



Dynamic Modeling and Transient Analysis of a Molten Salt Heated Recompression Supercritical CO₂ Brayton cycle

European sCO₂ Conference

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Introduction

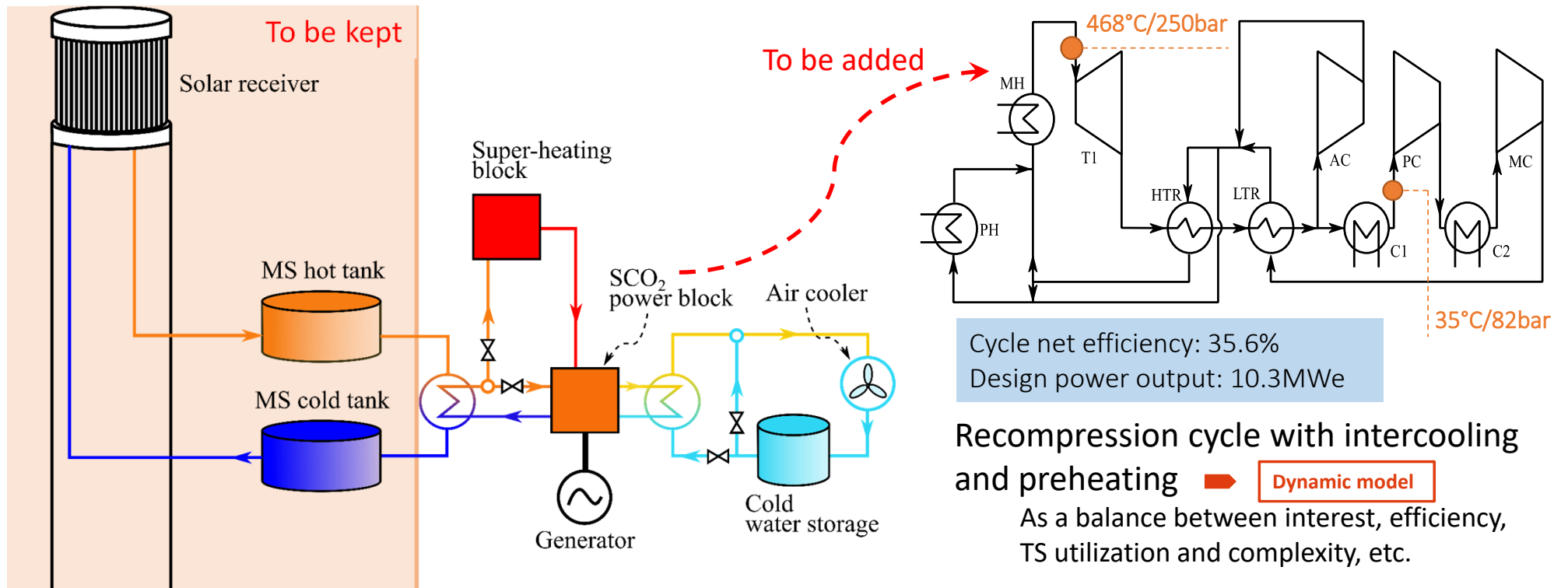
Supercritical CO₂ Cycle + CSP



- **In China, 160 \$/MWh, Year 2019 – Too expensive**
- SCO₂, together with high temperature (> 500 °C) molten salt CSP solutions, could achieve higher efficiency than steam solutions.
- **Shouhang – EDF 10MWe sCO₂ demonstration project**
 - 1) Investigate the technical feasibility of SCO₂ cycle
 - 2) Industrial scale SCO₂ equipment, including turbine, compressor, recuperator, etc.
 - 3) Cycle control and operation

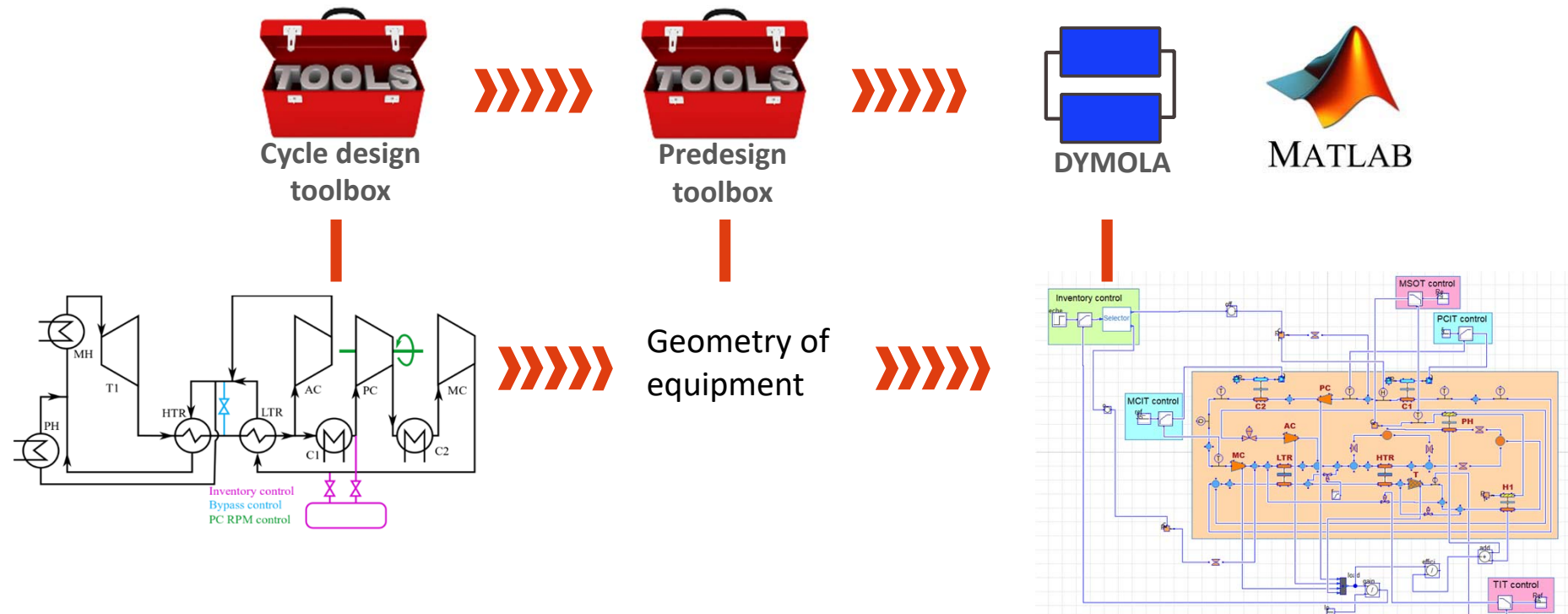
Introduction

System design concept



Introduction

Tools used for development of dynamic model



Model Description

Cycle model

Water/CO₂ HX

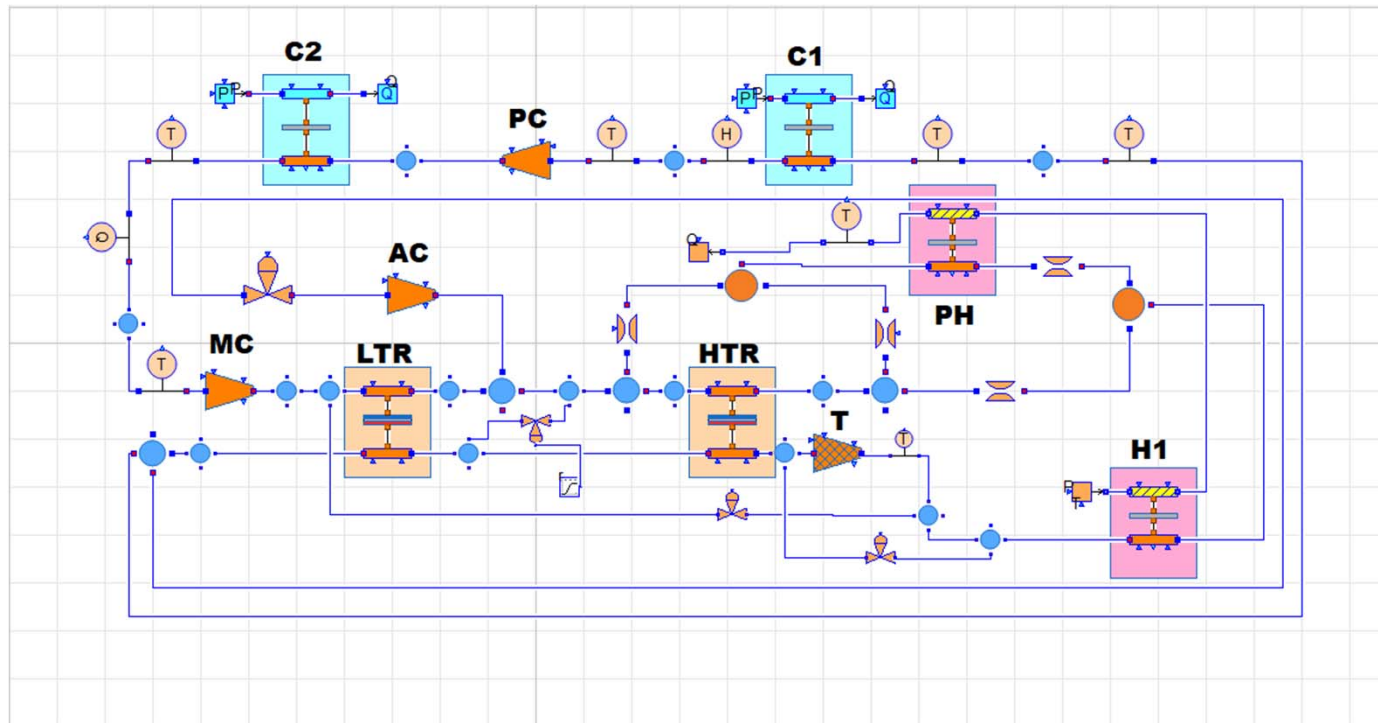
Shell and tube heat exchangers

Thermodynamic properties

CO₂ prop. is calculated by dynamic call of REFPROP

Recuperators

Straight channel printed circle heat exchangers (PCHE)



Turbomachinery

Mass flow rate dependent compression ratio and isentropic efficiency

Auxiliary equipment

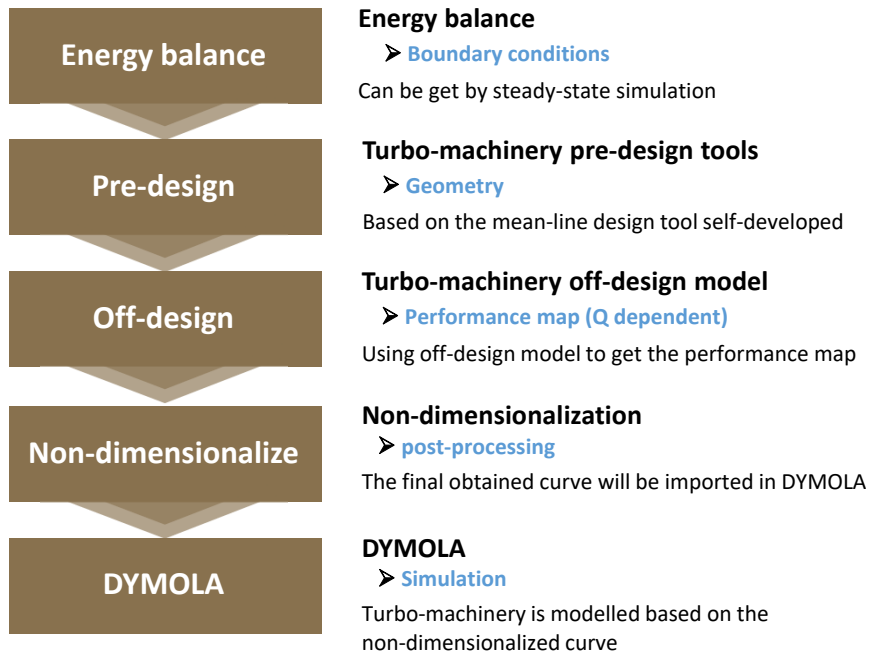
Simplified pipes, sensors and valves

Molten salt/CO₂ HX

Shell and tube heat exchangers

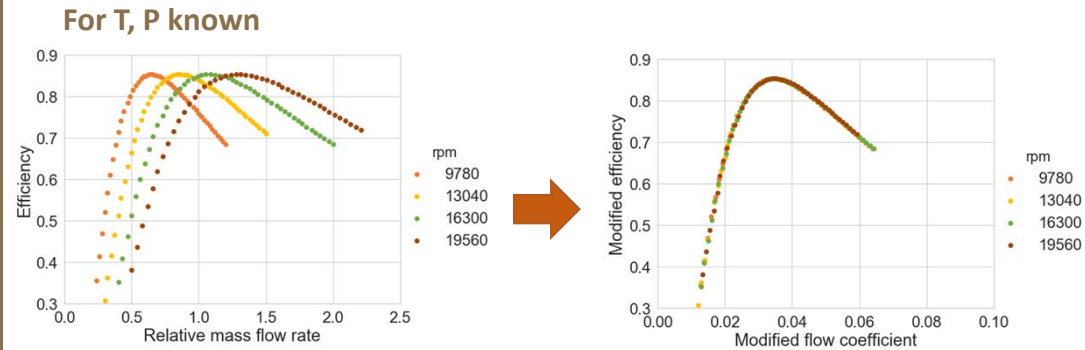
Model Description

Turbo-machinery performance model

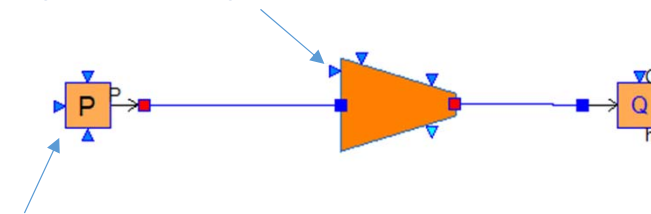


➤➤➤ A realistic model which predicts performance (isentropic efficiency and compression ratio) depending on:

Inlet conditions
 Mass flow rate
 Rotation speed



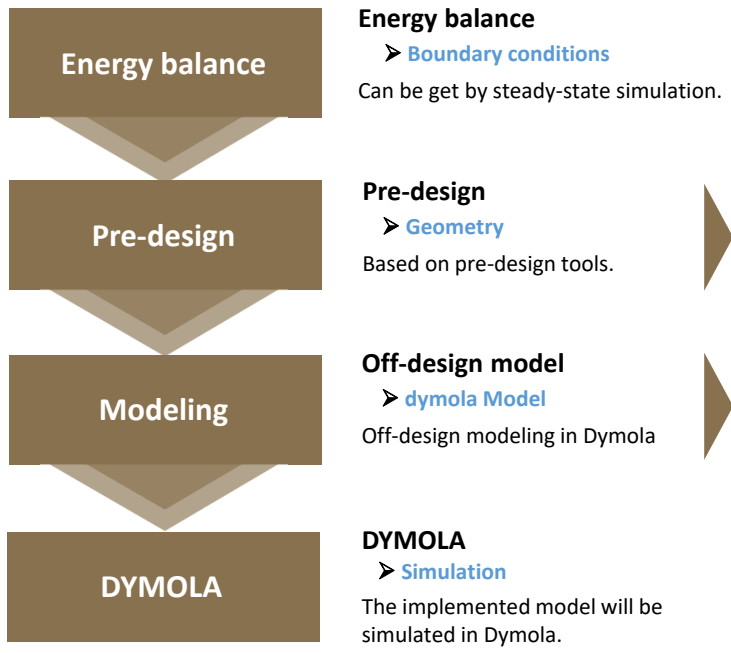
Input rotation speed



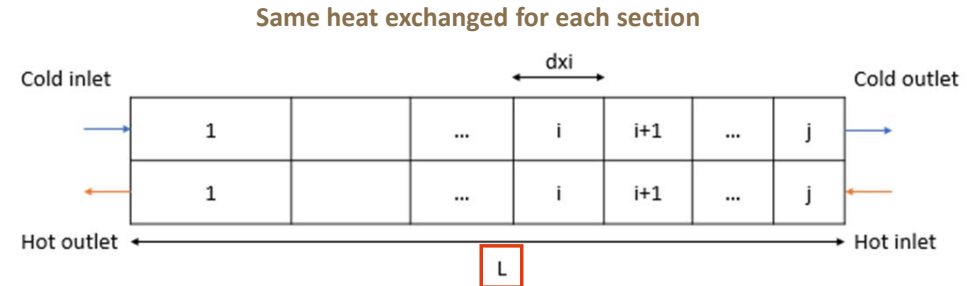
Input fluid properties

Model Description

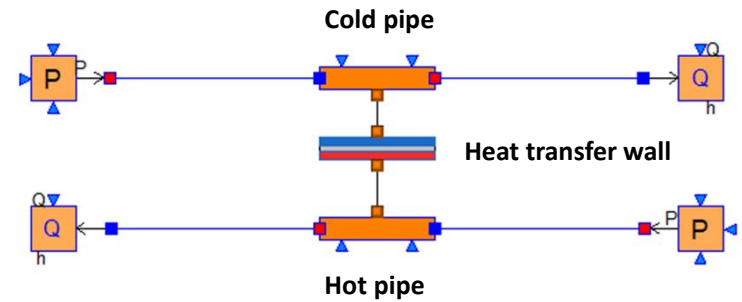
Heat Exchanger Modeling



➤➤➤ A realistic model which predicts on-design and off-design performance of heat exchanger



- Heat transfer calculation: Gnielinski's Correlation
- Pressure drop calculation: Chen's correlation

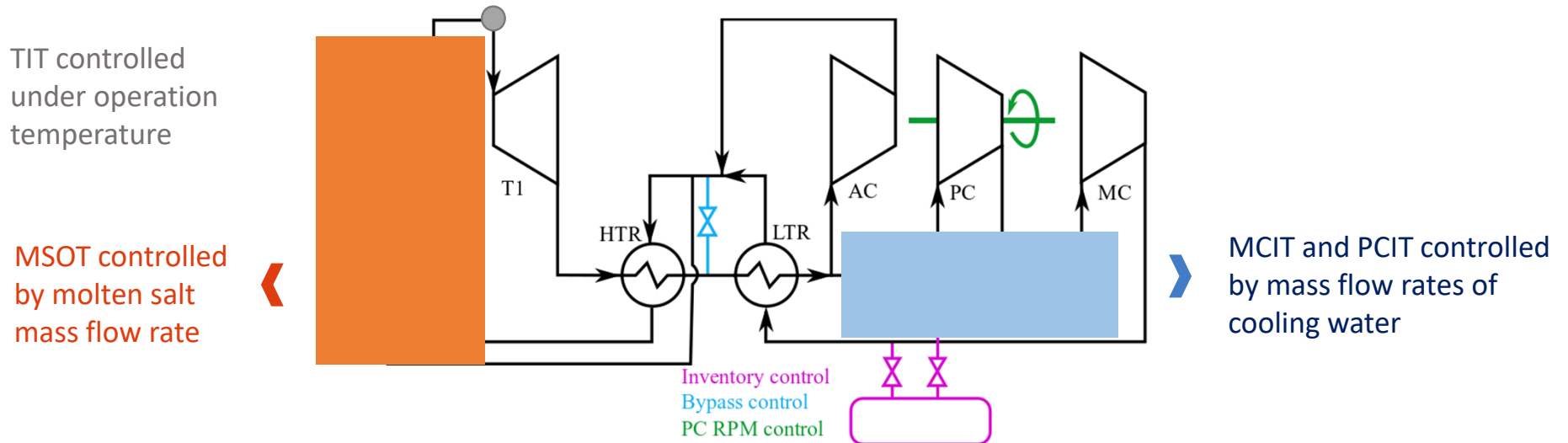


Control System

Elementary controllers

Temperature control loops integrated in the model to ensure:

- Safe operation of turbomachinery
- Molten salt beyond its freezing point (290°C)

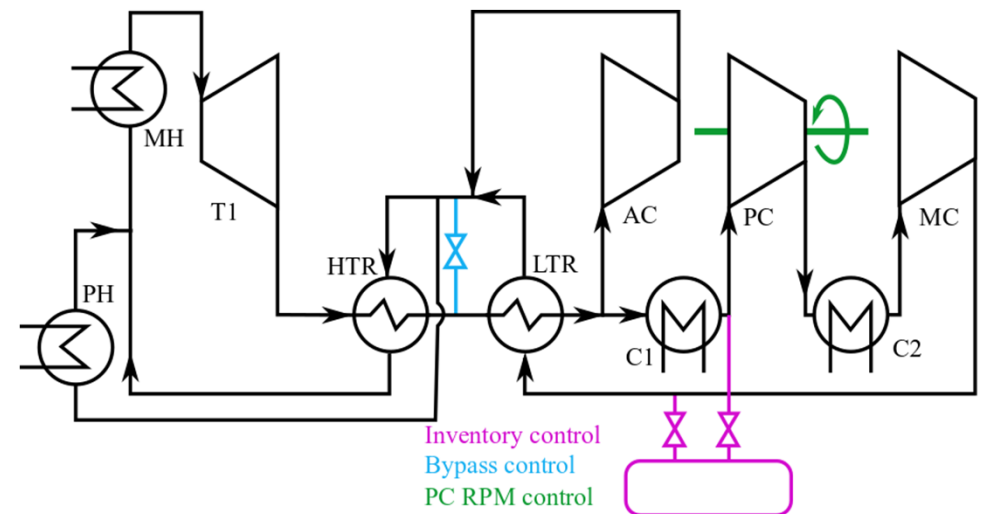


Control System

Part load control strategy

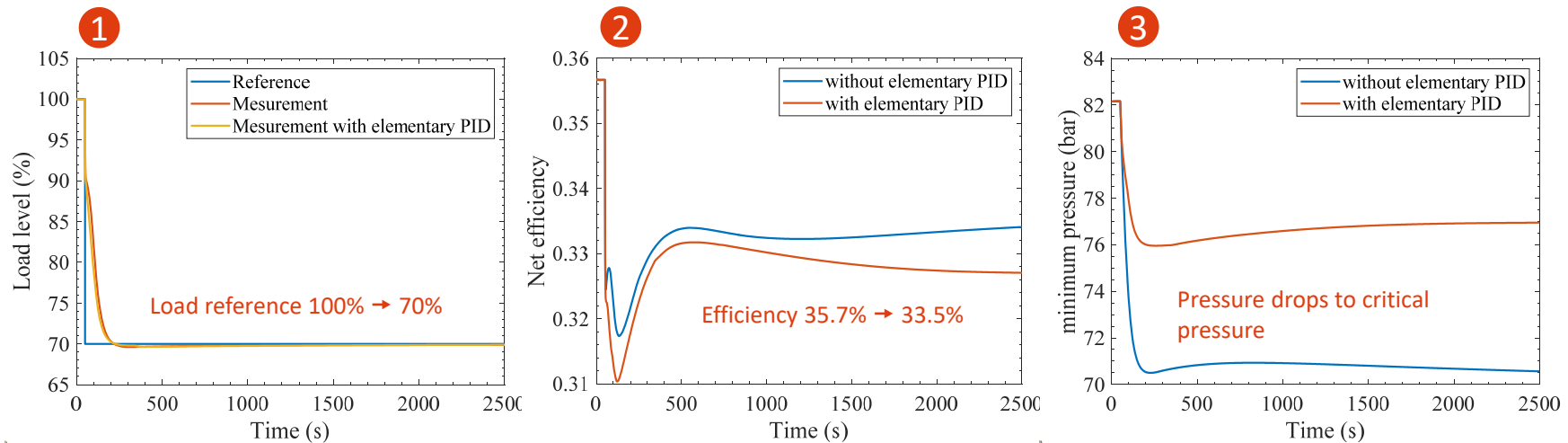
Three methods to control the cycle load level

- Inventory control: inject or release $s\text{CO}_2$ from the cycle
- Bypass control: bypass the fluid from outlet of LTR cold side to outlet of HTR hot side
- Variable PC rotation speed control: adjust the rotation speed of pre-compressor



Part-load Control Strategies and Result Analysis

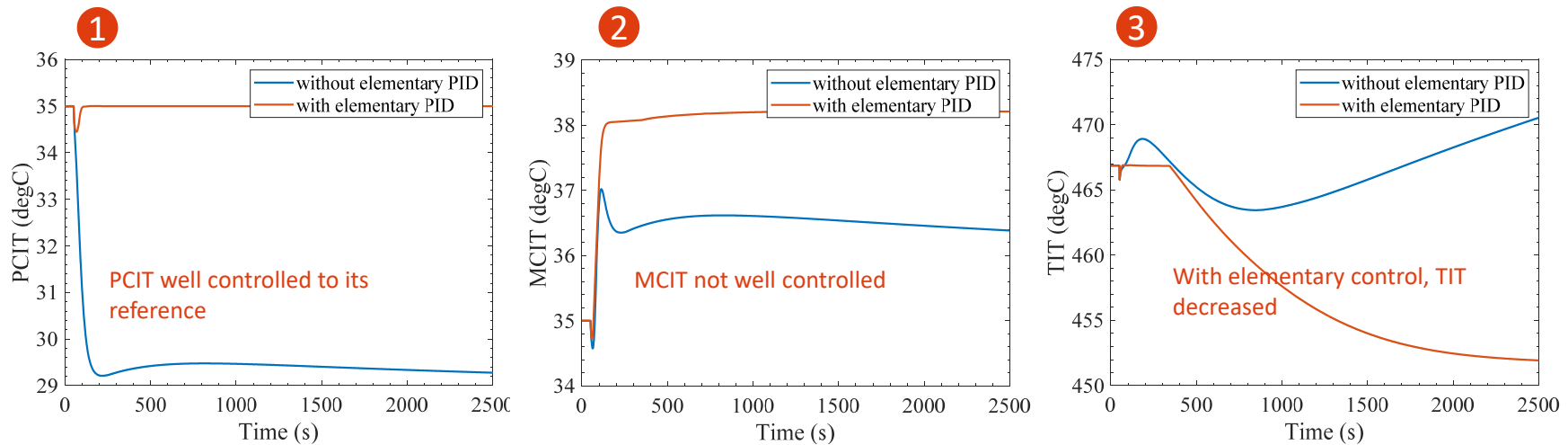
Inventory control (1)



- Response time (to reference): ~150s
- Cycle efficiency: a drop of 2.2%
- Pressure protection is important to protect compressor operation

Part-load Control Strategies and Result Analysis

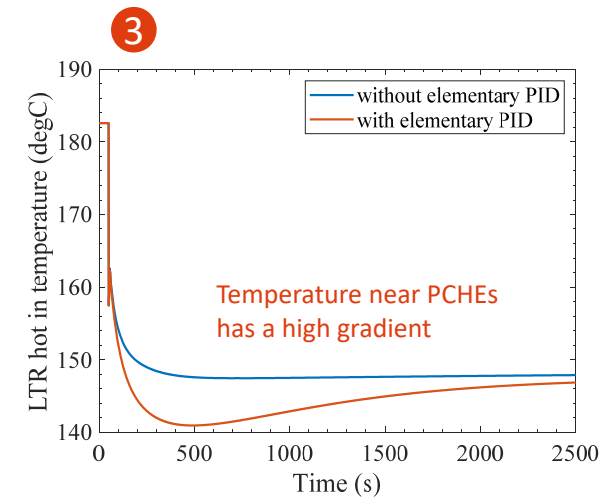
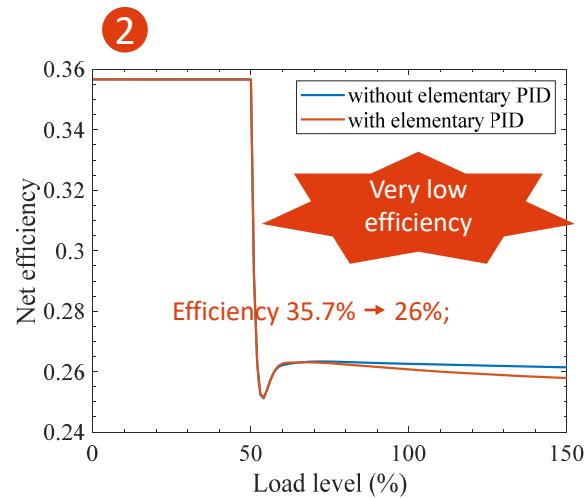
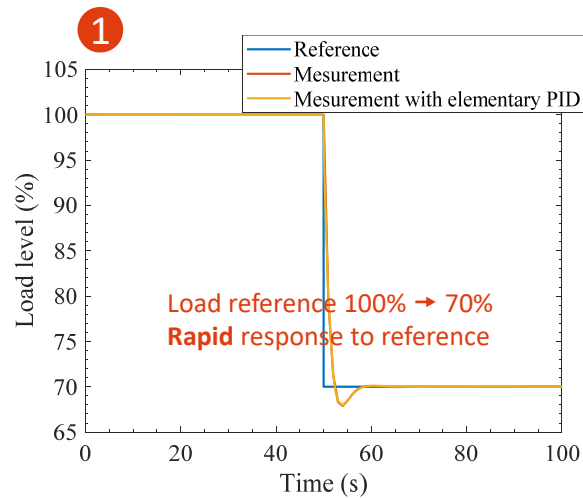
Inventory control (2)



- MCIT not well controlled: limit of pressure drop in water side of cooler 2 when the cooling water mass flow rate augments to decrease MCIT
- Conflict between MSOT and TIT control

Part-load Control Strategies and Result Analysis

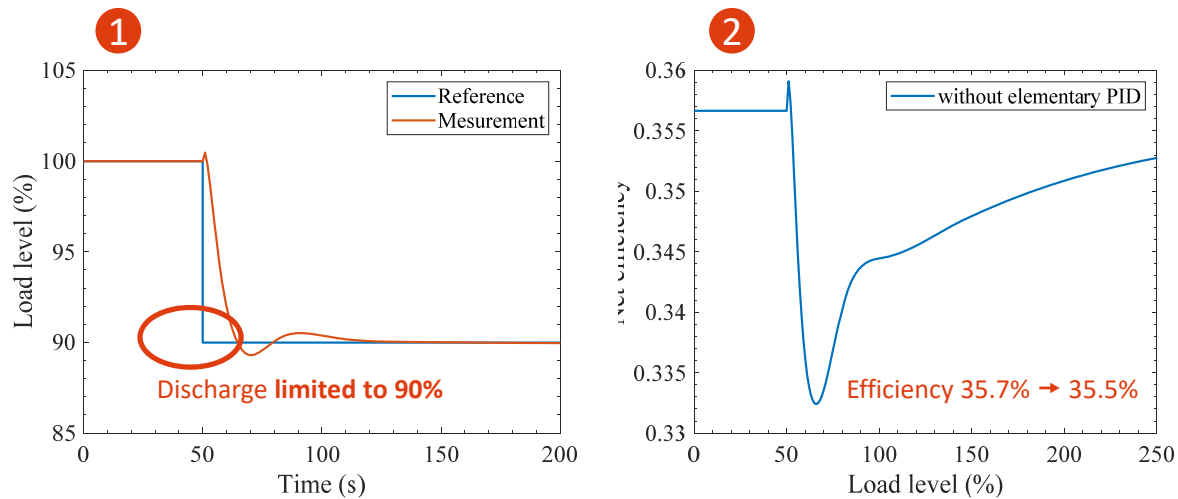
Bypass control



- Response time (to reference): <10s
- Cycle efficiency: a drop of 9.7%
- High gradient of temperature for PCHEs

Part-load Control Strategies and Result Analysis

Variable PC rotation speed control



- Response time (to reference): ~80s
- Cycle efficiency: a drop of 0.2%

Conclusion

Conclusions and perspectives

- A dynamic model developed for a sCO₂ recompression cycle with intercooling and preheating in Dymola
- Importance of elementary temperature control loops
- Advantages and disadvantages of three control strategies
 - Inventory control: maintain the cycle efficiency within a certain range but the response time is relatively slow
 - Bypass control is rapid but would have a drop on cycle efficiency
 - Variable PC rotation speed can keep the cycle efficiency better than inventory control but it is limit on the achievable load level
- Combination of three methods could help propose an optimized global control strategy with a good **balance between efficiency and response speed** for the whole range of load

Questions?