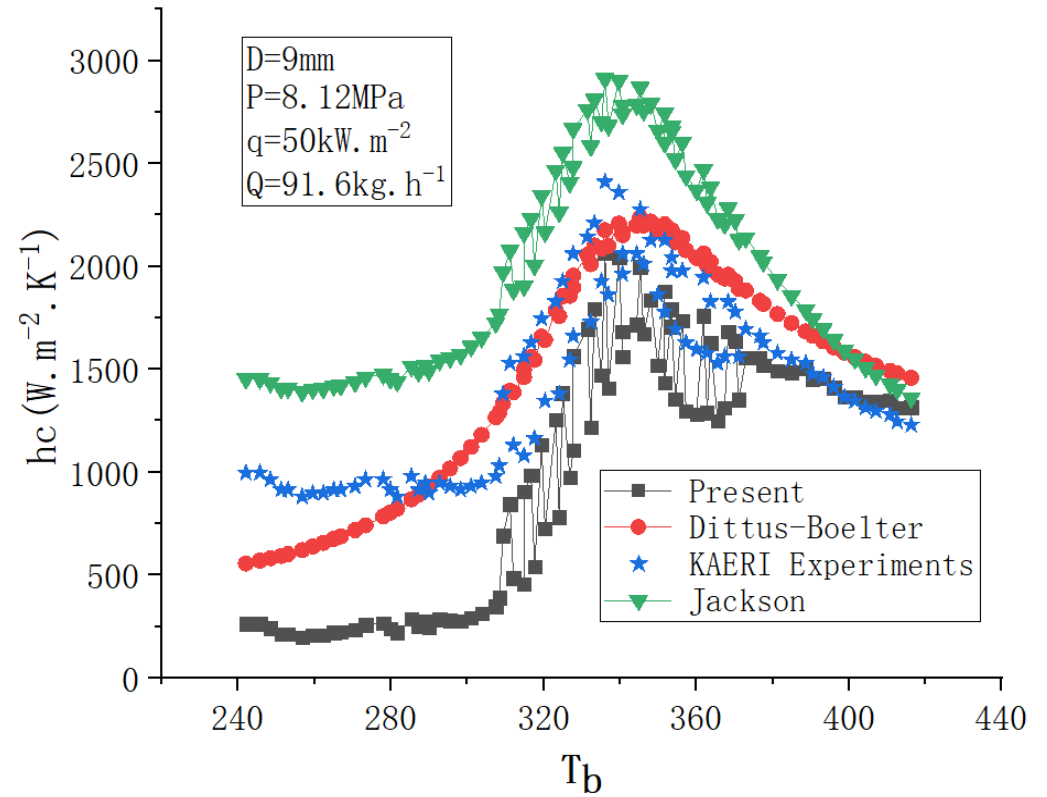
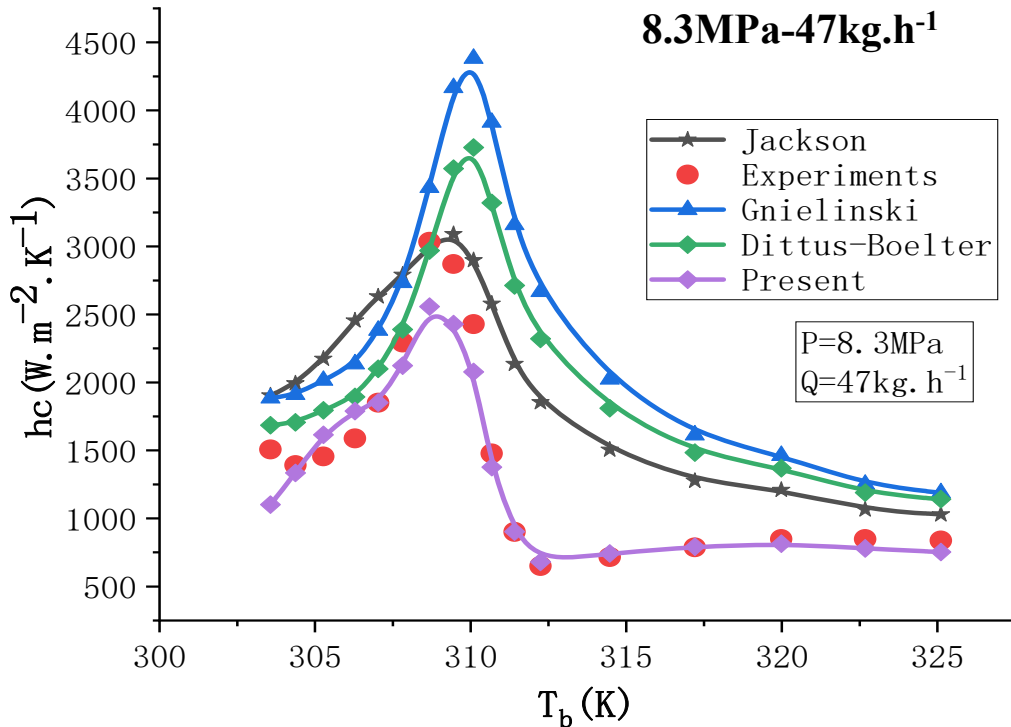
- As Q increases, the HTC increases too.
- Near the pseudo-critical temperature, heat transfer coefficient (HTC) reaches the peak point;
- For temperature $>100^\circ\text{C}$, HTC is quite stable.

Effect of Pressure



- The higher pressure resulted in the lower HTC peak;
- when $T > 100 \text{ }^\circ\text{C}$, the effect of pressure is not significant.

Correlations comparison

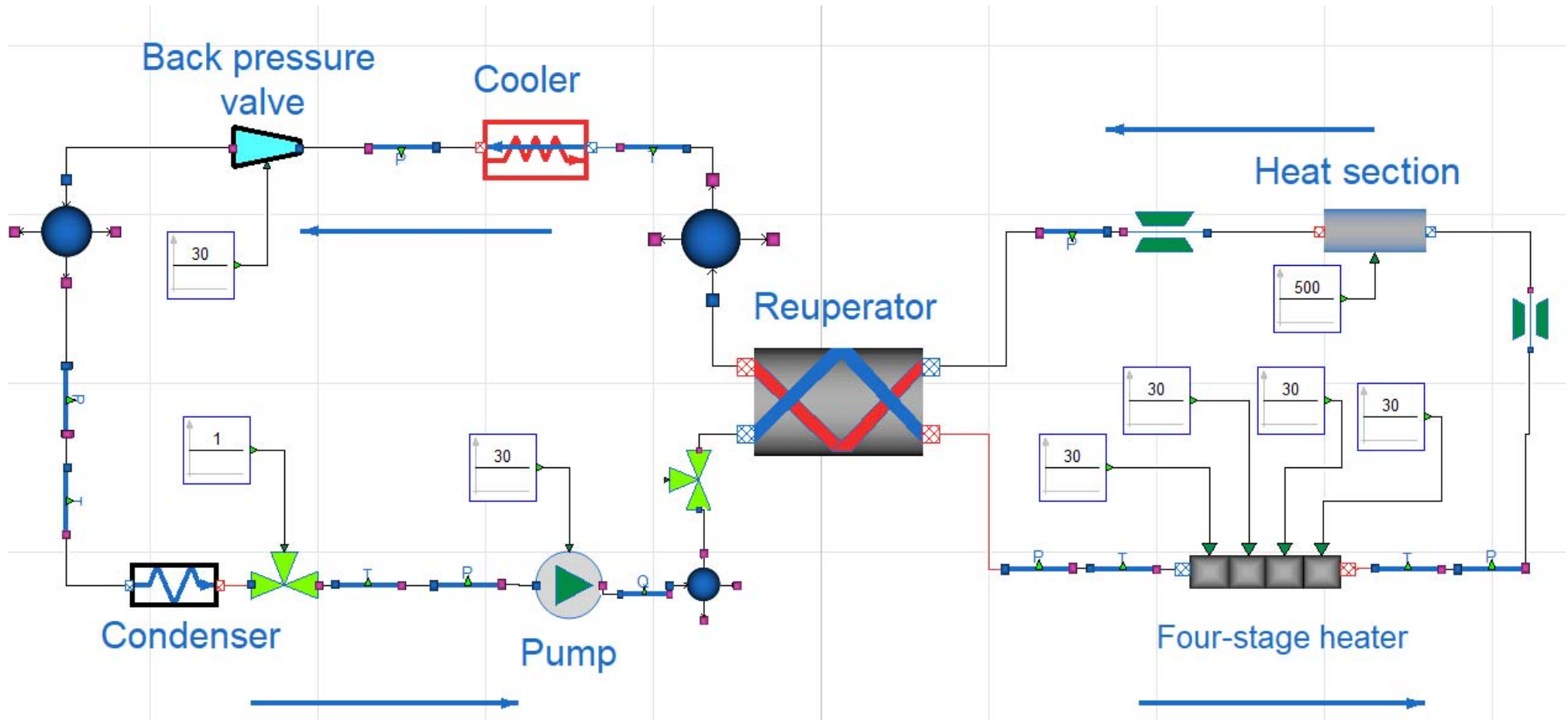


Concluded correlation:

$$Nu = 32.39 Re_b^{1.0084} Pr_b^{1.9876} \left(\frac{\rho_w}{\rho_b}\right)^{2.2123} \left(\frac{c_{p,w}}{c_{p,b}}\right)^{0.7389} q^{+0.9935} c_t^{6.1590}$$

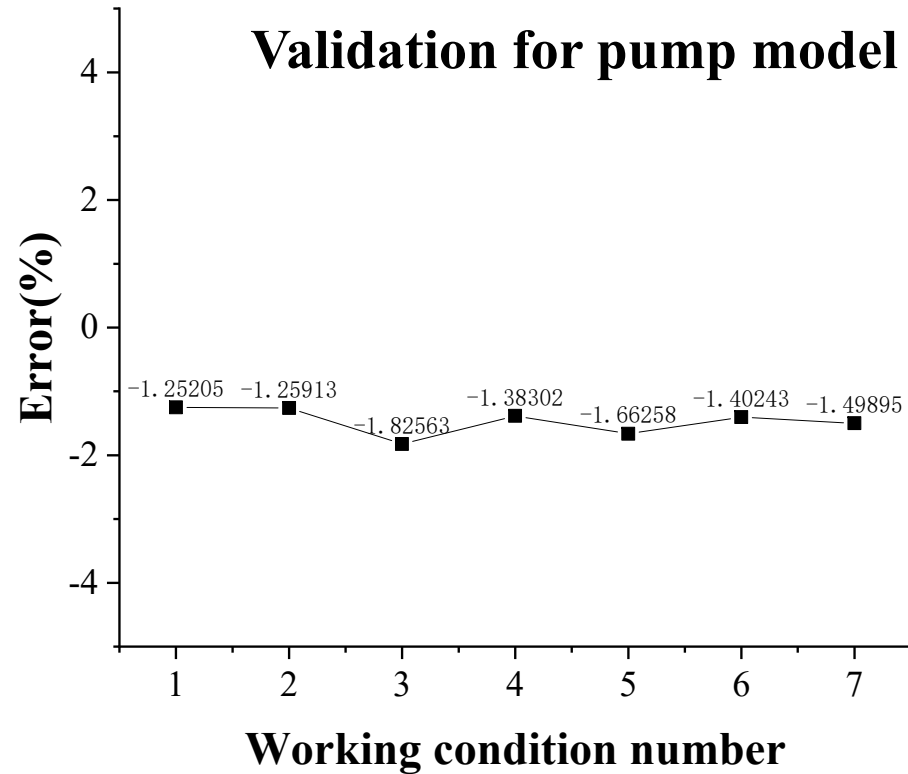
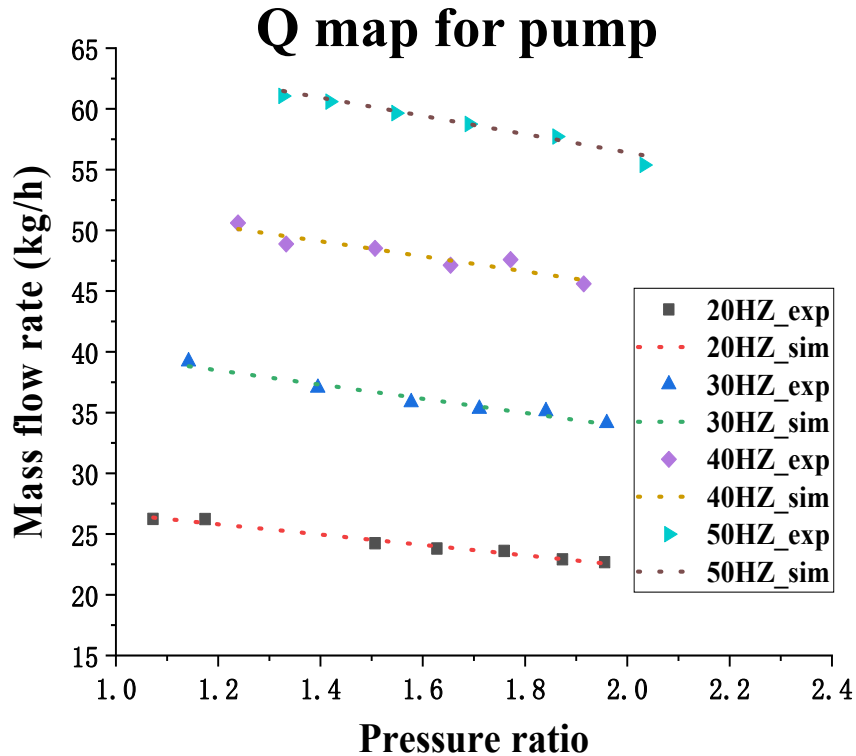
Data from: Bae Y-Y, Kim H-Y. Convective heat transfer to CO₂ at a supercritical pressure flowing vertically upward in tubes and an annular channel. Experimental Thermal and Fluid Science. 2009;33:329-39.

Simulation tool



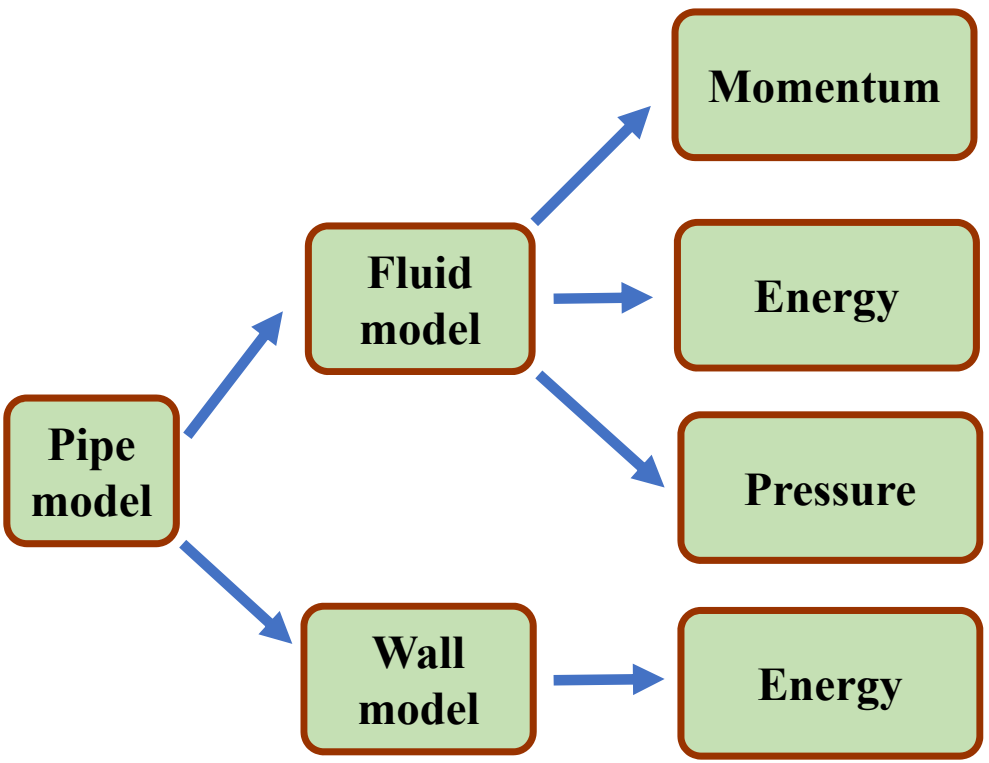
Dymola-sCO₂ test loop model

Pump model and steady state validation



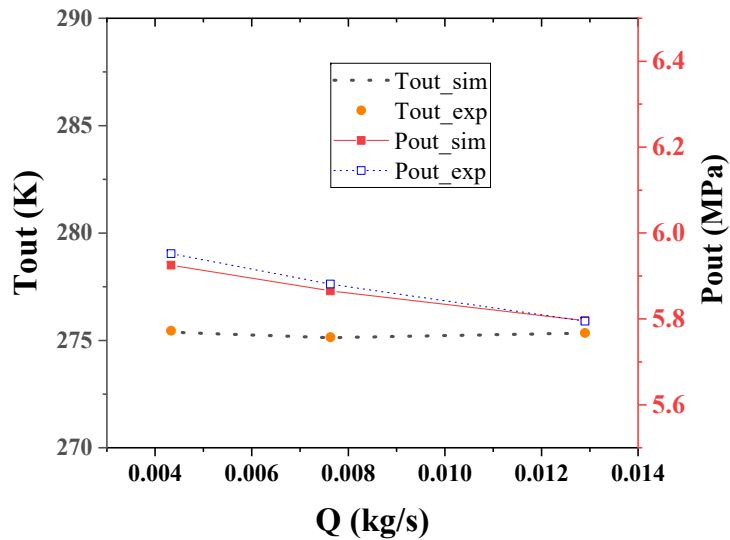
- The maximum error of the mass flow rate is $\pm 1.67\%$.
- The maximum error for the outlet temperature is $\pm 0.4\%$.

Pipe model

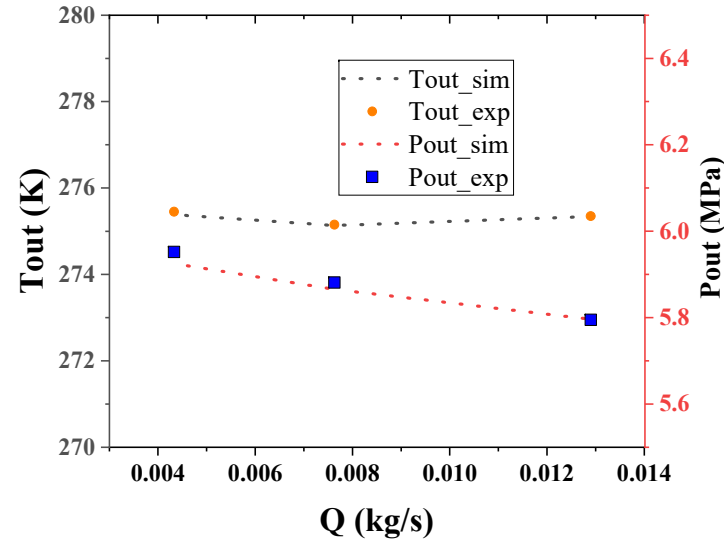


Heat exchanger	Pipe diameter Inner/Outer (mm)	Pipe length	Wall condition
recuperator	6/10	12	Normal heat loss to ambient ($T_0=15\text{ °C}$)
heater	6/10	12×4	Heating power (500W*4) PID control; Normal heat loss to ambient ($T_0=15\text{ °C}$)
Cooler	4/6	6	Heat loss to cooling water ($T_0=0\sim 10\text{ °C}$)
Condenser	4/6	12	Heat loss to cooling water ($T_0=-5\sim 4\text{ °C}$)
Heat section	8/14	2	Heating power (0~7.2 kW); Normal heat loss to ambient ($T_0=15\text{ °C}$)

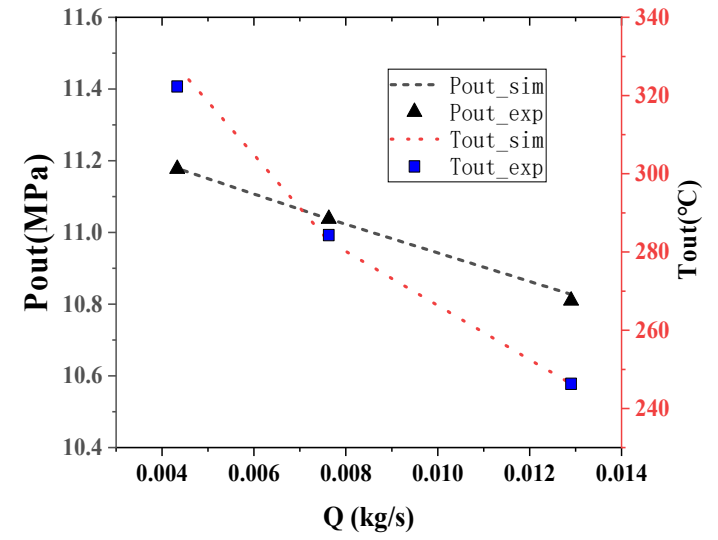
Steady state validation for components



P_{out}/T_{out} -cooler



P_{out}/T_{out} -condenser



P_{out}/T_{out} -test section

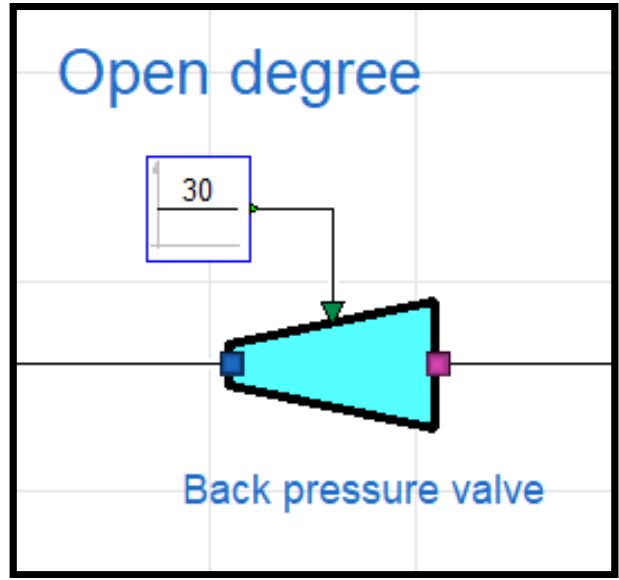
Components	Cooler		Condenser		Test section	
	Pout	Tout	Pout	Tout	Pout	Tout
Maximum Error (± %)	0.1	0.3	0.1	0.5	1.6	0.2

Valve models

Back pressure valve

Pressure drop:

$$\Delta P_f = \frac{Q^2}{2\rho} K \quad K = signal \cdot 10^{12}$$

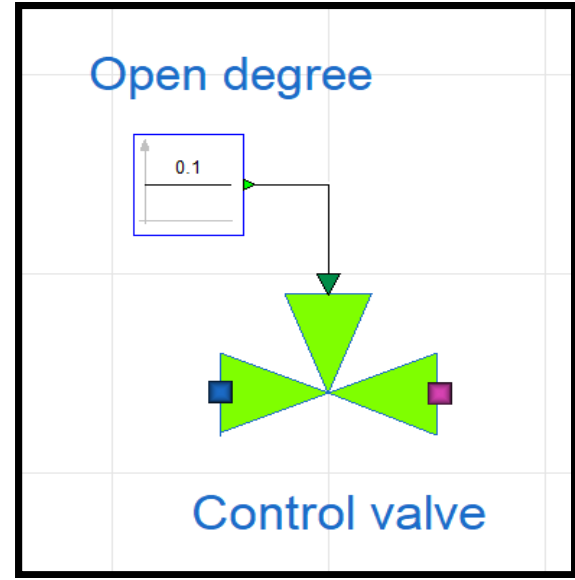


Control valve

Pressure drop:

$$\Delta P C_v^2 = K \frac{Q^2}{\rho^2} \quad C_v = C_{v_{max}} signal$$

$$K = 1.733 \times 10^{12} \quad C_{v_{max}} = 8005.42$$



Conclusion

- The HTC reaches the peak value near the pseudo-critical temperature, but is stable when $T > 100$ °C.
- A new correlation is concluded for the working conditions in this test loop. It is used in the test loop simulation model to give a better prediction of HTC.
- The steady state validation for the main components have been done. The error between simulation and experiment results are ranged from ± 0.1 % to ± 1.67 %.

Future work

□ More comprehensive steady state validation.

- All components should be validated with more experiment results.

□ More Experimental and simulation work on dynamic conditions.

- Start-up and shut-down operations for the sCO₂ test loop.
- Smart control strategies

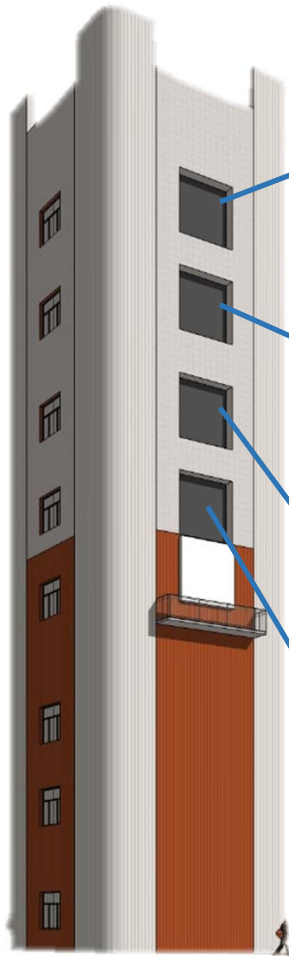
□ To Build a 150 kW sCO₂ Brayton test loop combined with a MWth solar tower built in Zhejiang University.

1MW_{th} solar tower test platform



- Solar thermal power: 1 MW_{th}
- Tower height: 40 m
- Heliostats area: 2000 m² (100*20m²)
- High temperature receiver > 900 °C
- Thermal storage > 800 °C
- Brayton cycle (air, sCO₂)
- Stirling cycle
- PETE (photon enhanced thermionic emission)

MWth solar tower test platform



Gas turbine system, Air receiver and Thermochemical storage.
Height: 34.85m

- Air Brayton cycle:
 - 1) Power output: 100 kW
 - 2) Efficiency: 30%

Particle receiver and storage, S-CO₂ system.
Height: 30.35m

- S-CO₂ system:
 - 1) Power output: 150 kW
 - 2) Efficiency: ~30%

Molten salt system and Receiver.
Height: 25.35m

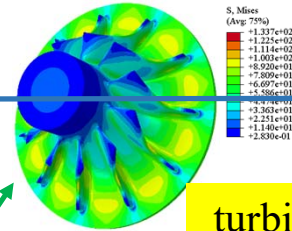
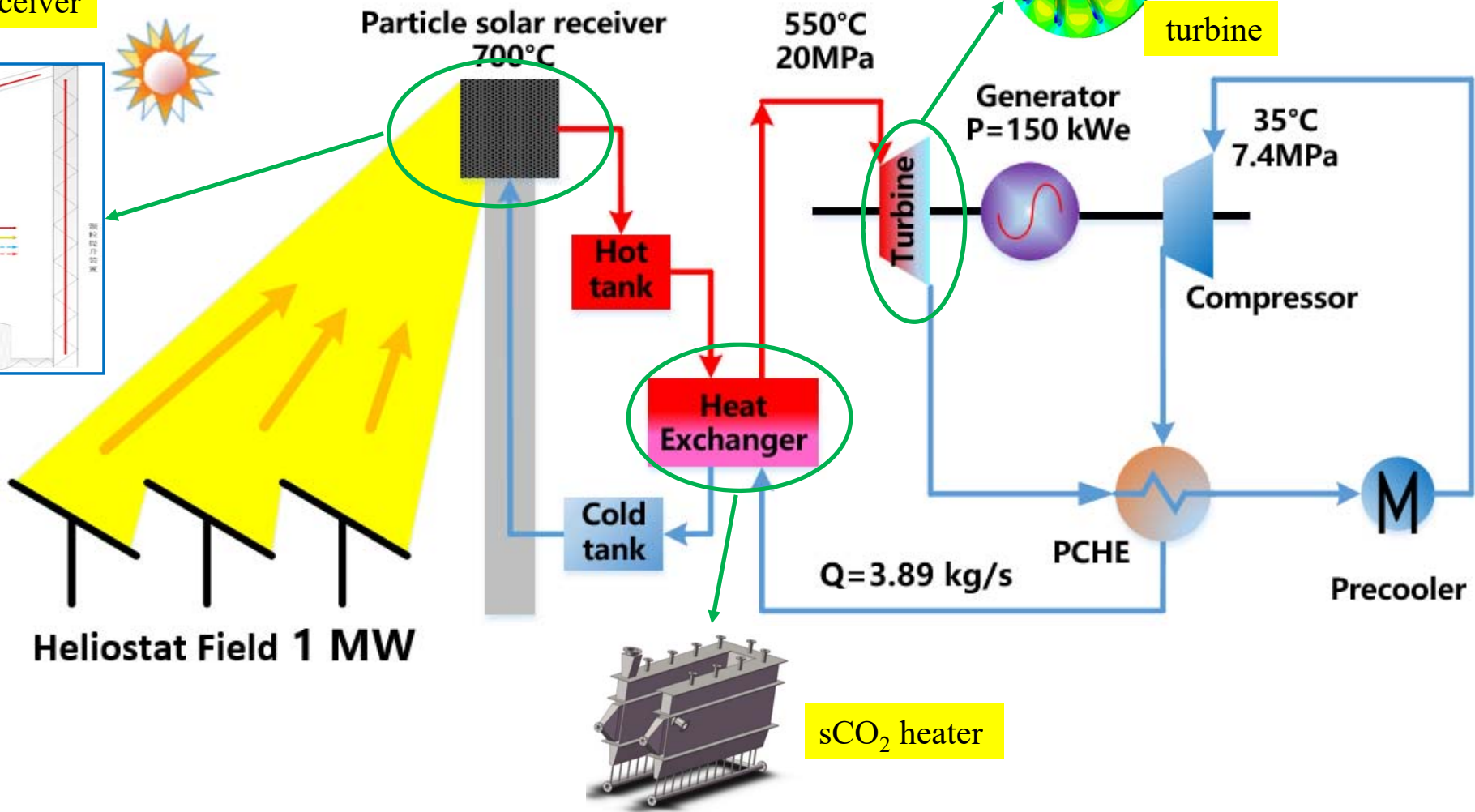
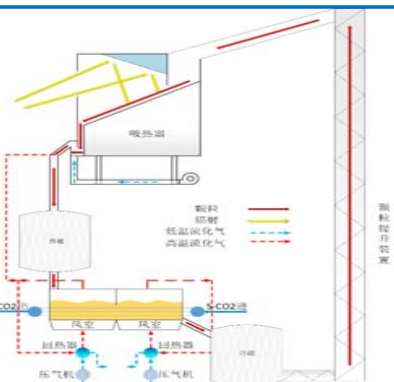
- Molten salt system:
 - 1) T_{in} : 290 °C
 - 2) T_{out} : 560 °C

PETE and Stirling engine.
Height: 20.85m

- Stirling engine:
 - 1) 1~30kW
 - 2) Efficiency: 20-30%

150 kW S-CO₂ Brayton cycle system

Solid particle receiver



Thank you!

Thanks to EDF (China)

