

# Development and Testing of Dry Gas Seals for Turbomachinery in Multiphase CO<sub>2</sub> Applications

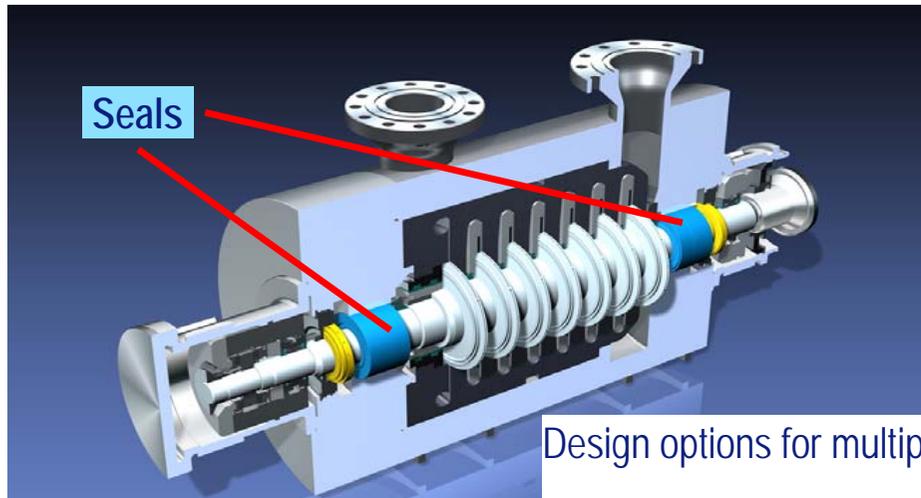
3<sup>rd</sup> European supercritical CO<sub>2</sub> Conference  
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Armin Laxander, Andreas Fesl, Benjamin Hellmig

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## Multiphase Seals in Turbomachinery Applications

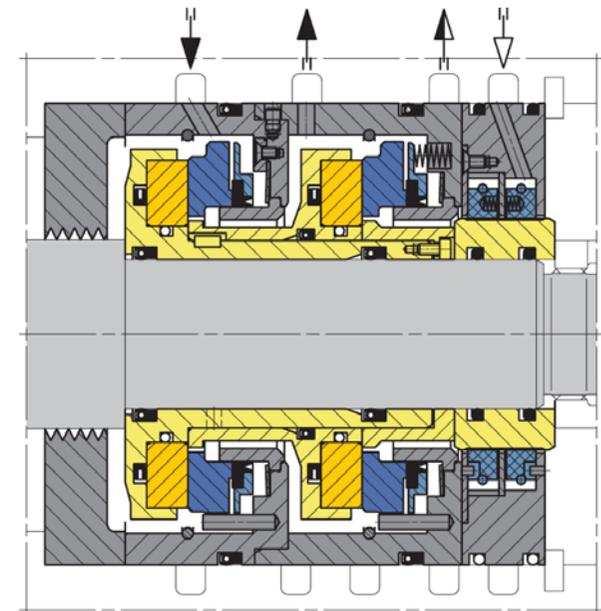
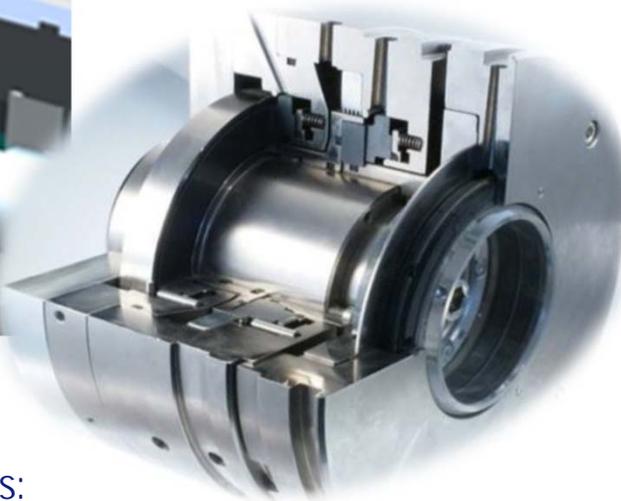
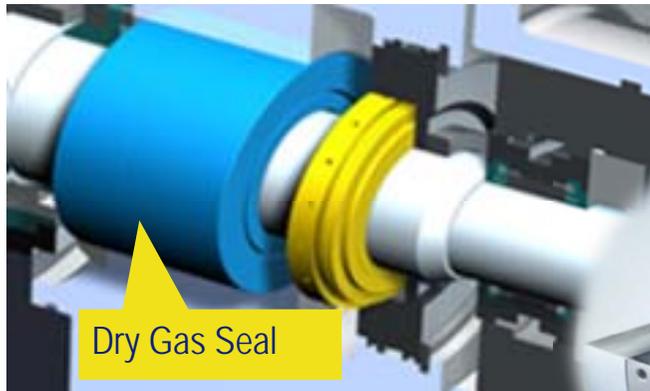


Low leakage demands require **mechanical seals!**

Design options for multiphase applications:

- A) Liquid Seal      contacting seal, small sealing width, low speed limits, low liquid leakage, cannot work with pure gas
- B) Dry Gas Seal      non-contacting, large sealing width, material determined speed limits, can work with liquids (in a limited range), very low gas leakage, high liquid leakage
- C) Liquid/Gas Seal      features of both seal designs are combined

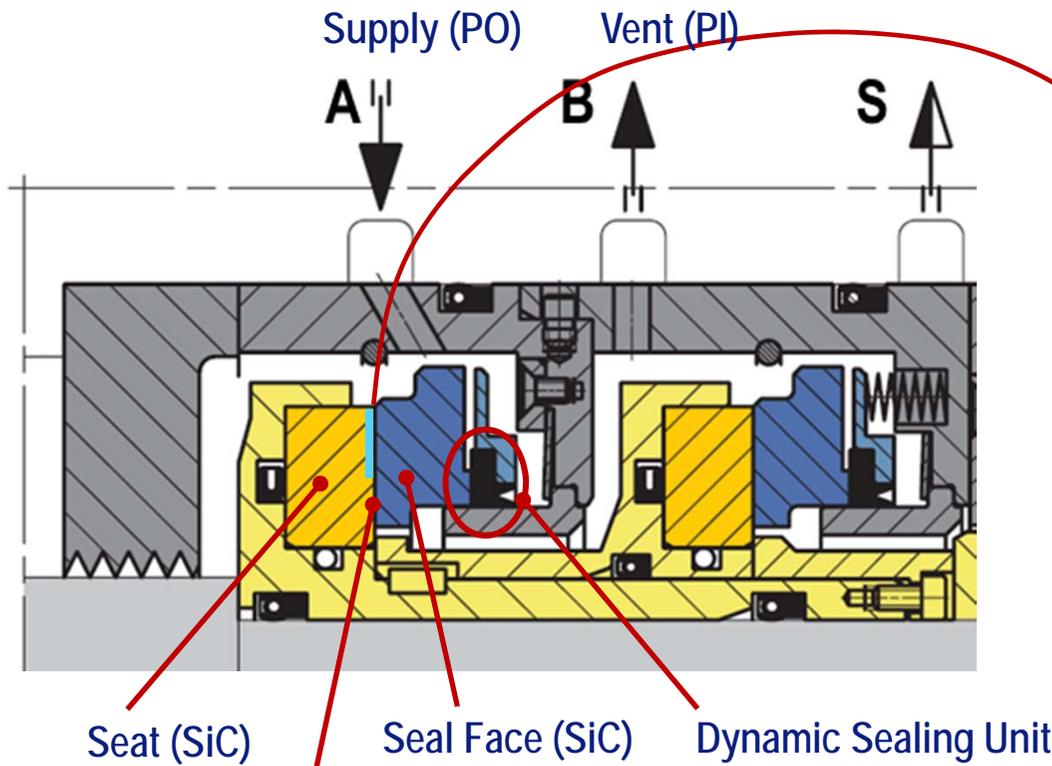
# Multiphase Seal



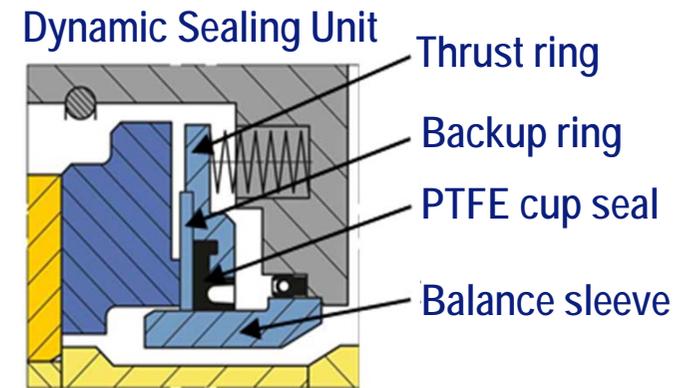
## Dry Gas Seal Characteristics:

- Low gas leakage
- Low friction losses
- No wear in sliding face

# Dry Gas Seal (DGS) – Design

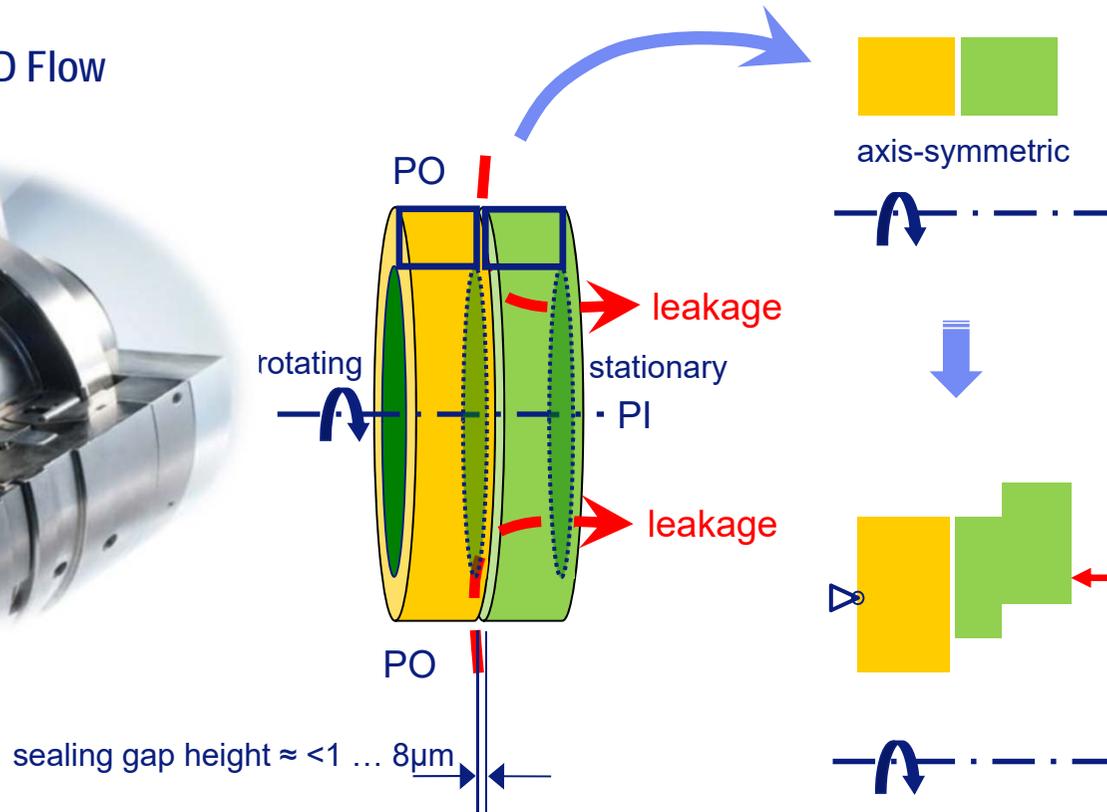
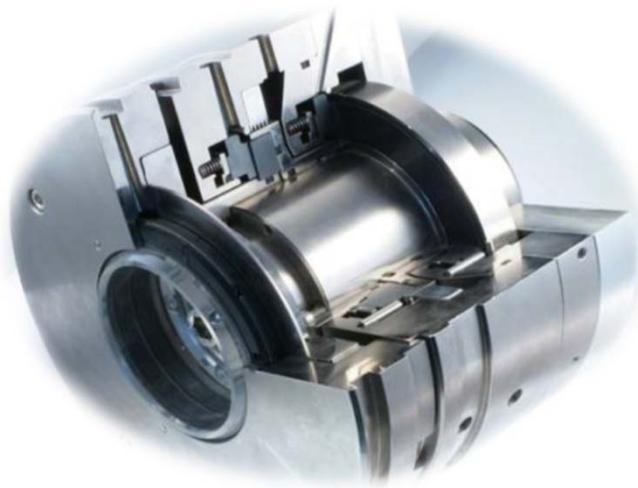


Sealing Gap (opens up to few micrometer when subjected to pressure and/or rotation)

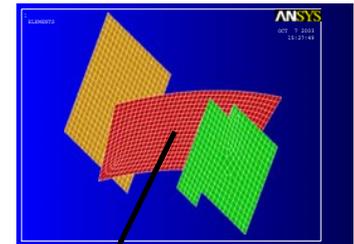


# Dry Gas Seal – Analysis

3D Structure / 3D Flow



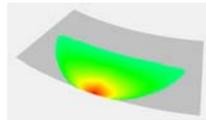
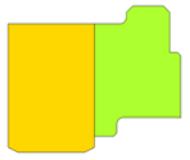
2D Structure / 2D Flow



$$\frac{1}{r} \frac{\partial}{\partial \theta} \left( \frac{\rho h^3}{12\eta} \frac{\partial p}{\partial r} \right) + \frac{\partial}{\partial r} \left( \frac{r \rho h^3}{12\eta} \frac{\partial p}{\partial r} \right) = \frac{r\omega}{2} + \frac{\partial}{\partial \theta} (\rho h)$$

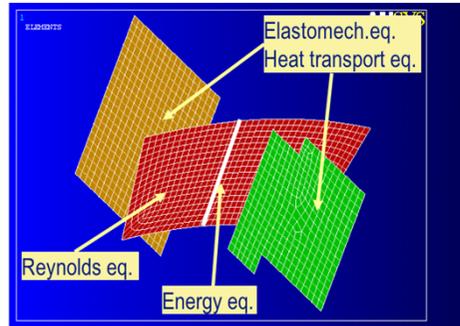
Reynolds Equation

# Sealanalysis – Coupled Fluid-Structure-Analysis



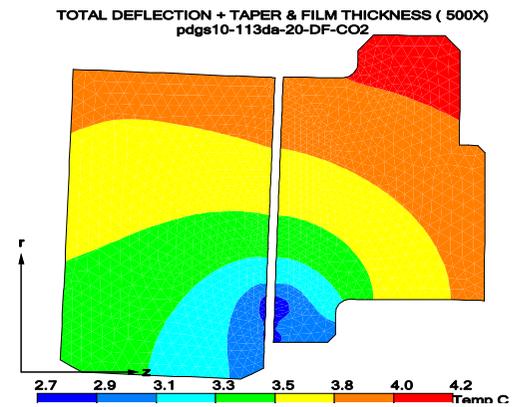
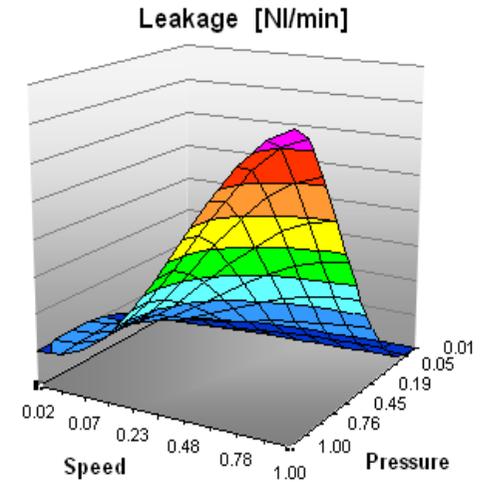
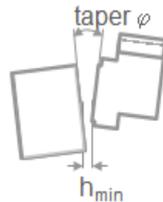
Design Data  
Operating Data

Fluid  
Properties



**SEALANALYSIS**  
Additional Calculational Design Tools

Gap flow:  $p, h, v$  cyclic symmetric,  $f(r, \theta)$   
 Interface:  $T, q$   $f(r)$   
 Ring System:  $T, u, q$  axis-symmetric,  $f(r, z)$



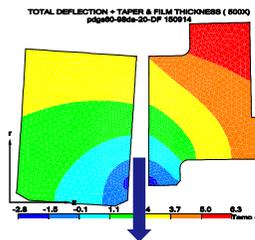
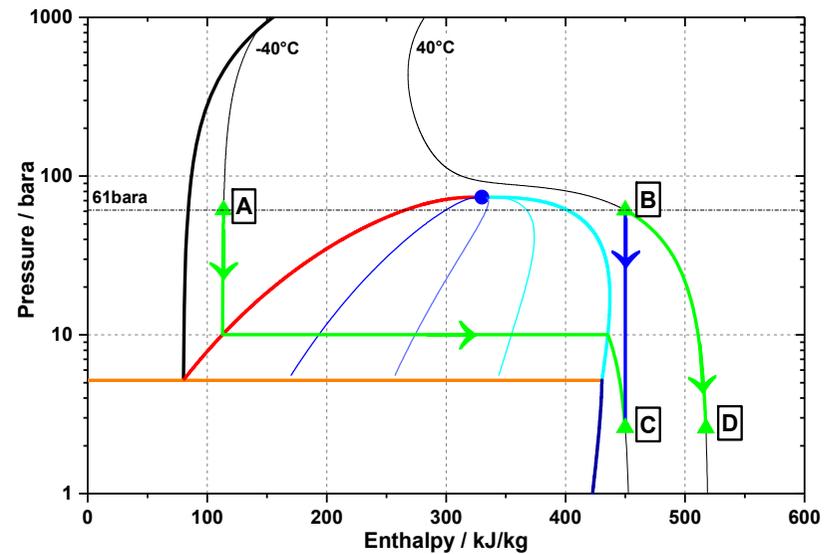
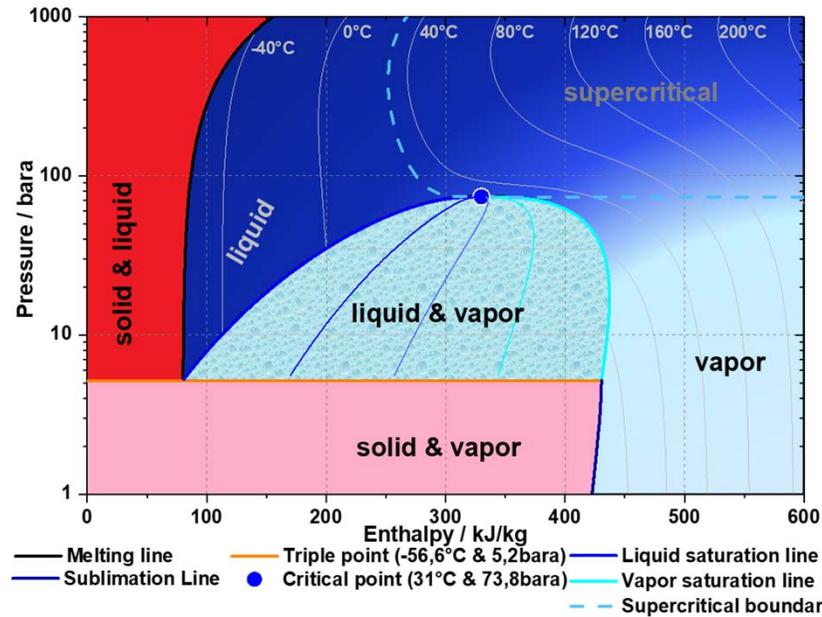
## DGS for CO<sub>2</sub> Multiphase Applications

### What's different with CO<sub>2</sub> compared to most other fluids?

- Gas properties, in particular in transcritical region.
- Operation without additional heater possible?
- Are numerical predictions correct?

=> **Verification / validation of design by internal test campaign!**

# Criticality of CO<sub>2</sub> Sealing Applications



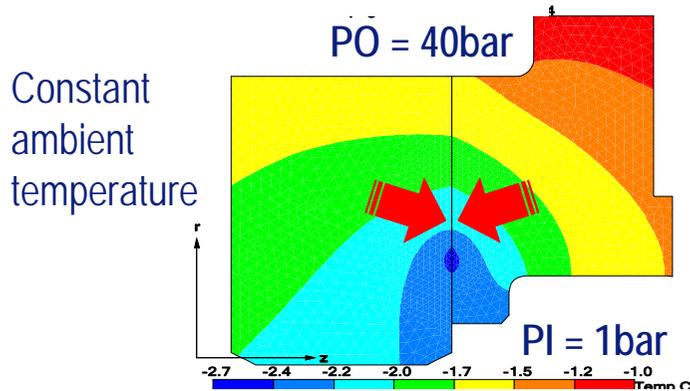
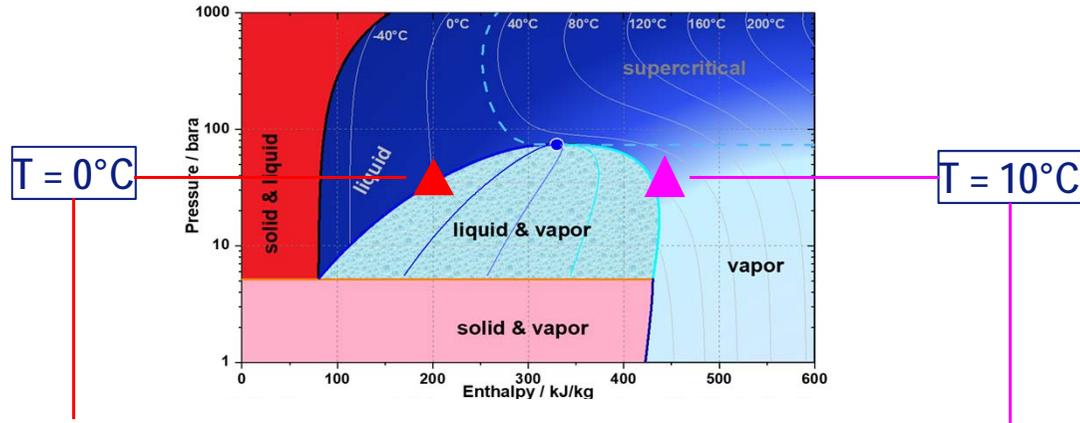
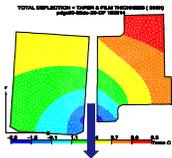
A → C ... isothermal,  $\Delta T = 0K$

B → C ... isenthalpic,  $\Delta T = -80K$

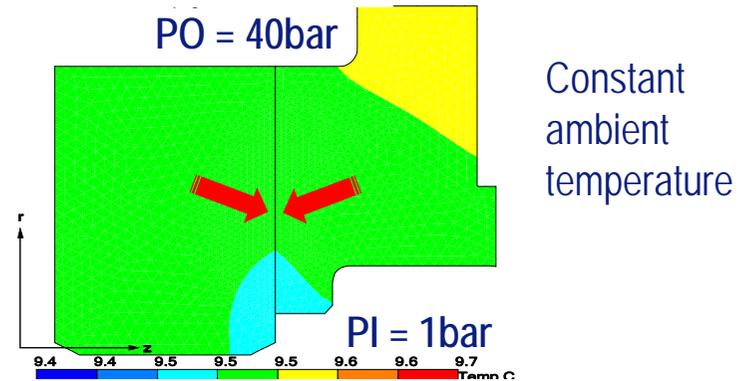
B → D ... isothermal,  $\Delta T = 0K$

# (Almost) Isothermal Expansion – What does it really mean?

PO = 40bar, PI = 1bar  
CO<sub>2</sub>, Static



Expansion with only little temperature drop in the ring system is referred to as **almost isothermal** or simply **isothermal!**



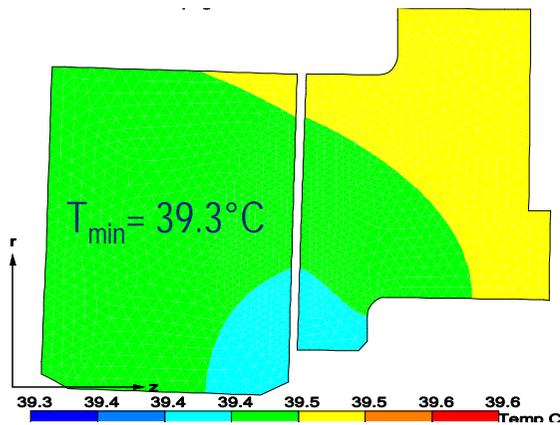
$T \gg -56.6^\circ\text{C}!$

# Criticality of CO<sub>2</sub> Sealing Applications

PO = 60barg, PI = 0barg, **T = 40°C**, CO<sub>2</sub>, Static

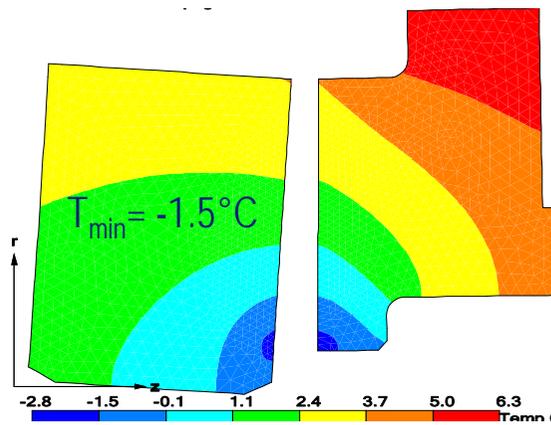
Result plots: Total deflection and isotherms (scale 500X)

Reference



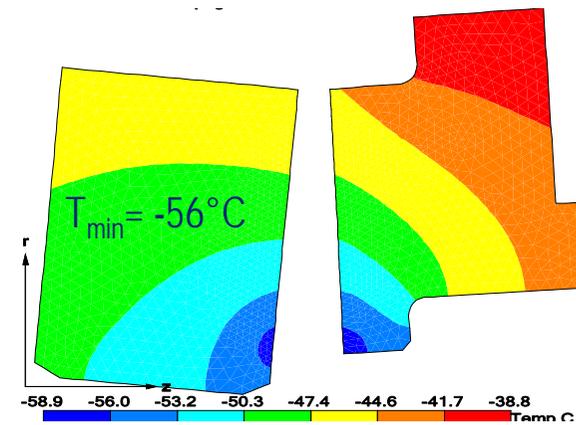
Leakage: 2.2 NI/min

Inappropriate gap design 1



107 NI/min

Inappropriate gap design 2

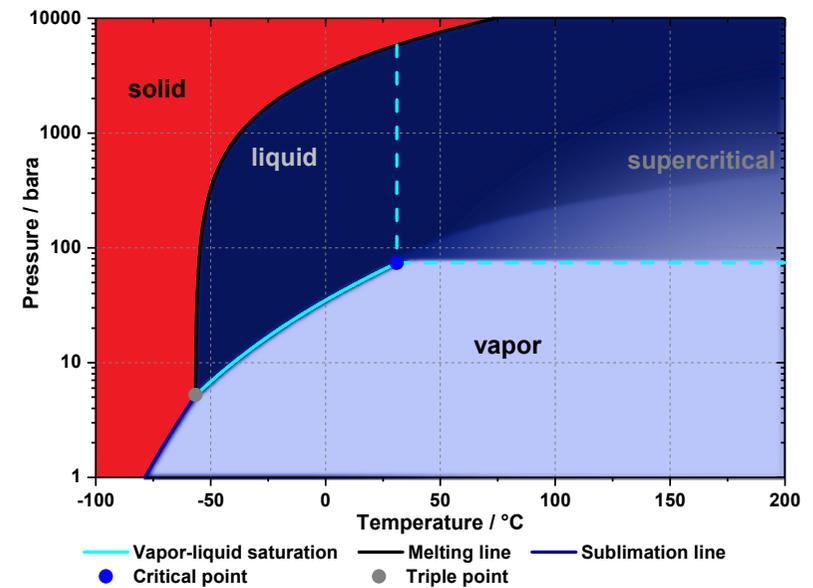


260 NI/min

**Avoiding adverse effects on seal performance requires extremely low leakage levels!**

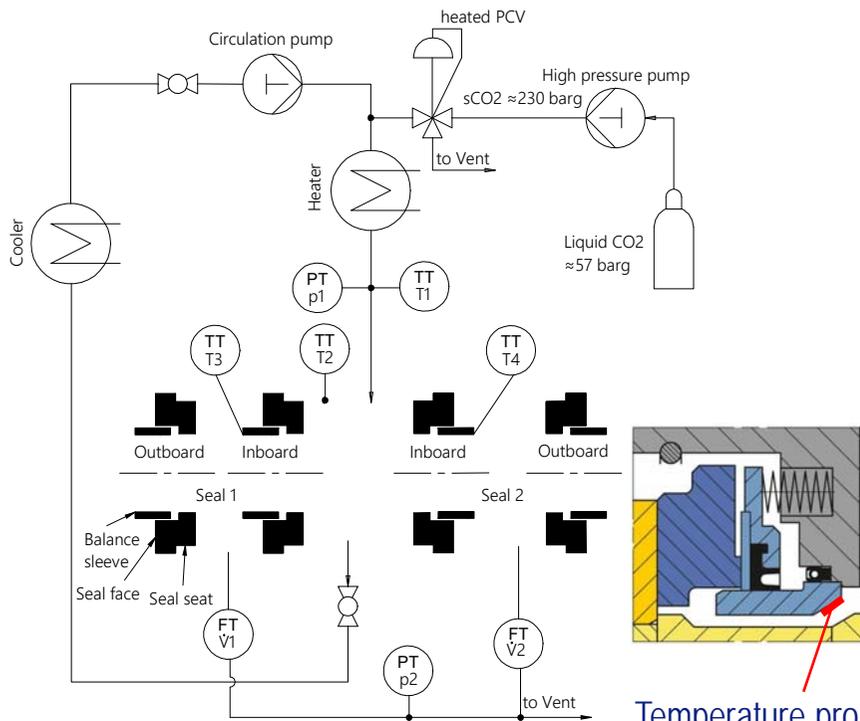
## Test Set-up and Testing Range (Pressure/Temperature)

Multiphase suitability: Seal can operate in liquid, two-phase, vapor and supercritical region **without additional heater!**



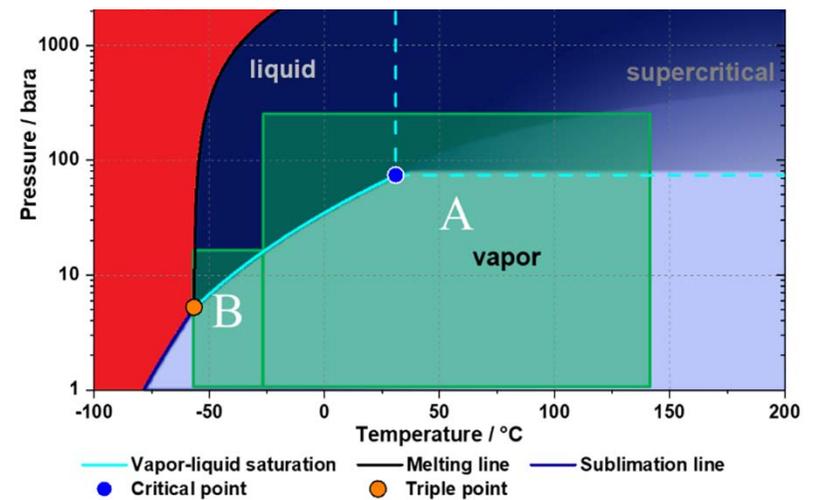
# Test Set-up and Testing Range (Pressure/Temperature)

## Simplified PID



Multiphase suitability: Seal can operate in liquid, two-phase, vapor and supercritical region **without additional heater!**

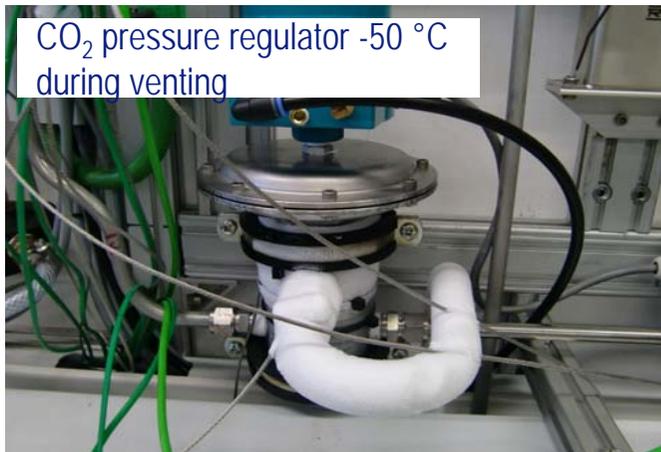
## P-T Range of Testing



A ... normal operating range

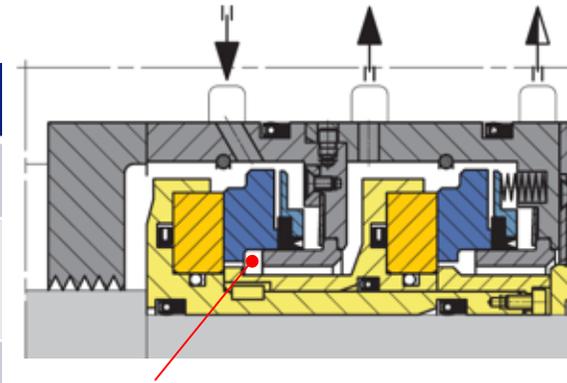
B ... failure test

# CO<sub>2</sub> Test Facility



## Test Program

		Pressure	Speed	Temperature	Time
		barg	rpm	°C	h
Tandem seal	static	60 / 80 / 200	-	0 ... 120	
	static	60	-	0 ... 100	18
	dynamic	60 / 80 / 180	3600	0 ... 120	
Single seal	static	60	-	ambient	48
	static	200	-	ambient	14



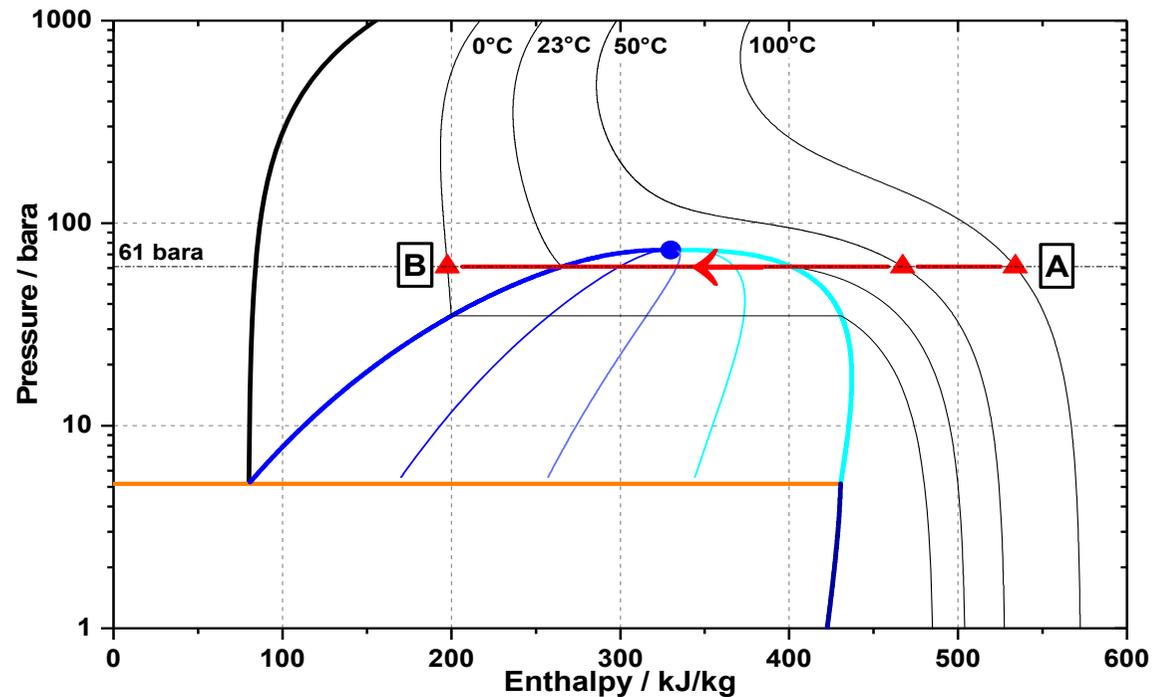
Low pressure area:

- optional protected by N<sub>2</sub> (tandem seal)
- exposed to ambient conditions (single seal)

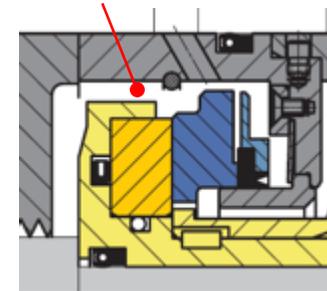
## Additional: Seal failure simulation

# 60barg CO<sub>2</sub> Static Test, Decreasing Temperature

Test section: Cool down phase (18h) after dynamic run with hot CO<sub>2</sub>



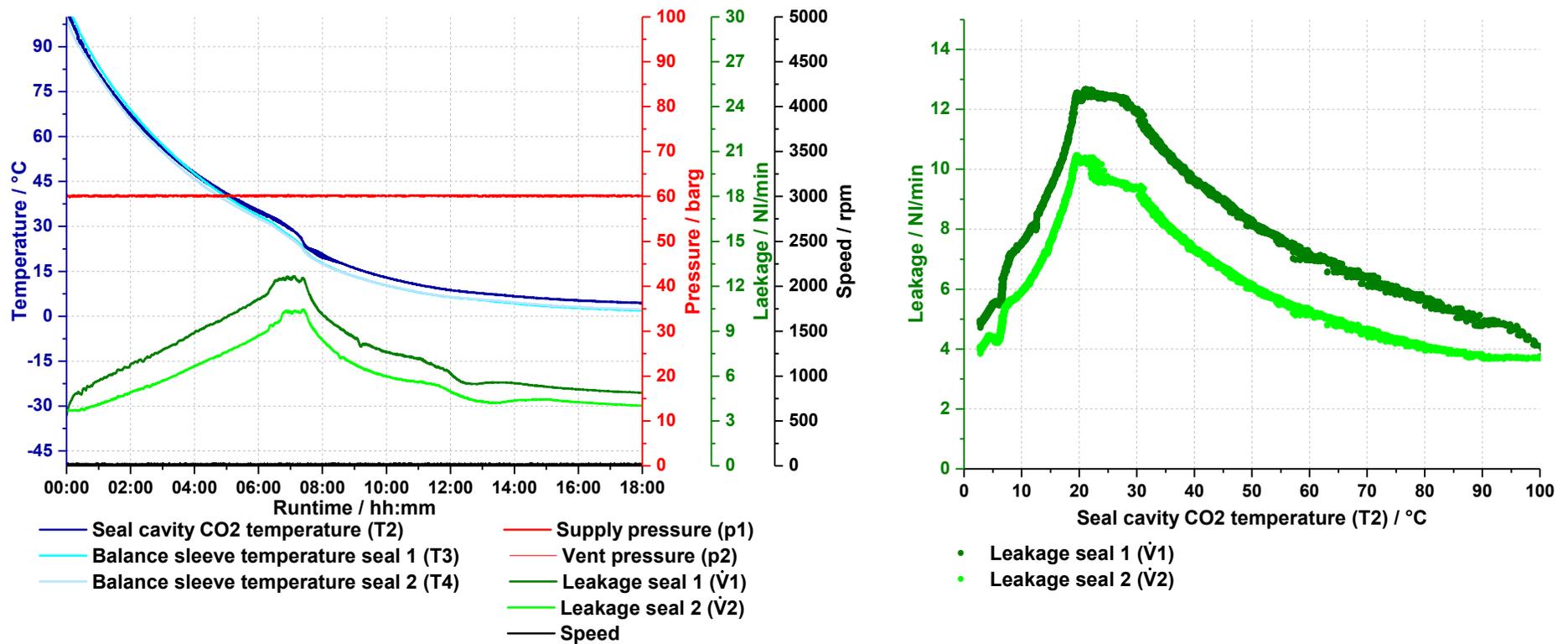
P const., T decreasing



- A Start in gaseous region  
60barg/100°C
- B End in liquid region  
60barg/0°C

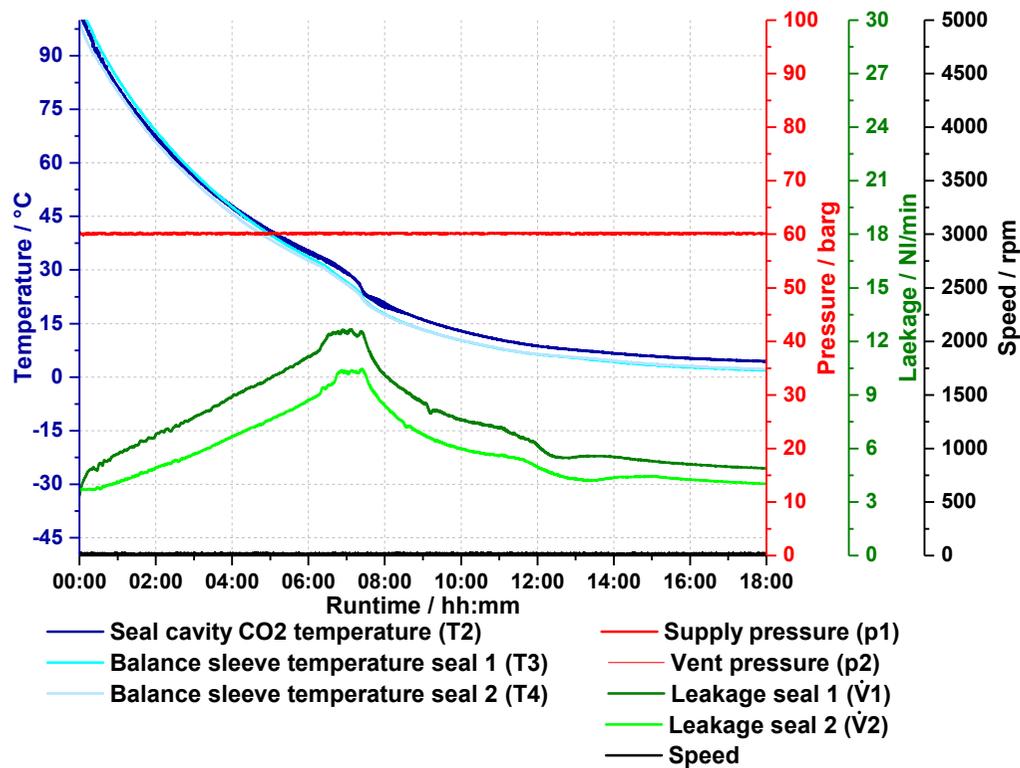
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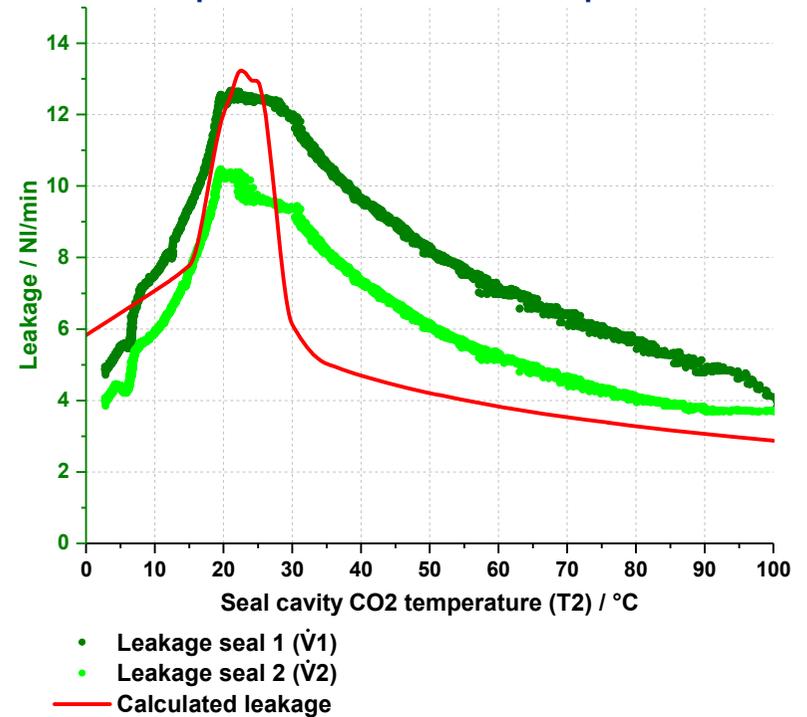


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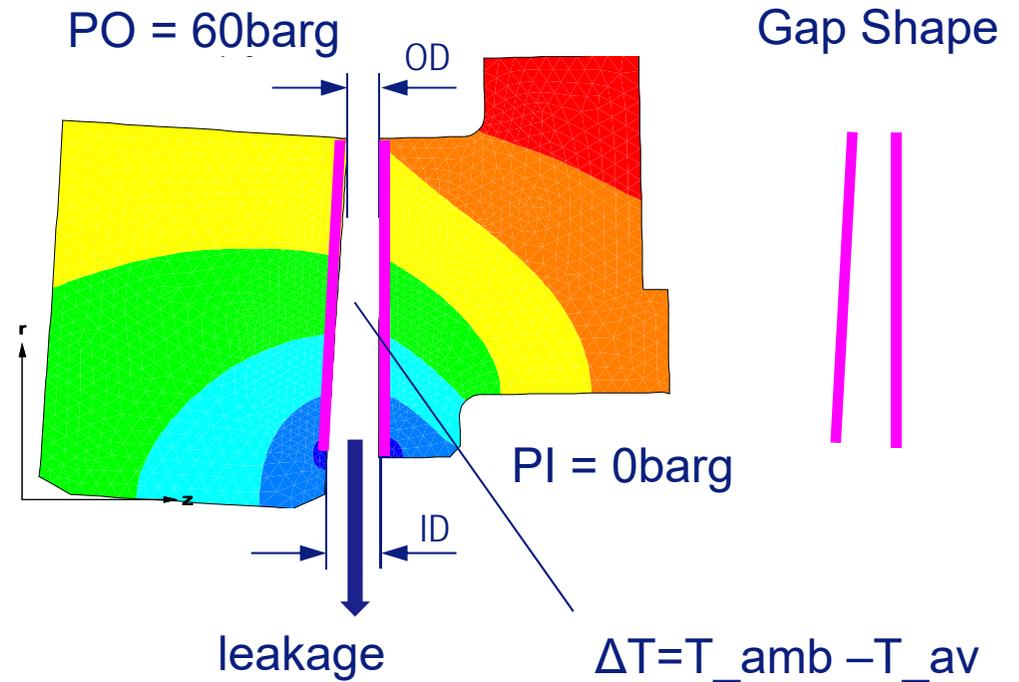
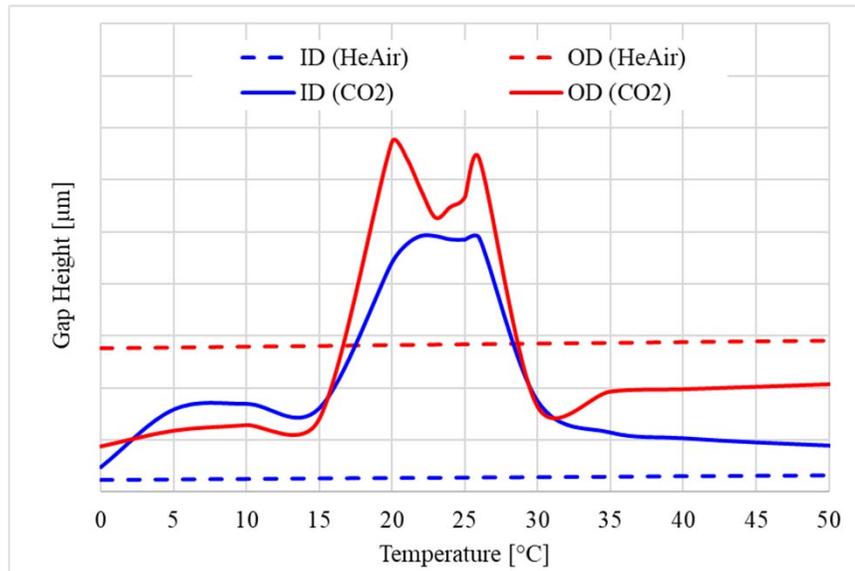


## Comparison with numerical prediction



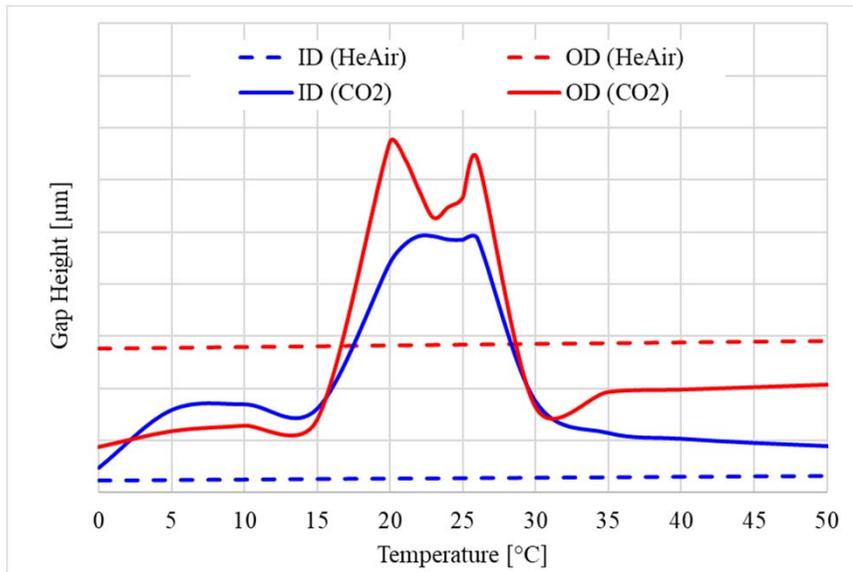
# 60barg CO<sub>2</sub> Static Test, Decreasing Temperature – Analysis

## Numerical prediction of gap shape, leakage and temperature

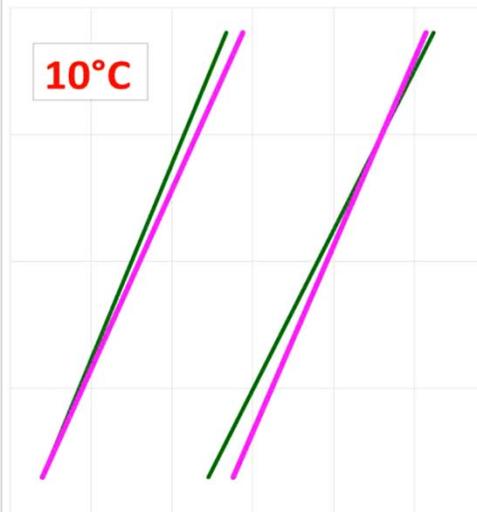


# 60barg CO<sub>2</sub> Static Test, Decreasing Temperature – Analysis

## Inner/outer height of sealing gap

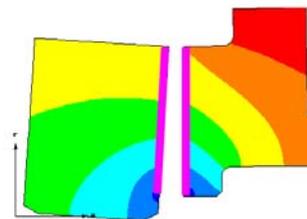
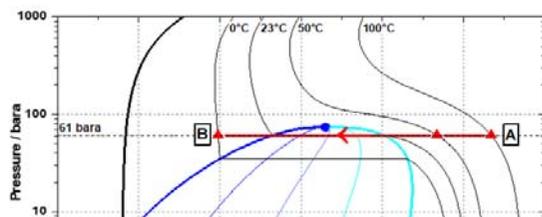
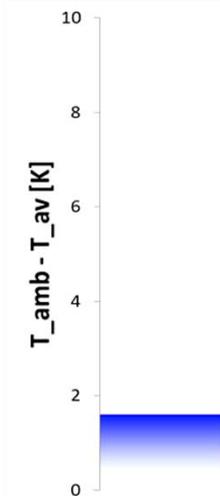
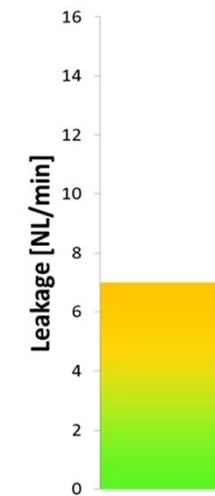


## Gap shape

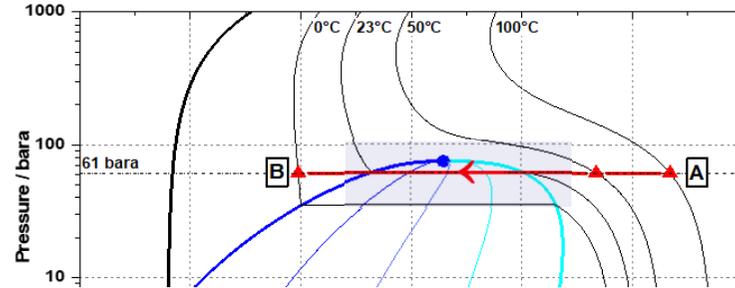
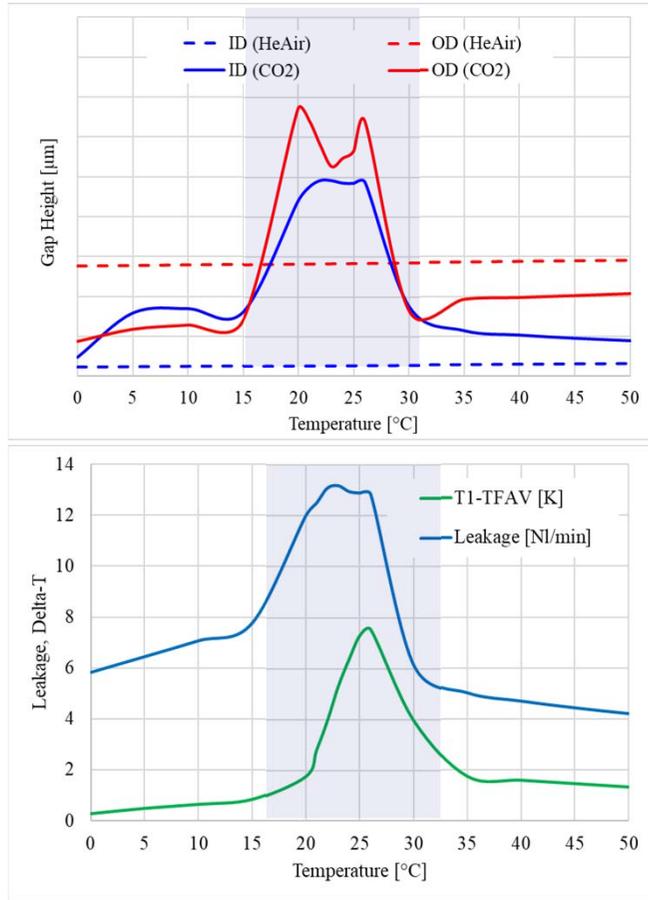


$\dot{V}$

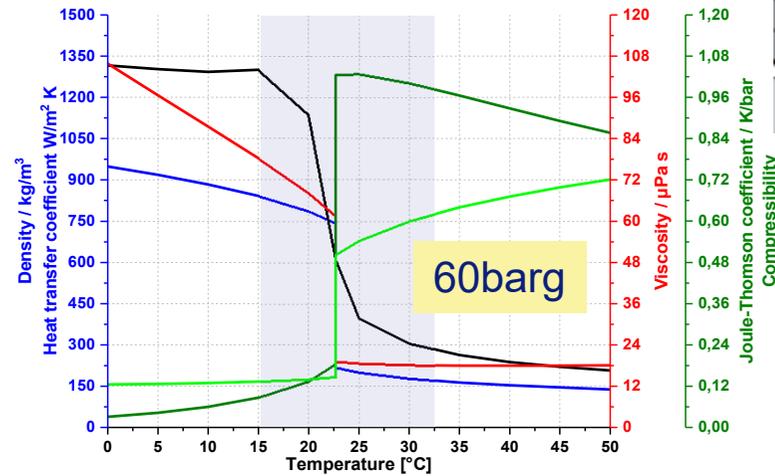
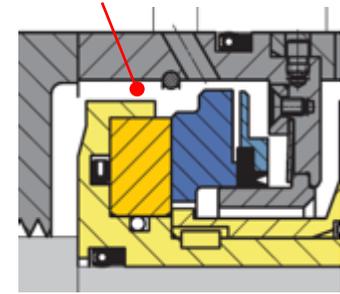
$\Delta T$



# 60barg CO<sub>2</sub> Static Test, Decreasing Temperature – Analysis



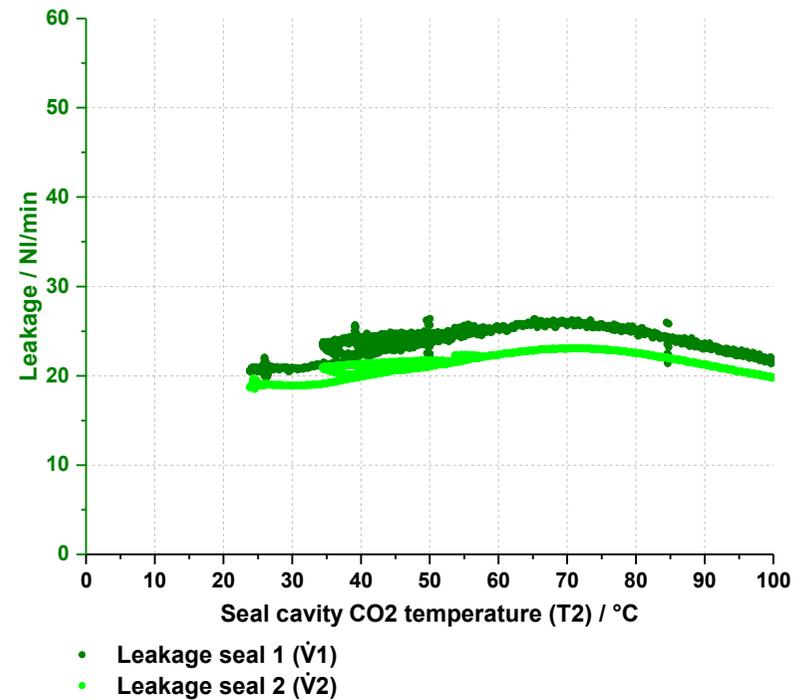
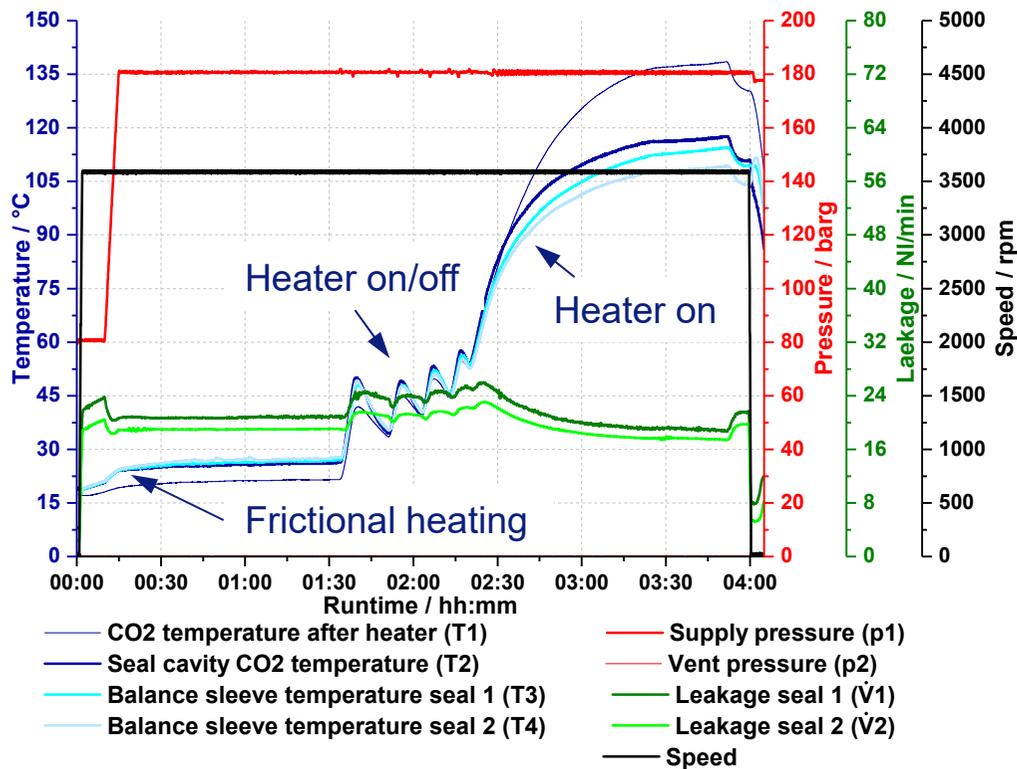
P constant  
 $P_{ar} = F(T)$



- Density
- Heat transfer coefficient
- Viscosity
- Joule-Thomson coefficient
- Compressibility

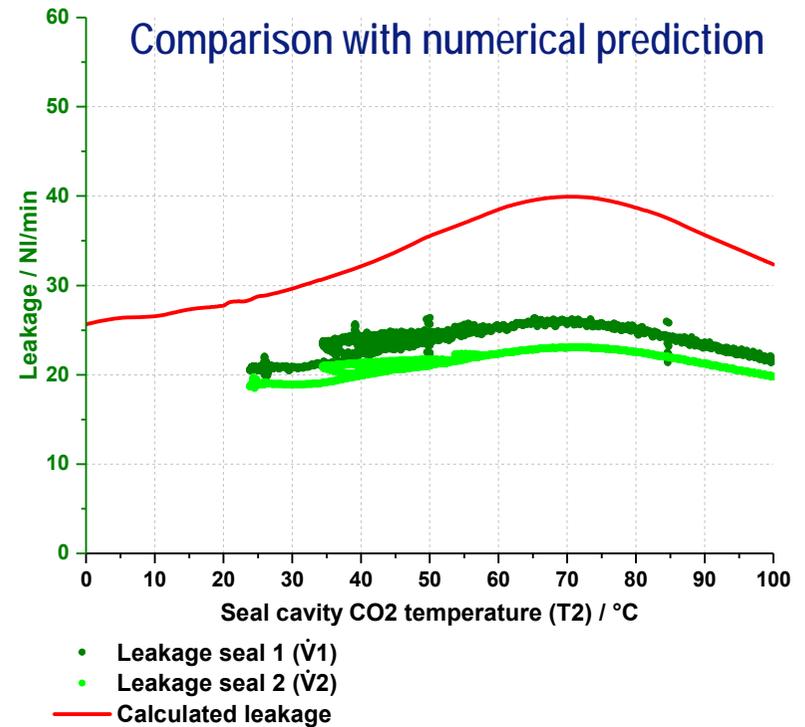
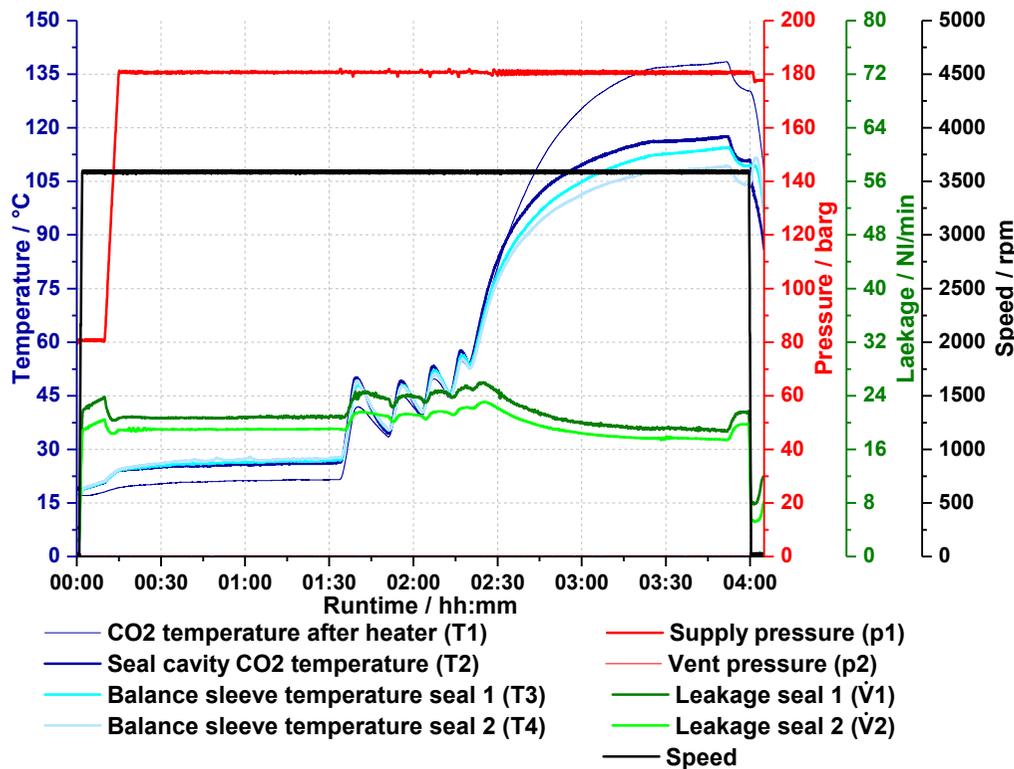
# 180barg CO<sub>2</sub> Dynamic Test, Increasing Temperature

Test section: Dynamic run (180barg/3600rpm), CO<sub>2</sub> temperature control: 20°C / 50°C / 120°C

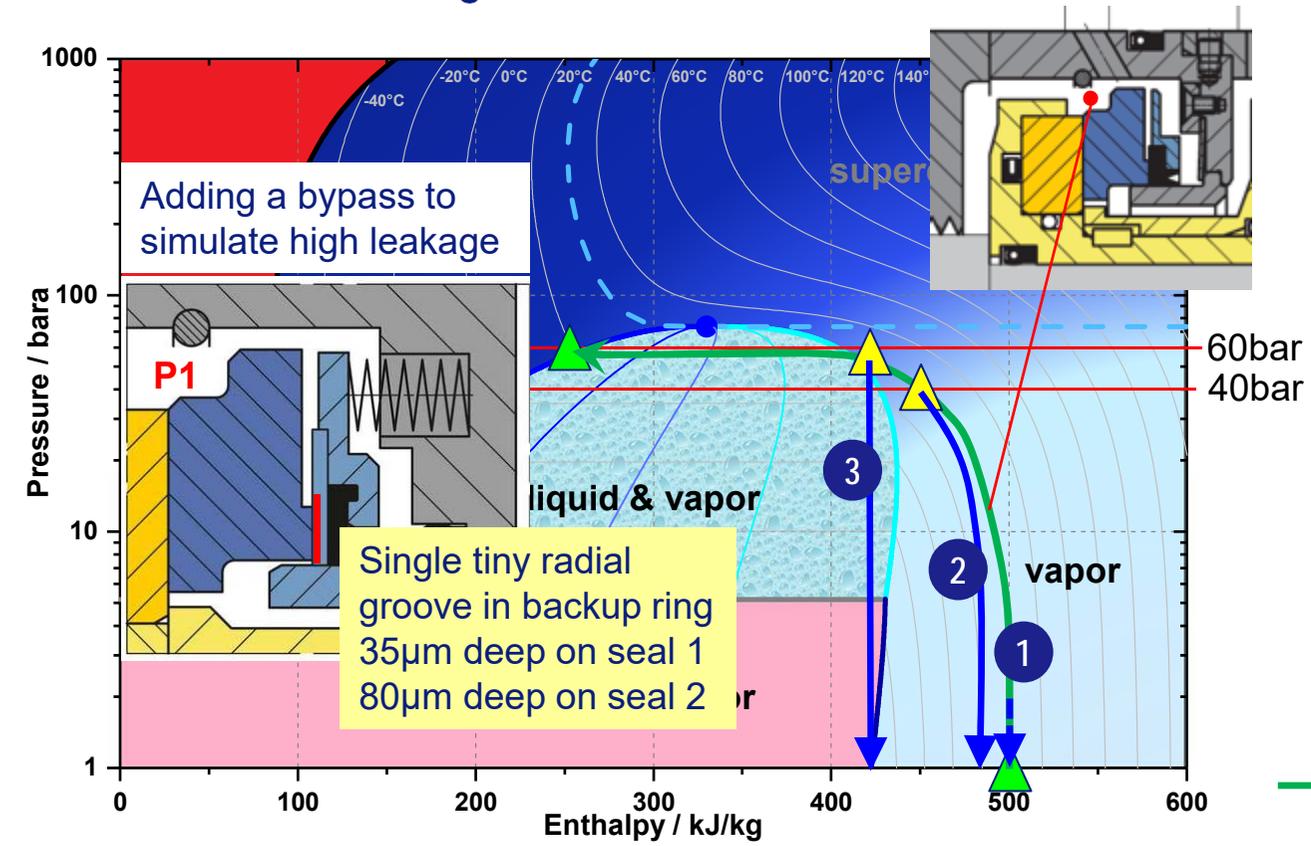


# 180barg CO<sub>2</sub> Dynamic Test, Increasing Temperature

Test section: Dynamic run (180barg/3600rpm), CO<sub>2</sub> temperature control: 20°C / 50°C / 120°C



# Static Test Simulating a Seal Failure



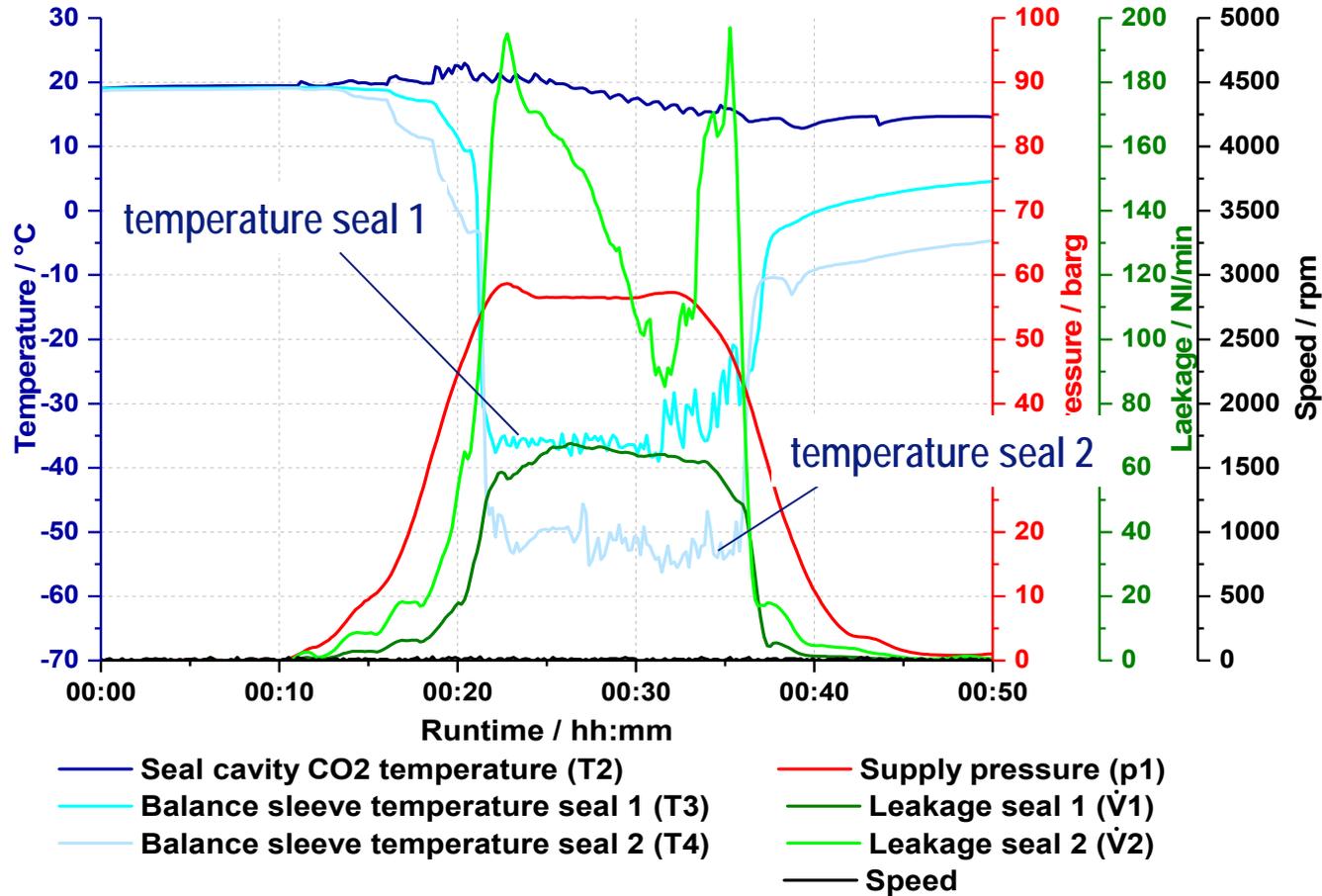
- 1 Sealing cavity pressure increase at constant temperature 20°C
- 2 At about 40bar remarkable deviations from isothermal expansion. Seal temperature about 0°C
- 3 Beyond 55bar isenthalpic expansion down to triple point

→ Sealing cavity pressure PO

→ Expansion through sealing gap & bypass

— Melting line      — Triple point (-56,6°C & 5,2bar)      — Liquid saturation line  
 — Sublimation Line      ● Critical point (31°C & 73,8bar)      — Vapor saturation line  
 — — Supercritical boundary

# Static Test Simulating a Seal Failure – Results



## Summary

- Dry Gas Seal design
  - large seal width provides good lift-off capability and thus wear-free operation
  - Safe non-contacting dynamic operation
  - Offers modification for compressor applications
- Virtually isothermal expansion due to extremely low leakage
- Works with liquid, two-phase, gaseous and supercritical CO<sub>2</sub> without the need for additional heating of the high-pressure sealing cavity
- Sound numerical predictive capability even close to critical CO<sub>2</sub> conditions and phase transitions

**Rely on excellence**

**Thank you  
for your attention!  
Questions?**

EagleBurgmann Germany GmbH & Co. KG  
Aeussere Sauerlacher Strasse 6-10  
82515 Wolfratshausen  
Germany



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# Dry Gas Seal (DGS) – Basic Components

