



# The Research of S-CO<sub>2</sub> cycles at CTU in Prague

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# Introduction

## Research at CTU in Prague

- Study of thermodynamic properties of CO<sub>2</sub>
  - Effect of mixtures in S-CO<sub>2</sub> power cycle
- Study of S-CO<sub>2</sub> power cycle - configuration of cycle layout

## Experimental loop:

- Net power – 10 MW
- Turbine inlet temperature – 550 °C
- Compressor inlet temperature – 32 °C



# Investigated cycles

Experimental loop:

- Research of cycles layouts for basic S-CO<sub>2</sub> cycles

The six basic cycles:

- Simple Brayton cycle
- Re-compression cycle
- Pre-compression cycle
- Split expansion cycle
- Partial cooling cycle
- Partial cooling with improved regeneration

# Design of heat exchangers

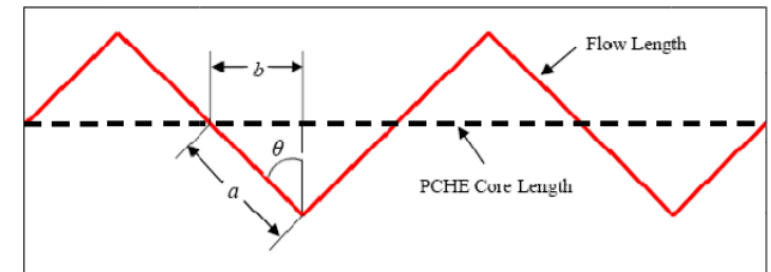
Type of heat exchangers:

PCHE – Printed Circuit Heat Exchangers

- The minimum temperature drop can be only 2 ° C
  - CO<sub>2</sub>-CO<sub>2</sub>
  - CO<sub>2</sub>-molten salts or (helium, water)

Parameters for calculation:

- Diameter of the channel - 0.002 m
- Angle cluching channels -  $\alpha = 128^\circ$
- Length - 0.004 m
- The wall thickness - 0.0006 m
- The height of the tip of the channel - 0.0026 m
- The plate thickness - 0.0016 m
- Thermal conductivity of austenite - 50W / mK
- The thermal conductivity of titanium - 21W / mK



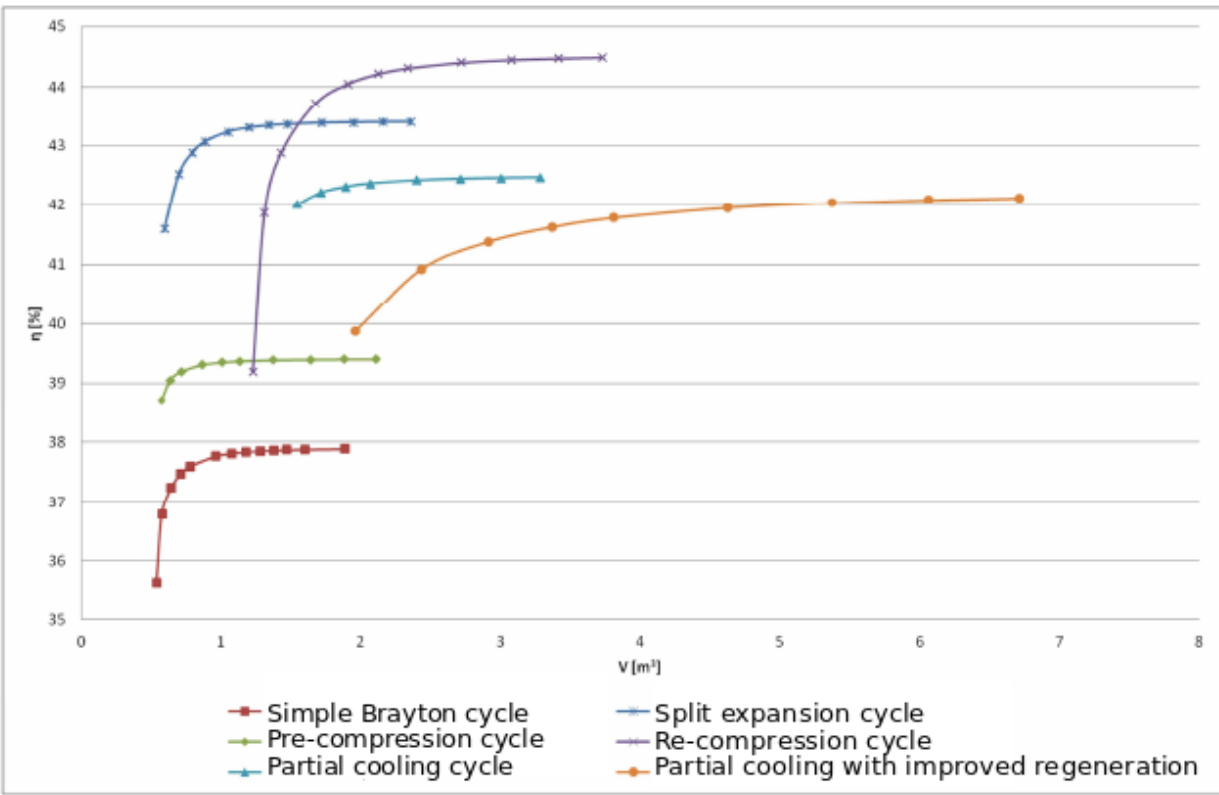


# Design of experimental loop

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The main goal:

- Determining the minimum number of heat exchangers
- The dependence of the total sum of the individual volumes of heat exchangers from basic layouts of cycles on their efficiency.

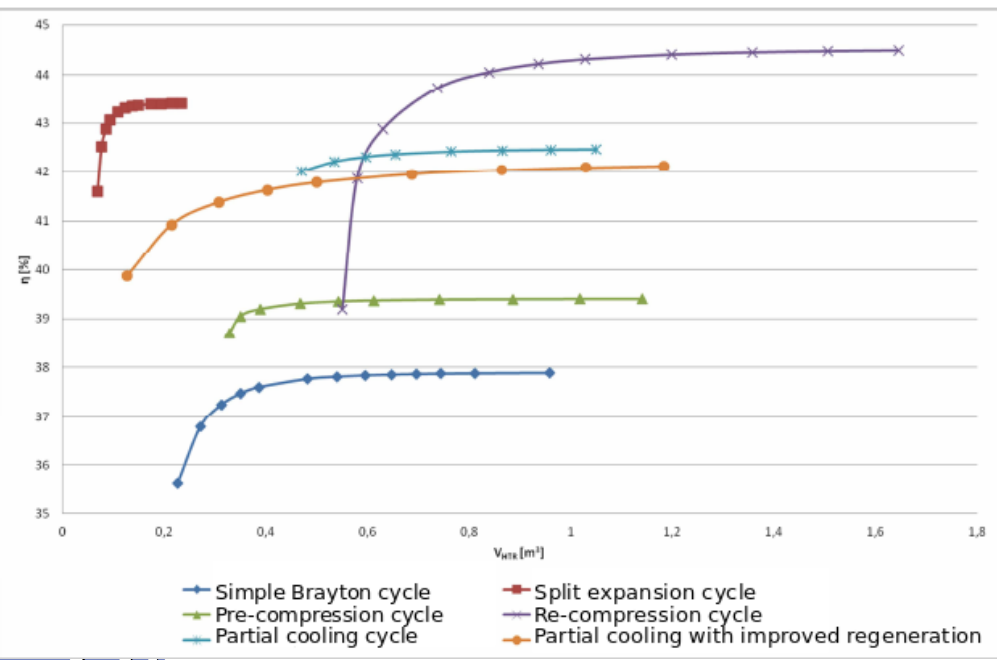


- Number of channels: 300 000

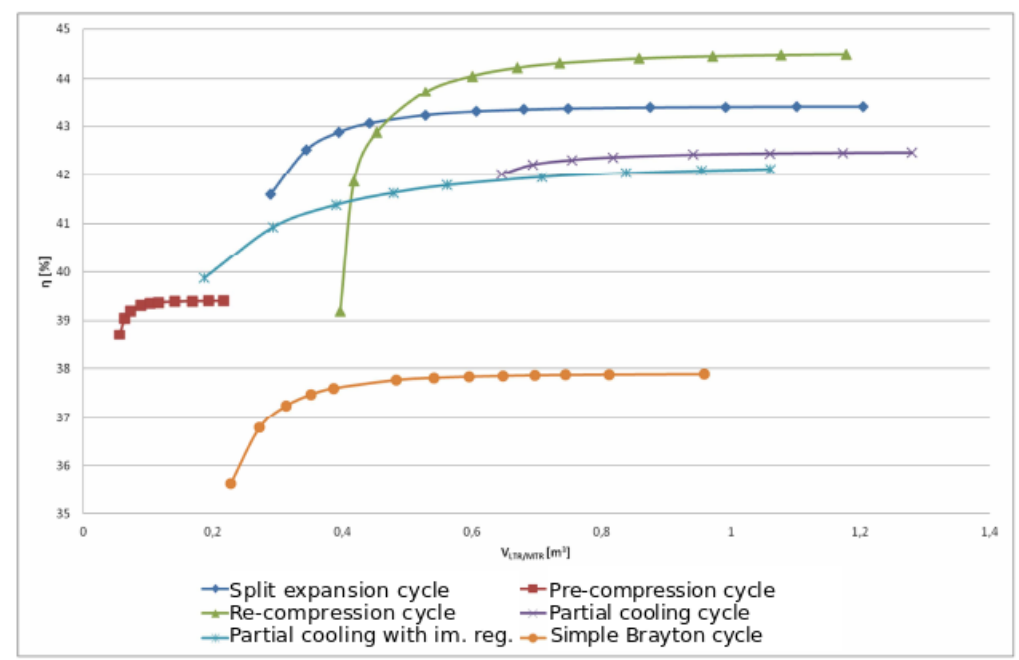
# The total volume of HTR/LTR



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The dependence of the cycle efficiency on the total volume of the HTR

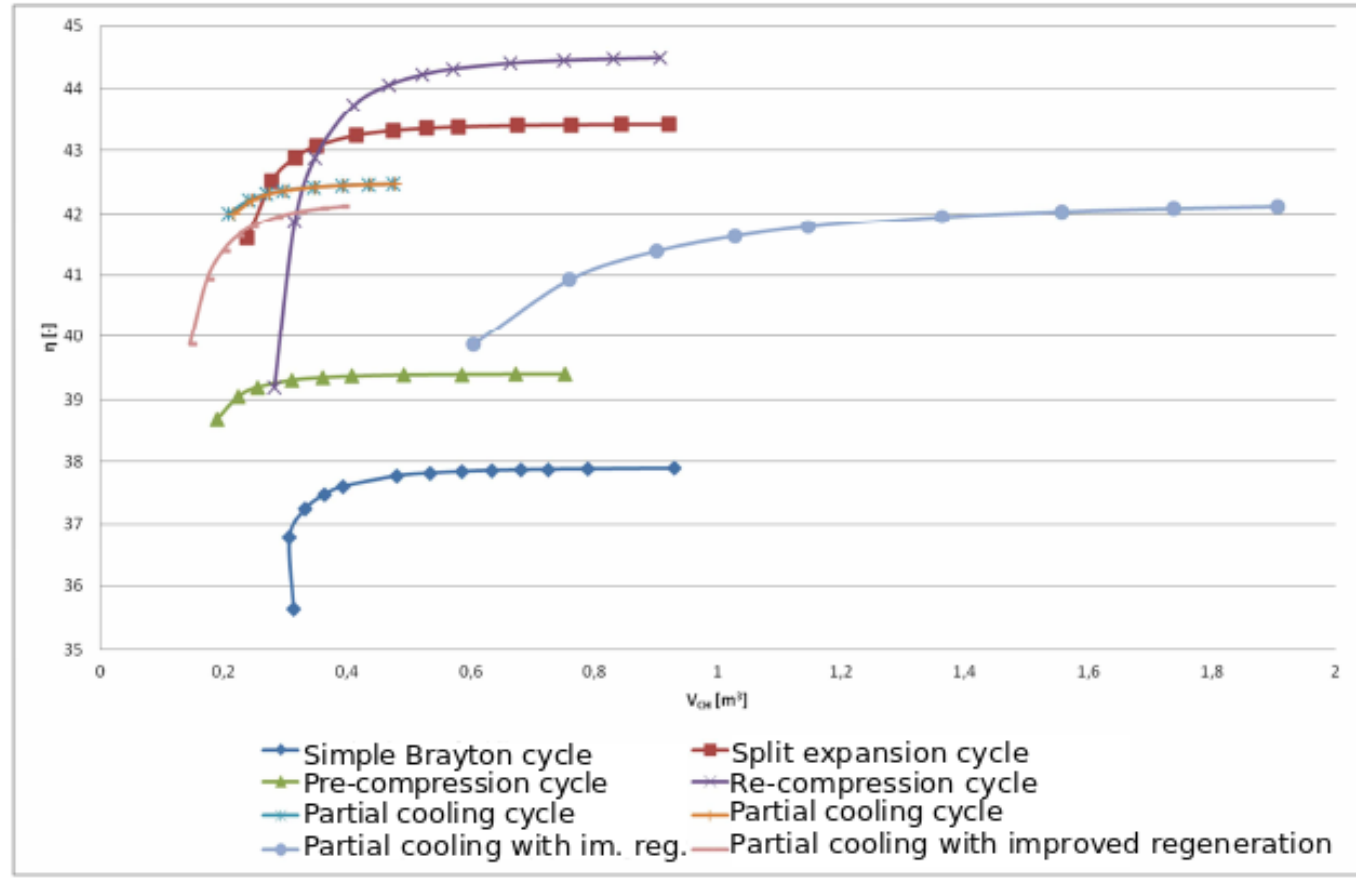


The dependence of the cycle efficiency on the total volume of the LTR

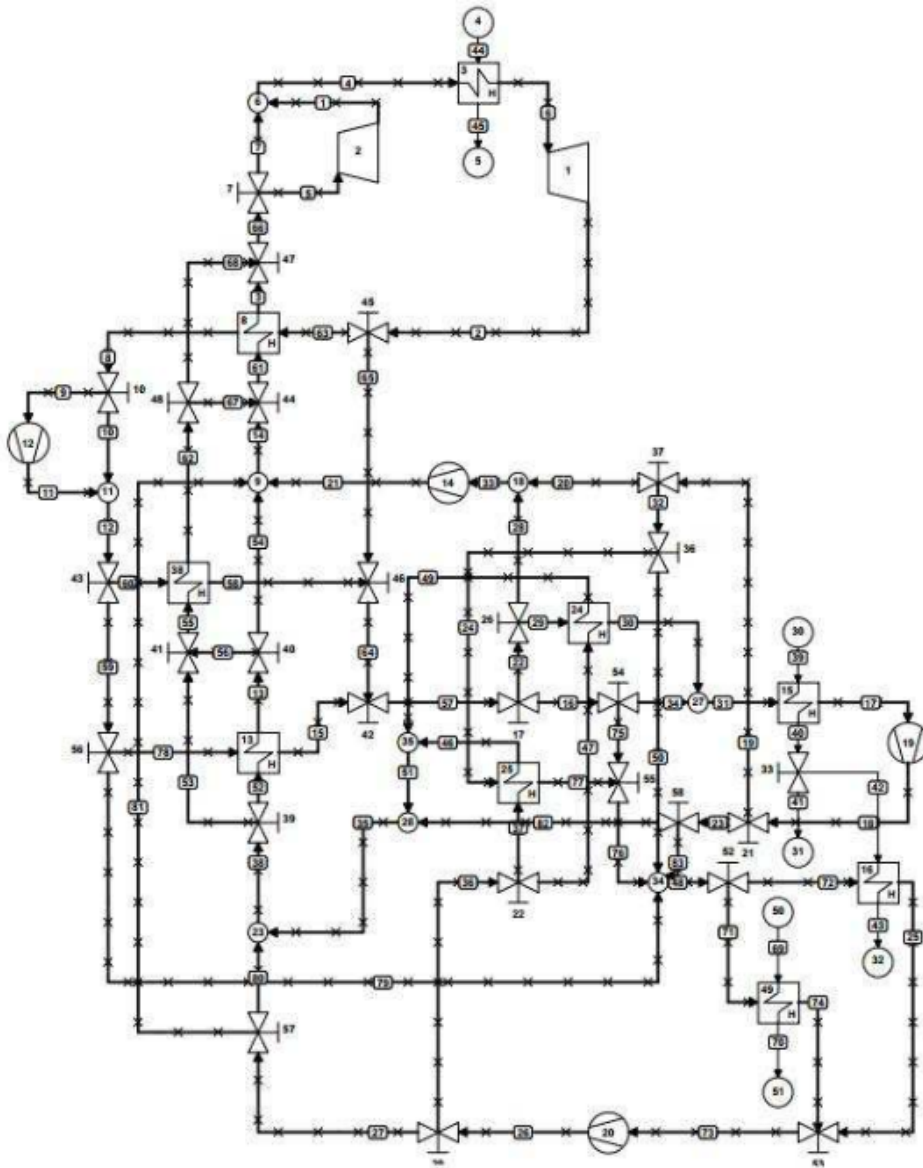
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# The total volume of cooler



# The layout of experimental loop



	Number in Figure	Volume [m3]
HEX no.1	8	0.95
HEX no.2	13	1
HEX no.3	38	0.23
HEX no.4	24	0.8
HEX no.5	25	1.43
Cooler no.1	49	0.93
Cooler no.2	15	0.45
Cooler no.3	16	0.39

	$\eta_{id}$ [%]	$\eta_r$ [%]	$\Delta$ [%]
Simple Brayton cycle	37.88	37.27	1.6
Re-compression cycle	43.41	42.56	1.9
Pre-compression cycle	39.4	38.9	1.2
Split expansion cycle	44.9	42.15	6.2
Partial cooling cycle	42.47	41.8	1.5
Partial cooling with improved regeneration	42.11	39.9	5.2

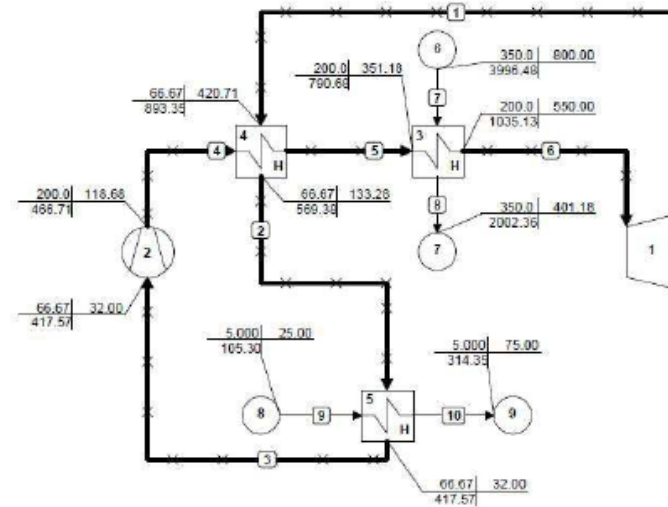
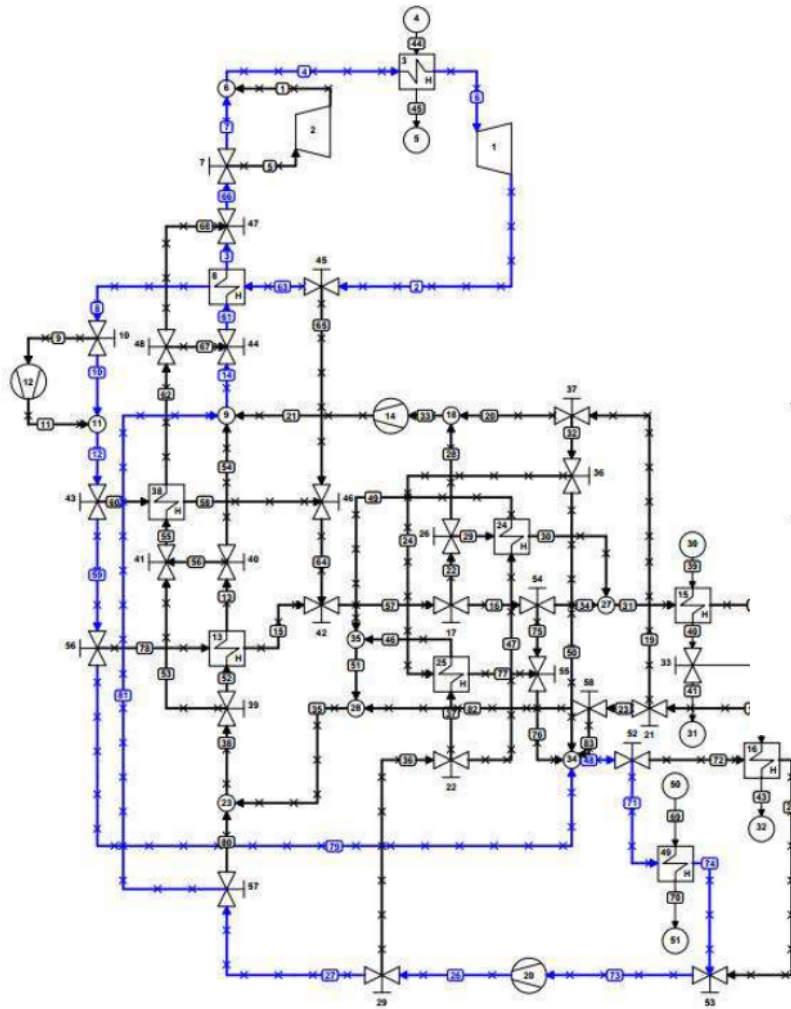
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# Simple Brayton cycle

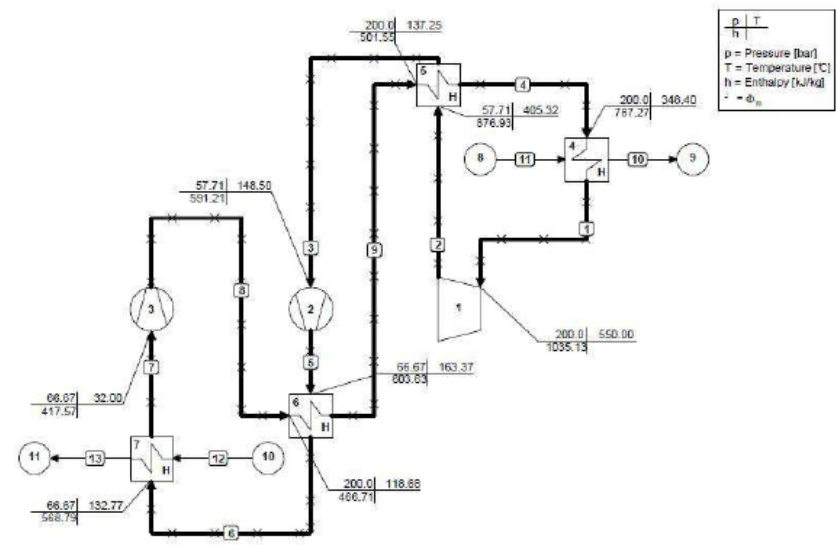
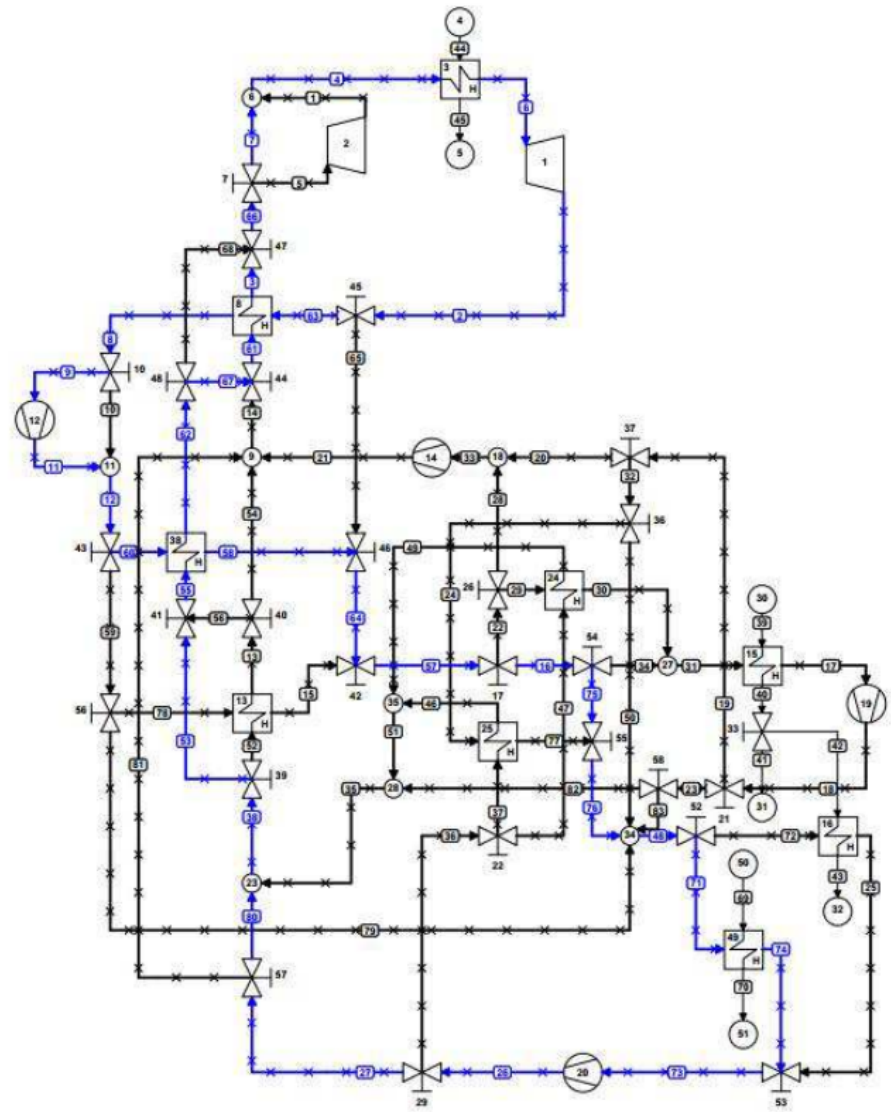


p	T
h	

p = Pressure [bar]  
T = Temperature [°C]  
h = Enthalpy [kJ/kg]  
 $\dot{Q} = \dot{q}_m$

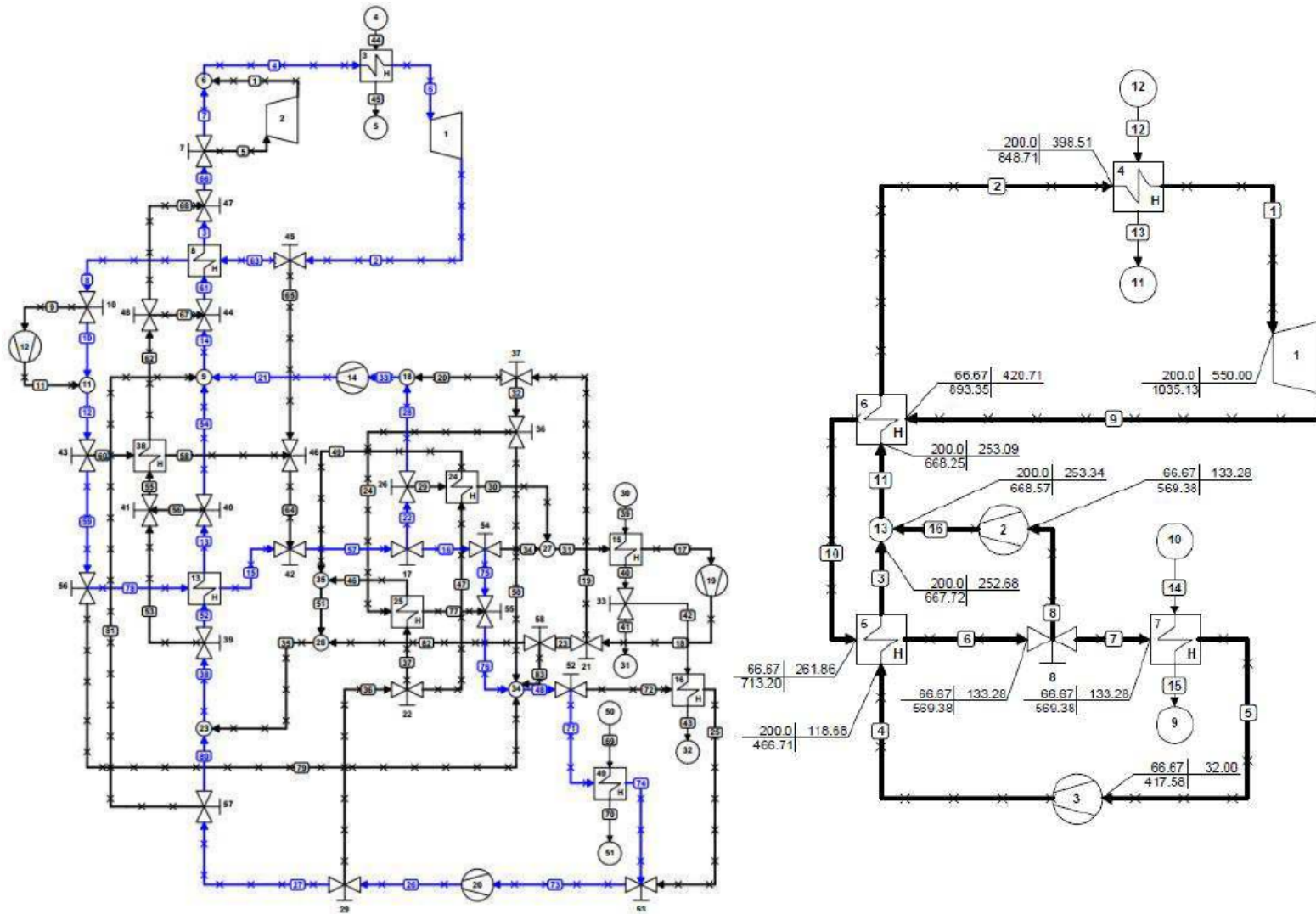


# Pre-compression cycle





# Re-compression cycle

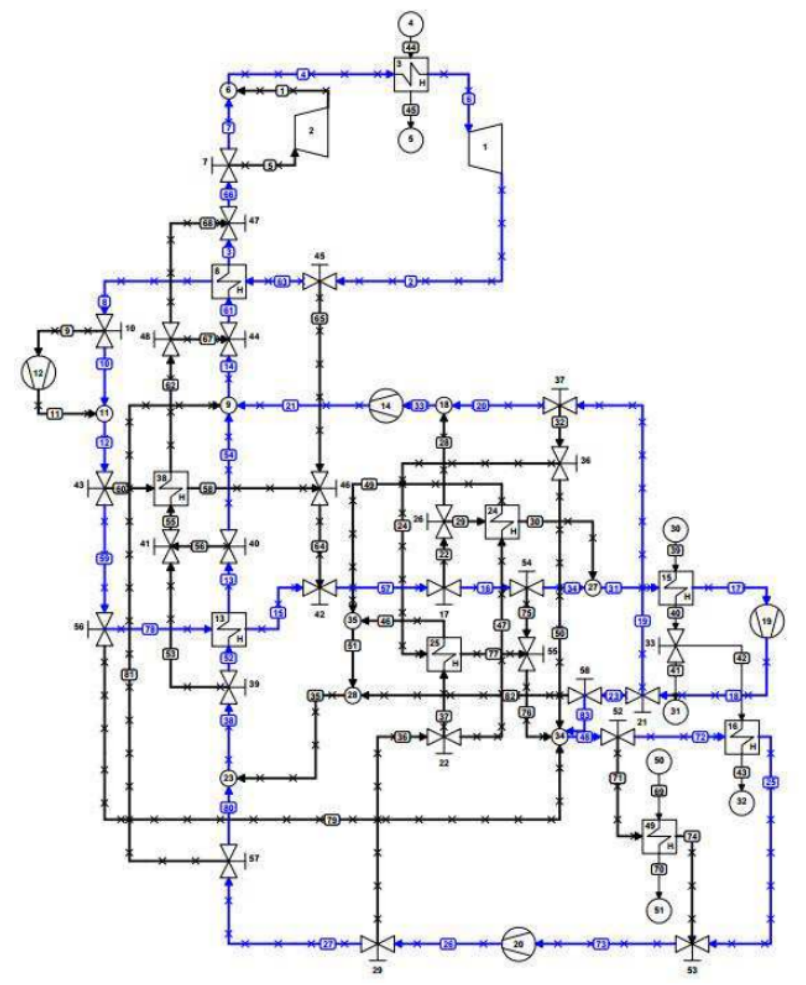
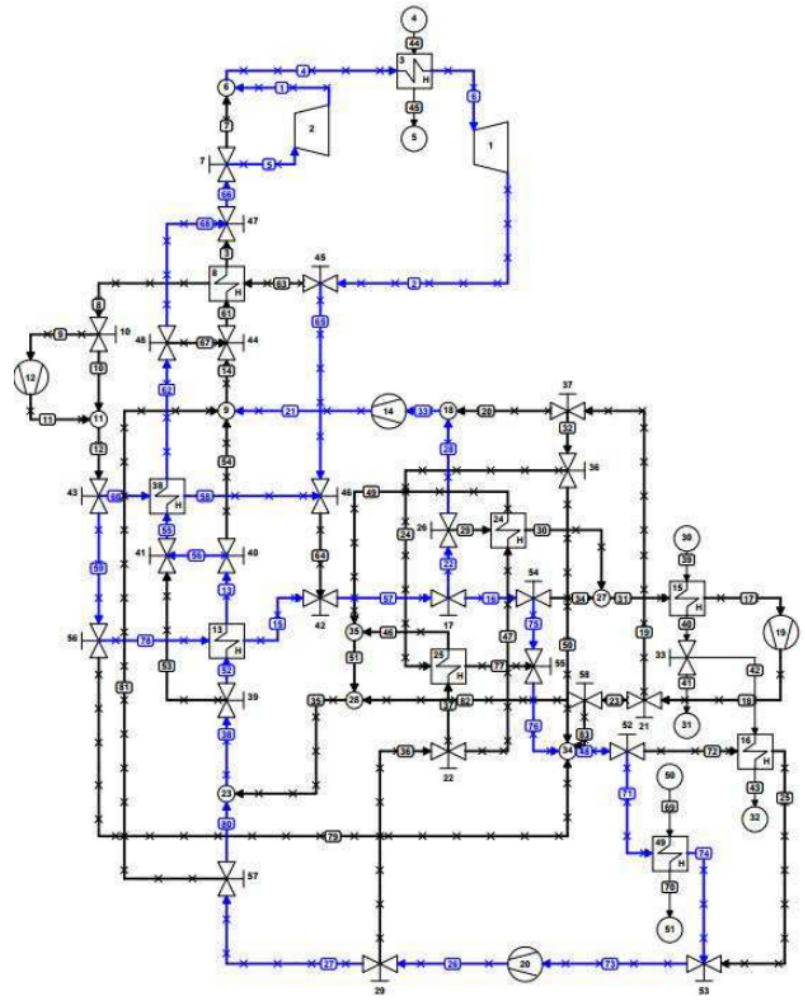


	p	T
h		

p - Pressure [bar]  
 T - Temperature [°C]  
 h - Enthalpy [kJ/kg]  
 j -  $\phi_m$

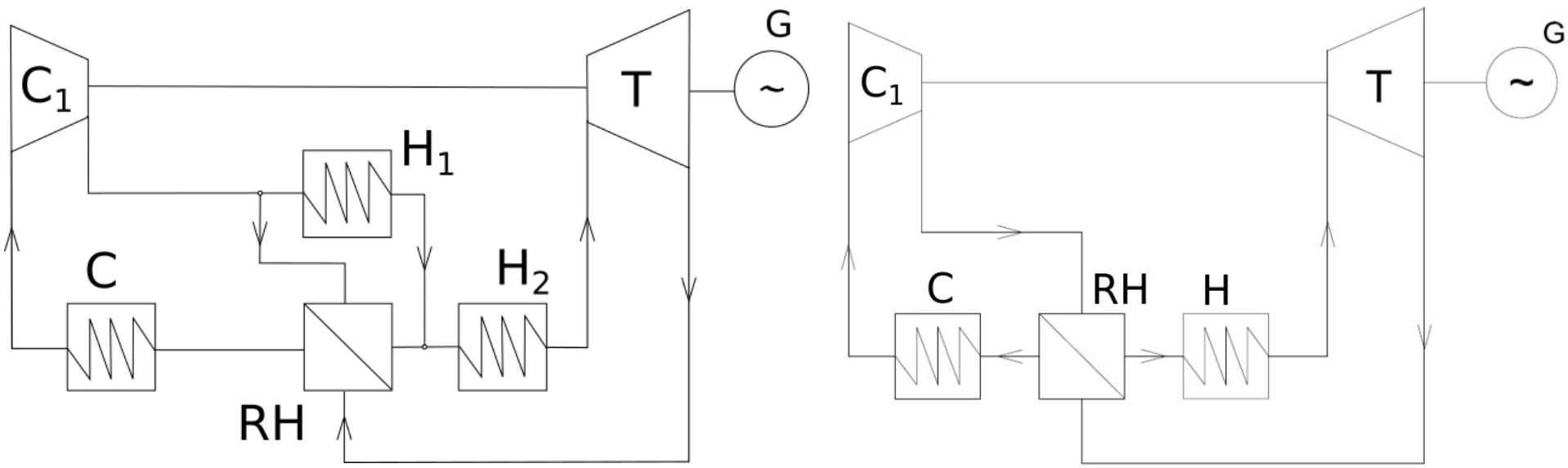


# Split expansion cycle Partial cooling cycle





# Waste heat recovery systems



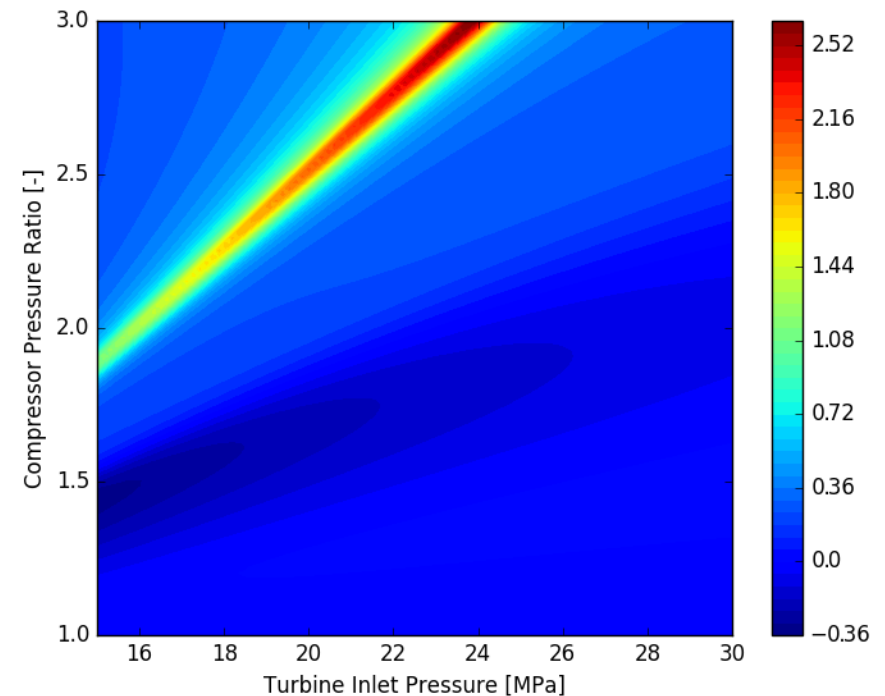
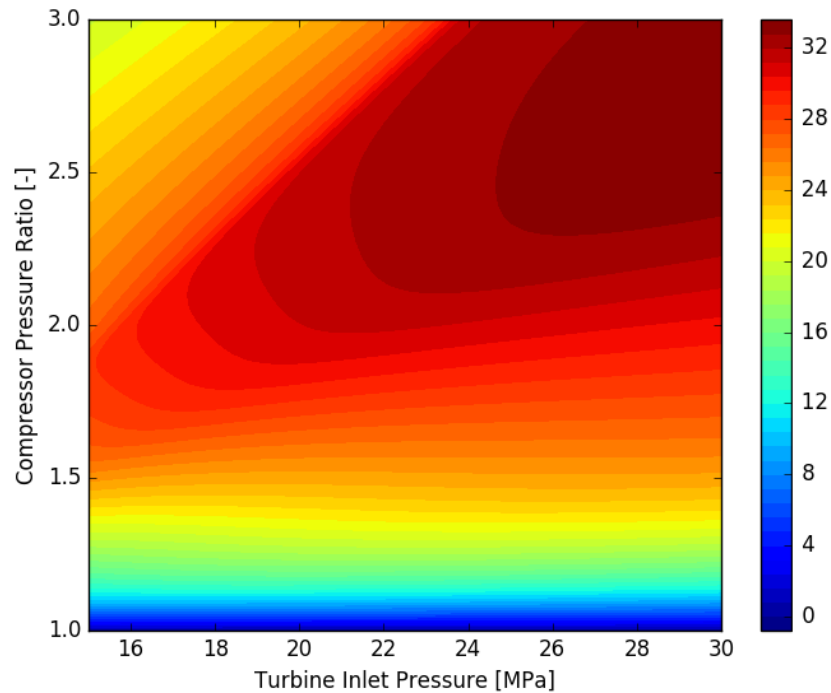
	Preheating C.	Simple C.	
Cycle efficiency	32.1	27	%
Net power output	9.8	6,9	MW
Compressor input power	3,1	2.9	MW
Turbine power output	12.9	9.8	MW



# Effect of mixture

The **maximum cycle efficiency** (pure CO<sub>2</sub>) - **33 %**.

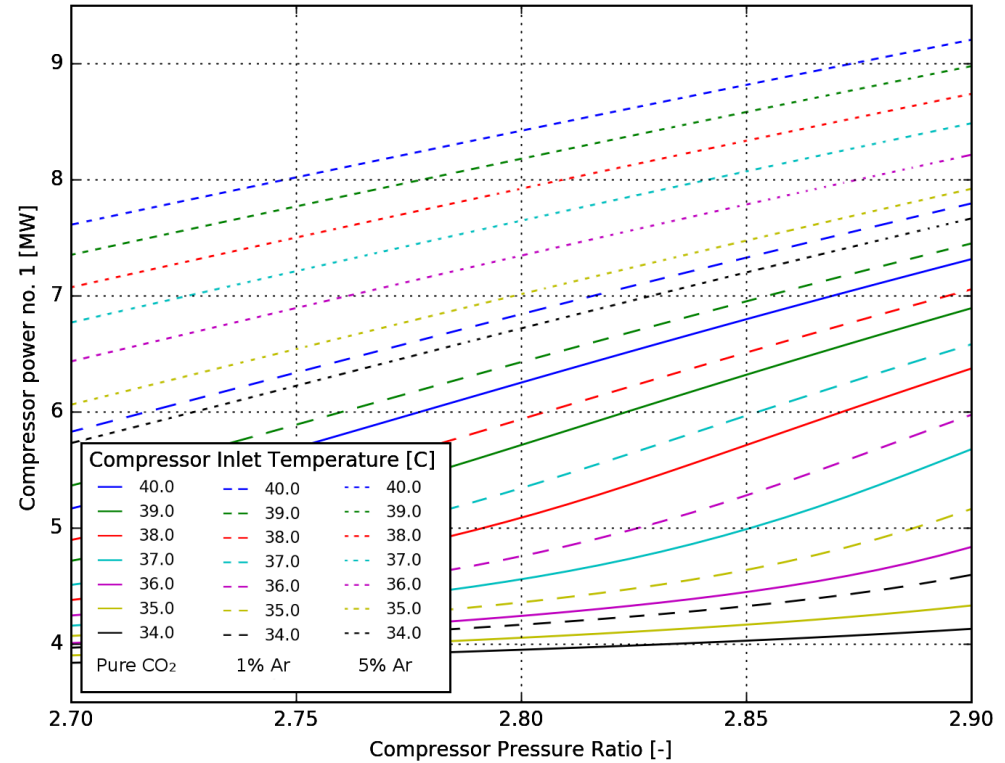
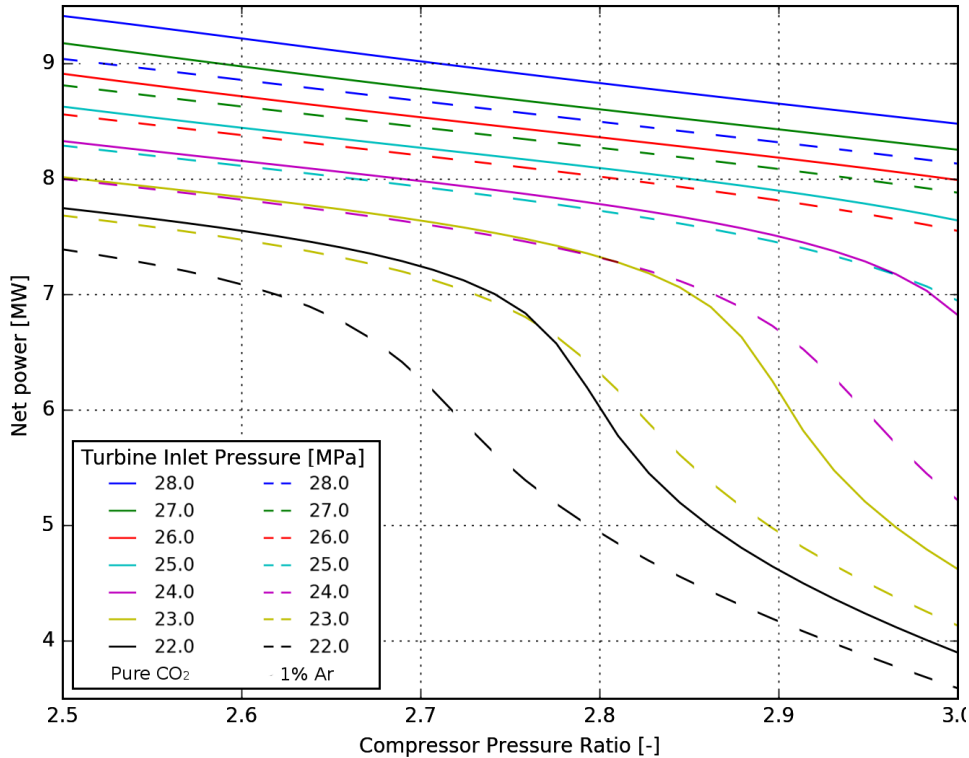
- The difference of cycle efficiency is up to 2.5 %.
- The results is for 0.01 mole fraction of secondary substance.
- Results are for mixture CO<sub>2</sub> – Ar.



Vesely L., Dostal V., Stepanek J., Effect of Gaseous Admixtures on Cycles with Supercritical Carbon Dioxide, 2016: Proceedings of ASME TurboExpo 2016: Turbomachinery Technical Conference and Exposition.



# Effect of mixture



Vesely L., Dostal V., Stepanek J., Effect of Gaseous Admixtures on Cycles with Supercritical Carbon Dioxide, 2016: Proceedings of ASME TurboExpo 2016: Turbomachinery Technical Conference and Exposition.



# Thanks for your attention

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