

Commercialization of Supercritical CO₂ (sCO₂) Power Cycles

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Echogen Power Systems



Founded 2007

Mission:

Commercialization of
sCO₂ power cycles

Designed, fabricated
and tested only MW-
scale sCO₂ power cycle



Echogen leads the industry in sCO₂ power cycle development



15KW Lab system



EPS100 – 8 MW



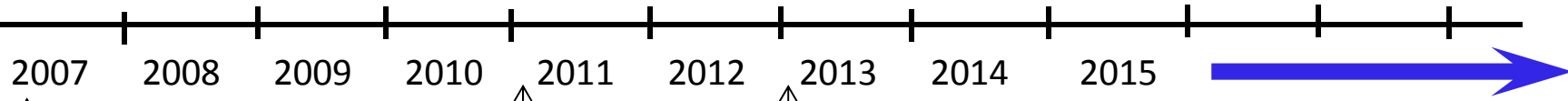
5KW Lab system



250 KW Pilot system



EPS30M – 1.5MW marine



Initial funding

DRESSER-RAND
SIEMENS

GE Marine

Echogen Power Systems

Commercialization of sCO₂ power cycles

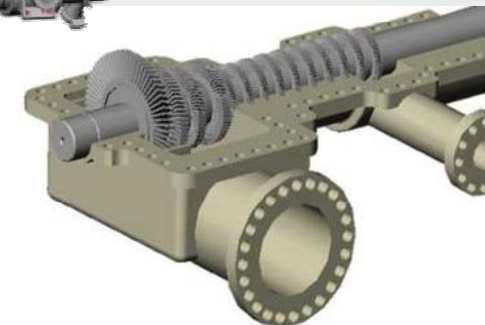
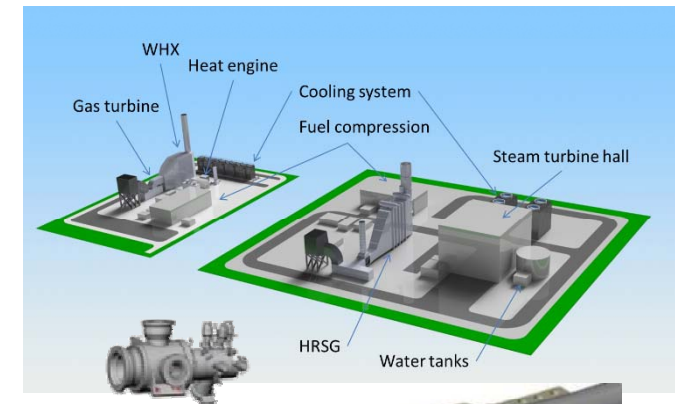
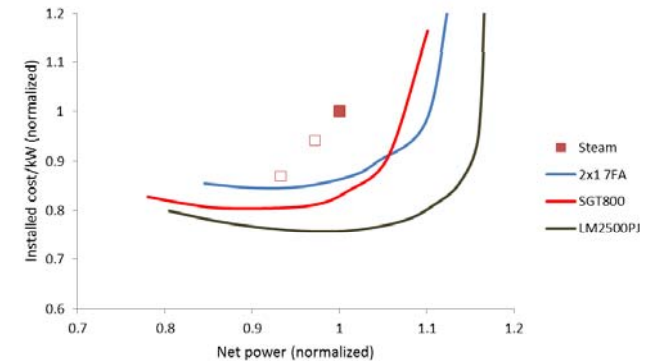


- Challenges and obstacles
 - Reluctance to assume risk of a new technology
 - First-of-a-kind costs vs 100-year-old technology
 - Current low energy costs unfavorable to investment in efficiency
 - Fear of the unknown...

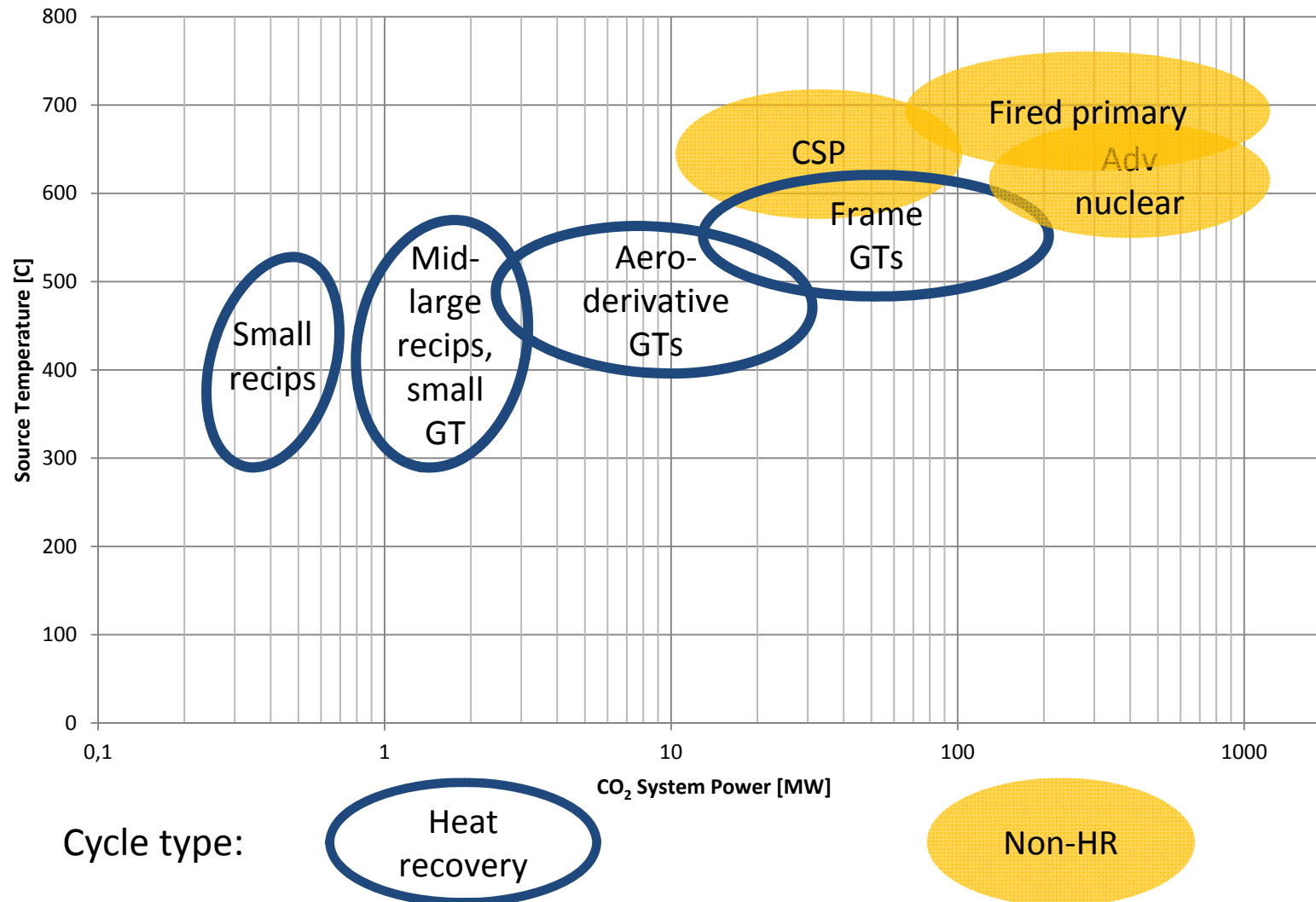
Commercialization of sCO₂ power cycles



- Opportunities and value proposition
 - Higher efficiency at lower cost (or some combination thereof)
 - Physical size / footprint
 - Startup and turndown capability
 - Air-cooled = zero water power plant
 - O&M cost
 - Reliability & availability



The application space



HR vs non-HR cycles



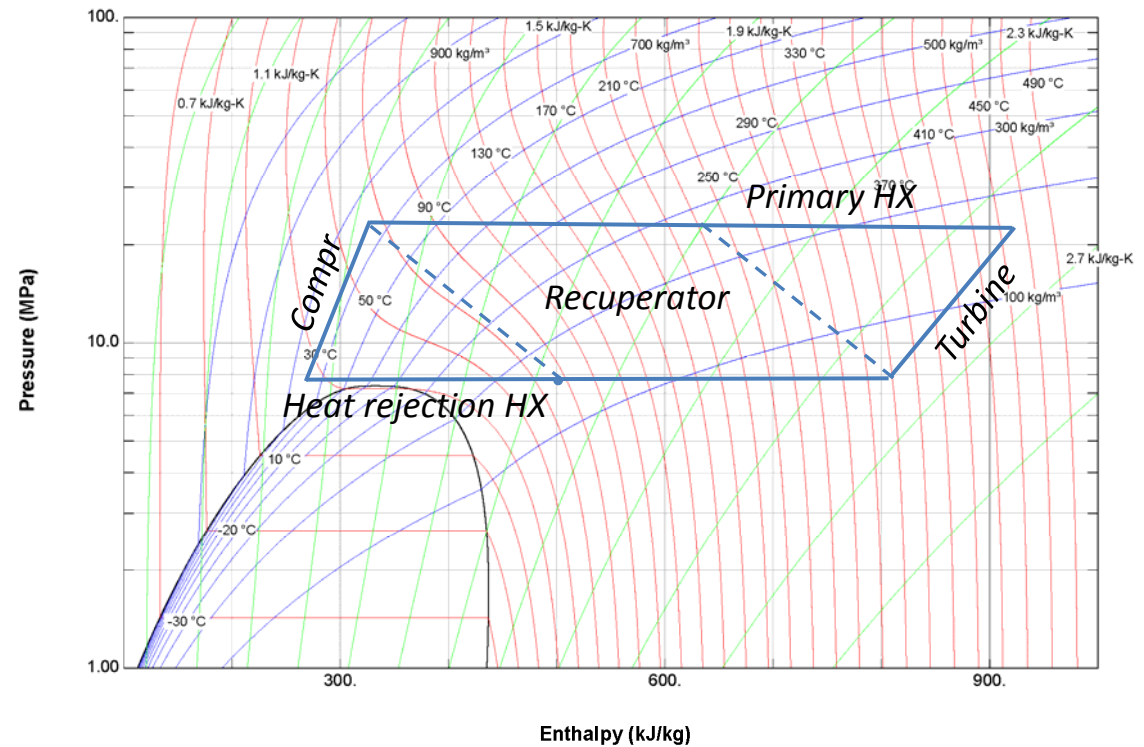
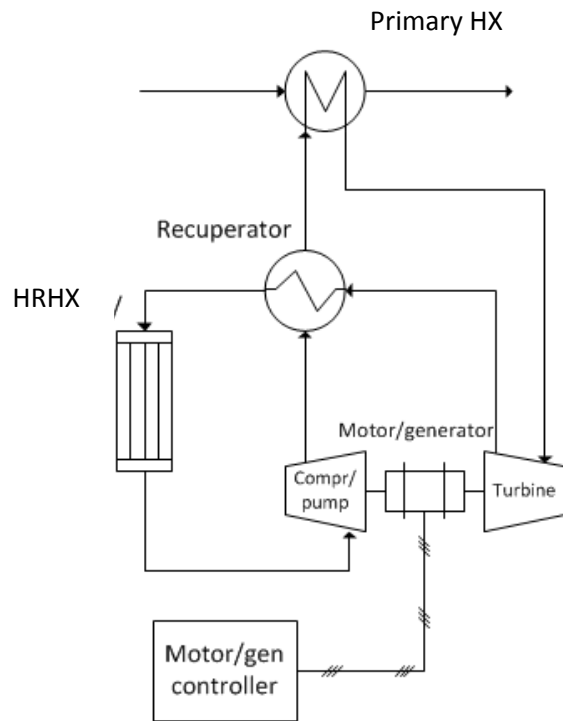
- Heat recovery cycle
 - GT exhaust is a classic example
 - Heat source is non-recycled – any heat not recovered by the power cycle is lost
 - Primary metric is power output for a given application
 - Goal is to maximize both recovered heat and recuperated heat simultaneously

HR vs non-HR cycles



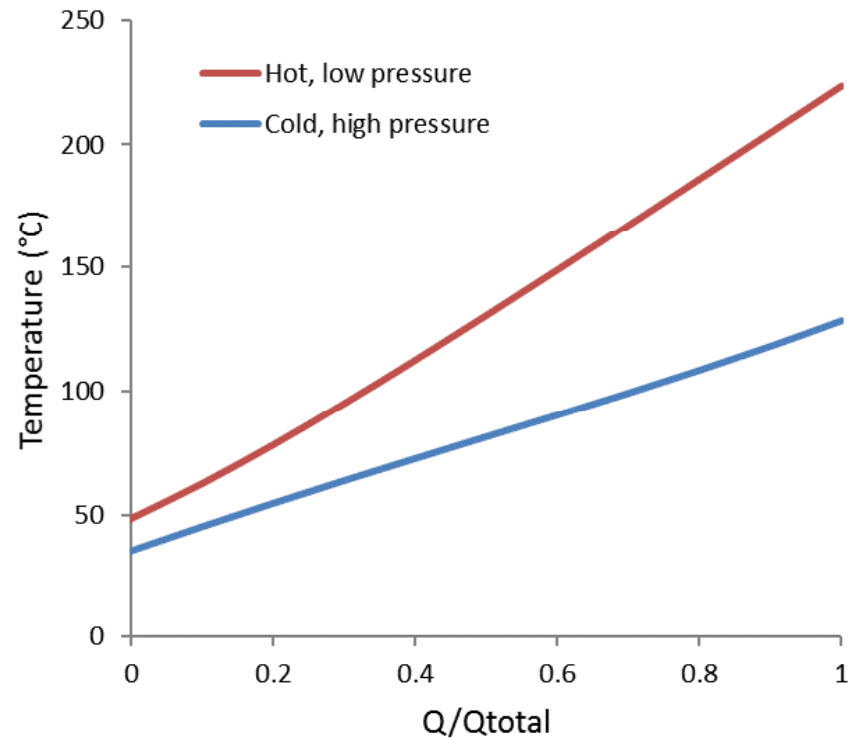
- “non-Heat recovery” cycle (a.k.a. “recompression” cycle)
 - Advanced nuclear power is a classic example
 - Heat source is fully recycled
 - Primary metric is efficiency
 - Goal is to approximate a Carnot cycle – heat addition at very small temperature differential
 - “In-between” applications – e.g. CSP with thermal storage

Simple recuperated cycle – somewhere in the middle ground



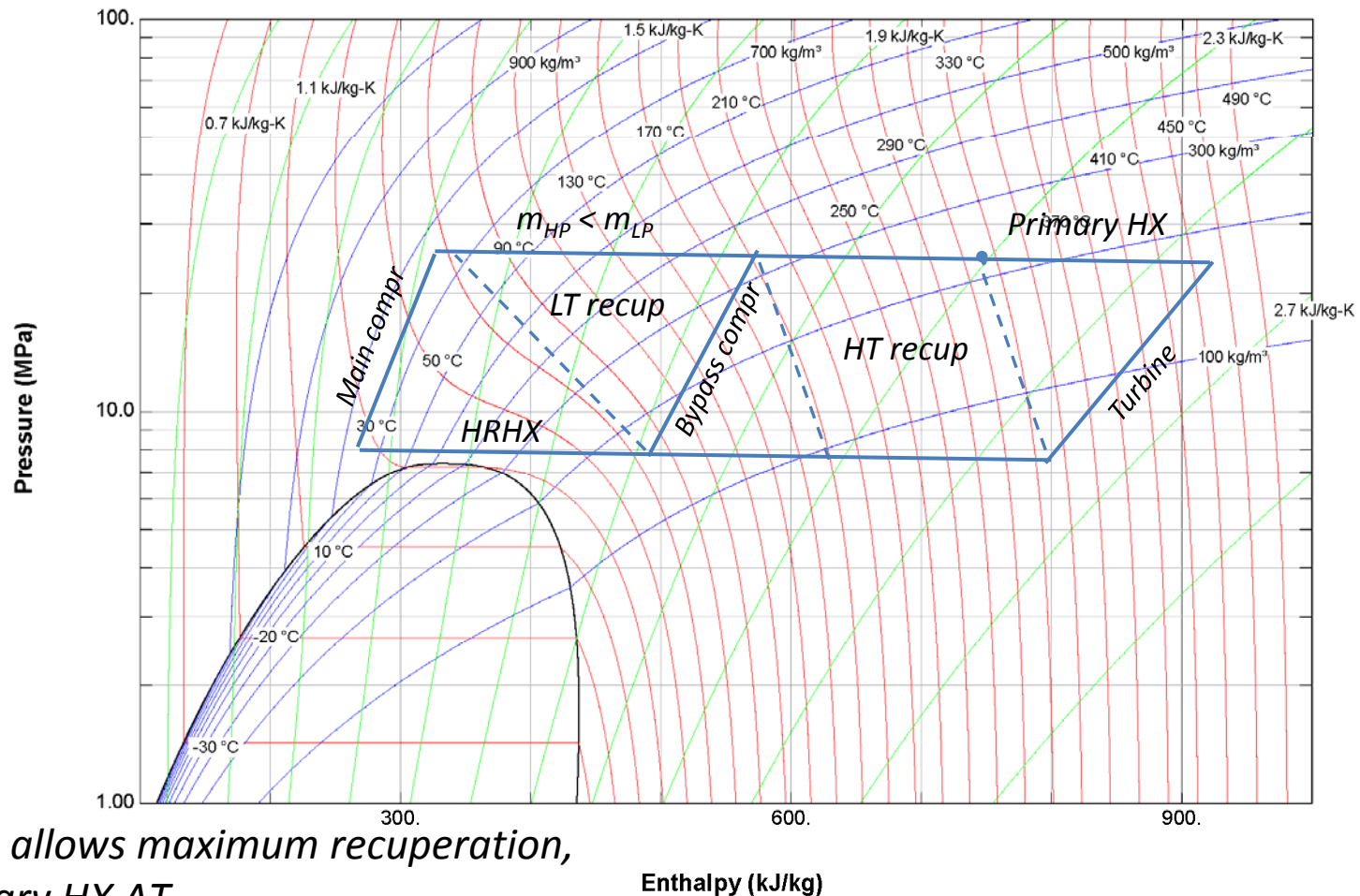
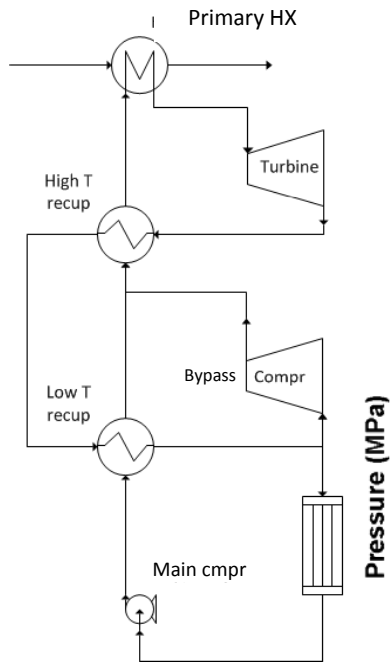
Minimum temperature in primary HX too high for heat recovery, too low for good Carnot efficiency

Recuperator characteristics



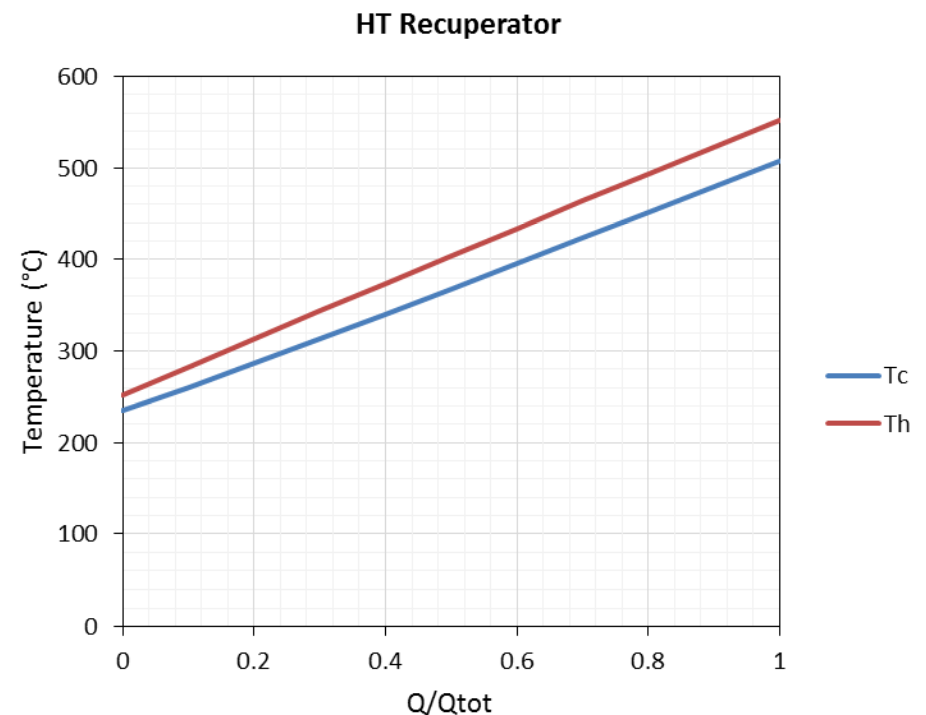
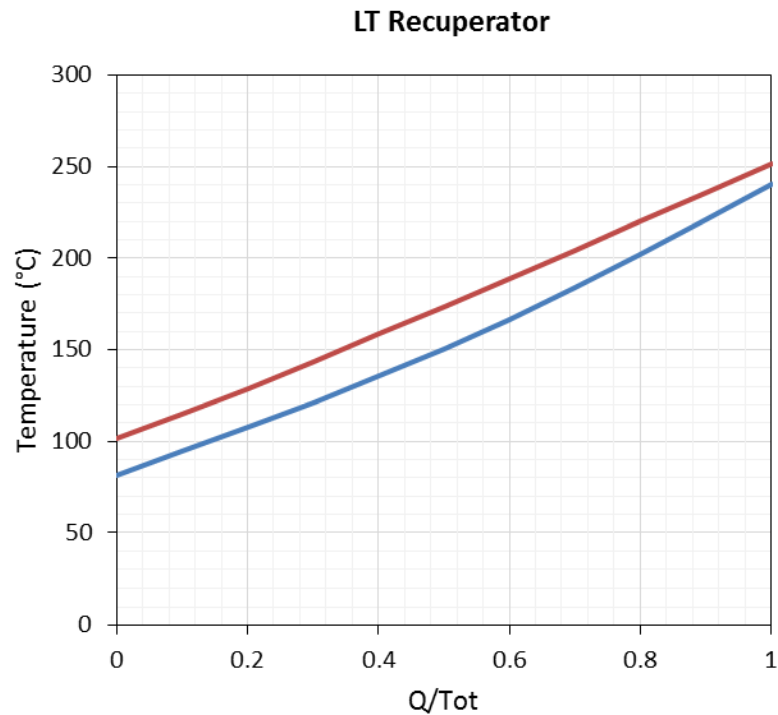
- Simple recuperated cycle – recuperator “pinches” at low-temperature end
- Consequence of large c_p mismatch between high-pressure and low-pressure CO_2 , equal mass flows
- Large exergy destruction with temperature glide mismatch

“Recompression” (LT recup bypass) cycle maximizes avg PHX temperature



*LT recup bypass allows maximum recuperation,
minimizes primary HX ΔT*

Recuperator characteristics

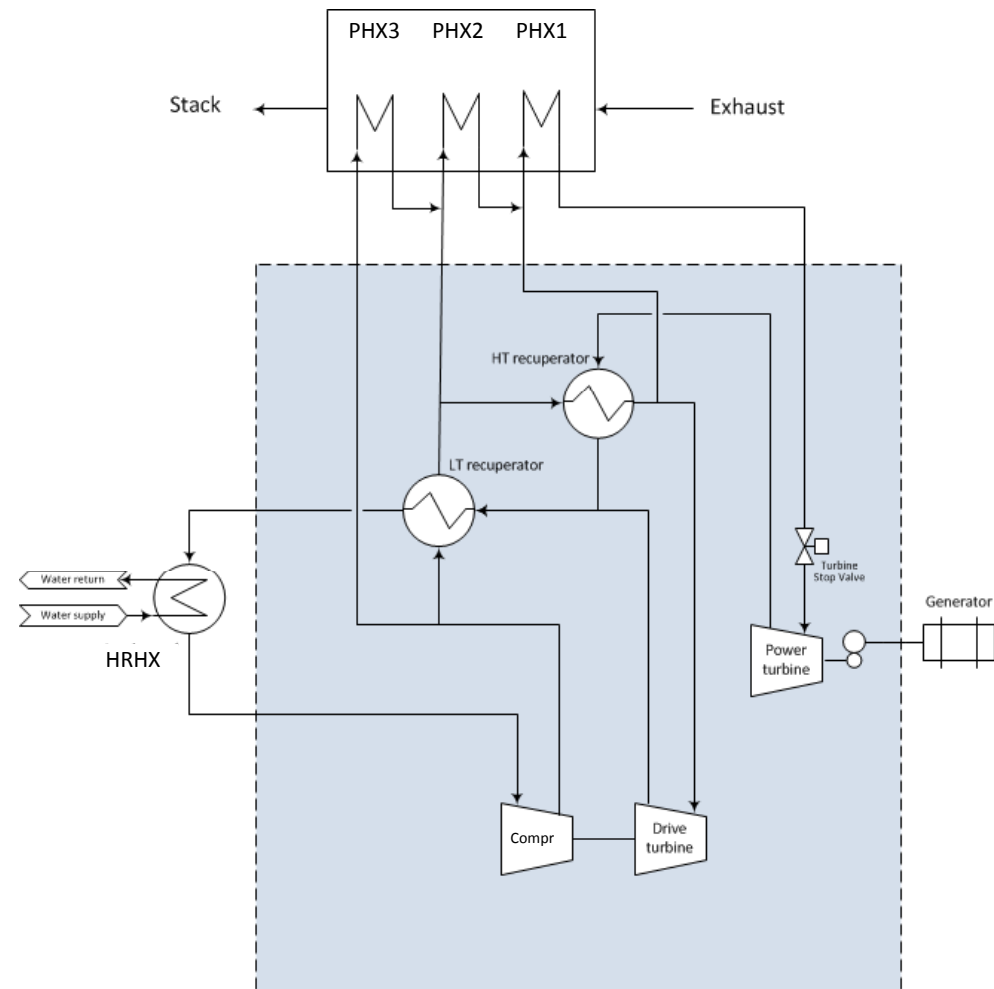


- Cycle optimization drives C_r (C_{\min}/C_{\max}) toward 1
- Equal slope minimizes exergy destruction
- However, equal slope also implies large UA

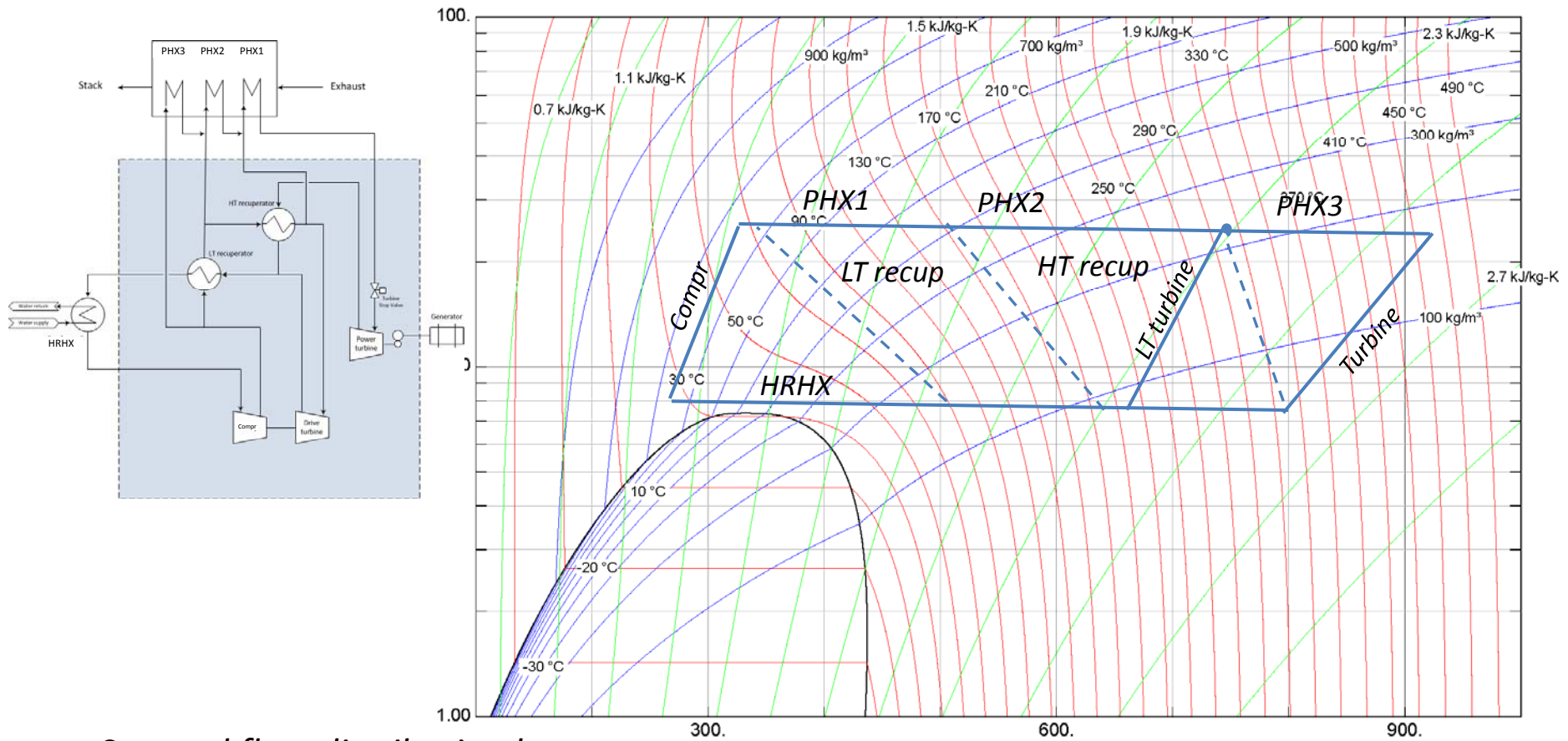
Heat recovery cycle



- “Dual rail” cycle
 - Patent pending
 - Sequence of heat additions via “recuperation rail” and “primary heat exchanger rail”
- Key characteristics:
 - Primary heat transfer over a wide range of temperatures
 - Variable flow splits as progress down primary heat exchanger, matches mc_p of exhaust stream
 - Dual turbines

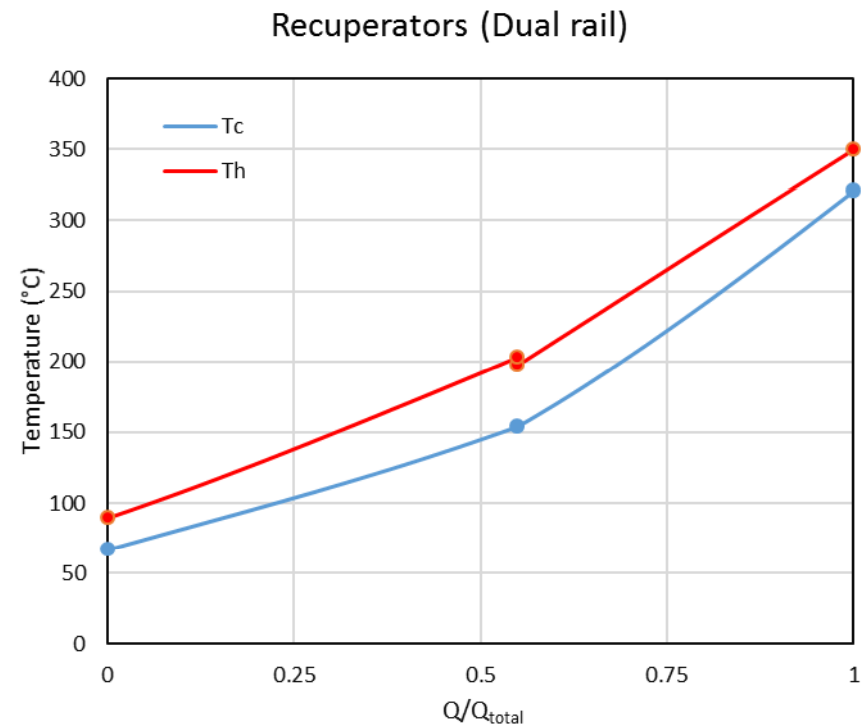
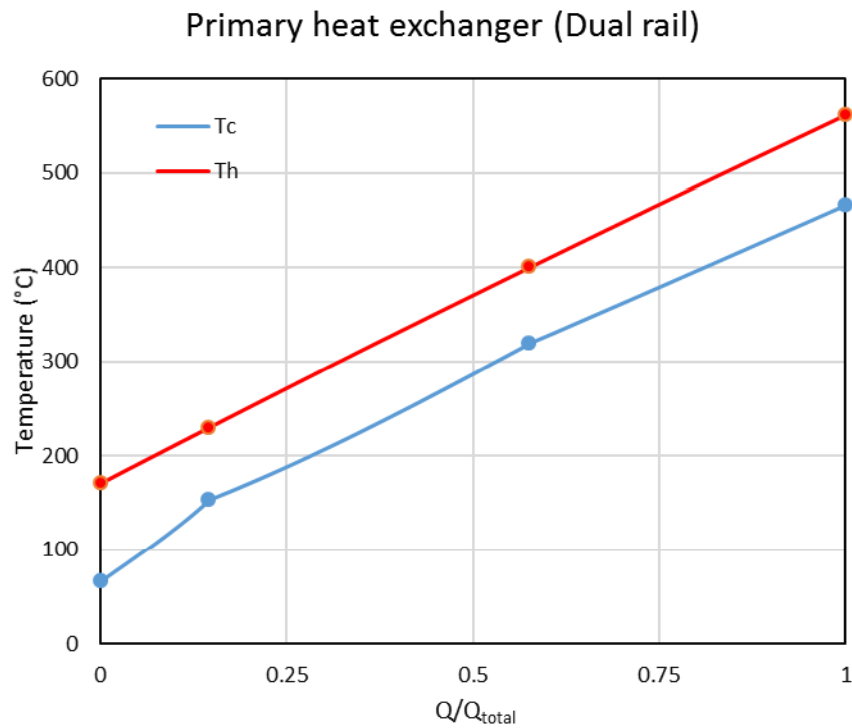


Dual rail cycle maximizes combined utilization of external and internal (recuperated) heat



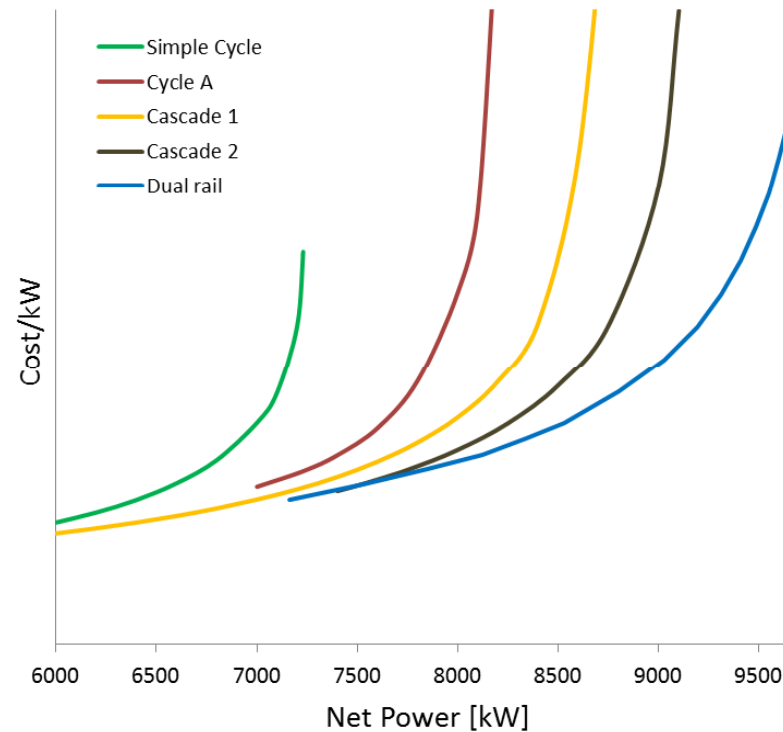
Stepped flow distribution between recuperator path and PHX path allows better mc_p matching

Heat recovery primary heat exchanger



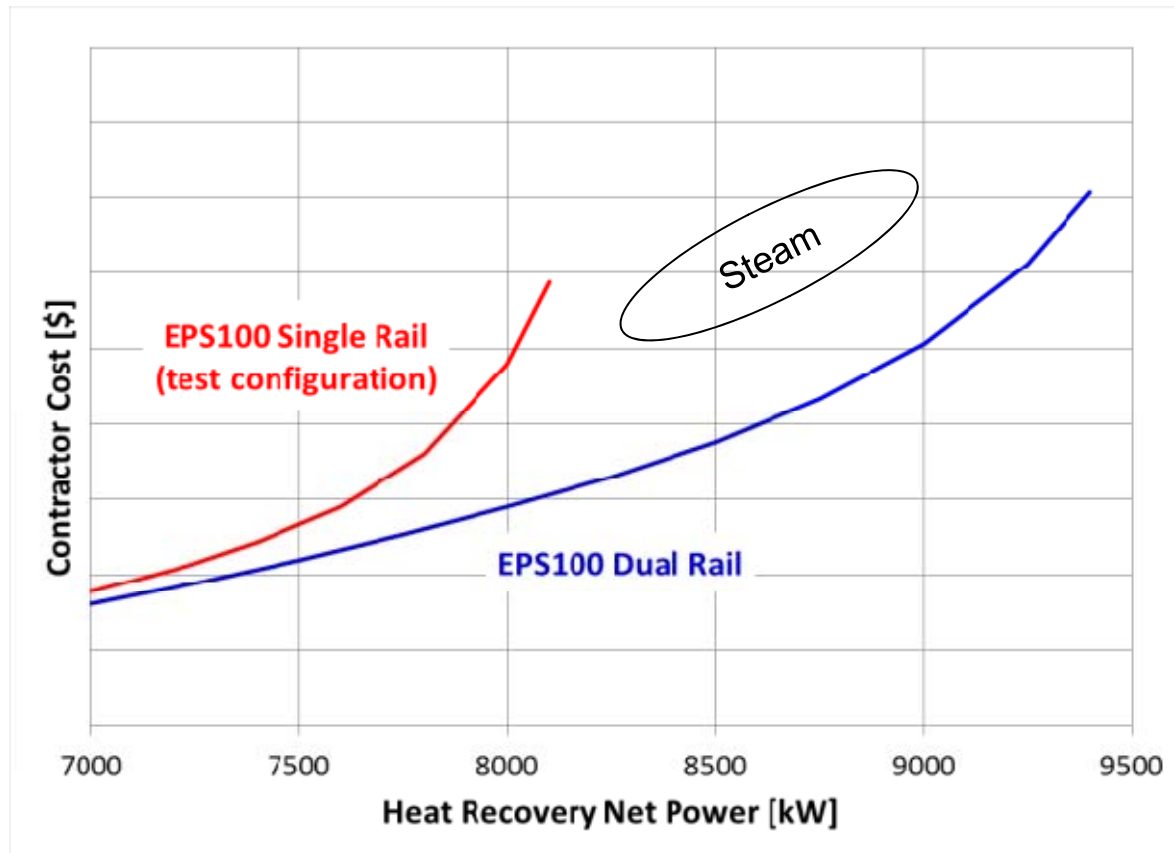
- Optimization drives flow splits and heat exchanger UAs towards equal temperature glide

Cycle / cost modeling



- Optimization process defines cycle with minimum cost for given power output
- Multiple solutions generates curves of cost vs power
- Allows selection of optimal cycle architecture

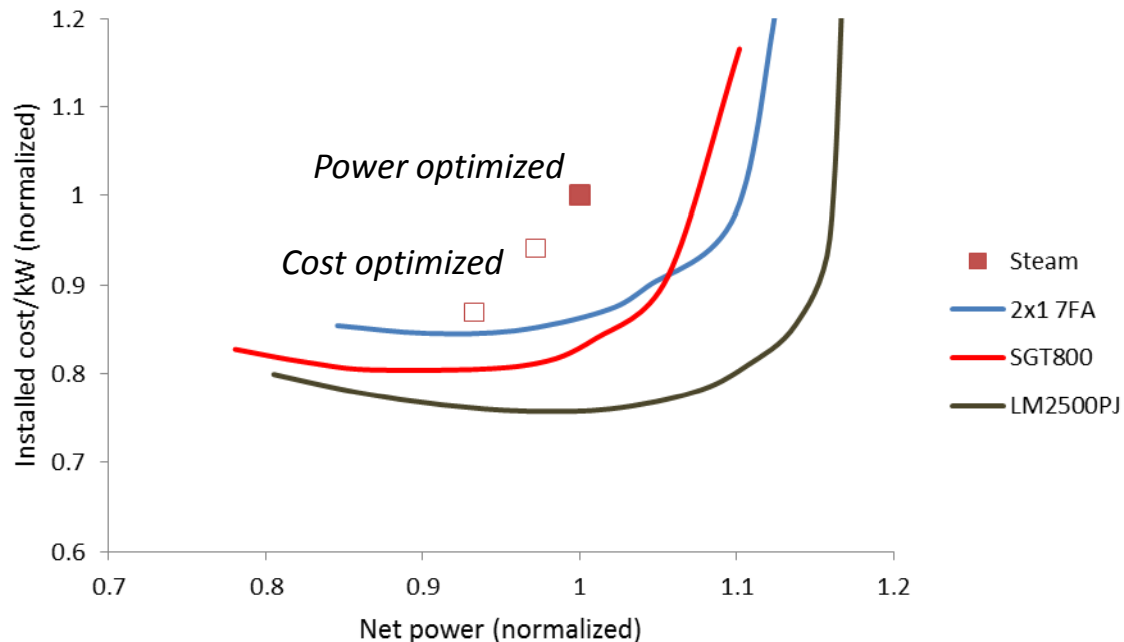
Continued sCO₂ Cycle Improvements



- Comparison of sCO₂ cycles
 - EPS100 (patents pending)
 - Dual Rail (patents pending)
- Current design of EPS100 at 7.3 MW net
- Dual rail cycle offers substantial improvement in performance, outperforms steam at a lower cost

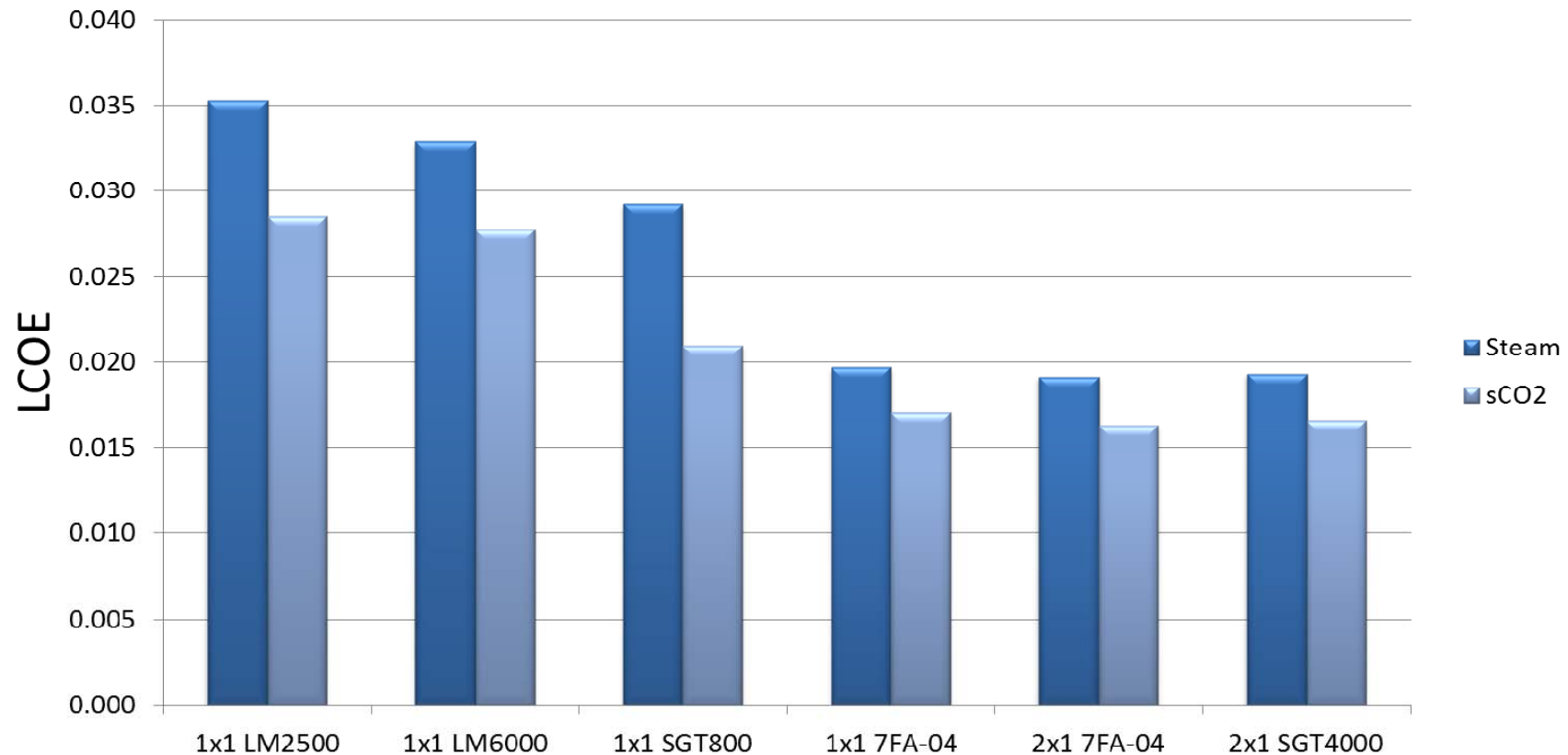
Echogen sCO₂
= lower CAPEX & lower Levelized Cost of Electricity

sCO₂ vs steam – GTCC applications



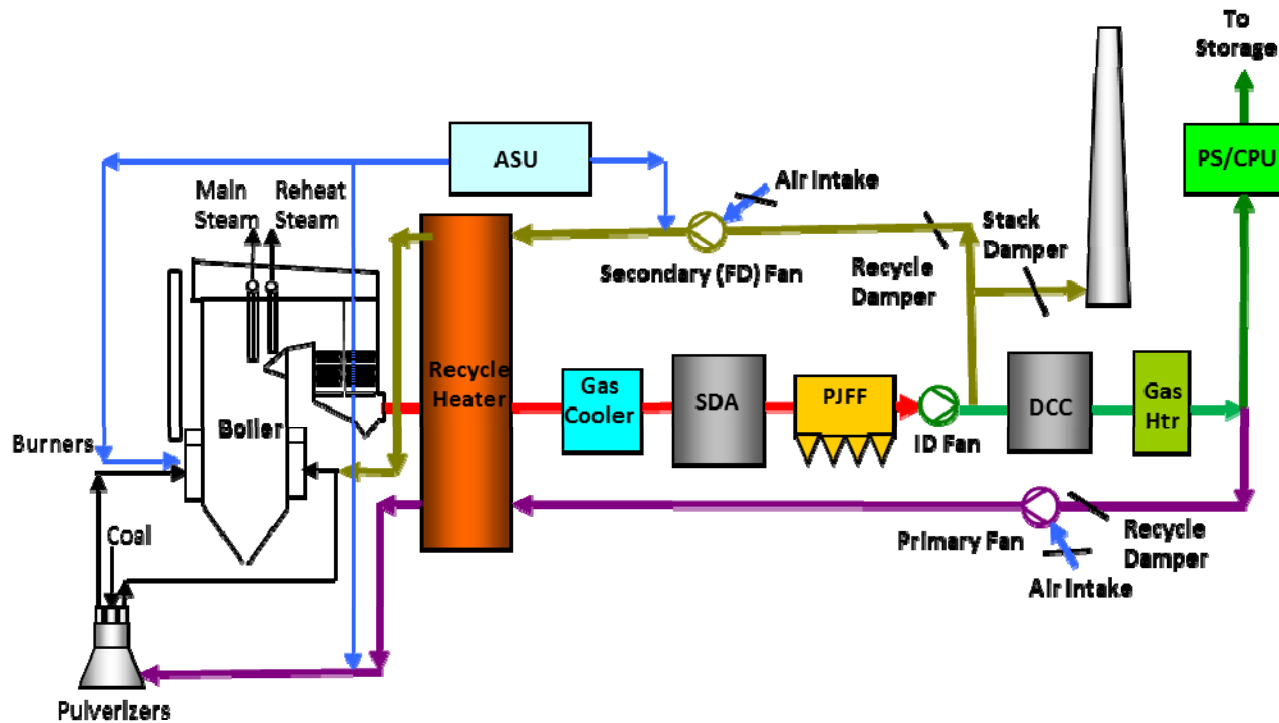
- Normalized to steam power & cost from GT-Pro, “power-optimized” solutions (“cost-optimized” point shown for reference)
- Same exhaust and boundary conditions used for sCO₂
- 10-20% lower cost for same power
- 7-14% higher power for same cost

LCOE – GTCC applications



- Case studies covering 30-800+MW
- Bottoming cycle LCOE consistently lower with sCO₂

Primary power applications



- EPRI-led oxy-coal sCO₂ integration study
- Comparisons to baseline steam cases

sCO₂ – Steam Power Cycle Comparison

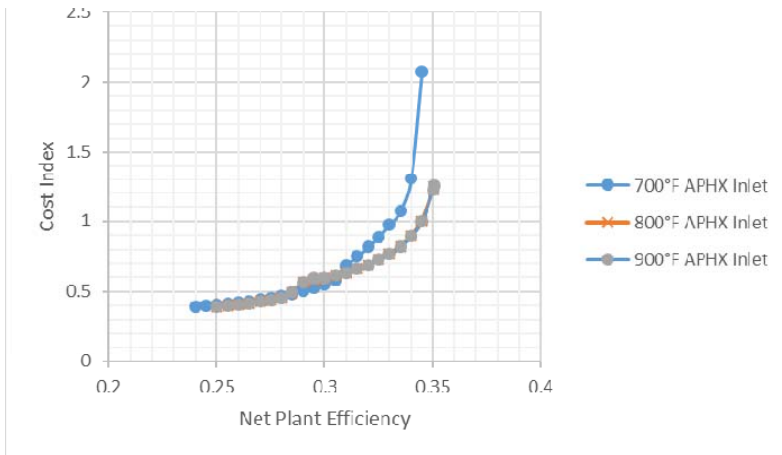


- Purpose / Goals:
 - Develop power plant process designs that optimally integrate sCO₂ power cycles with oxy-fired coal heaters for comparison to advanced steam cycles
- Method
 - Performance optimization of sCO₂ cycles
 - Varied cycle architectures, cooling sources, power cycle heat exchanger sizes and pressure drops
- Approach
 - System economics within sCO₂ cycle also optimized
 - Heat exchanger cost sensitive to thermal size “UA” and pressure drop.
 - Optimize sCO₂ cycle heat exchanger cost (recuperators and coolers) versus net cycle efficiency
 - Combinations and variants of cascade and recompression cycles— including architectures with multiple compression steps and reheat— were considered

sCO₂ Power Cycle - Effect of Air Preheater Inlet Temperature



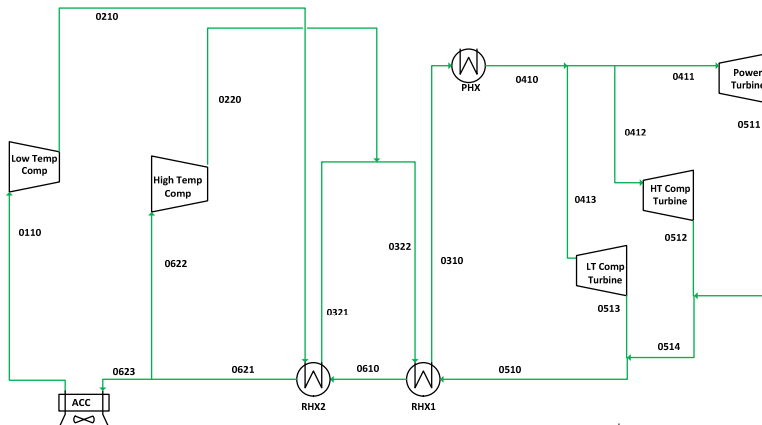
550 MW – Effects of Air Preheat Inlet Temp Case 1:



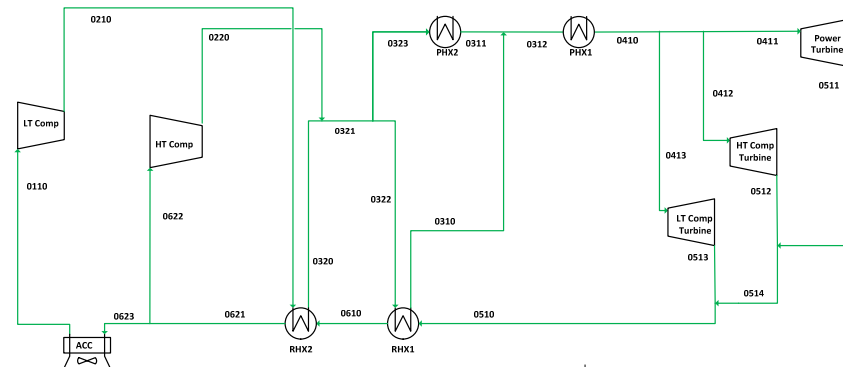
Result:

- Positive effect of air preheater inlet air temperature on cycle efficiency is limited by recuperation of sCO₂ cycle.
- For lower temperature application ($T_4 = 593^\circ\text{C}$)
 - Increasing air preheater inlet temperature above 427°C has little effect on cycle efficiency
- With the addition of low grade heat recovery cycle optimum cycle efficiencies can be achieved with lower air preheat inlet temperature (371°C)

Recompression Cycle:



Recompression Cycle – LG Heat Recovery



Steam – sCO₂ Power Cycle Comparison Summary

| Test Case | Power Turbine Inlet Condition | Net Gen (MW _e) | Gross Gen (Mwe) | Cycle Heat Input (MW _{th}) / Heater Efficiency | Net sCO ₂ Plant Efficiency (HHV) | sCO ₂ Cycle Efficiency | Baseline Steam Net Plant Efficiency | Baseline Steam Cycle Efficiency |
|-----------|-------------------------------|----------------------------|-----------------|--|---|-----------------------------------|--|---------------------------------|
| 1 | 593°C / 241 bar | 550 | 736.2 | 1407 / 88.3% | 34.5% | 52.3% | 31.0% | 47.0% |
| 2 | 730°C / 27.6 bar | 550 | 713.4 | 1295 / 88.3% | 37.5% | 57.2% | 35.0% | 50.6% |
| 3 | 593°C / 241 bar | 550 | 651.2 | 1286 / 90% | 38.5% | 50.6% | 35.8% | 46.9% |
| 4 | 730°C / 27.6 bar | 550 | 640.5 | 1151 / 90% | 43.0% | 55.6% | 41.0% | 52.3% |
| 5 | 593°C / 241 bar | 90 | 101.0 | 210 / 85.1% | 36.5% | 48.1% | 33.0% (538°C/107 bar no reheat, no CO ₂ capture) | 38.8% |
| 6 | 730°C / 27.6 bar | 90 | 99.2 | 186 / 85.1% | 41.0% | 53.1% | | |

- Test Case 1 – 2 – Integration with Oxy-fired Pulverized Coal Heater
- Test Case 3 – 4 – Integration with Oxy-fired Chemical Looping Heater
- Test Case 5 – 6 – Integration with Air-fired Pulverized Coal Heater

EPS100

First commercial-scale sCO₂ heat engine

Description and test results



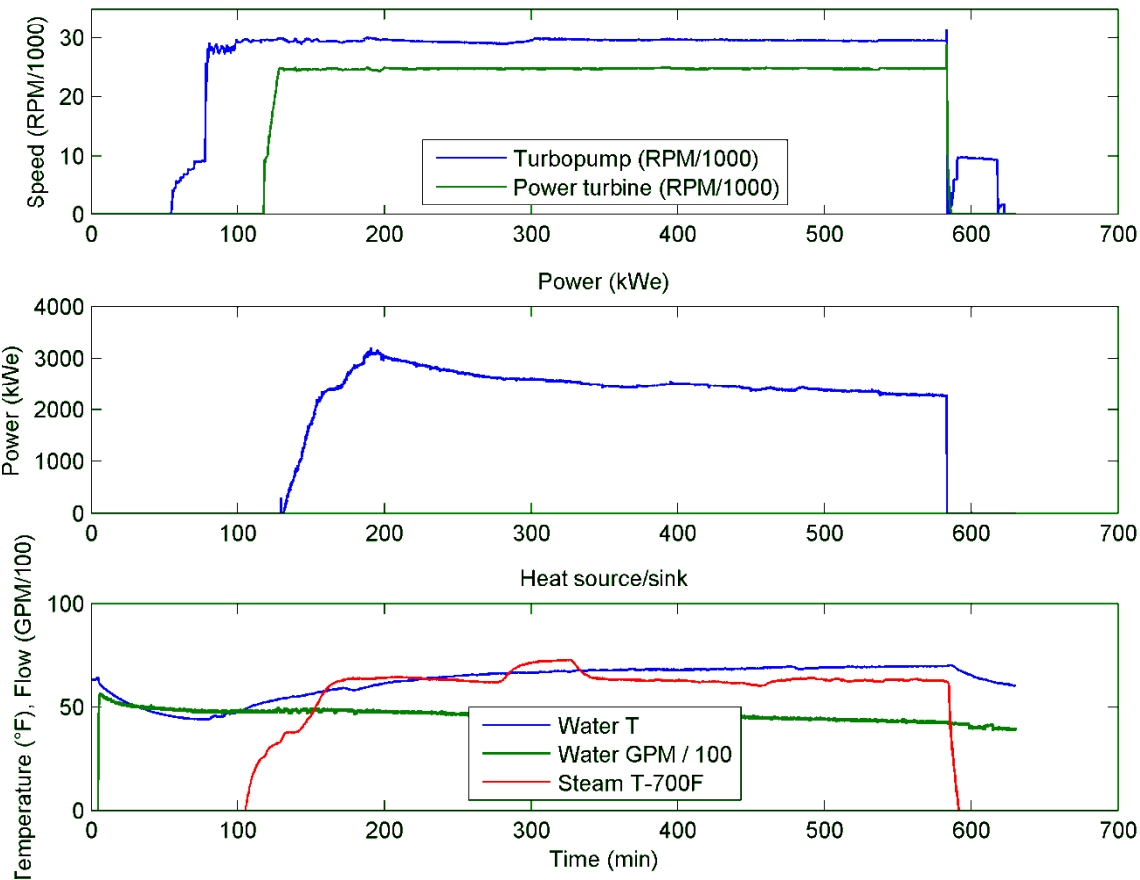
The EPS100

- Designed for 25 MW Aeroderivative GTs
 - GE LM2500PE/PJ
 - R-R RB211 C62
 - Solar Titan 250
 - 8.0 MW gross
 - 7.3 MW net
- Physical Configuration
 - Process skid (right)
 - Power skid (above)
 - Control house
 - CO₂ storage tank and transfer system
 - Cooling system (air or water)



GTs = Gas Turbines

Operational summary – typical test day



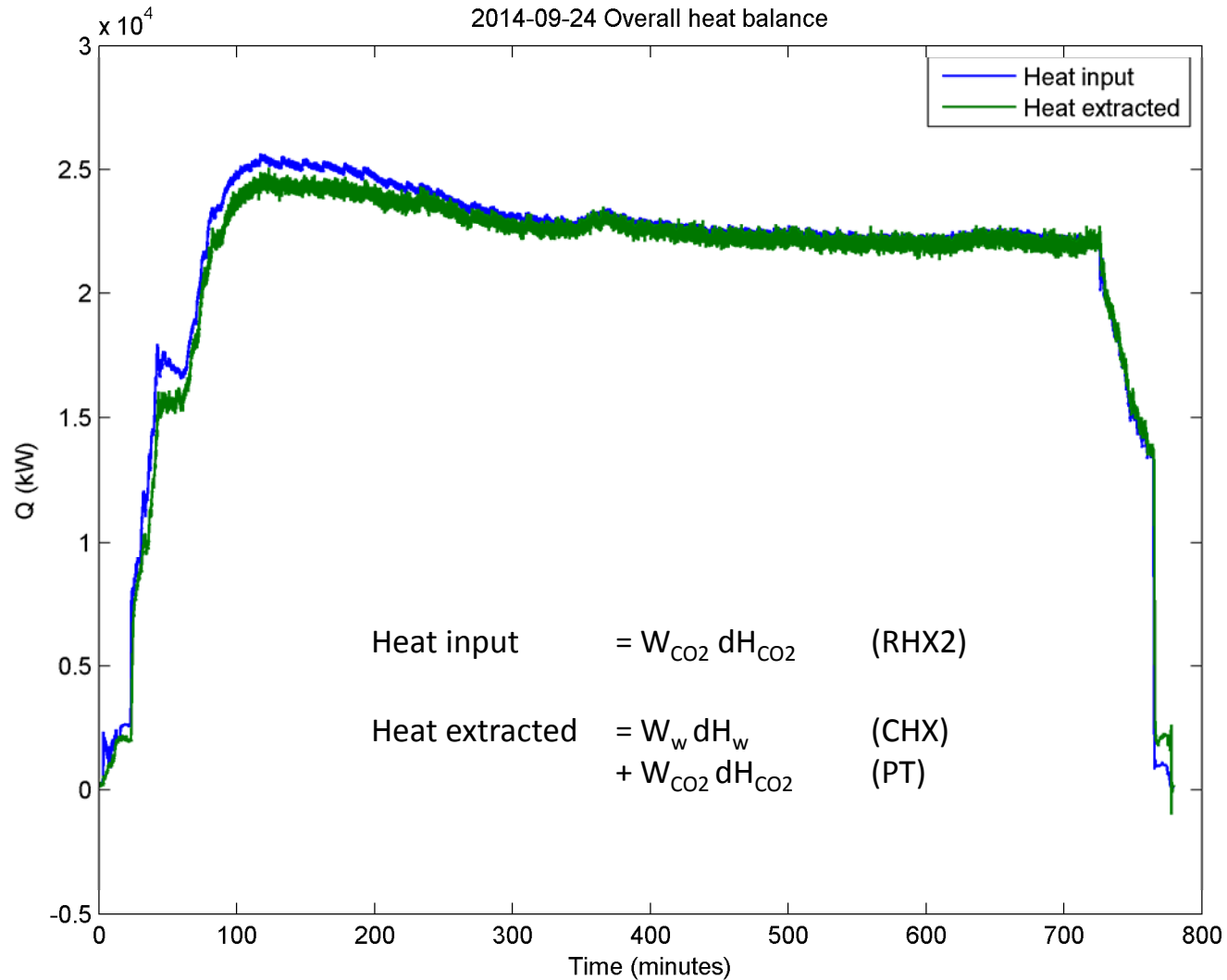
- Maximum power = 3.1 MWe – limited by heat source and water temperatures
- Run terminated by load bank fault. System tripped automatically and safely

A typical test day (compressed to 3 minutes)



- [Play video from file](#)

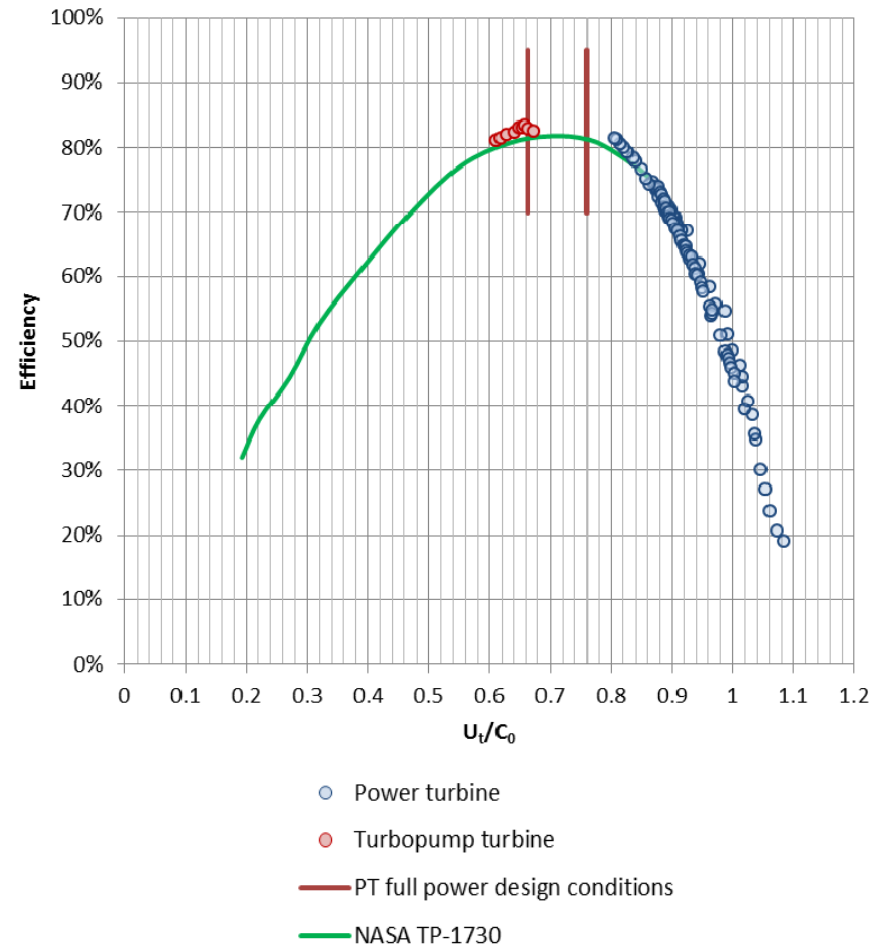
Overall heat balance



Turbomachinery Validation



- Power turbine and turbocompressor efficiencies demonstrate excellent agreement with reference curve derived by NASA
- Turbocompressor test data represent operation near full power
- Power turbine data represent significantly off-design conditions of the test cycle configuration. At full power conditions efficiency is expected to be similar to turbocompressor

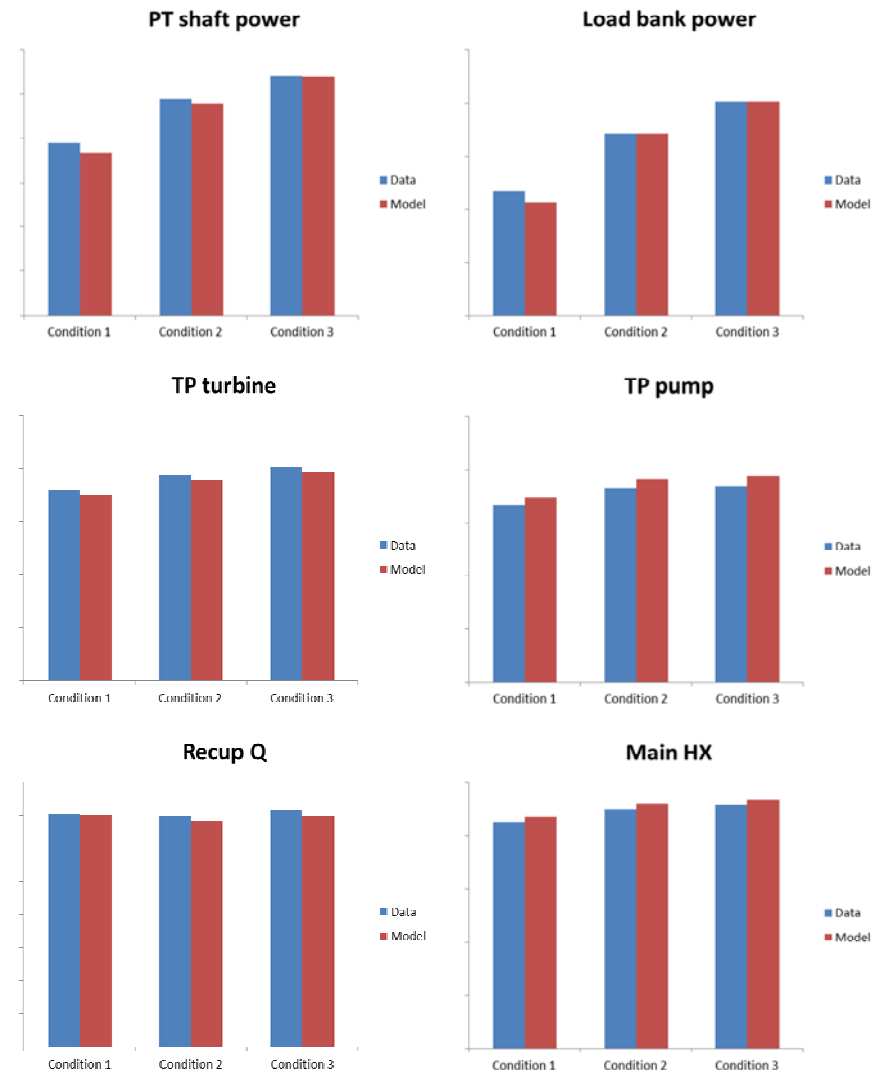


Turbine performance vs NASA TP-1730 curve. Note that TP-1730 curve ends at approximately $U_t/C_0 = 0.9$.

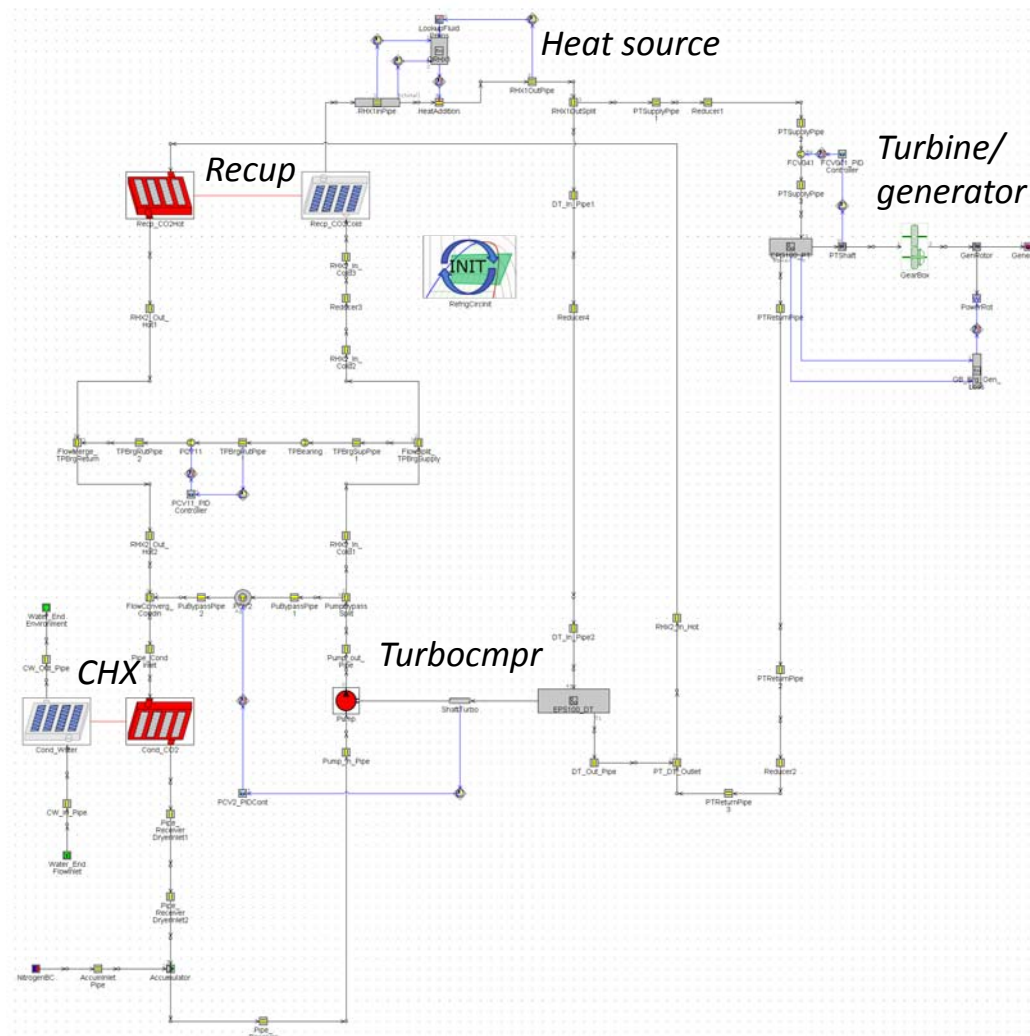
Steady-state cycle model validation



- Detailed cycle model
- Includes off-design component performance submodels
- Inputs:
 - Compressor inlet and outlet pressures
 - Heat source temperature & flow
 - Cooling water temperature and flow
 - PT speed
- Outputs:
 - TP speed
 - All other cycle points
 - Power output



Transient system model



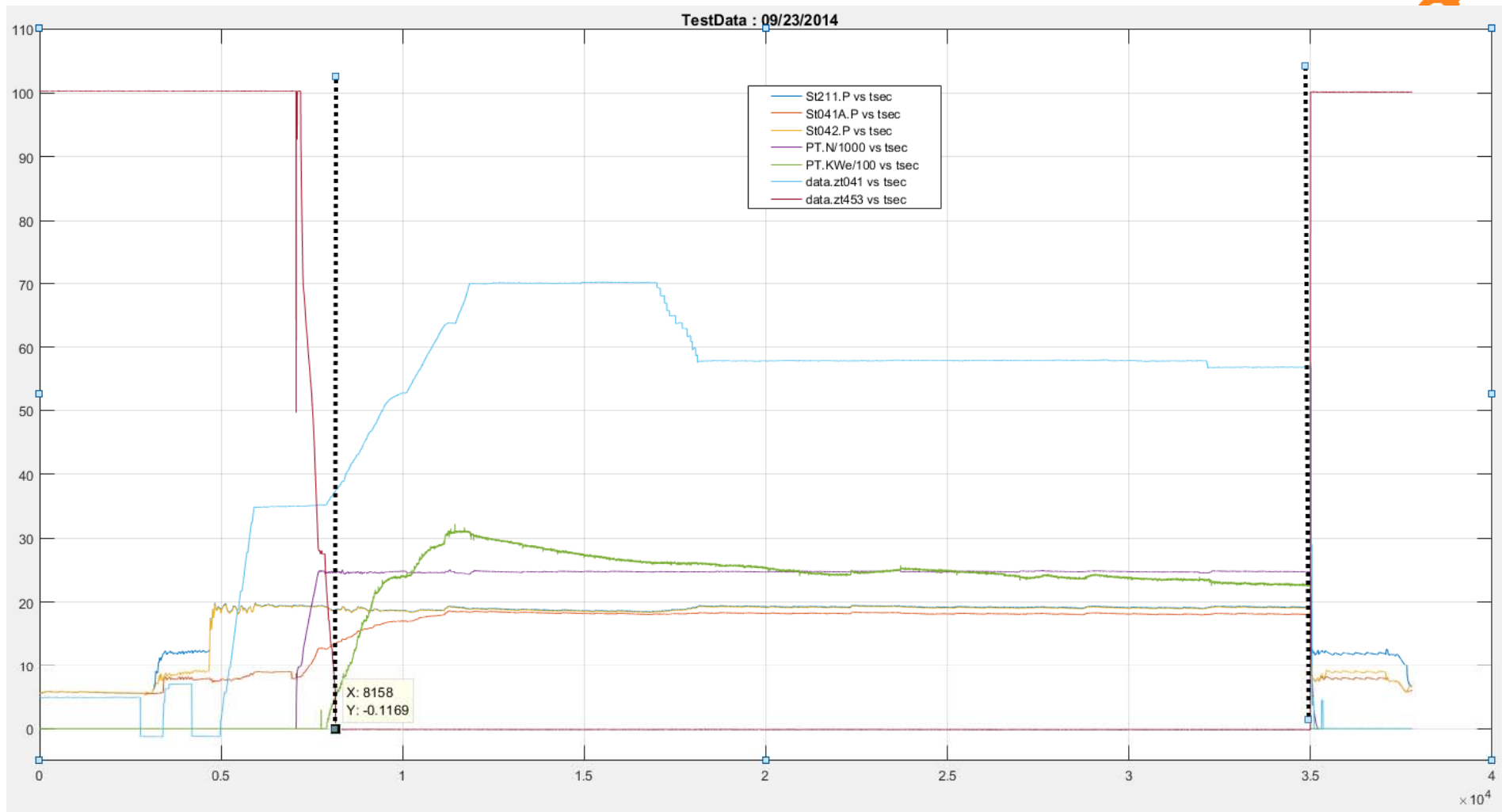
Boundary conditions:

- Cooling water flow rate & temperature
- Heat source input
- Generator load

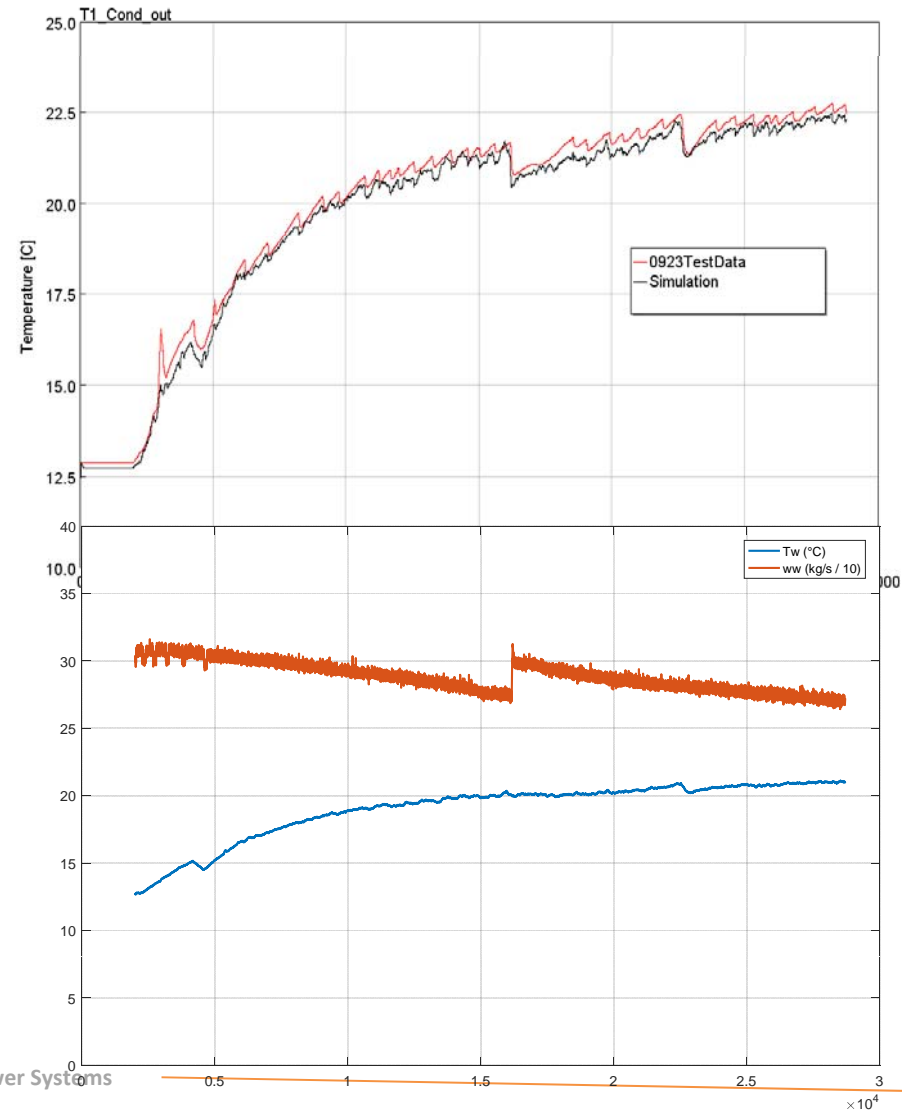
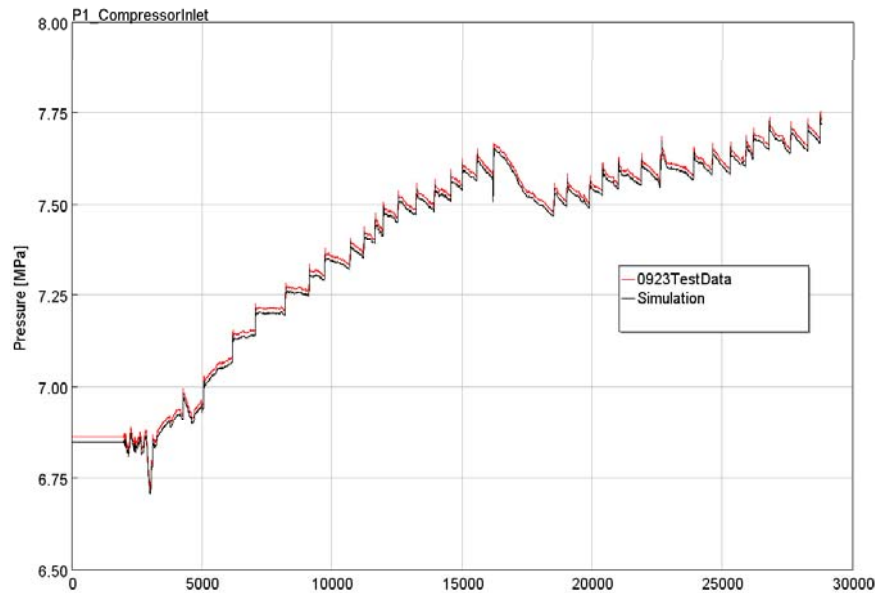
PID loop controls:

- Turbocompressor speed
- Power turbine speed
- Compressor inlet pressure

Test Data Considered for System Simulation

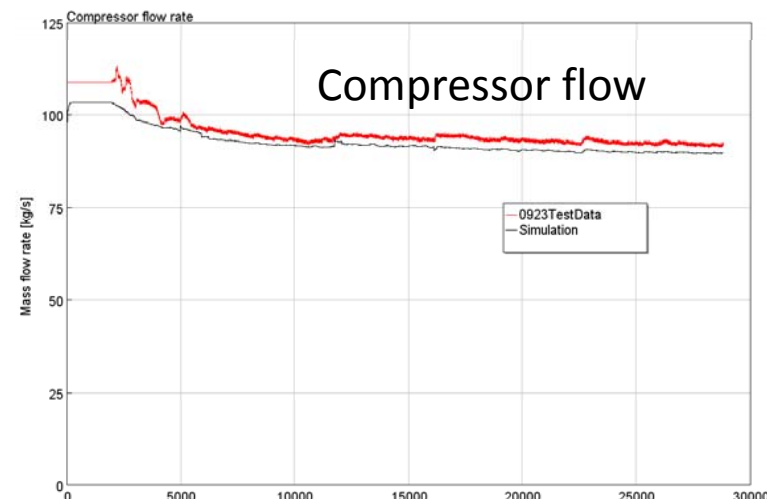
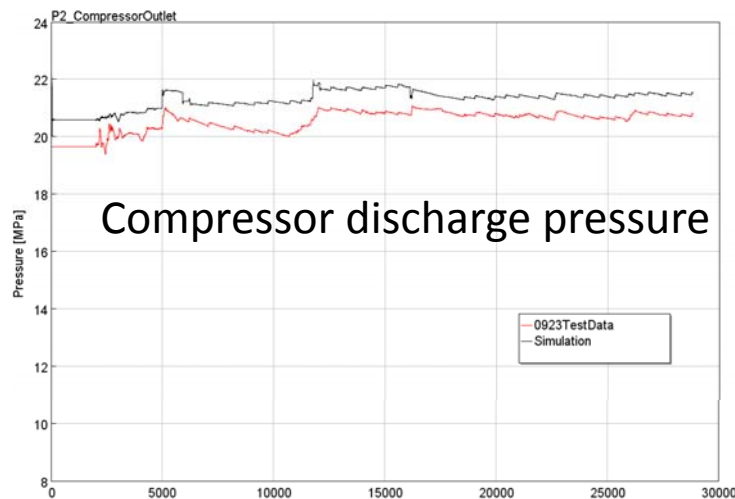
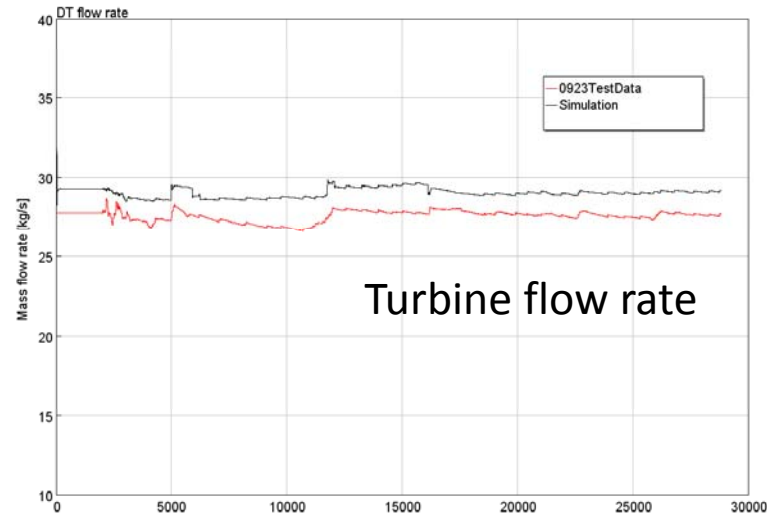
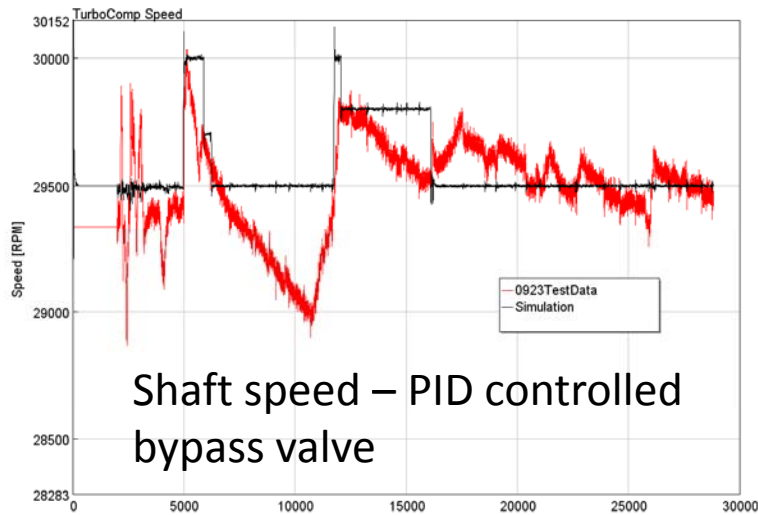


HRHX performance

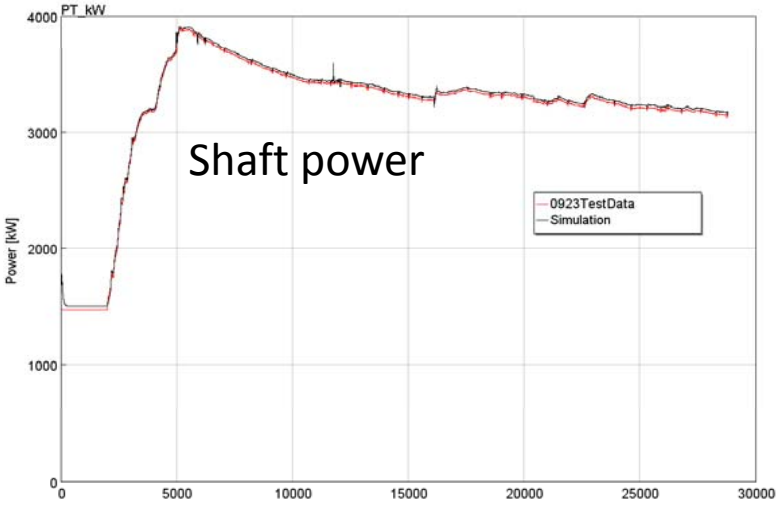
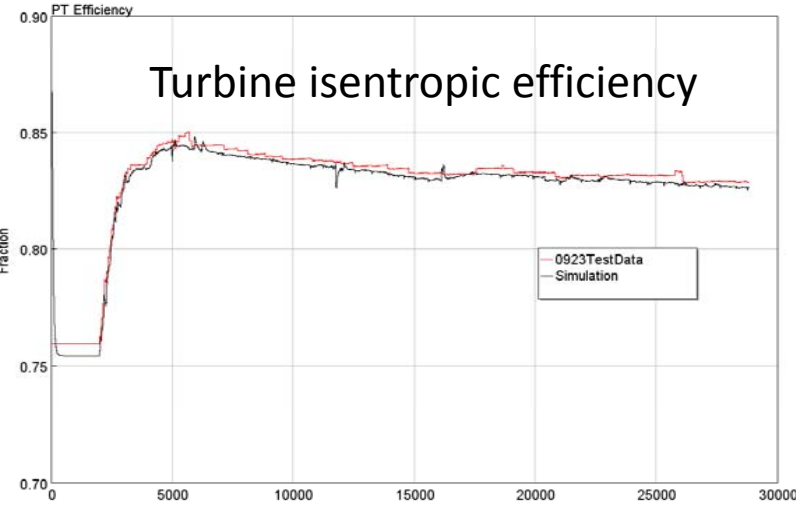
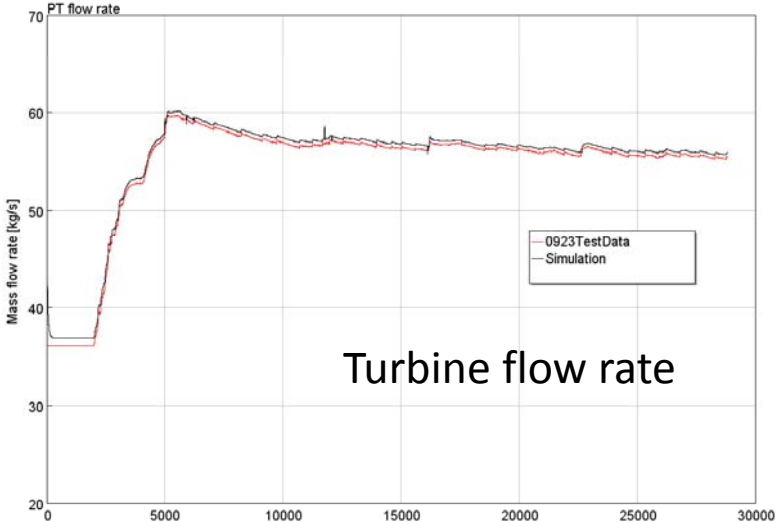
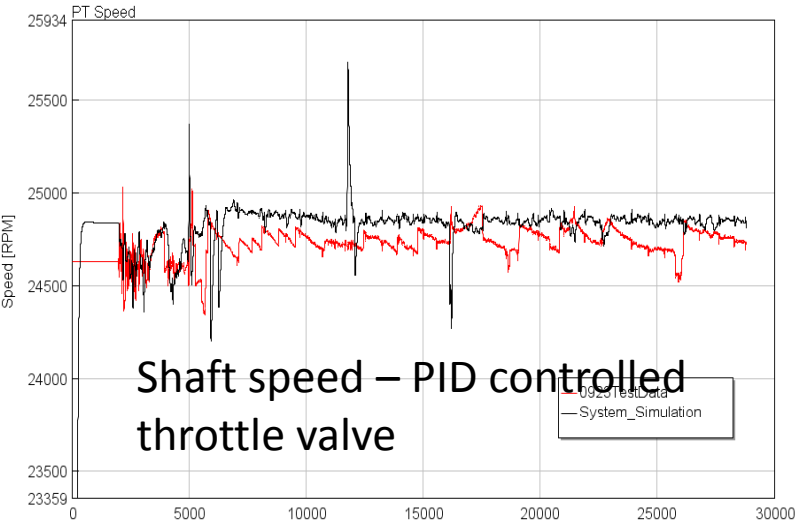


- Pressure controlled by inventory management
- Temperature varies based on cooler performance, water temperature and flow rate, CO₂ flow rate, temperature and pressure, etc.

Turbocompressor control & performance



Power turbine control & performance



EPS100 Testing – Key Accomplishments

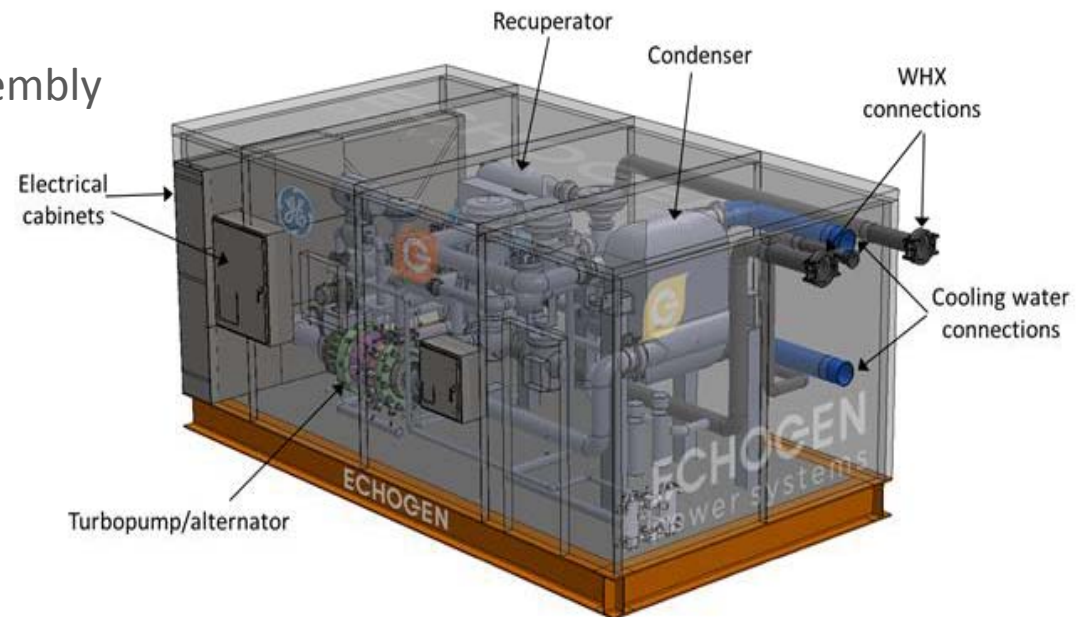


- System control and stability fully demonstrated
- Component performances meet or exceed expectations
- Turbocompressor run to max power (3.0 MW shaft)
- Generator speed control stability demonstrated
- Power turbine electrical output = 3.10 MWe
 - Limited by available heat on test stand
- 310 hours turbocompressor run time
- 151 hours power turbine run time

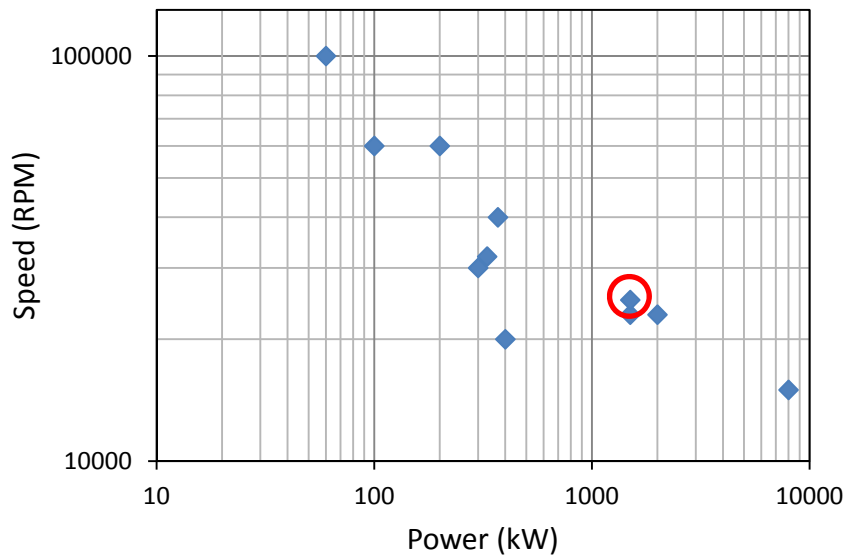
Echogen's EPS30 System



- Multi-platform solution currently in final design stage
 - 1.35 MW rated output (net)
 - Commercial availability late 2016
 - Compatible with medium-speed diesels and small gas turbines
- Builds on prior Echogen technology development
 - Single-shaft, dual-coil HX architecture
 - Advanced hermetically-sealed turbine/compr/alternator assembly
 - Water cooled (1,800 gpm)
 - 60 Hz, 480V output
- Designed for marine installations
 - Easily adapted for land-based applications as well
 - Can replace water cooling with air cooling
- Designed for remote operation and minimal maintenance

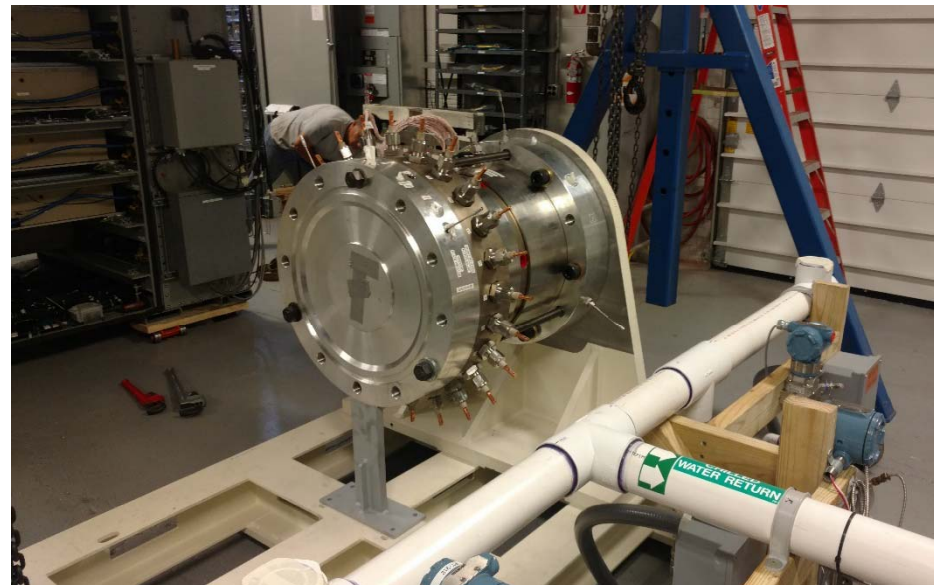


High speed alternator – EPS30M product



- 1500kW permanent magnet alternator
- 25,000 RPM
- Combination water-cooled stator, CO₂ cooled rotor & stator

- Motor-generator test in preparation
- Full speed, full load
- Test of windage & cooling models



Summary



- sCO₂ offers significant advantages in numerous heat conversion applications
 - Waste/Exhaust heat technology offers a path to technology introduction in a market that is available today
 - Primary power opportunities limited at small scale, but can offer path to utility-scale
- Echogen sCO₂ heat engine technology delivering on the predicted system performance
- Test program provided key learnings, and insight into the challenges and opportunities of sCO₂ technology
 - Current test facility limited operational envelope
 - Working toward full power demonstration facility
- On the path to commercialization