

Design considerations on a small scale supercritical CO₂ power system for industrial high temperature waste heat to power recovery applications

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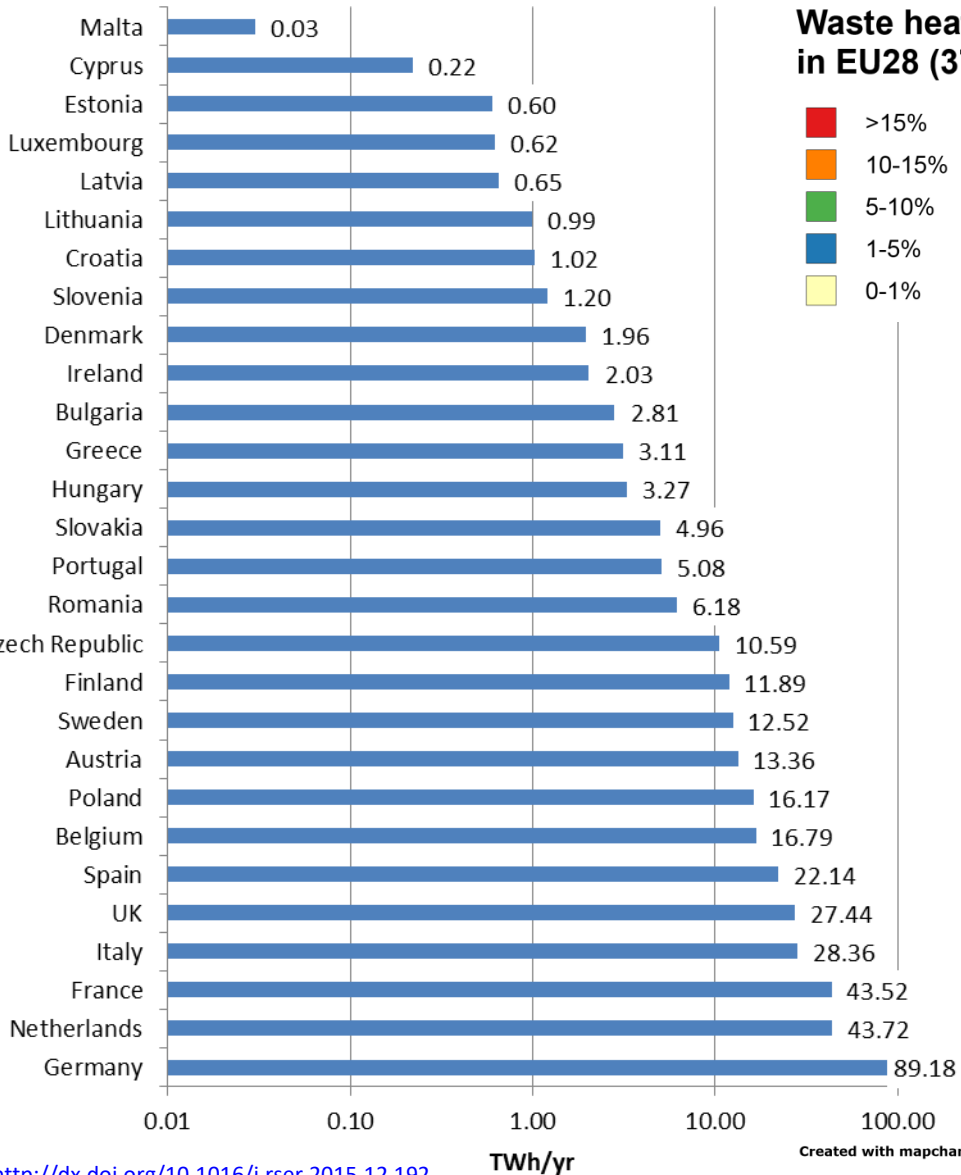


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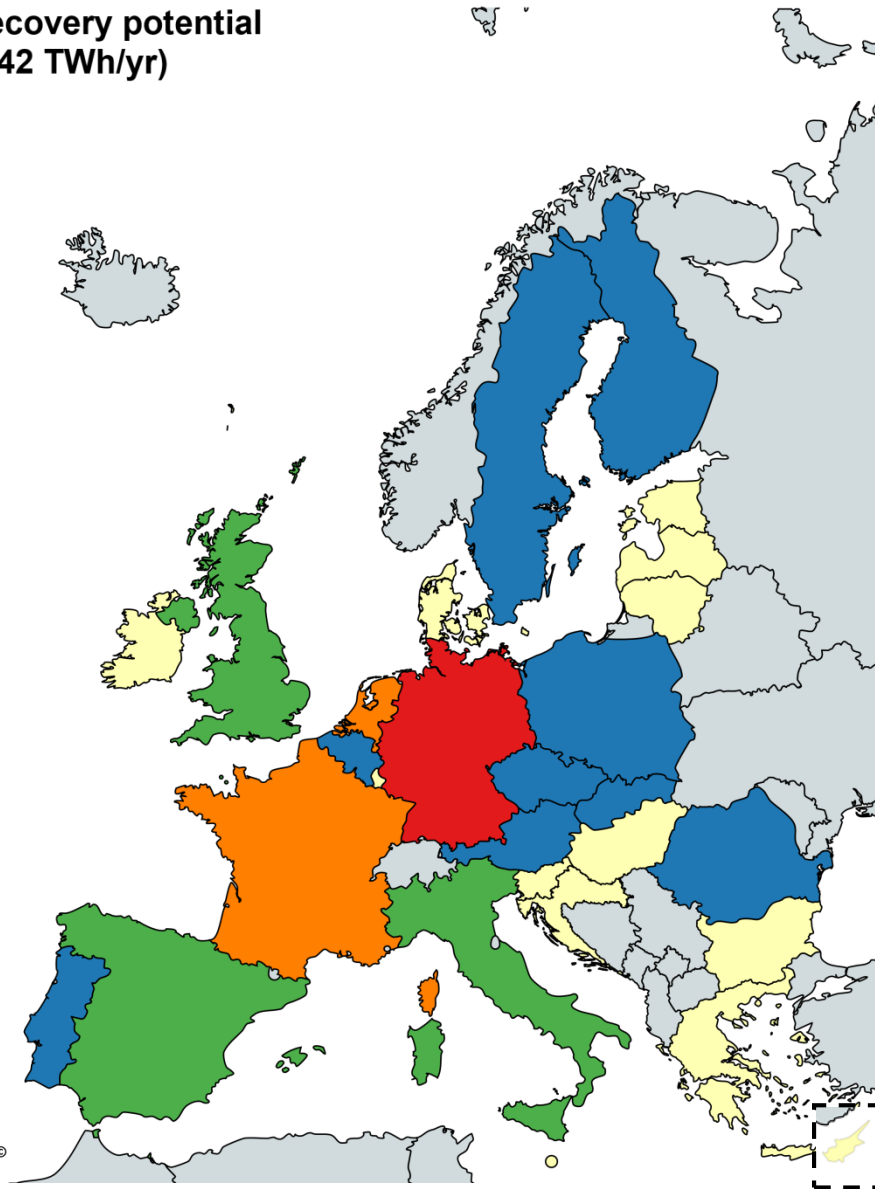
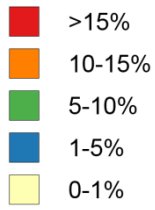




1st European Seminar on Supercritical CO₂ (sCO₂) Power Systems



Waste heat recovery potential in EU28 (370.42 TWh/yr)



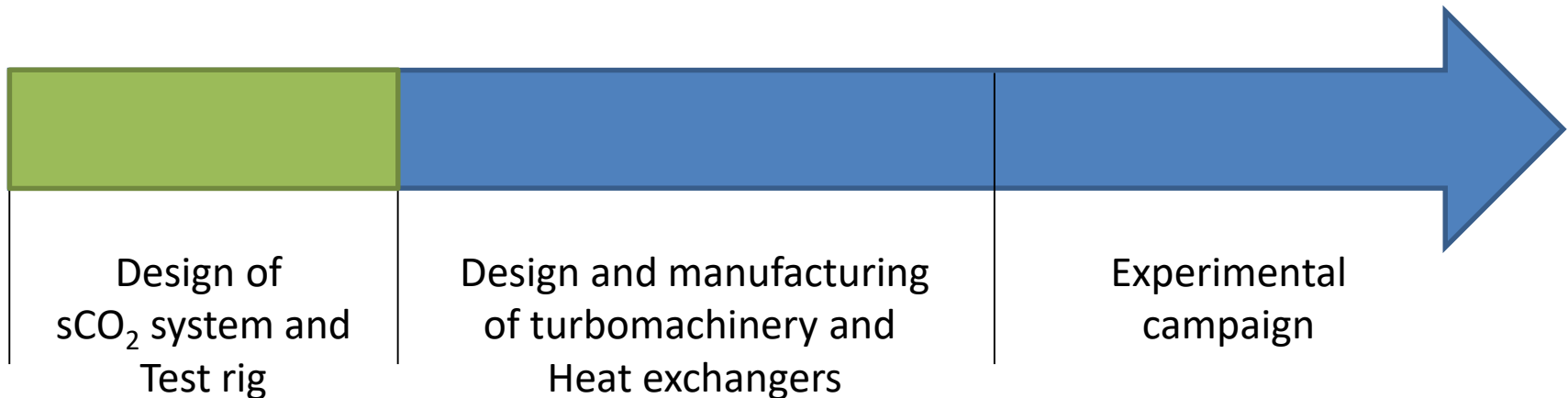
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<http://dx.doi.org/10.1016/j.rser.2015.12.192>



Scope of the I-ThERM's sCO₂ project

- Power output 50 ÷ 100 kWe
- 1st law efficiency \approx 20 %
- Low CAPEX (short PBP)



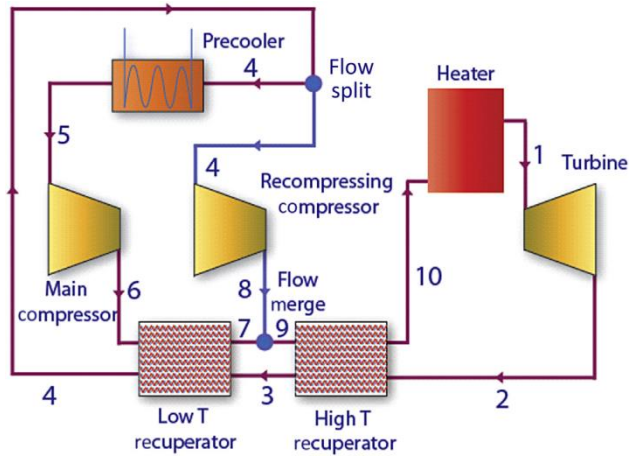


Outline

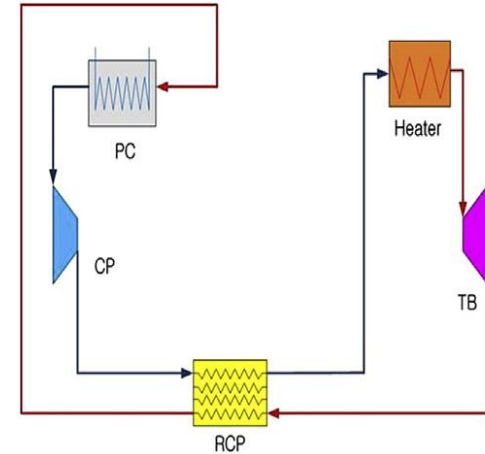
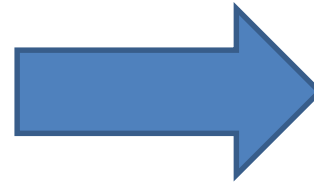
- Reference thermodynamic cycle
- Preliminary turbomachinery design
- Heat exchangers
- Simulation platform
- Results and discussion
- Future work

Thermodynamic cycle

Recompressing cycle layout is the optimal configuration for large sCO₂ installations (~MW) such as nuclear and CSP ones



2 compressors + 2 recuperators



1 compressors + 1 recuperator

However, if target output power is smaller, **simple regenerated cycle** becomes the most suitable architecture

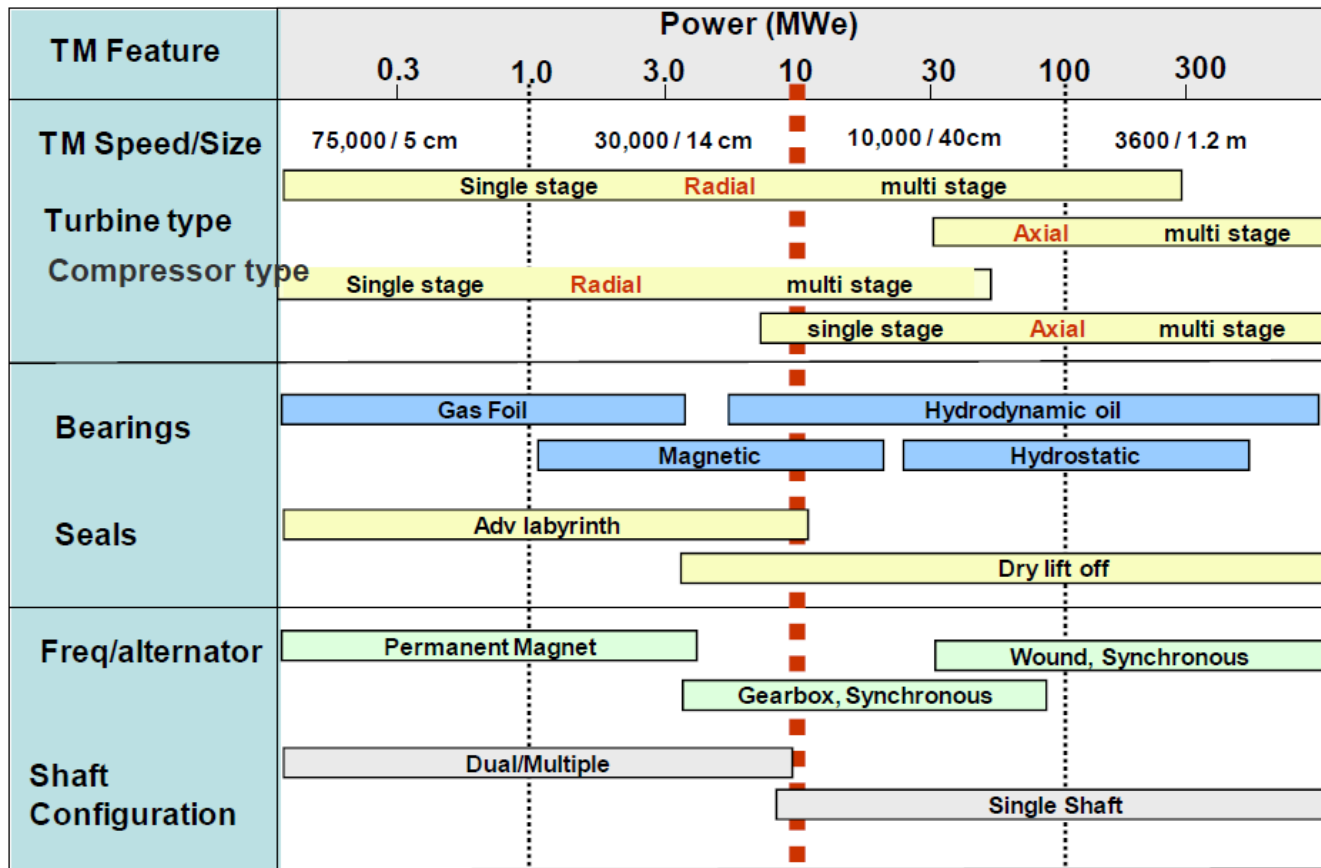
<http://dx.doi.org/10.1016/j.energy.2015.03.066>
<http://dx.doi.org/10.1016/j.net.2015.06.009>

The comparison of existing S-CO₂ integral test loops.

	Sandia National Lab	Knolls Atomic Power Lab & Bettis Atomic Power Lab	Institute of Applied Energy
Turbomachinery feature	2-TAC	1-TAC, 1-turbine	1-TAC (2-recuperators)
Cycle layout	Recompressing Fig. 1.	Simple recuperated Fig. 2.	Simple recuperated Fig. 3.
Heat, kW	780	834.9	160
Efficiency	31.5	14.7	7
Mass flow rate, kg/s	3.5 (target)/2.7 (achieved)	5.35 (target)/3.54 (achieved)	1.1 (achieved)
T.I.T., °C	537 (target)/342 (achieved)	300 (target)	277 (achieved)
Pressure ratio	1.8 (target)/1.65 (achieved)	1.8 (target)/1.44 (achieved)	1.4 (achieved)
Rotating speed, × 1000 rpm	75 (target)/52 (achieved)	75 (target)/55–60 (achieved)	69 (achieved)
Turbine efficiency, %	86 (turbine-1)/87 (turbine-2)	79.8 (Power turbine)/79.7 (C-driving turbine)	65
Compressor efficiency, %	67 (MC)/70 (RC)	60.8	48



Turbomachinery for sCO₂ systems

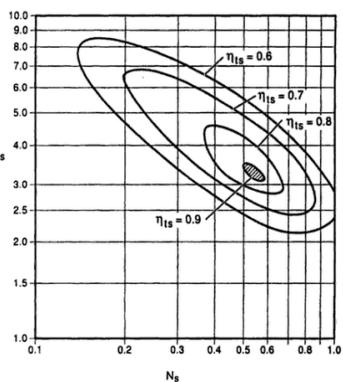


Siemicki et al. (2011)

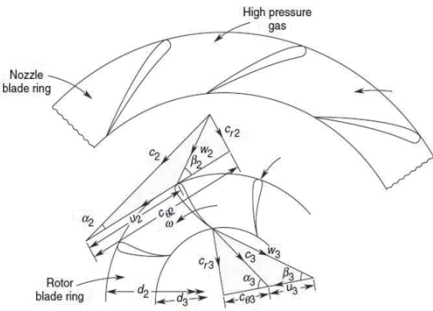
High revolution speeds + small impeller diameters



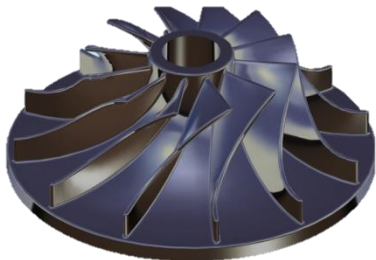
Turbomachinery Design



Specific speed and diameter

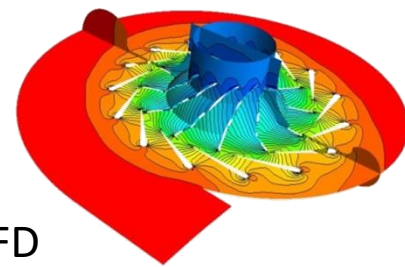


Velocity triangles

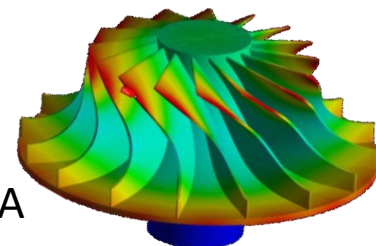


CAD

- Balje's charts available for air and water turbo machines
- Loss correlations available for air
- Need of coupling CFD tools with thermo-physical properties of CO₂ (dll libraries or look-up tables)
- Need of importing thermomechanical properties in FEA tools if custom materials are employed



CFD

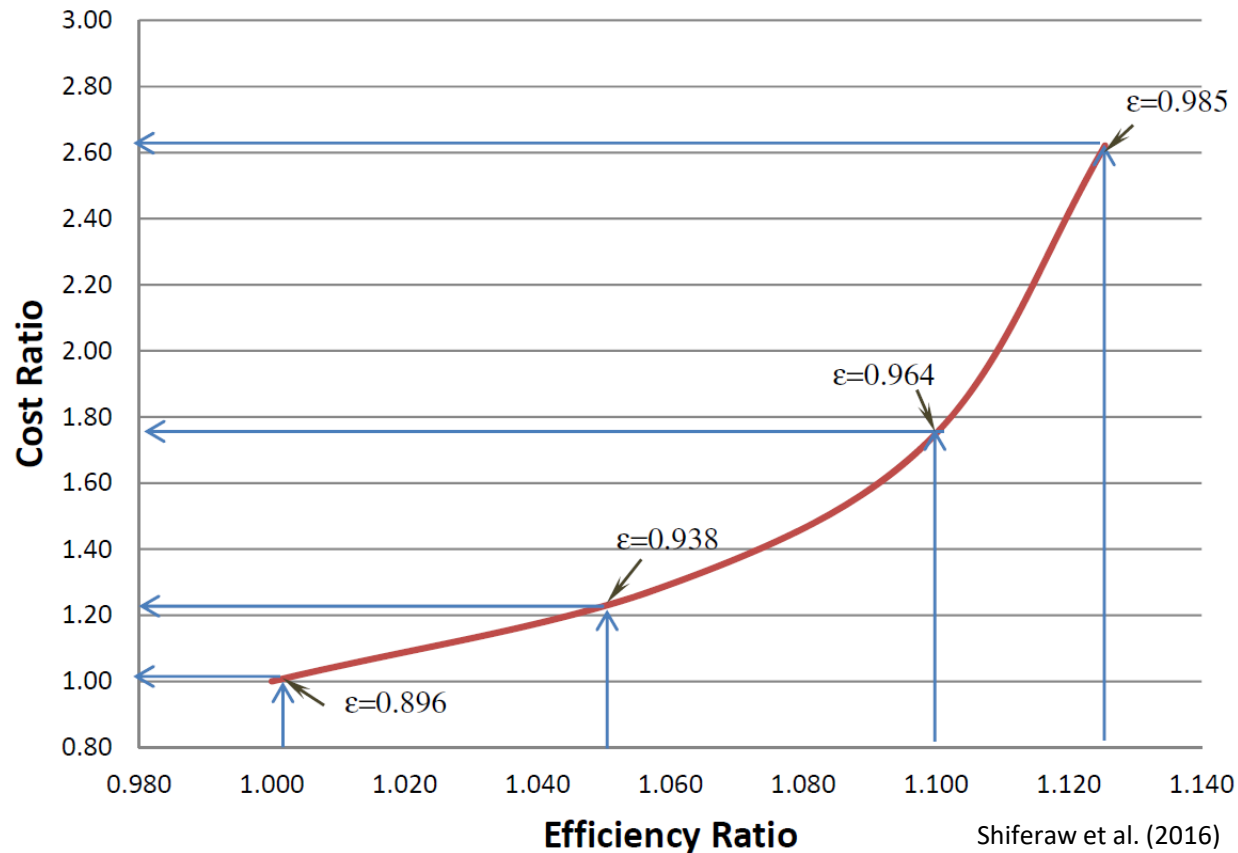


FEA



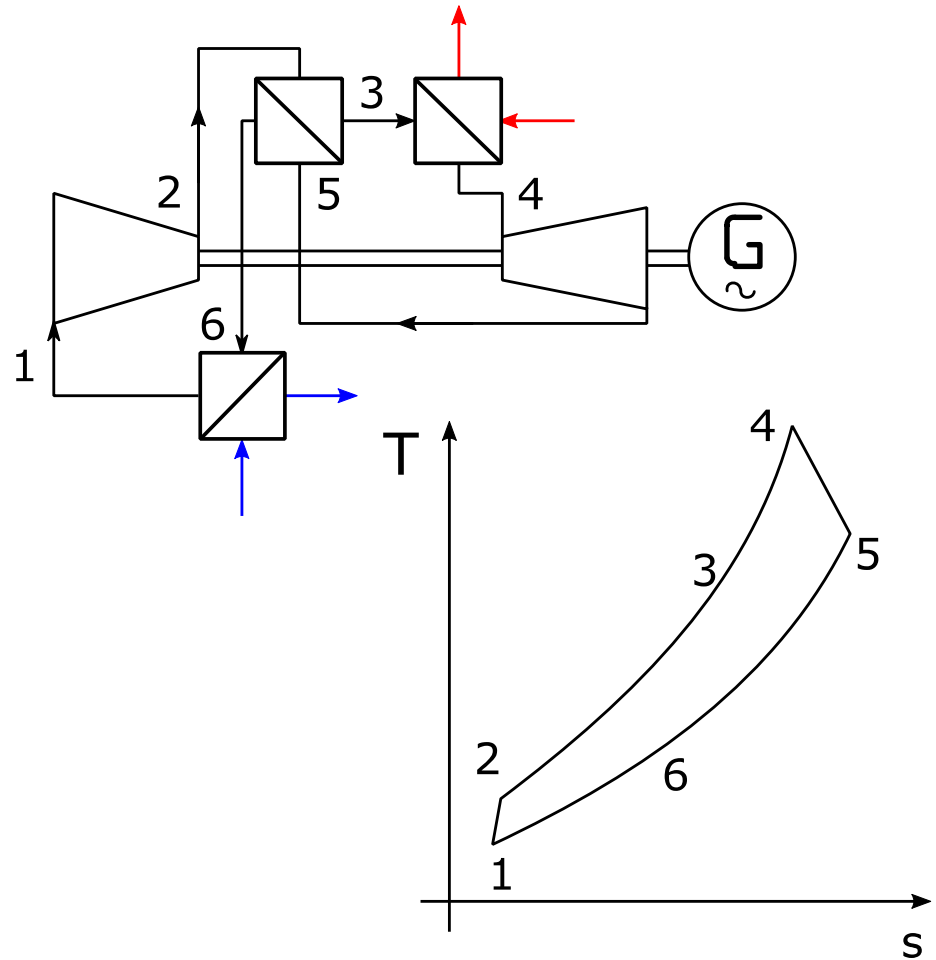
Heat exchangers

- Multiple technologies currently available
- Corrosion issues to be considered
- High thermal stresses
- HXs account for up to 90% of the overall CAPEX
- Aggressive designs might spoil the overall economic feasibility of system



sCO₂ Modelling approach

- Simple regenerated cycle
- Real gas properties
- 1st and 2nd law analyses
- Detailed loss breakdown
- Steady state approach
- Implemented in EES

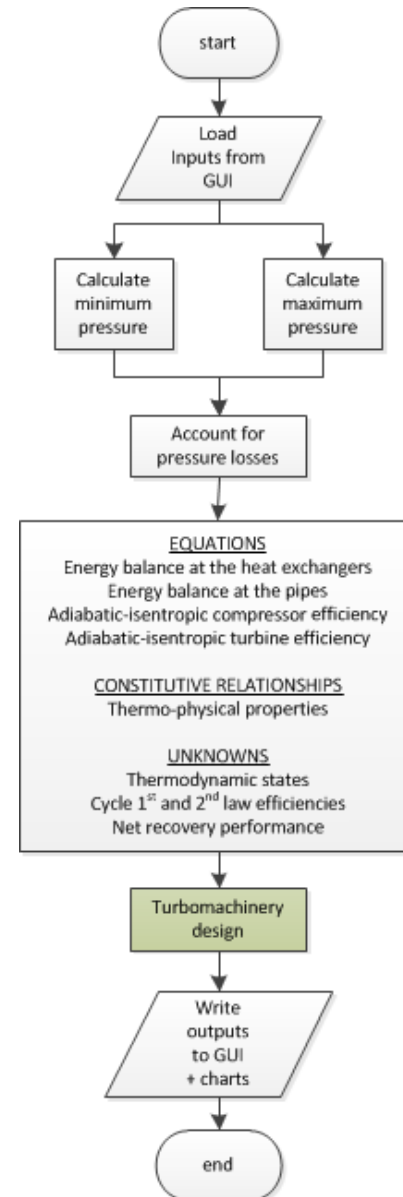




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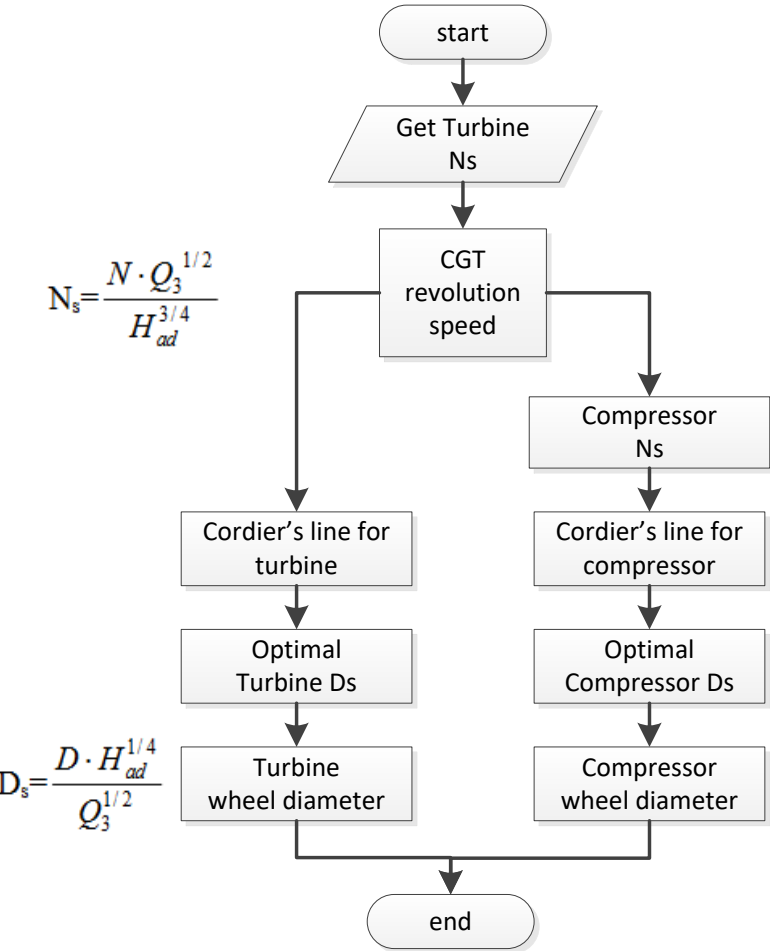


- Input data:
 - Inlet conditions of hot heat source (**exhaust gas**)
 - Inlet conditions of cold heat source (**water**)
 - HXs and machines efficiencies
 - Pipes pressure and heat losses
- Parameters:
 - Min and max temperature
 - Min and max pressure
 - Recuperation ratio (R)
- Output data:
 - Electrical power recovered
 - Cycle efficiencies (1st, 2nd law)
 - Loss breakdown
 - Turbomachinery design





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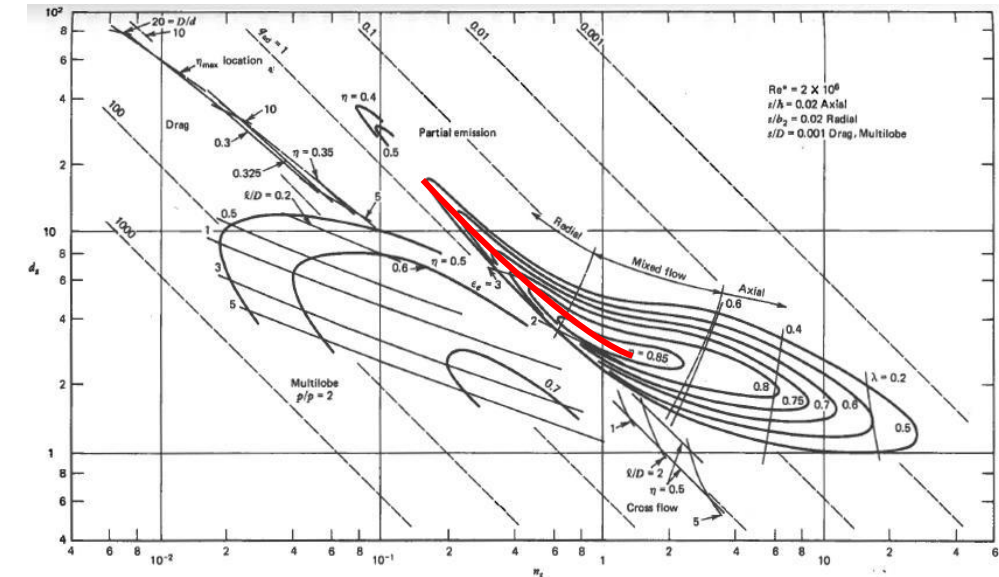
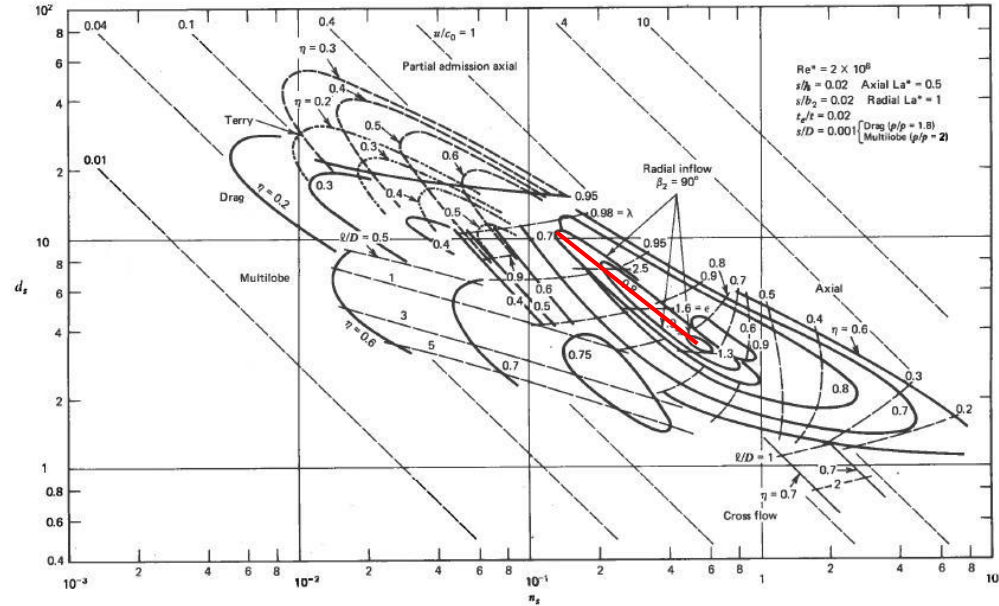
$$N_s = \frac{N \cdot Q_3^{1/2}}{H_{ad}^{3/4}}$$

$$D_s = \frac{D \cdot H_{ad}^{1/4}}{Q_3^{1/2}}$$

$$D_{s,c} = 2.719 N_{s,c}^{-1.092}$$

$$D_{s,t} = 2.056 N_{s,t}^{-0.812}$$

only for radial machines





Design choices

- Turbomachinery
 - Revolution speed <100 kRPM
 - Wheel diameters >40 mm
 - Subsonic flows
- Heat exchangers
 - Adequate pinch point ΔT
 - Moderate temperature levels



Assumptions

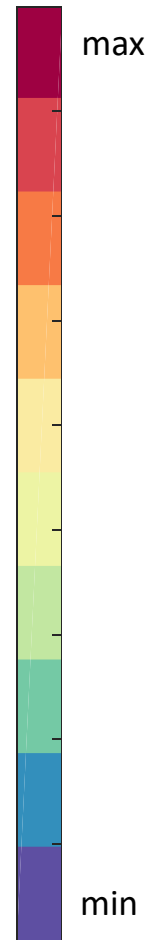
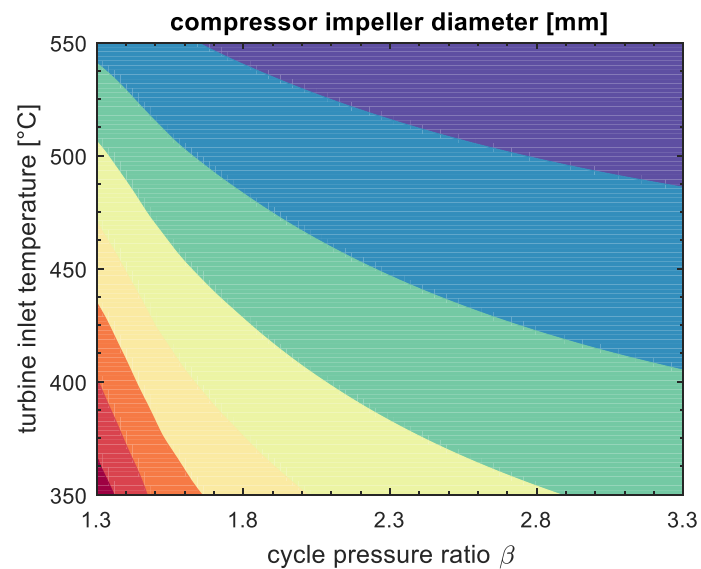
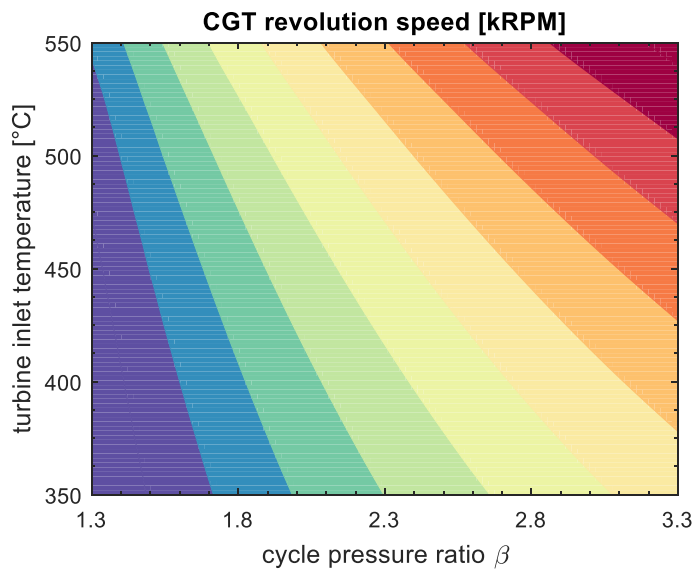
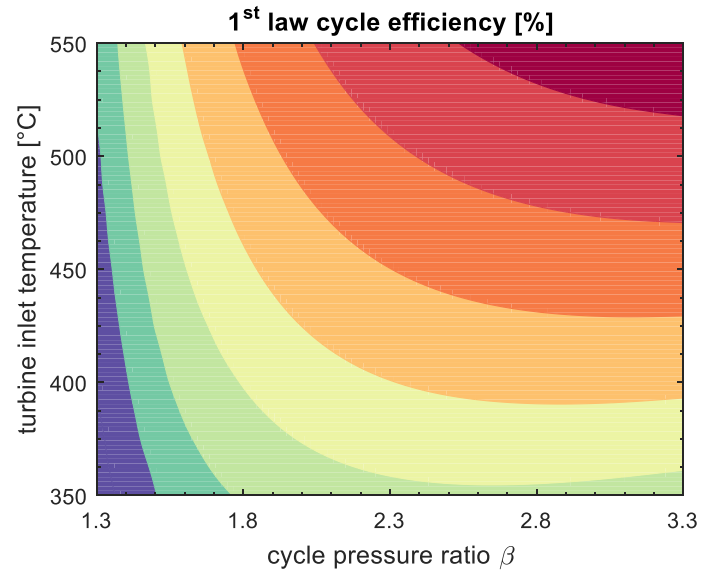
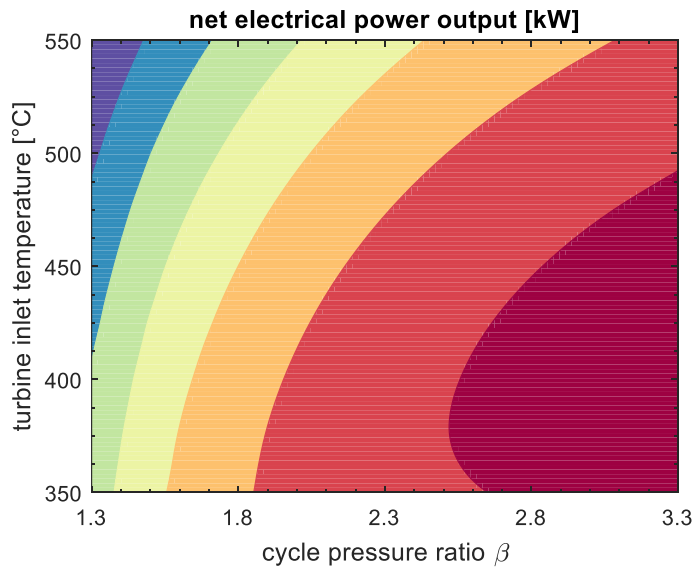
- Constant compressor and turbine isentropic efficiencies
- Constant HXs effectiveness
- Gaseous fluid at compressor inlet
- No pipe pressure drops or thermal losses

Simulation parameters

- Turbine inlet temperature and pressure (i.e. cycle pressure ratio)
- Inlet conditions of exhaust gases (flow rate and temperature)
- Influence of recuperation
- Turbine specific speed

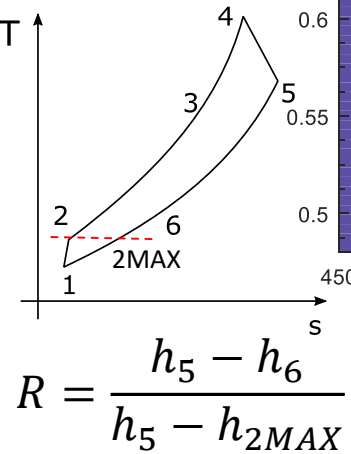
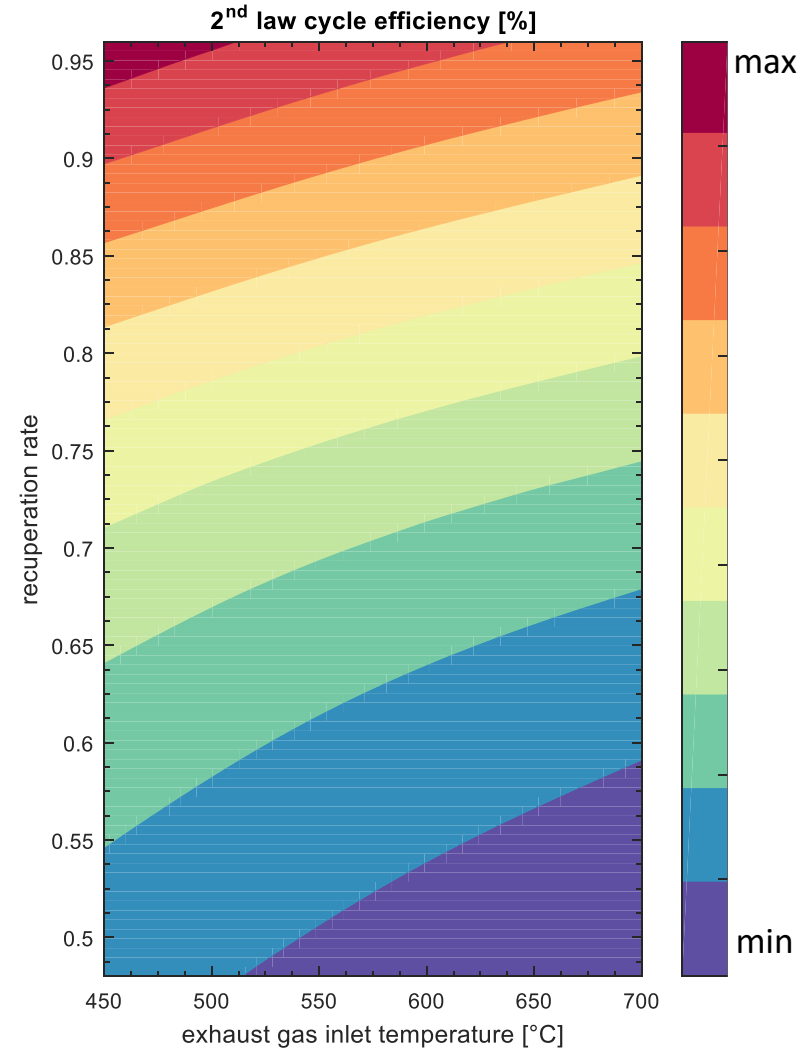
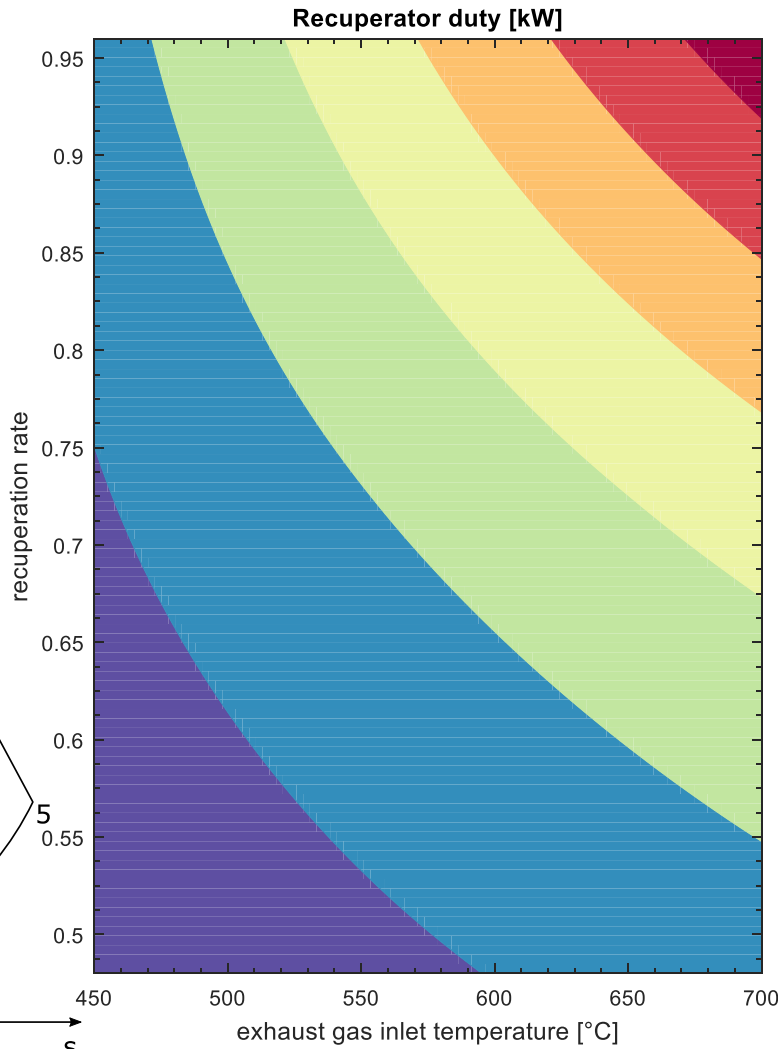


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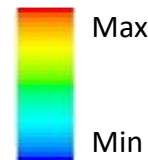
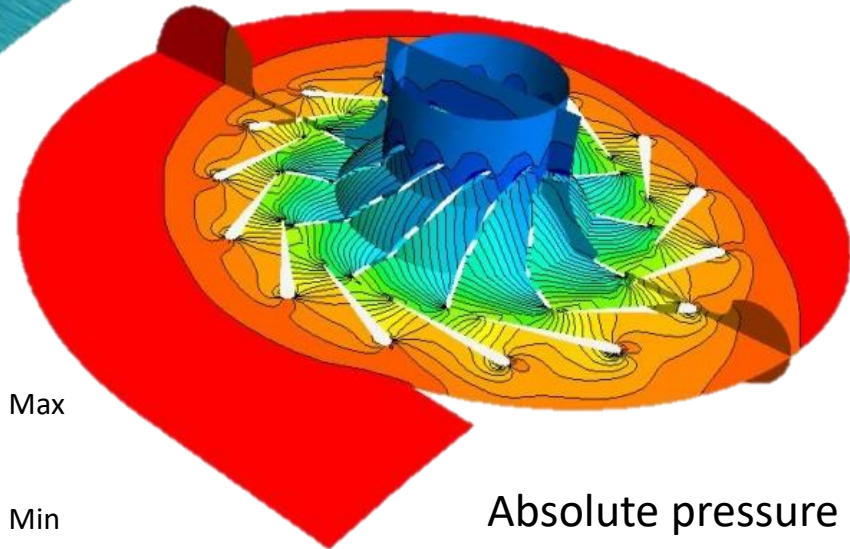
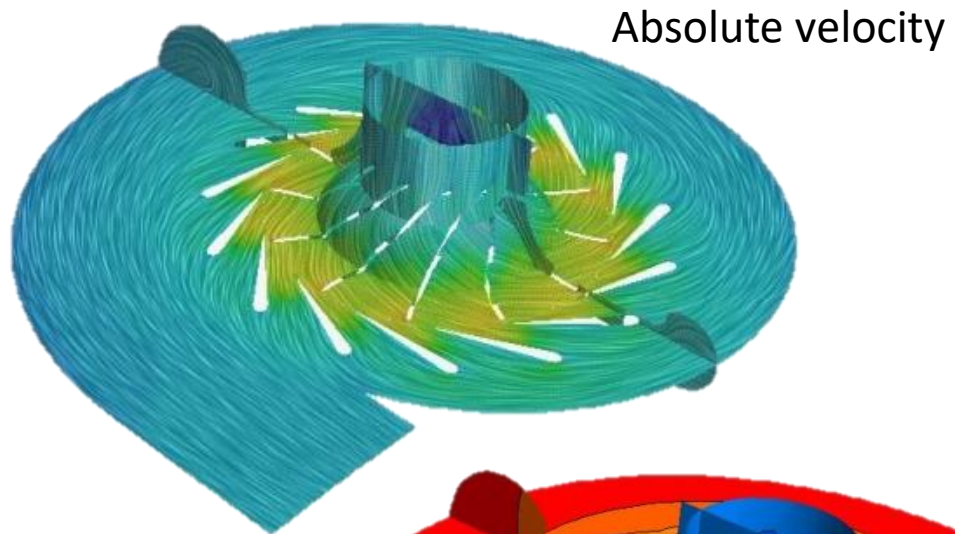
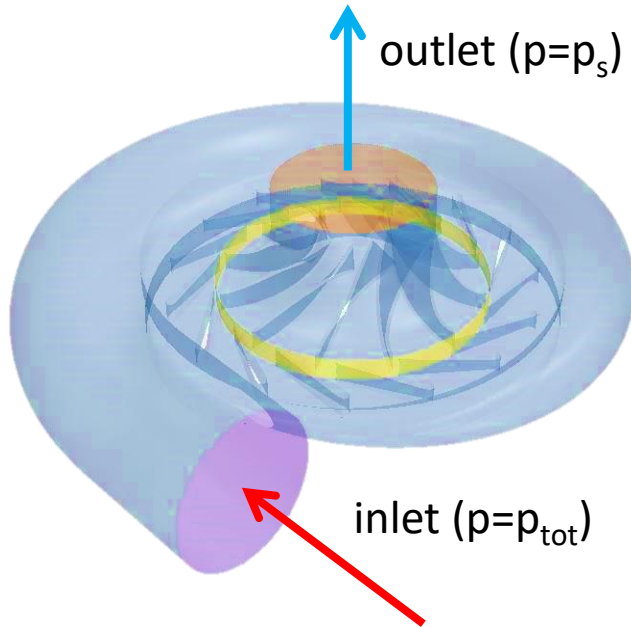




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Turbine design



- Mixing plane approach
- RANS equations
- Steady state simulations
- Peng-Robinson EOS
- Star-CCM+ software



Conclusions

- sCO₂ systems could be successfully applied on industrial waste heat to power generation applications
- The most limiting device in small-scale sCO₂ units (50-100 kWe) is the compressor
- Theoretical performance of the I-ThERM's demonstration unit exceed 21% global cycle efficiency



Future work

- Design and manufacturing of the compressor-turbine-generator (CGT) unit and its controls
- HXs selection and design
- Transient modelling of the sCO₂ system
- Experimental campaign

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