



# Shouhang – EDF 10MWe Supercritical CO<sub>2</sub> Cycle for CSP Demonstration Project

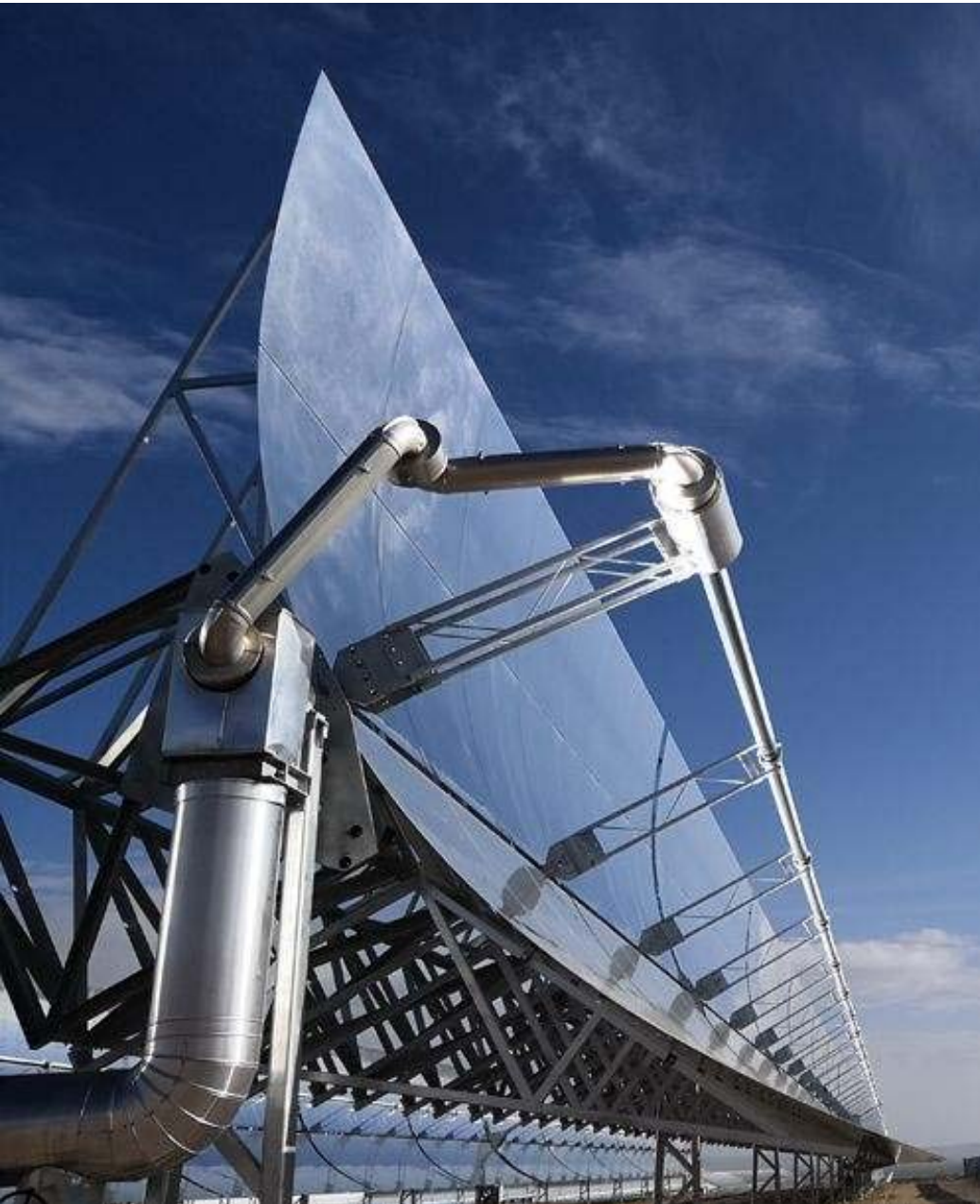
3<sup>rd</sup> European sCO<sub>2</sub> Conference

EDF R&D China

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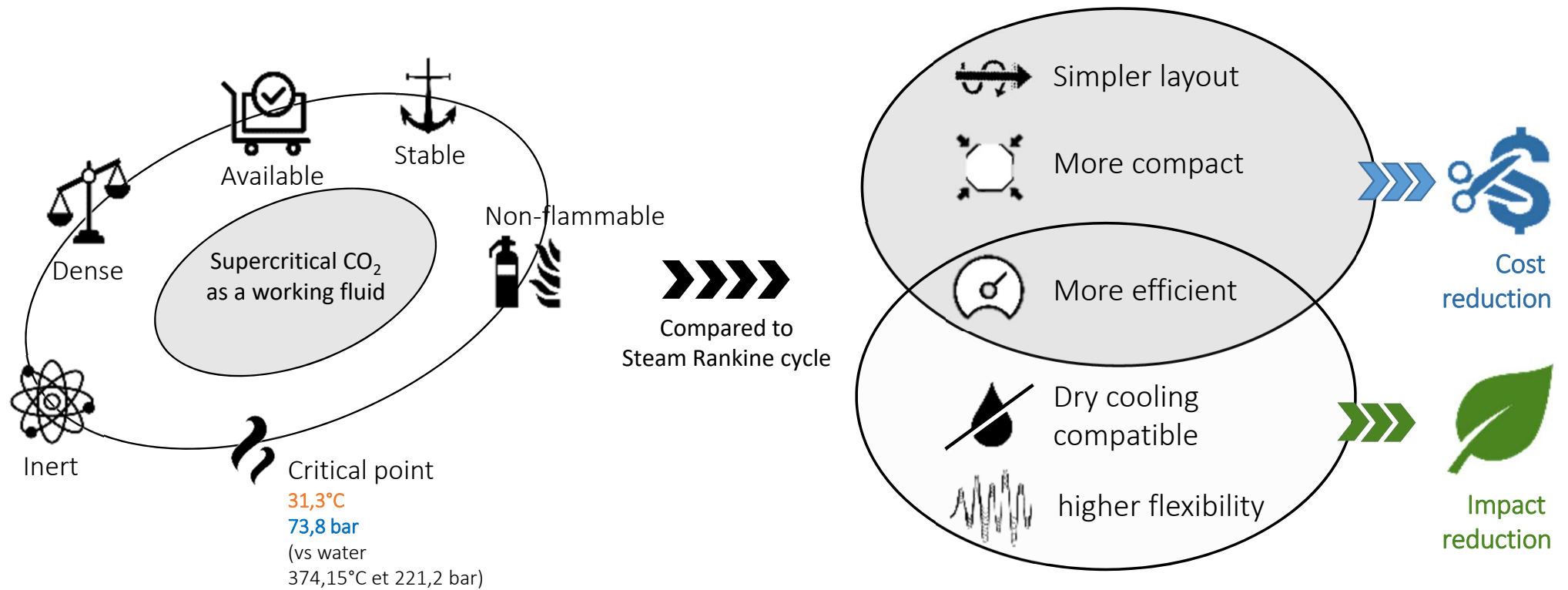


## OUTLINE

1. Introduction
2. System design of the sCO<sub>2</sub> cycle
3. Superheating and cooling system
4. Brief planning of the project
5. Conclusion

## Introduction

# Why using Supercritical CO<sub>2</sub> cycle for power generation?





## Introduction

# Shouhang – EDF 10MWe sCO<sub>2</sub> demonstration project (1)

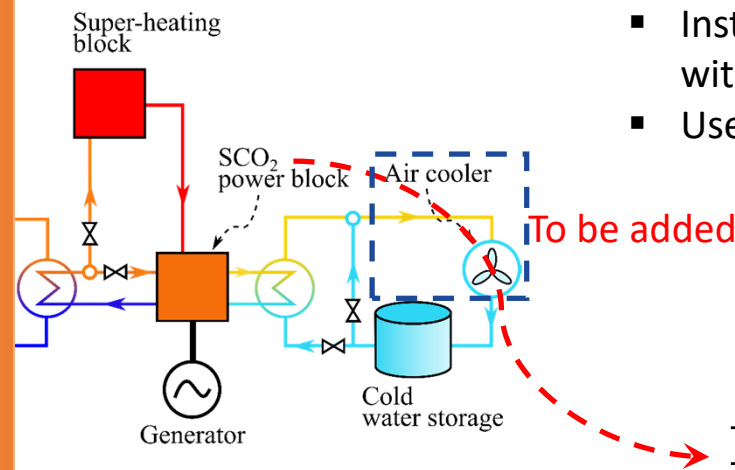
- Collaboration signed in 2018
- Retrofit Shouhang's 10MWe CSP plant with sCO<sub>2</sub> cycle
- To investigate:
  - Optimal sCO<sub>2</sub> cycle design for CSP
  - Industrial scale sCO<sub>2</sub> equipment
  - Cycle control and operation
  - Material test
- Operate and evaluate the performance of the demo cycle
- Current 10MWe CSP with steam Rankine cycle
  - Situated in Dunhuang
  - 15h thermal storage with molten salt



## Introduction

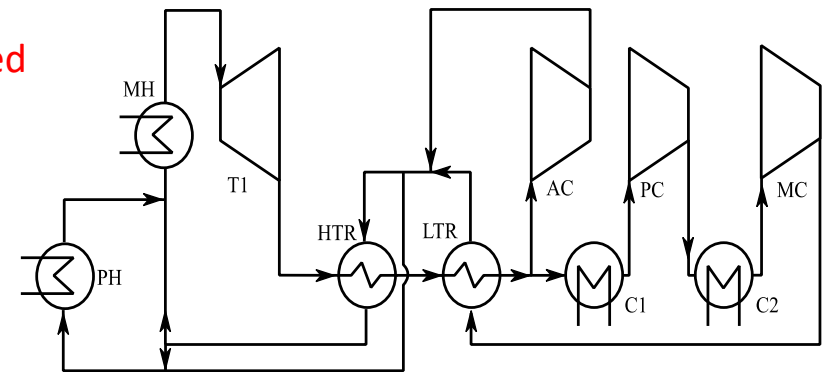
# Shouhang – EDF 10MWe sCO<sub>2</sub> demonstration project (2)

To be kept



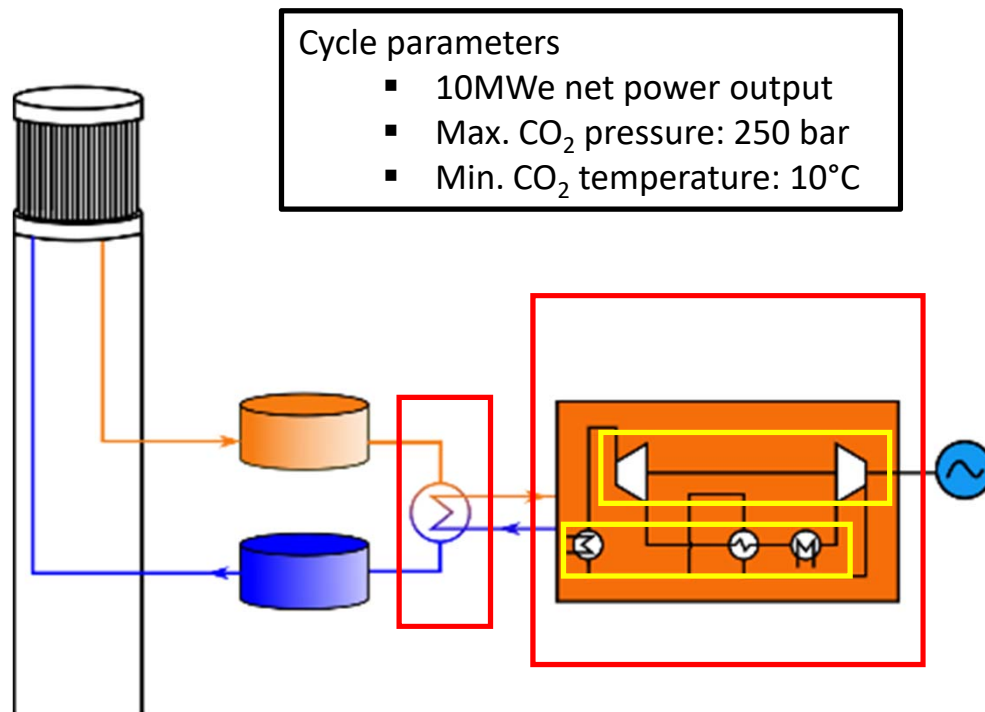
### System design concept

- Keep the current solar field and thermal storage system
- Install a 10MWe sCO<sub>2</sub> power block in parallel with the current steam Rankine cycle
- Use indirect dry cooling



## System design of the sCO<sub>2</sub> cycle

# Boundary conditions of cycle design



### Cycle parameters

- 10MWe net power output
- Max. CO<sub>2</sub> pressure: 250 bar
- Min. CO<sub>2</sub> temperature: 10°C

### Turbomachinery related parameters

- Isentropic efficiency : 80% for compressor and 85% for turbine

### Heat exchanger related parameters

- Min. pinch: 10°C
- Pressure drop: 1 bar

### Molten salt related parameters

- 290°C < Molten salt exhaust temperature < 320°C
- Max. temperature: 530°C
- Mass flow rate: 80 kg/s

## System design of the sCO<sub>2</sub> cycle

# sCO<sub>2</sub> cycle design (1)

### Optimization-driven design with 2 approaches:

1. « Classic design » by simulation based on expertise  
learn and understood the design drivers
2. Global optimization tool coupled with a cycle superstructure  
sure to not miss a good solution and explore out of the box ideas

Cycle	Max .T	Min. P	CO <sub>2</sub> flow	Split ratio	Power	Eff.	MS Outlet T <sup>+</sup>	HX UA (100% = 4857 kW/°C)*	Complexity (Nbr. Turbomachinery)
	°C	bar	Kg/s	%	MWe	%	°C	%	
<b>RG-IC</b>	520	68.5	96.2	-	10.06	34.6	290	100.00	3 <b>Pinch problem</b>
<b>RC-IC</b>	438	82.6	145.9	31.67	9.95	34.2	290	107.47	4 <b>Low output power</b>
<b>RC-IC</b>	470	82.0	126.5	33.04	9.33	36.6	320	98.68	4
<b>RC-PH</b>	439	87.1	162.94	34.17	10.01	34.4	290	133.05	3 <b>30% more heat exchangers</b>
<b>RC-DPH</b>	464	86.9	141.8	24.92	10.18	34.9	290	100.29	3
<b>RC-IC-PH</b>	468	82.1	137.7	27.74	10.35	35.6	290	113.87	4
<b>PartC-PH</b>	485	72.3	122.0	41.32	10.40	35.8	290	101.00	4 <b>Transcritical operation</b>

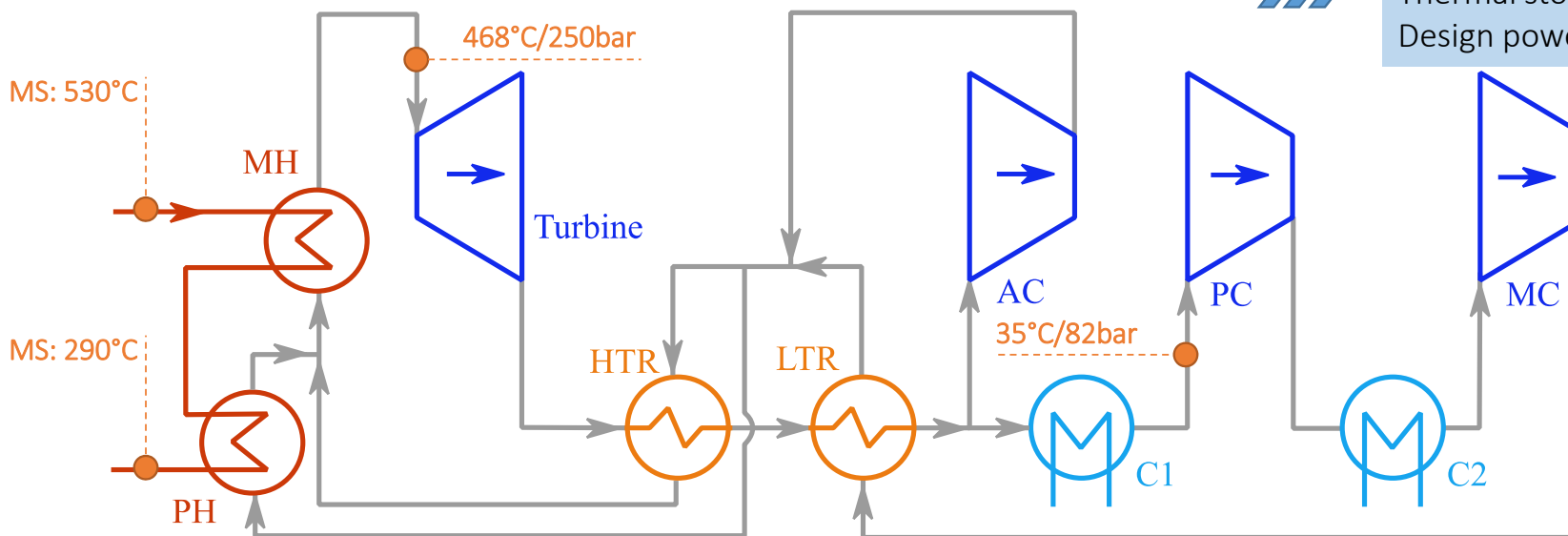
6 Cycles  
selected

## System design of the sCO<sub>2</sub> cycle

# sCO<sub>2</sub> cycle design (2)

### Key cycle features:

- Recompression to increase the recuperation effectiveness
- Intercooling to reduce compressor consumption and to increase thermal storage utilization
- Pre-heating to better utilize the low-temperature molten salt



➤➤➤  
Cycle net efficiency: 35.6%  
Thermal storage utilization: 100%  
Design power output: 10.3MWe



## Superheating and cooling system

# Superheating subsystem

Advantage of sCO<sub>2</sub> cycle is evident at high temperature



Necessity of superheating subsystem

1. Direct heating of sCO<sub>2</sub>

2. Heating of high temperature heat transfer fluid



Storage tank

- Storage system not able to withstand 600°C
- High investment



Gas engine

- No available gas engine with an exhaust gas T above 650°C
- Reduce lifetime cost of the demonstration



Gas combustion

- Expensive
- Low efficiency of boiler

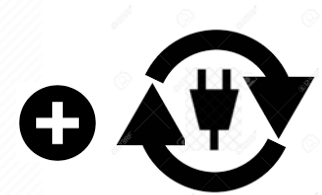
- Expensive
- Low efficiency of boiler



PV solar farm

- More investment
- Policy complexity

- Able to demonstrate the HTF/CO<sub>2</sub> HX and HTF heater

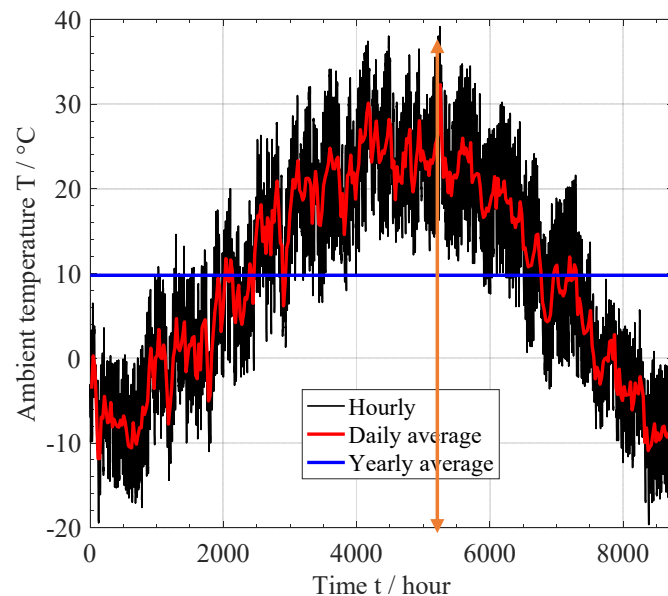


Auto-consumption

- Expensive electric heater

## Superheating and cooling system

# Cooling system with cold storage (1)



Annual temperature difference: 58.7°C

Annual average: 9.78°C

High daily temperature difference



Ideal case to test cold storage

A **simplified dynamic model** to test the performance of cold storage:

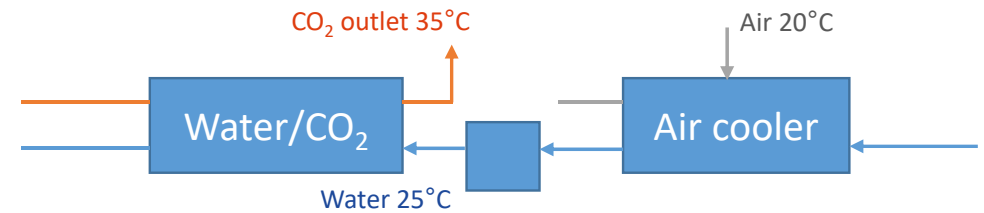
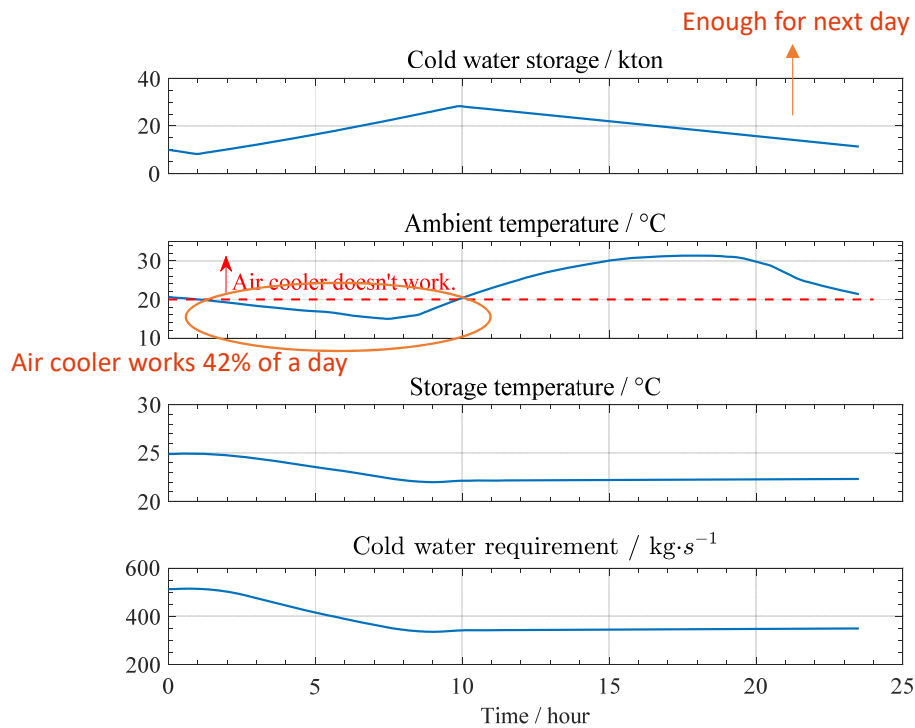
- Air cooler with ideal controller to control the outlet water T
- Water/CO<sub>2</sub> heat exchanger
- Cold storage water tank perfectly stirred

Working logical:

Air cooler operates when ambient temperature below designed  $T_{amb}$   
Cold storage discharged when the cooling water is needed at required flow rate

## Superheating and cooling system

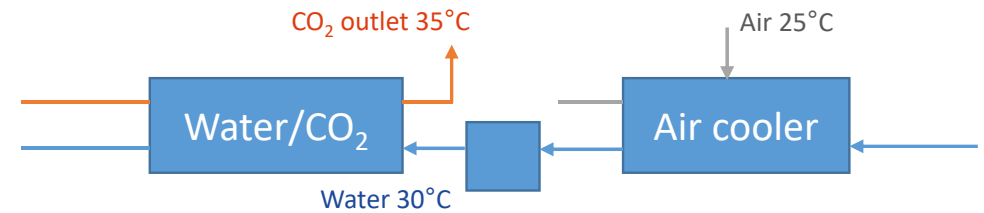
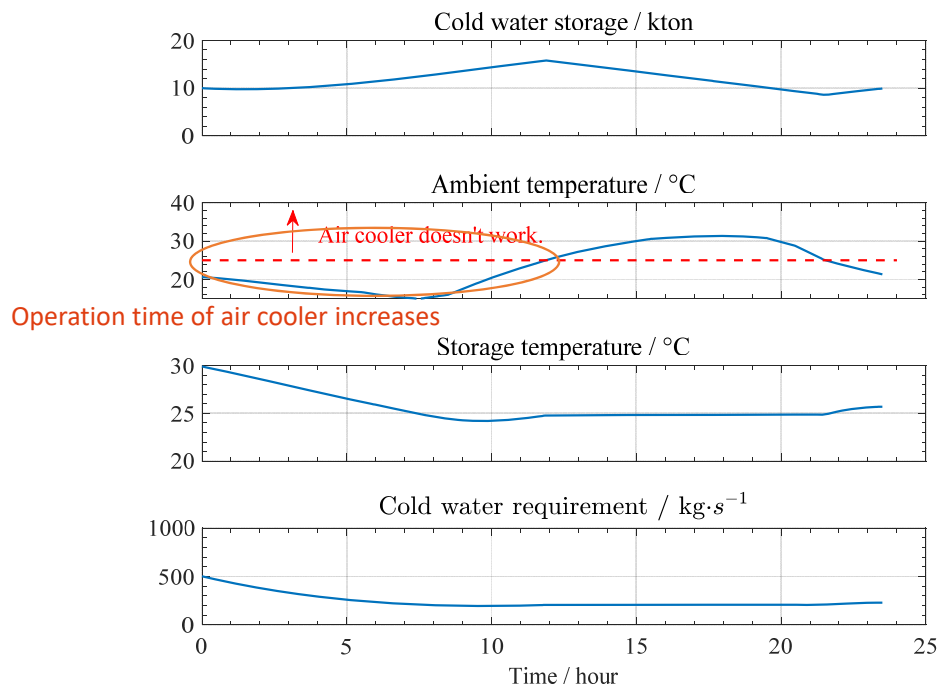
# Cooling system with cold storage (2)



- 24-hour full load continuous cycle operation at the hottest month
- Suppose:
  - 10°C pinch for water/CO<sub>2</sub> heat exchanger
  - 5°C pinch for air cooler
- Air cooler works when ambient temperature below 20°C

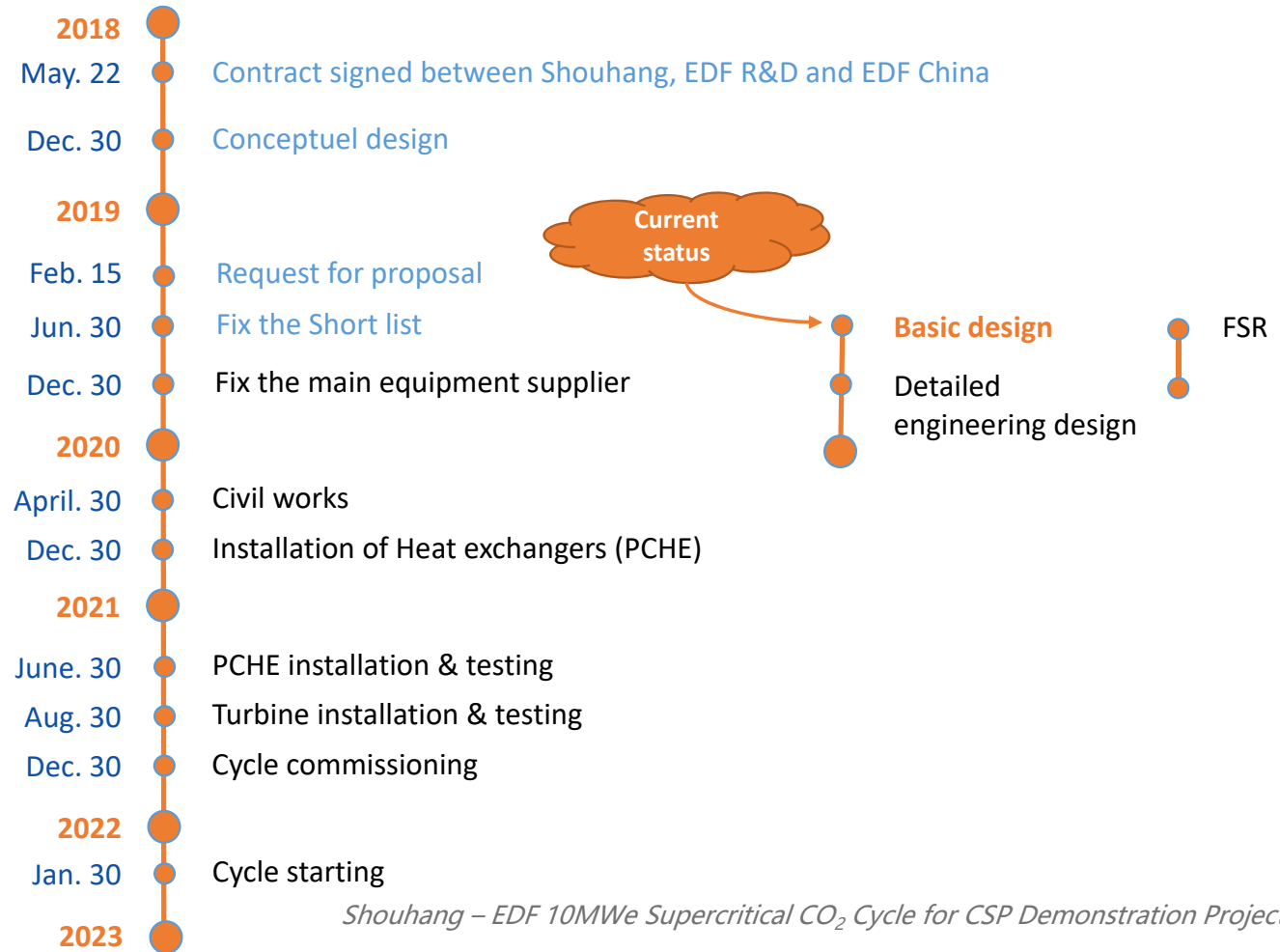
## Superheating and cooling system

# Cooling system with cold storage (3)



- 24-hour full load continuous cycle operation at the hottest month
- Suppose:
  - 5°C pinch for water/CO<sub>2</sub> heat exchanger
  - 5°C pinch for air cooler
- Air cooler works when ambient temperature below 25°C

# Shouhang-EDF 10MWe $\text{SCO}_2$ demo project: Brief planning





# Conclusions

## An industrial scale sCO<sub>2</sub> project integrated with a commercial CSP plant:

- sCO<sub>2</sub> RC-IC-PH is selected as a compromise of demonstration interest for future salt utilization, cost, complexity and efficiency
- Able to demonstrate equipment design, system design and operation that could be scaled up to large industrial application of sCO<sub>2</sub> cycle
- Superheating solutions under investigation
- Suitable location to test cold storage

## Next steps:

- Basic design & final budget evaluation
- Supplier selection



Questions?

